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Diffusion barriers and adaptive carbon uptake strategies enhance the modeled performance of the algal CO₂-concentrating mechanism.

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Abstract

Many photosynthetic organisms enhance the performance of their CO₂-fixing enzyme Rubisco by operating a CO₂-concentrating mechanism (CCM). Most CCMs in eukaryotic algae supply concentrated CO₂ to Rubisco in an organelle called the pyrenoid. Ongoing efforts seek to engineer an algal CCM into crops that lack a CCM to increase yields. To advance our basic understanding of the algal CCM, we develop a chloroplast-scale reaction-diffusion model to analyze the efficacy and the energy efficiency of the CCM in the green alga Chlamydomonas reinhardtii. We show that achieving an effective and energetically efficient CCM requires a physical barrier such as thylakoid stacks or a starch sheath to reduce CO2 leakage out of the pyrenoid matrix. Our model provides insights into the relative performance of two distinct inorganic carbon uptake strategies: at air-level CO₂, a CCM can operate effectively by taking up passively diffusing external CO₂ and catalyzing its conversion to HCO₃, which is then trapped in the chloroplast; however, at lower external CO₂ levels, effective CO₂ concentration requires active import of HCO₃. We also find that proper localization of carbonic anhydrases can reduce futile carbon cycling between CO2 and HCO3, thus enhancing CCM performance. We propose a four-step engineering path that increases predicted CO₂ saturation of Rubisco up to seven-fold at a theoretical cost of only 1.5 ATP per CO₂ fixed. Our system-level analysis establishes biophysical principles underlying the CCM that are broadly applicable to other algae and provides a framework to guide efforts to engineer an algal CCM into land plants.

Significance Statement

Eukaryotic algae mediate approximately one-third of CO₂ fixation in the global carbon cycle. Many algae enhance their CO₂-fixing ability by operating a CO₂-concentrating mechanism (CCM). Our model of the algal CCM lays a solid biophysical groundwork for understanding its operation. The model's consistency with experimental observations supports existing hypotheses about the operating principles of the algal CCM and the functions of its component proteins. We provide a quantitative estimate of the CCM's energy efficiency and compare the performance of two distinct CO₂ assimilation strategies under varied conditions. The model offers a quantitative framework to guide the engineering of an algal CCM into land plants and supports the feasibility of this endeavor.

Main Text

Introduction

The CO₂-fixing enzyme Rubisco mediates the entry of roughly 10¹⁴ kilograms of carbon into the biosphere each year (1–3). However, Rubisco is rather inefficient at performing this essential task (4), fixing CO₂ at just 10% of its maximum rate under atmospheric levels of CO₂ (*SI Appendix*, Fig. S1). Moreover, O₂ competes with CO₂ for the active site of Rubisco (5), resulting in the loss of fixed carbon and nitrogen through a process known as photorespiration (6). To overcome Rubisco's inefficiency, many photosynthetic organisms, including cyanobacteria, eukaryotic algae, and some land plants, have evolved CO₂-concentrating mechanisms (CCMs) (7–10). Such mechanisms elevate CO₂ levels in the vicinity of Rubisco, thus enhancing CO₂ fixation and decreasing photorespiration.

Eukaryotic algal CCMs mediate approximately one-third of global CO₂ fixation (11), yet they remain poorly characterized at a molecular and functional level. In addition to their importance for global biogeochemistry, there is growing interest in engineering an algal CCM into C₃ crops such as wheat and rice to improve yields and nitrogen- and water-use efficiency (12, 13). Here, we advance our

understanding of the eukaryotic algal CCM by developing a reaction-diffusion model of this mechanism based on the molecularly best-characterized alga, *Chlamydomonas reinhardtii* (Chlamydomonas hereafter). As is commonly the case among algae (14), the Chlamydomonas CCM is built around a structure called the pyrenoid, which consists of three elements: (i) a spheroidal matrix, comprised of phase-separated Rubisco (11, 15, 16), (ii) traversing thylakoid tubules (17), which are thought to deliver CO₂ to the Rubisco (18), and (iii) a surrounding starch sheath, which has been proposed to serve as a diffusion barrier to slow CO₂ escape from the pyrenoid (19, 20) (Fig. 1A).

 CO₂ is supplied to the pyrenoid by the concerted action of carbonic anhydrases and HCO₃⁻ transporters (Fig. 1A) (13, 21, 22). External inorganic carbon (Ci: CO₂ and HCO₃⁻) is transported across the plasma membrane by LCI1 and HLA3 (23–25), and accumulates in the chloroplast stroma in the form of HCO₃⁻, either via direct transport across the chloroplast membrane by the HCO₃⁻ transporter LCIA (24, 26) or via conversion of CO₂ to HCO₃⁻ by the putative stromal carbonic anhydrase LCIB/LCIC complex (LCIB hereafter) (27–29). Once in the stroma, HCO₃⁻ is proposed to travel via the putative HCO₃⁻ channels BST1–3 (30) into the thylakoid lumen, where the carbonic anhydrase CAH3 (31–33) converts HCO₃⁻ into CO₂. This CO₂ can then diffuse from the thylakoid lumen into the pyrenoid, where Rubisco catalyzes fixation.

Ci fluxes in this system are thought to be powered by two distinct mechanisms: one using pH differences between compartments, and the other using active pumping of HCO₃⁻ across membranes. Proton pumping during the light reactions of photosynthesis results in a more acidic pH in the thylakoid lumen (pH 6) compared to the stroma (pH 8) (34–36). Since the pH of a compartment dictates the equilibrium ratio of CO₂ to HCO₃⁻, the intercompartmental pH differences can drive intercompartmental Ci concentration gradients, and hence Ci fluxes (18, 21). Additionally, any of the transmembrane HCO₃⁻ transporters could be active pumps that would drive Ci fluxes in the system.

Previous modeling works assuming active HCO₃- import (37–39) have supported the above mechanisms, but many unanswered questions remain: Does the CCM require active import of Ci? What is the energetic cost of operating the CCM? Do effective CCM strategies change with environmental CO₂ concentrations? What function does the starch sheath play in the CCM? And, how do the localization patterns of carbonic anhydrases benefit the CCM?

Our reaction-diffusion model suggests that diffusion barriers preventing CO₂ efflux from the pyrenoid matrix are essential to an effective and energetically efficient CCM. At air-level CO₂, these diffusion barriers enable a "passive" CCM that lacks any form of active Ci transport and is driven solely by intercompartmental pH differences. Our model of the CCM further reveals two distinct Ci uptake strategies, namely a passive CO₂ uptake strategy that employs a stromal carbonic anhydrase (LCIB) to convert a diffusive influx of CO₂ into HCO₃-, and an active HCO₃- uptake strategy that employs an active pump (LCIA) to directly import external HCO₃-. Moreover, the feasible Ci uptake strategies to support an effective CCM vary with external CO₂ levels: both strategies function at air-level CO₂, while active HCO₃- uptake is necessary under lower CO₂ conditions. We also demonstrate that proper spatial localization of carbonic anhydrases reduces futile carbon cycling, thereby enhancing CCM performance. Thus, our model illustrates the key biophysical principles necessary to build an effective and energetically efficient algal CCM. Based on these principles, we propose a stepwise engineering path to install an algal CCM into land plants.

Results

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A multi-compartment reaction-diffusion model of the Chlamydomonas CCM.

- 94 When adapted to air-level CO₂ conditions, chloroplasts isolated from Chlamydomonas show an
- ability to concentrate Ci similar to that of whole cells (40, 41). Thus, we model the chloroplast (Fig.
- 96 1A), with constant cytosolic CO₂ and HCO₃- concentrations representing external Ci conditions and
- 97 presumably maintained by the diffusion or import of Ci into the cytosol (see SI Appendix).
- 98 For simplicity, our reaction-diffusion model is spherically symmetric while taking into account the
- 99 essential spatial organization of the Chlamydomonas CCM (17). Specifically, we model the
- 100 chloroplast as a sphere comprised of three compartments: a spherical pyrenoid matrix in the center,
- a surrounding stroma bounded by a chloroplast envelope, and thylakoids that traverse both the
- 102 matrix and stroma (Fig. 1B). In Chlamydomonas, the thylakoids enter the pyrenoid matrix in the
- 103 form of roughly cylindrical membrane tubules, and near the center of the matrix they become
- interconnected to form a reticulated meshwork (17). In our spherically symmetric model, we
- account for this geometry implicitly by varying the local volume fraction and surface-to-volume ratio
- of the thylakoids (Fig. 1B, *Materials and Methods*, and *SI Appendix*, Section IC and Fig. S2).
- To understand how Ci is delivered from the cytosol outside the chloroplast to the pyrenoid matrix,
- we track Ci in each compartment in the form of CO₂, HCO₃-, and H₂CO₃ (with concentrations
- denoted by C, H^- , and H^0 , respectively), assuming that H_2CO_3 is always in equilibrium with HCO_3 -
- 110 (42, 43). For simplicity, we assume that the ratio of CO_2 to HCO_3^- is fixed by $H^- = 10C$ in the cytosol
- 111 (the consequences of different cytosolic Ci levels are discussed in SI Appendix). The first step in
- 112 Ci concentration is the entry of Ci into the chloroplast. We assume that CO_2 and H_2CO_3 diffuse
- across the chloroplast envelope at velocities of $\kappa^c = 300 \, \mu \text{m/s}$ and $\kappa^{H^0} = 30 \, \mu \text{m/s}$, respectively
- 114 (44, 45). By contrast, HCO₃- is negatively charged and thus has a much lower baseline velocity
- 115 $\kappa^{H^-} = 0.05 \,\mu\text{m/s}$ (44). Below, we will refer to the velocity of membrane permeation κ as
- 116 "permeability". Previous experiments suggest that LCIA, a formate/nitrite transporter homolog, is
- involved in HCO₃- transport across the chloroplast envelope (24, 46, 47). We model the action of
- LCIA with a tunable rate $\kappa_{\text{LCIA}}^{H^-}$. It is presently unclear whether LCIA is an active pump or a passive
- 119 channel; thus, we model LCIA with a tunable reversibility of inward HCO₃- transport across the
- 120 chloroplast envelope (Materials and Methods).
- Once Ci species enter the chloroplast stroma, the CO₂ to HCO₃ ratio is adjusted by the stromal
- 122 carbonic anhydrase (CA) LCIB, which catalyzes the reaction $CO_2 + H_2O \leftrightarrow HCO_3^- + H^+ (27-29)$.
- Since the interconversion of CO₂ and HCO₃- involves a proton, the equilibrium ratio of CO₂ to HCO₃-,
- $K^{\text{eq}} = 10^{6.1-\text{pH}}$, depends on the pH in each compartment (48) (*Materials and Methods*). Based on
- previous measurements and estimates, we set a pH of 8 in the pyrenoid matrix and stroma (34,
- 126 35), strongly favoring Ci in the form of HCO_3^- with an equilibrium ratio of approximately $H^- = 80C$.
- 127 In our model, the CA-mediated interconversion between CO₂ and HCO₃⁻ is described by reversible
- 128 Michaelis-Menten kinetics (Materials and Methods and SI Appendix, Section IB). Below, we will
- refer to the first-order rate constant of CO₂ to HCO₃ conversion of a given CA as the "rate" of that
- 130 enzyme.
- 131 All Ci species in the chloroplast can diffuse radially inside compartments and exchange between
- compartments (Fig. 1B and *Materials and Methods*). In particular, we assume that all Ci species
- diffuse across the thylakoid membranes, with a permeability of κ^{C} for CO₂, $\kappa^{H^{0}}$ for H₂CO₃, and

- $(\kappa^{H^-} + \kappa_{\rm BST}^{H^-})$ for HCO₃. Here, the tunable parameter $\kappa_{\rm BST}^{H^-}$ represents the additional permeability to
- 135 HCO₃- allowed by bestrophin-like channels that traverse the thylakoid membranes (30).
- 136 The lumen of the thylakoids has a pH of 6 (35, 36), favoring a roughly equal partition between CO₂
- and HCO₃, which is mediated by the luminal carbonic anhydrase CAH3 (31–33). Due to the pH
- differences, HCO₃ in the stroma can diffuse into the thylakoid lumen and be converted to CO₂ by
- 139 CAH3. This CO₂ can then diffuse into the pyrenoid matrix and be fixed by Rubisco. We assume
- that CO₂ fixation follows Michaelis-Menten kinetics with a maximum rate $V_{\text{max,Rbc}}^{C} = 15 \text{ mM/s}$, and
- an effective $K_{\rm m}$, $K_{\rm m}^{\rm eff}=76\,\mu{\rm M}$, taking into account competitive inhibition by O₂ (Materials and
- Methods, and SI Appendix, Table S1 and Section IB). CO₂ within the pyrenoid matrix can also
- diffuse back out into the stroma. Two chloroplast structures have been suggested to act as barriers
- preventing this diffusion, namely the starch sheath that surrounds the pyrenoid matrix and the
- stacks of thylakoid membranes present in the chloroplast stroma (Fig. 1A).
- In summary, the flux balance of intra-compartment reaction and diffusion and intercompartment
- 147 exchange sets the steady-state concentration profiles of Ci species in all compartments (Fig. 1B;
- see Materials and Methods for details). All of the model parameters were estimated from the
- 149 literature (Table 1, and SI Appendix, Table S1) except for the enzymatic rates of CAH3 and LCIB
- and the kinetic parameters of BST and LCIA transporters, for which we performed a systematic
- 151 scan within a range of reasonable values.
- We first present results for our baseline model, with LCIB diffuse throughout the stroma, BST
- 153 channels uniformly distributed across the thylakoid membranes, CAH3 localized to the thylakoid
- lumen within the pyrenoid, and Rubisco condensed within the pyrenoid matrix (Fig. 1C and D). The
- 155 baseline model lacks LCIA and the potential diffusion barriers to Ci mentioned above; we introduce
- these elements in later sections.

The baseline CCM model suffers from CO₂ leakage out of the pyrenoid matrix.

- 158 A functioning CCM must be out of thermodynamic equilibrium: it elevates the CO₂ concentration
- 159 locally around Rubisco. This nonequilibrium system is powered in part by the influx of light energy
- 160 collected by photosystems I and II, which is used to pump protons into the thylakoid lumen and
- thereby maintain a pH differential between compartments (49). Thus, we first ask: how effectively
- 162 can this pH gradient drive CCM function?
- 163 In our baseline model, CO₂ diffusing into the chloroplast is converted to HCO₃- in the high-pH
- stroma. Since passive diffusion of HCO₃⁻ back out across the chloroplast envelope is slow, HCO₃⁻
- becomes trapped in the chloroplast, resulting in a high level of HCO₃ in the stroma and the
- thylakoids that traverse it (Fig. 1C). The lower pH in the thylakoid lumen is then leveraged to convert
- 167 HCO₃ back to CO₂ within the pyrenoid radius (Fig. 1D). This CO₂ can enter the pyrenoid matrix,
- leading to an enhanced concentration of CO₂ at the location of Rubisco.
- 169 Despite enhancing CO₂ concentration around Rubisco, our baseline CCM model suffers from
- 170 significant CO₂ leakage out of the matrix (Fig. 1D). The first-order rate constant of Rubisco-
- 171 catalyzed CO₂ fixation is $V_{\rm max,Rbc}^{\it C}/K_{\rm m}^{\rm eff} \approx 200~{\rm s}^{-1}$. Thus, the average time required for a free CO₂
- molecule to be fixed by Rubisco in the pyrenoid matrix is $\tau = \left(V_{\text{max,Rbc}}^{c}/K_{\text{m}}^{\text{eff}}\right)^{-1} \approx 5 \text{ ms.}$ Over the
- same period of time, that molecule can diffuse over a typical distance $(D^c \tau)^{1/2} \approx 3 \mu m$, larger than
- 174 the radius of the pyrenoid $R_{\rm pyr} \approx 1 \, \mu m$. As a result, ~95% of CO₂ molecules that diffuse into the
- 175 pyrenoid matrix from the thylakoids leave the matrix without being fixed by Rubisco (SI Appendix,

Section IH and Fig. S3). Once this CO₂ reaches the stroma, it is recycled back into HCO₃⁻ by LCIB. While this HCO₃⁻ can re-enter the thylakoid lumen where it is again converted into CO₂ by CAH3 (Fig. 1D, black dashed loop), this recycling of Ci does not enhance the efficacy of the CCM, since the vast majority of CO₂ released in the pyrenoid does not remain there long enough to be fixed by Rubisco. One might think that increasing the rate at which HCO₃⁻ diffuses into the chloroplast could overcome this deficit of the system. However, adding LCIA as a passive channel for HCO₃⁻ at the chloroplast envelope does not solve the intrinsic deficiency caused by CO₂ leakage. In fact, there is no combination of LCIB catalytic rate and LCIA and BST channel rates that can achieve half-saturation of Rubisco with CO₂ (Fig. 2 A and B, and *SI Appendix*, Fig. S4 A and B). Thus, in the absence of a diffusion barrier, pH differences alone are not enough to concentrate sufficient CO₂ in the pyrenoid matrix to half-saturate Rubisco.

Structural barriers to CO₂ diffusion out of the pyrenoid matrix enable an effective CCM driven only by intercompartmental pH differences.

In order to operate a more effective CCM, the cell must reduce CO₂ leakage from the pyrenoid matrix. We examine whether adding a diffusion barrier to the baseline CCM model would be sufficient to concentrate substantially more CO₂ around Rubisco. We consider two *in vivo* structures of the Chlamydomonas chloroplast as potential barriers for Ci molecules leaving the matrix. The first is the thylakoid stacks, which comprise layers of membranes surrounding the pyrenoid that could effectively slow the diffusion of Ci in the stroma (17, 38) (Fig. 1A). In our spherically symmetric model, we treat the stroma traversed by thylakoid stacks as a homogeneous compartment where diffusion of each Ci species is slowed, as molecules must diffuse between or through the interdigitated thylakoid stacks (*Materials and Methods*). Indeed, a realistic geometry of the thylakoid stacks increases the diffusion path length of Ci in the stroma, reducing effective diffusion coefficients to as low as 3% of their unrestricted values (*SI Appendix*, Section IG and Fig. S5).

Another potential barrier is the starch sheath (Fig. 1A). This sheath forms around the pyrenoid matrix under the same environmental conditions that induce CCM activity in Chlamydomonas and has been suggested to reduce Ci efflux out of the matrix (19, 20). For simplicity, we model the starch sheath as a thin semi-permeable barrier around the matrix, with the same permeability κ_{starch} to all Ci species (*Materials and Methods*). Adding a starch sheath to the baseline model creates a discontinuity in carbon concentration across the matrix-stroma interface (*SI Appendix*, Fig. S6). We find that even a relatively high permeability $\kappa_{\text{starch}} \sim 100 \, \mu\text{m/s}$, a value similar to the permeability of a single lipid membrane bilayer to CO₂, renders the starch barrier effective enough that more than half of CO₂ leakage from the matrix occurs instead via the thylakoid tubules, which provide passages through the starch barrier (*SI Appendix*, Fig. S7). A somewhat lower starch sheath permeability, equivalent to 10 lipid bilayers, yields a CO₂ fixation flux almost identical to that of a totally impermeable starch sheath. Since starch consists of many lamellae of crystalline amylopectin (50–52), we hypothesize that its permeability to Ci is low enough that it can be neglected. Thus, we focus below on the case of impermeable starch, i.e., $\kappa_{\text{starch}} = 0$.

We find that adding either thylakoid stacks or a starch sheath to the baseline CCM model drastically reduces CO_2 leakage from the pyrenoid matrix to the stroma (SI Appendix, Figs. S6 and S7). As a result, the addition of either barrier under air-level CO_2 (10 μ M cytosolic) leads to a highly effective CCM that raises CO_2 concentrations in the matrix above the Rubisco K_m using only the nonequilibrium pH differential and passive Ci uptake (Fig. 2 E and H). The performance of a model including both barriers closely resembles the case with only an impermeable starch sheath (SI Appendix, Fig. S8); thus, we omit such a combined model from further discussion.

The optimal passive Ci uptake strategy utilizes cytosolic CO₂, not HCO₃.

- In addition to the requirement for a diffusion barrier, the efficacy of the CCM depends on enzyme
- 223 and HCO₃- channel rates (Fig. 2). What is the best strategy to passively transport and uptake Ci
- 224 when the CCM is powered only by the pH differences between compartments?
- 225 Since the algal CCM relies on CAH3 to convert HCO₃ to CO₂ for fixation by Rubisco, it is important
- 226 for stromal HCO₃- to enter the thylakoid lumen and reach CAH3. Indeed, our model shows that
- 227 Rubisco CO₂ fixation flux increases with BST passive HCO₃⁻ channel rates across the thylakoid
- membranes under all conditions explored in Fig. 2 (SI Appendix, Fig. S4).
- 229 To achieve an effective CCM, it is equally important to maintain a high level of HCO₃- in the
- 230 chloroplast stroma. Depending on LCIB activity, there are two possible passive Ci uptake strategies
- 231 to achieve this goal. If LCIB activity is low, CO₂ fixation flux increases with higher rates of the LCIA
- 232 HCO₃ channels (Fig. 2 B, E, and H), which facilitates the diffusion of cytosolic HCO₃ into the
- 233 chloroplast stroma (Fig. 2 C, F, and I). In contrast, if LCIB activity is high, CO₂ fixation flux is
- maximized when LCIA channel rates are low (Fig. 2 B, E, and H); in this case, a diffusive influx of
- 235 CO₂ into the chloroplast is converted by LCIB into HCO₃-, which becomes trapped and concentrated
- in the chloroplast (Fig. 2 C, F, and I). Under this scenario, fast HCO₃- channel transport across the
- 237 chloroplast envelope is detrimental, since it allows HCO₃-converted by LCIB to diffuse immediately
- back out into the cytosol (Fig. 2 B, E, and H).
- 239 Interestingly, for both modeled diffusion barriers we find that the highest CO2 fixation flux is
- achieved by employing LCIB for passive CO₂ uptake, not by employing LCIA channels for passive
- 241 HCO₃⁻ uptake (Fig. 2), even though HCO₃⁻ is more abundant than CO₂ in the cytosol. Key to this
- result is our assumption that the stroma (at pH 8) is more basic than the cytosol (at pH 7.1), which
- 243 allows LCIB to create a pool of HCO₃⁻ in the chloroplast stroma at a concentration higher than in
- the cytosol.

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- We note that LCIB activity is not always beneficial to CCM function, even when LCIA HCO₃-channel
- 246 rates are low. Specifically, without a starch sheath, high LCIB activity in the stroma draws more
- 247 CO₂ efflux out of the pyrenoid matrix by rapidly converting to HCO₃- some CO₂ molecules which
- 248 would otherwise diffuse back into the matrix (SI Appendix, Section IV and Fig. S9). In this case, the
- highest CO₂ concentration in the pyrenoid occurs at an intermediate LCIB activity (Fig. 2B and E,
- and *SI Appendix*, Fig. S9D). As an alternative to blocking CO₂ escape from the matrix with a starch
- sheath, this detrimental efflux of CO₂ can be reduced by localizing LCIB away from the pyrenoid,
- which leads to a monotonic increase of CO₂ fixation flux with LCIB activity (SI Appendix, Fig. S11).

Feasible Ci uptake strategies depend on the environmental level of CO₂.

- 254 While the passive CO₂ uptake strategy employing LCIB activity and pH differences can power the
- 255 CCM under air-level CO₂ (10 µM cytosolic), the Ci uptake rate is ultimately limited by the diffusion
- of CO₂ across the chloroplast envelope. Thus, we questioned whether this strategy is feasible at
- even lower environmental CO₂ concentrations. The largest possible flux of CO₂ diffusing into the
- 258 chloroplast is $\kappa^{C}C_{cyt}$, which is proportional to the cytosolic CO₂ concentration C_{cyt} . Consequently,
- when C_{cvt} is lower than 2 μ M, this diffusive influx becomes insufficient to achieve half-saturation of
- 260 Rubisco with CO₂ (SI Appendix, Section IIID). Indeed, our simulations show that under very low
- 261 CO₂ conditions (1 µM cytosolic) (53), a chloroplast using the passive CO₂ uptake strategy can

achieve at most 25% of its maximum CO₂ fixation flux, even in the presence of barriers to Ci diffusion (Fig. 3).

What strategies could Chlamydomonas use to continue growing well under very low CO₂ conditions? Previous research has shown that at very low CO₂ an LCIB single mutant is viable while an LCIB-LCIA double mutant fails to grow (46), suggesting that HCO₃⁻ uptake by LCIA is crucial to growth under this condition. Since passive HCO₃⁻ uptake cannot concentrate more Ci than passive CO₂ uptake (Fig. 2), we hypothesize that LCIA could actively pump HCO₃⁻ into the chloroplast under very low CO₂ conditions. To test whether active HCO₃⁻ uptake can function as an alternative import mechanism to create a high concentration of stromal HCO₃⁻, we considered a model employing active LCIA HCO₃⁻ pumps without LCIB activity (Fig. 3 A, D, and G). We find that, indeed, HCO₃⁻ pumping enables saturating CO₂ fixation by Rubisco under both air-level CO₂ and very low CO₂ conditions (Fig. 3 and *SI Appendix*, Fig. S12).

While light energy drives the passive CO₂ uptake strategy by pumping protons across the thylakoid membranes to establish pH differences between compartments, active pumping of HCO₃⁻ requires additional forms of energy expenditure. What is the energy cost of a CCM that employs active HCO₃⁻ uptake, and how does this cost compare to that of the passive CO₂ uptake strategy? To answer these questions, we follow the theoretical framework of nonequilibrium thermodynamics to compute the energy cost of different Ci uptake strategies (*SI Appendix*, Section IIB) (54). Our calculation shows that futile-cycle fluxes, including Ci recycling flux through LCIB and Ci leakage flux out of the chloroplast, increase the energy cost of the CCM (*SI Appendix*, Figs. S13 and S14). Indeed, a chloroplast without diffusion barriers suffers from a very large futile-cycle flux (Fig. 1D) and hence runs a much more energetically expensive CCM than a chloroplast with diffusion barriers (Fig. 3). We note that free energy is also dissipated by nonequilibrium diffusion processes. Thus, a well-mixed compartment model assuming fast intra-compartment Ci diffusion and fast BST-mediated HCO₃-diffusion across the thylakoid membrane (*Materials and Methods* and *SI Appendix*, Section III and Fig. S15) yields a higher energetic efficiency than the full model with finite rates of diffusion (Fig. 3 H and I, black dashed curves).

Interestingly, the most energy-efficient Ci uptake strategy depends on both the type of diffusion barrier employed and the environmental CO_2 conditions. At air-level CO_2 with a starch sheath diffusion barrier, the passive CO_2 uptake strategy has a slightly higher energy efficiency than the active HCO_3^- uptake strategy (Fig. 3H). Without a starch sheath, however, the active HCO_3^- uptake strategy is energetically less expensive (Fig. 3 B and E). Additionally, we find under very low CO_2 conditions that no amount of energy input can power CO_2 concentration to a level higher than the Rubisco $K_{\rm m}$ using passive CO_2 uptake. Therefore, HCO_3^- pumping is required for an effective CCM at very low CO_2 (Fig. 3 F and I, and *SI Appendix*, Fig. S16). Our results may thus provide mechanistic insights into the observation that Chlamydomonas employs different CO_2 -concentrating strategies depending on the external concentration of CO_2 (46). Specifically, for a modeled chloroplast with a starch sheath, at air-level external CO_2 the least costly strategy that allows for half-saturation of Rubisco is activating LCIB for passive CO_2 uptake. At lower levels of external CO_2 , the least costly strategy is active HCO_3^- pumping across the chloroplast envelope combined with LCIB activity to recapture CO_2 that leaks from the pyrenoid matrix (*SI Appendix*, Figs. S17 and S18).

Localization of carbonic anhydrases alters Ci fluxes in the chloroplast.

In response to varying external CO₂ conditions, changes occur not only in the Ci uptake strategy but also in the enzyme localization patterns in the Chlamydomonas CCM. In particular, LCIB

localization varies, changing from diffuse throughout the stroma under air-level CO₂ to localized at the pyrenoid periphery under very low CO₂ (46, 55). It has also been suggested that CAH3 localizes toward the intra-pyrenoid portion of the thylakoid tubules under air-level CO₂ (33). These findings prompted us to wonder whether CA localization could impact the performance of the modeled CCM.

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To explore this question, we vary the start radius $R_s^{\rm LCIB}$ of LCIB, i.e., how close to the chloroplast center LCIB localization starts, and the end radius $R_{\rm e}^{\rm CAH3}$ of CAH3, i.e., how far CAH3 extends through the thylakoid tubules (Fig. 4A). We explore this in our spherically symmetric model while maintaining the total number of molecules of each CA. Our simulations reveal three CA localization patterns that would compromise CCM performance. First, when LCIB extends into the pyrenoid matrix, i.e., when $R_s^{\rm LCIB}$ is smaller than the pyrenoid radius $R_{\rm pyr}$, LCIB converts Rubisco's substrate, CO₂, into HCO₃⁻. Since HCO₃⁻ cannot be fixed by Rubisco, this localization of LCIB decreases CO₂ fixation (Fig. 4 B, D, and F, region i). Second, when CAH3 is distributed in the thylakoids outside the pyrenoid, CO₂ molecules produced by this CAH3 may diffuse directly into the stroma, where they can be converted to HCO₃- by LCIB. While this HCO₃- can then diffuse back into the thylakoid lumen and undergo conversion to CO₂ again, such futile cycling decreases both the efficacy and energy efficiency of the CCM (Fig. 4 B-F, region ii, and SI Appendix, Fig. S19). Finally, concentrating CAH3 to a small region of thylakoid lumen in the center of the pyrenoid increases the distance over which HCO₃-needs to diffuse before it is converted to CO₂, thus lowering the CO₂ production flux by CAH3 (Fig. 4 B, D, and F, region 3). All these results hold true both at air-level CO₂ employing passive CO₂ uptake (Fig. 4) and at very low CO₂ employing active HCO₃ uptake (SI Appendix, Fig. S20). Thus, our model shows that proper CA localization is crucial to overall CCM performance.

Activity and localization of LCIB could reduce Ci leakage out of the chloroplast.

To better understand the role of LCIB and its in vivo localization pattern at very low CO2, we next consider a model employing HCO $_3$ pumping across the chloroplast envelope. Here, we fix $R_s^{\rm LCIB} =$ $R_{\rm pvr}$ and vary both the end radius of LCIB, $R_{\rm e}^{\rm LCIB}$, which defines how far LCIB extends toward the chloroplast envelope, and the total number of LCIB molecules (Fig. 5A). In the absence of a starch sheath, localizing LCIB to the pyrenoid periphery harms the CCM; such localization results in a large CO₂ efflux out of the matrix due to rapid conversion to HCO₃⁻ (SI Appendix, Fig. S21). Thus, we focus on a model employing a starch sheath barrier. Since actively accumulating Ci in the form of HCO₃ costs energy, it is energetically wasteful if any Ci molecules diffuse out of the chloroplast without being fixed (Fig. 5 B-C, region iii). Consequently, localizing LCIB near the starch sheath increases energy efficiency by recapturing CO₂ molecules that diffuse out of the matrix and trapping them as HCO₃ in the chloroplast (Fig. 5 B-C, region i). In contrast, diffuse LCIB is suboptimal because LCIB near the chloroplast envelope could rapidly convert HCO3- pumped into the chloroplast into CO₂, which can then immediately diffuse back out into the cytosol (Fig. 5 B-C, region ii). This futile cycle occurs when HCO₃- pumping across the chloroplast envelope is fast and irreversible (SI Appendix, Fig. S22). Our model thus suggests that under very low CO2 and in the presence of a strong CO₂ diffusion barrier around the pyrenoid, localizing LCIB at the pyrenoid periphery allows for efficient Ci recycling, therefore enhancing CCM performance.

Possible stepwise engineering strategies for transferring algal CCM components to land plants.

Many land plants, including most crop plants, are thought to lack any form of CCM. Engineering an algal CCM into land plants has emerged as a promising strategy to potentially increase crop yields through enhanced CO₂ fixation (12, 13). Despite early engineering advances (47, 56), it remains to

be determined what minimal set of engineering steps is needed and in what order these steps should be implemented to establish an effective algal CCM in a plant chloroplast.

To address this question within our model, we measured the efficacy and energetic efficiency of 216 configurations of chloroplast-based CCM, varying the presence and localization of Rubisco, thylakoid and stromal CAs, HCO₃- channels on the thylakoid membranes and the chloroplast envelope, and diffusion barriers (*SI Appendix*, Fig. S23). Note that we restrict our focus to modeled CCMs that employ passive Ci uptake strategies at 10 µM cytosolic CO₂, which is close to the CO₂ levels experienced by plant chloroplasts (57). The use of the passive Ci uptake strategy simplifies the engineering problem by eliminating the needs to engineer active HCO₃- transport at the chloroplast envelope and to decrease carbonic anhydrase activity in the stroma.

To the best of our knowledge, the typical land plant chloroplast contains diffuse CA and diffuse Rubisco in the stroma, and lacks HCO₃⁻ channels and diffusion barriers (58) (Fig. 6A). Studies have also suggested the presence of native plant CAs diffuse in the thylakoid lumen (59), so we have included these CAs in our modeled plant chloroplast configuration. This configuration supports only 10% of the maximum CO₂ fixation flux through Rubisco, and its efficacy is identical to that of the same configuration without thylakoid CAs (*SI Appendix*, Table S4). By contrast, the configuration that achieves the highest CO₂ fixation flux, >70% of the maximum, corresponds to a Chlamydomonas chloroplast employing passive CO₂ uptake and a strong diffusion barrier around the pyrenoid (Figs. 2D and 6A).

We next chart an engineering path from the configuration representing a plant chloroplast (Fig. 6, starting configuration) to the Chlamydomonas configuration that maximizes CO₂ fixation flux (Fig. 6, desired configuration). While forming the pyrenoid matrix through the condensation of Rubisco and excluding LCIB from this matrix could be considered two separate engineering steps, previous research suggests that the matrix might inherently exclude proteins larger than ~78 kDa (55). Since the plant stromal CA is thought to form complexes with a molecular weight larger than 78 kDa (60), we assume that localizing Rubisco into a matrix and localizing the plant stromal CA outside that matrix can be achieved in a single engineering step. Thus, the four necessary engineering steps are to localize Rubisco and the stromal CA, to localize the thylakoid CA, to add HCO₃⁻ channels spanning the thylakoid membranes, and to add a starch sheath around the newly created pyrenoid matrix (Fig. 6B). (Note that for simplicity we consider adding HCO₃⁻ channels uniformly to both the matrix/thylakoid interface and the stroma/thylakoid interface.) In addition, the spatial proximity between the pyrenoid matrix and the thylakoids is important for the engineered CCM, which we address in the Discussion.

We find that the order in which these engineering steps are implemented matters for the efficacy and efficiency of the CCM in intermediate stages. Notably, adding HCO₃- channels on the thylakoid membranes before the stromal and thylakoid CAs are localized leads to an energetically inefficient configuration (Fig. 6B, blue oval) due to the futile cycling generated by overlapping CAs (Fig. 4, region ii). Additionally, adding a starch sheath before HCO₃- channels are added to the thylakoids does not increase CO₂ fixation (Fig. 6B, gray oval), because without channels HCO₃- cannot readily diffuse to the thylakoid CA to produce CO₂, and the diffusion of CO₂ to Rubisco from the stroma is impeded by a starch sheath.

Finally, we suggest a four-step engineering path that avoids intermediate configurations with decreased efficacy or extreme energetic inefficiency (Fig. 6B, green arrows): The first two steps are the localization of Rubisco and the stromal CA and the localization of the thylakoid CA to the thylakoids inside the newly formed pyrenoid matrix. These steps do not yield notable changes to

either the efficacy or the efficiency of the CCM, and they could be implemented in either order. The next step is to introduce HCO₃- channels to the thylakoid membranes, which increases the CO₂ fixation flux by ~100%. This step also increases the cost of the CCM to around 10 ATP per CO₂ fixed; such a high-cost step cannot be avoided, and all other possible paths with increasing efficacy at each step have more costly intermediate configurations (Fig. 6B and Table S4). The final step of the suggested path is to add a starch sheath, which drastically increases the efficacy and energy efficiency of the CCM by blocking CO₂ leakage from the pyrenoid matrix.

One additional benefit of this path is that it provides opportunities for assessing the success of introducing HCO₃- channels spanning the thylakoid membranes. The increased CO₂ fixation flux resulting from this step in the proposed path would provide evidence that the installed channels are functional, and could also be used to apply a selective pressure to aid engineering in the event that merely transforming BST channels into plants does not yield HCO₃- transport across the thylakoid membranes.

An effective CCM requires Ci uptake, transport, and trapping.

What are the essential building blocks of an effective pyrenoid-based CCM? Investigating the performances of the various CCM configurations described in the previous section reveals three central modules of an effective CCM (Fig. 7A): (i) an effective Ci uptake strategy that employs either a carbonic anhydrase (LCIB) to convert a diffusive influx of CO₂ into HCO₃⁻ or an active pump (LCIA) to import external HCO₃⁻ into the chloroplast (Fig. 3), (ii) a system consisting of an HCO₃⁻ channel (BST) in the thylakoid membranes and another carbonic anhydrase (CAH3) that together transport HCO₃⁻ to near Rubisco and then convert the HCO₃⁻ to CO₂, and (iii) a pyrenoid matrix that houses Rubisco, surrounded by diffusion barriers that trap CO₂ inside the matrix. We find that CCM configurations lacking any one of these modules show a compromised ability to concentrate CO₂ (Fig. 7B). Thus, our characterization illustrates the minimal functional modules for an algal CCM.

Discussion

The algal CCM elevates CO_2 around Rubisco, thereby enhancing photosynthesis. This CCM has the potential to be transferred into crop plants to increase their photosynthetic efficiency. To better understand how the algal CCM works, we develop a multi-compartment reaction-diffusion model based on the Chlamydomonas chloroplast. We provide a quantitative framework to evaluate overall CCM performance, considering both the efficacy and the energetic efficiency of the CCM (SI Appendix, Sec. IIC and Fig. S24). While previous works have suggested the operational principles underlying an effective CCM, our analysis lays a quantitative and biophysical groundwork for these principles as discussed below.

According to our model, a diffusion barrier that blocks CO₂ leakage out of the pyrenoid matrix is essential to an effective CCM in Chlamydomonas. Indeed, previous modeling works have demonstrated the necessity of diffusion barriers for the cyanobacterial CCM (61, 62). Recent experiments in Chlamydomonas showed that mutants either lacking the starch sheath or having a thinner starch sheath have decreased CO₂-concentrating activity, suggesting that the starch sheath is required for an effective CCM (20). Further experiments are needed to clarify the role of starch sheath in the CCM, and physical properties of the starch sheath such as its permeability to inorganic carbon need to be defined. Our modeling results provide additional testable predictions for experiments to examine a role for starch as a barrier to CO₂ escape. For example, if indeed the starch sheath functions as an effective diffusion barrier, our model predicts that overexpressing

LCIB in wildtype cells will not affect their growth in air (Fig. 2H). By contrast, we predict that overexpressing LCIB in a starchless mutant of Chlamydomonas will lead to a growth defect under air-level CO₂ — the LCIB will effectively "pull" CO₂ from the pyrenoid matrix (Fig. 2E). Testing these mutant phenotypes will shed light on the nature of the diffusion barriers present in the algal CCM.

Our results demonstrate two distinct Ci uptake strategies, i.e., employing LCIB for passive CO₂ uptake and employing LCIA for active HCO₃- pumping. Our modeling shows that an effective CCM must use the active HCO₃ uptake strategy to function under very low CO₂. Thus, we suggest that the algal CCM may switch from passive CO₂ uptake under air-level CO₂ to active HCO₃ uptake under very low CO2. This proposal is consistent with and provides a mechanistic explanation for previous experiments studying LCIA and LCIB mutants (27, 46, 63); compared to wildtype cells, the *lcia* mutant shows a significantly decreased photosynthetic activity across varying external Ci levels at pH 9.0 where almost all Ci is in the form of HCO3-, presumably due to the lack of a functional HCO₃ uptake system (46). The photosynthetic activity of the *lcia* mutant is raised at pH 7.3, where more Ci is in the form of CO₂, consistent with our model that LCIB facilitates CO₂ uptake in this mutant. The *lcib* mutant fails to grow in air, presumably due to the lack of a functional CO₂ uptake system, but recovers growth under very low CO₂ — an effect we attribute to the activation of an HCO₃ uptake system under this condition (24, 46). Indeed, further knockdowns of genes encoding putative HCO₃- transporters LCIA or HLA3 in the *lcib* mutant result in dramatic decreases in Ci uptake and growth under very low CO₂ (23, 46). Our model predicts that there must be an active HCO₃⁻ pump in Chlamydomonas, possibly LCIA, which has yet to be shown experimentally. At this time, only the diatom and bacterial homologs of LCIB have been explicitly shown to have carbonic anhydrase activity (29), but our model and the observed *lcib* mutant phenotypes together strongly suggest that LCIB has carbonic anhydrase activity. Future functional characterizations of Chlamydomonas LCIA and LCIB will be crucial to verify their proposed roles in Ci uptake. Interestingly, the additional mutation of cah3 in the lcib mutant rescues the air-dier phenotype of the latter (63), while our modeled configurations corresponding to these two mutants show similarly low CO₂ concentrating activity (Table S4), which would predict that they both have growth defects. Further experimentation is thus required to shed light on how Ci is taken up by the chloroplast and how sufficient CO₂ reaches the pyrenoid in the *cah3-lcib* double mutant.

Compared to the active HCO₃⁻ uptake strategy, our model suggests that the passive CO₂ uptake strategy has a similar performance under air-level CO₂ and has a much lower efficacy under very low CO₂ (Fig. 3). One may ask: what are the potential benefits of employing passive CO₂ uptake? One possibility is that, by employing both Ci uptake strategies, the algal CCM can remain effective under environments with various Ci compositions (*SI Appendix*, Fig. S25). Another possibility regards the feasibility of maintaining cytosolic Ci levels. Since there is no known carbonic anhydrase in the Chlamydomonas cytosol, maintaining HCO₃⁻ levels requires expressing HCO₃⁻ transporters at the cell membrane, while cytosolic CO₂ can be replenished by external CO₂ diffusing across the cell membrane.

In addition to the Ci uptake strategy employed, the localization of LCIB also changes *in vivo* in response to different external Ci levels. Specifically, under air-level CO₂ LCIB is distributed throughout the stroma, while the enzyme is localized around the starch sheath under very low CO₂ (28, 46, 55). Our model suggests that such differences in localization could improve performance under the corresponding Ci uptake strategies: when the passive CO₂ uptake strategy is used at air-level CO₂, varying LCIB localization only minimally affects CCM performance as long as the enzyme is confined to the stroma (*SI Appendix*, Fig. S21). In contrast, when HCO₃⁻ is actively pumped into the chloroplast, localizing LCIB near the pyrenoid periphery and away from the chloroplast envelope is advantageous to avoid the conversion of HCO₃⁻ near the chloroplast

envelope into CO₂, which can immediately leak back out into the cytosol (Fig. 5). Thus, our model predicts that diffuse LCIB in the chloroplast *in vivo* at very low external CO₂ could lead to a CCM-deficient phenotype — similar to the phenotype observed when an exogenous CA was introduced diffusely into the cytosol of cyanobacteria that employ active HCO₃⁻ transport across the cell membrane (7). Understanding experimentally how LCIB localization impacts Ci fluxes in the chloroplast would advance our understanding of the Chlamydomonas CCM.

The analysis of Ci fluxes in our model supports the long-held view that the thylakoid tubules traversing the pyrenoid and converging in the pyrenoid center are capable of delivering stromal HCO₃⁻ to the pyrenoid, where it can be converted to CO₂ by CAH3 (18, 21). However, this unique architecture of thylakoid tubules is not essential for transporting HCO₃⁻ and producing CO₂. Indeed, algae display a variety of thylakoid tubule morphologies, such as multiple non-connecting parallel thylakoid stacks passing through the pyrenoid, a single disc of thylakoids bisecting the pyrenoid matrix, or thylakoid sheets surrounding but not traversing the pyrenoid (64–67). Our calculations support the idea that different morphologies could in principle allow the functioning of an effective CCM, as long as HCO₃⁻ can diffuse into the low-pH thylakoid lumen and the thylakoid CA is localized near the pyrenoid to convert HCO₃⁻ to CO₂ (SI Appendix, Fig. S26).

In our model, thylakoid tubules traversing the starch sheath are the main route for CO₂ escape from the pyrenoid, which is detrimental to CO₂ concentration. Additionally, this particular geometry is not required for HCO₃⁻ delivery to the pyrenoid (*SI Appendix*, Fig. S26 D–F). Nevertheless, Chlamydomonas cells appear to maintain these tubule structures *in vivo*. It is possible that, by connecting to the thylakoid network outside of the pyrenoid, thylakoid tubules can also serve as a route for protons to diffuse in, which helps to maintain the acidic pH in the lumen of the intrapyrenoid tubules. Future experimental studies will be important to investigate the trade-off between proton supply and CO₂ leakage in employing thylakoid tubules traversing the pyrenoid matrix.

A key driver of the algal CCM is the pH difference maintained across different compartments. However, our model does not explicitly consider the reaction-diffusion kinetics of protons, but rather assumes a uniform pH in each compartment. Previous *in vivo* measurements of the pH biosensor pHluorin in Chlamydomonas suggest that the pyrenoid matrix has a relatively uniform basic pH (34), yet it remains unclear how the uniformity is achieved. Protons are produced and consumed in the reactions catalyzed by CA. In addition, Rubisco CO₂ fixation yields two protons for every CO₂ fixed (5). Our calculations suggest that the concentrations of free protons at measured physiological pH values are too low to account for the corresponding fluxes without creating noticeable pH gradients (*SI Appendix*, Sec. VI). Thus, efficient transport of protons must involve proton carriers. A recent modeling work suggests that two metabolites, RuBP and 3-PGA, could play an important role in buffering the pH of CO₂-fixing Rubisco condensates (68) — these metabolites have pKa values of 6.7 and 6.5, respectively, and are present at millimolar concentrations in the pyrenoid and stroma (69). Understanding the molecular mechanisms underlying proton transport will be an important topic for future studies.

Based on the known molecular machinery of the Chlamydomonas CCM, we proposed a minimal set of engineering steps to install an effective CCM in plant chloroplasts (Fig. 6). In our favored engineering path, Rubisco first needs to be assembled into a CA-free pyrenoid-like condensate *in vivo*. A phase-separated pyrenoid matrix has been successfully reconstructed in Arabidopsis chloroplasts (56), but it remains to be verified whether the native stromal CA is excluded from the engineered pyrenoid. Then, the newly formed matrix needs to be positioned proximal to low-pH thylakoids, and the thylakoid CA needs to be localized to the pyrenoid-proximal thylakoid lumen. Recent work in Chlamydomonas has shown that a Rubisco-binding motif targets proteins to the

- pyrenoid, and appears to link the matrix to the intra-pyrenoid tubules and starch sheath (70), thus providing a framework for manipulating the organization of an engineered pyrenoid. For example, constructing a fusion protein of the plant thylakoid CA and a membrane protein containing the Rubisco-binding motif may promote the desired colocalization of the pyrenoid matrix, thylakoids, and thylakoid CA. The next step in our favored engineering path is to insert HCO₃⁻ channels through the thylakoid membranes, which could double the CO₂ fixation flux according to our calculation. Particularly important is targeting HCO₃⁻ channels specifically to the thylakoid membranes, but not to the chloroplast membrane, since adding HCO₃⁻ channels to the latter will lead to severe HCO₃⁻ leakage out of the chloroplast. Native thylakoids may naturally form a CO₂ diffusion barrier, which is expected to increase the performance of the CCM. Further studies of the pyrenoid starch sheath in Chlamydomonas will enable its reconstitution around the engineered pyrenoid, which we expect will maximize the efficacy and energetic efficiency of the CCM.
- We hope that our model provides practical information for engineers aiming to transfer algal machinery into plants, and that it will serve as a useful quantitative tool to guide basic CCM studies in the future.

Materials and Methods

See attached pdf.

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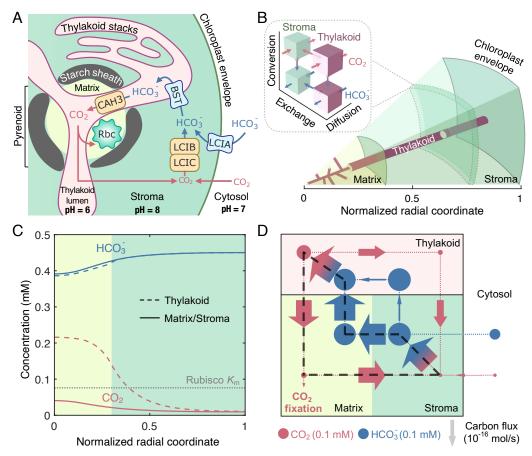


Fig. 1. A multi-compartment reaction-diffusion model describes the Chlamydomonas CCM. (A) Cartoon of a Chlamydomonas chloroplast with known CCM components. HCO₃- is transported across the chloroplast membrane by LCIA and across the thylakoid membranes by BST1-3 (referred to as BST henceforth for simplicity). In the acidic thylakoid lumen, a carbonic anhydrase CAH3 converts HCO₃- into CO₂, which then diffuses into the pyrenoid matrix, where the CO₂-fixing enzyme Rubisco (Rbc) is localized. CO2 leakage out of the matrix and out of the chloroplast can be impeded by potential diffusion barriers — a starch sheath and stacks of thylakoids — and by conversion to HCO₃⁻ by a CO₂ recapturing complex LCIB/LCIC (referred to as LCIB henceforth for simplicity) in the basic chloroplast stroma. (B) A schematic of the modeled CCM, which considers intra-compartment diffusion and inter-compartment exchange of CO₂ and HCO₃-, as well as their interconversion, as indicated in the *Inset*. Color code as in A. The model is spherically symmetric and consists of a central pyrenoid matrix surrounded by a stroma. Thylakoids run through the matrix and stroma; their volume and surface area correspond to a reticulated network at the center of the matrix extended by cylinders running radially outward. (C) Concentration profiles of CO₂ and HCO₃in the thylakoid (dashed curves) and in the matrix/stroma (solid curves) for the baseline CCM model that lacks LCIA activity and diffusion barriers. Dotted gray line indicates the effective Rubisco K_m for CO₂. Color code as in A. (D) Net fluxes of inorganic carbon between the indicated CCM compartments. The width of arrows is proportional to flux; area of circles is proportional to the average molecular concentration in the corresponding regions. The black dashed loop denotes the major futile cycle of inorganic carbon in the chloroplast. Color code as in A. For C and D, LCIAmediated chloroplast membrane HCO₃ channel transport rate $\kappa_{\rm chlor}^{H^-}$ = 10⁻⁸ m / s, BST-mediated

thylakoid membrane HCO_3^- channel transport rate $\kappa_{\rm thy}^{H^-}$ = 10^{-2} m / s, LCIB rate $V_{\rm LCIB}$ = 10^3 / s, and CAH3 rate = 10^4 / s (see *Materials and Methods* for details). Other parameters of the model are estimated from experiments (Table 1 and *SI Appendix*, Table S1).

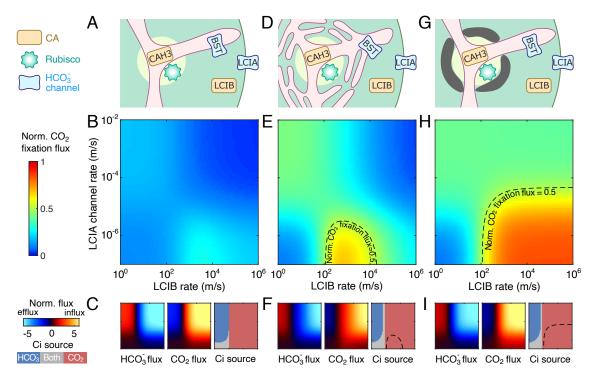


Fig. 2. Structural barriers to CO₂ diffusion out of the pyrenoid matrix enable an effective CCM driven only by intercompartmental pH differences. A model with no barrier to CO₂ diffusion out of the pyrenoid matrix (A–C) is compared to a model with thylakoid stacks slowing inorganic carbon diffusion in the stroma (D–F, see SI Appendix, Sec. IG) and a model with an impermeable starch sheath (G–I) under air-level CO₂ (10 μM cytosolic). (A, D, and G) Schematics of the modeled chloroplast. (B, E, and E) Heatmaps of normalized CO₂ fixation flux, defined as the ratio of the total Rubisco carboxylation flux to its maximum if Rubisco were saturated, at varying HCO₃- channel transport rates across the chloroplast envelope and varying LCIB rates. The HCO₃- channel transport rate across the thylakoid membrane is the same as in Fig. 1C and D. For E and E, dashed black curves indicate a normalized CO₂ fixation flux of 0.5. (E, E, and E) Overall fluxes of HCO₃- (E) (E) and CO₂ (E) (E) (E) and CO₃- channel transport rates across the chloroplast envelope and varying LCIB rates. Negative values denote efflux out of the chloroplast. The inorganic carbon (Ci) species with a positive influx is defined as the Ci source, shown in E0 (E1) subpanels. Axes are the same as E1, E2, and E3.

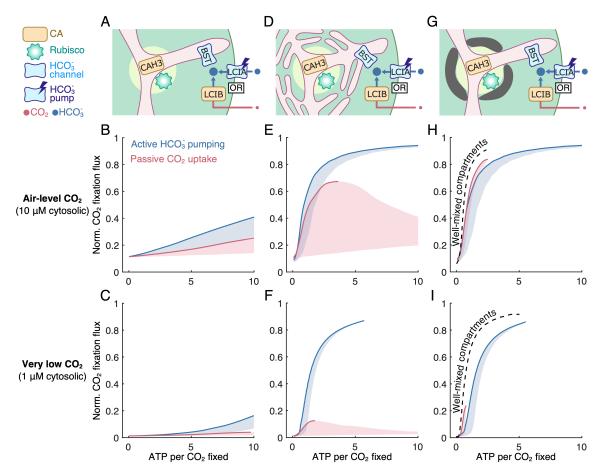


Fig. 3. Feasible inorganic carbon uptake strategies for the chloroplast depend on the environmental level of CO₂. Results are shown for (A–C) a model with no barrier to CO₂ diffusion out of the pyrenoid matrix, (D–F) a model with thylakoid stacks serving as diffusion barriers, and (G–I) a model with an impermeable starch sheath. (A, D, and G) Schematics of the modeled chloroplast employing LCIB for passive CO₂ uptake (red), or employing active HCO₃- pumping across the chloroplast envelope and no LCIB activity (blue). (B–C, E–F, and I–I) CCM performance under (B, E, and I) air-level CO₂ (10 μM cytosolic) and under (C, F, and I) very low CO₂ (1 μM cytosolic), measured by normalized CO₂ fixation flux versus ATP spent per CO₂ fixed, for the two inorganic carbon uptake strategies in A, D, and G. Solid curves indicate the minimum energy cost necessary to achieve a certain normalized CO₂ fixation flux. Shaded regions represent the range of possible performances found by varying HCO₃- transport rates and LCIB rates. Color code as in A. For H and I, dashed black curves indicate the optimal CCM performance of a simplified model that assumes fast intra-compartmental diffusion, fast HCO₃- diffusion across the thylakoid membranes, and fast equilibrium between CO₂ and HCO₃- catalyzed by CAH3 in the thylakoid tubules inside the pyrenoid (see *Materials and Methods* and SI *Appendix*, Sec. III).

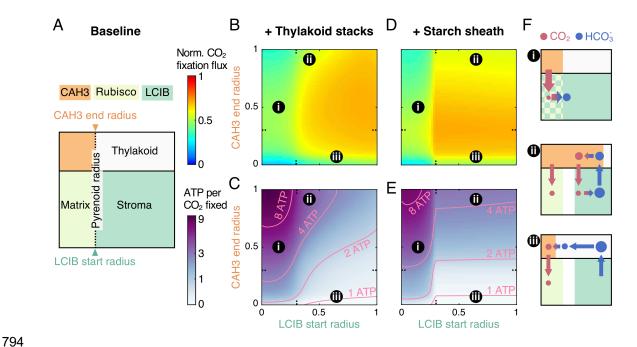


Fig. 4. Localization of carbonic anhydrases alters Ci fluxes in the chloroplast and enhances CCM performance. (A) Schematics of varying localization of carbonic anhydrases. The CAH3 domain starts in the center of the intra-pyrenoid tubules (radius r = 0), and the LCIB domain ends at the chloroplast envelope. CAH3 end radius and LCIB start radius are varied in a modeled chloroplast employing the passive CO₂ uptake strategy under air-level CO₂, (B-C) with thylakoid stacks slowing inorganic carbon diffusion in the stroma or (D-E) with an impermeable starch sheath. Color code is the same as in Fig. 1D. Orange denotes region occupied by CAH3. (B, D) Normalized CO₂ fixation flux and (C, E) ATP spent per CO₂ fixed when the localizations of carbonic anhydrases are varied. (E) Schematics of inorganic carbon fluxes for the localization patterns indicated in E-E. Color code is the same as in E and E and E and E is the same as in Fig. 1D. Simulation parameters are the same as in Fig. 1C and E.

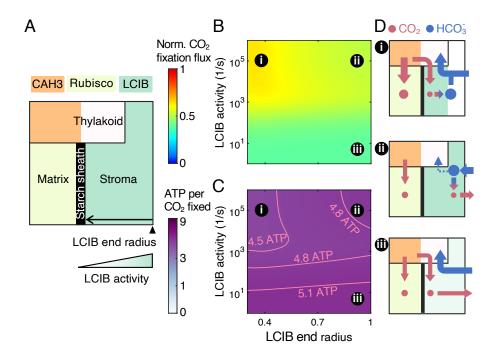


Fig. 5. Localization of LCIB around the pyrenoid periphery reduces Ci leakage out of the chloroplast. (*A*) Schematics of varying activity and end radius of LCIB in a modeled chloroplast employing an impermeable starch sheath and active HCO₃⁻ pumping across the chloroplast envelope under very low CO₂. Color code as in Fig. 4A. The LCIB domain starts at the pyrenoid radius (0.3 on the *x* axis in *B* and *C*). (*B*) Normalized CO₂ fixation flux and (*C*) ATP spent per CO₂ fixed when the designated characteristics of LCIB are varied. (*D*) Schematics of inorganic carbon fluxes for the LCIB states indicated in *B* and *C*. Color code as in Fig. 4F. Simulation parameters as in Fig. 4. Active HCO₃⁻ pumping is described by the rate κ_{chlor} = 10⁻⁴ m / s and the reversibility γ = 10⁻⁴. In order to show a notable variation in normalized CO₂ fixation flux, a model with shortened thylakoid tubules is simulated (see *Materials and Methods*). The qualitative results hold true independent of this specific choice.

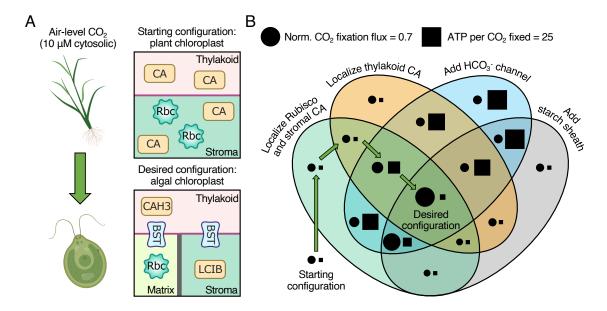


Fig. 6. Proposed engineering path for installing an algal CCM into land plants. (*A*) Schematics of (*Top*) the starting configuration representing a typical plant chloroplast that contains diffuse thylakoid CA, diffuse stromal CA, and diffuse Rubisco, and lacks HCO₃⁻ transporters and diffusion barriers, and (*Bottom*) the desired configuration representing a Chlamydomonas chloroplast that employs the passive CO₂ uptake strategy and a starch sheath (as in Fig. 2G). (*B*) Venn diagram showing the normalized CO₂ fixation flux (circle, area in proportion to magnitude) and ATP spent per CO₂ fixed (square, area in proportion to magnitude) of various configurations after implementing the designated changes. Green arrows denote the proposed sequential steps to transform the starting configuration into the desired configuration (see text). The starting configuration has a normalized CO₂ fixation flux of 0.11 and negligible ATP cost. All costs below 0.8 ATP per CO₂ fixed are represented by a square of the minimal size.

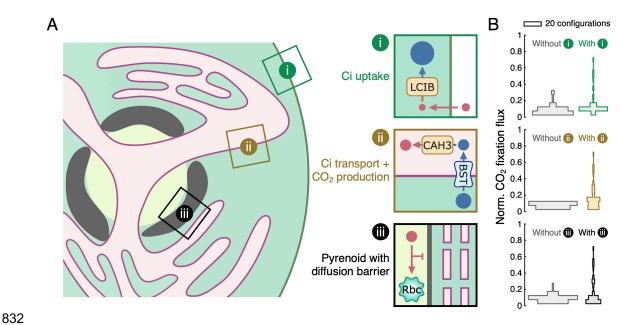


Fig. 7. An effective CCM is comprised of three essential modules. (*A*) Schematics of the three essential modules with designated functions. Same style as in Fig. 1A. In Chlamydomonas, LCIB can be used for passive uptake of CO₂ which is then trapped in the stroma as HCO₃⁻ (module i); BST allows stromal HCO₃⁻ to diffuse into the thylakoid lumen where CAH3 converts HCO₃⁻ into CO₂ (module ii); and a starch sheath and thylakoid stacks could act as diffusion barriers to slow CO₂ escape out of the pyrenoid matrix (module iii). (*B*) Histograms of normalized CO₂ fixation flux for CCM configurations without (*left*, gray) or with (*right*, colored) the respective module. We tested 216 CCM configurations by varying the presence and/or localization of enzymes, HCO₃⁻ channels, and diffusion barriers in the model (see *SI Appendix*, Fig. S23).

 Table 1. Summary of key parameter values used in the reaction-diffusion model of the algal CCM.

See attached pdf.

Materials and Methods

Reaction-diffusion model. To better understand the operation of the Chlamydomonas CO₂-concentrating mechanism (CCM), we developed a multi-compartment reaction-diffusion model that takes into account the key CCM enzymes and transporters and the relevant architecture of the Chlamydomonas chloroplast (17). For simplicity, our model assumes spherical symmetry and considers a spherical chloroplast of radius $R_{\rm chlor}$ in an infinite cytosol. Thus, all model quantities can be expressed as functions of the radial distance r from the center of the chloroplast (Fig. 1B). The modeled chloroplast consists of three compartments: a spherical pyrenoid matrix of radius R_{pyr} (pH 8) in the center, surrounded by a stroma (pH 8), with thylakoids (luminal pH 6) traversing both the matrix and stroma (Fig. 1) (34-36). At steady state, flux-balance equations set the spatially-dependent concentrations of CO_2 , HCO_3^- , and H_2CO_3 in their respective compartments (indicated by subscripts; see SIAppendix, Sec. I and Table S1):

$$D^{C}\nabla_{\text{thy}}^{2}C_{\text{thy}} - j_{\text{CAH3}} - j_{\text{sp}} - j_{\text{mem}}^{C}f_{\text{s}} = 0$$
 [1a]

$$D^{C}\nabla_{pyr}^{2}C_{pyr} - j_{LCIB} - j_{sp} - j_{Rbc} + j_{mem}^{C} \frac{f_{s}f_{v}}{1 - f_{v}} = 0$$
 [1b]

$$D_{\text{str}}^C \nabla_{\text{str}}^2 C_{\text{str}} - j_{\text{LCIB}} - j_{\text{sp}} - j_{\text{Rbc}} + j_{\text{mem}}^C \frac{f_{\text{s}} f_{\text{v}}}{1 - f_{\text{v}}} = 0 \qquad [1c]$$

$$D^{H}\nabla_{\text{thy}}^{2}H_{\text{thy}} + j_{\text{CAH3}} + j_{\text{sp}} - j_{\text{mem}}^{H}f_{\text{s}} = 0$$
 [16]

$$D^{H}\nabla_{\text{pyr}}^{2}H_{\text{pyr}} + j_{\text{LCIB}} + j_{\text{sp}} + j_{\text{mem}}^{H}\frac{f_{\text{s}}f_{\text{v}}}{1 - f_{\text{v}}} = 0$$
 [1e]

$$D_{\rm str}^H \nabla_{\rm str}^2 H_{\rm str} + j_{\rm LCIB} + j_{\rm sp} + j_{\rm mem}^H \frac{f_{\rm s} f_{\rm v}}{1 - f_{\rm v}} = 0. \qquad [1f_{\rm str}^H + j_{\rm LCIB}^H + j_{\rm sp}^H + j_{\rm mem}^H f_{\rm str}^H + j_{\rm LCIB}^H + j_{\rm sp}^H + j_{\rm mem}^H f_{\rm str}^H + j_{\rm LCIB}^H + j_{\rm sp}^H + j_{\rm mem}^H f_{\rm str}^H + j_{\rm LCIB}^H + j_{\rm sp}^H + j_{\rm mem}^H f_{\rm str}^H + j_{\rm LCIB}^H + j_{\rm sp}^H + j_{\rm mem}^H f_{\rm str}^H + j_{\rm LCIB}^H + j_{\rm sp}^H + j_{\rm mem}^H f_{\rm str}^H + j_{\rm LCIB}^H + j_{\rm sp}^H + j_{\rm mem}^H f_{\rm str}^H + j_{\rm LCIB}^H + j_{\rm sp}^H + j_{\rm mem}^H f_{\rm str}^H + j_{\rm LCIB}^H + j_{\rm sp}^H + j_{\rm mem}^H f_{\rm str}^H + j_{\rm LCIB}^H + j_{\rm sp}^H + j_{\rm mem}^H f_{\rm str}^H + j_{\rm LCIB}^H + j_{\rm sp}^H + j_{\rm mem}^H f_{\rm str}^H + j_{\rm LCIB}^H + j_{\rm sp}^H + j_{\rm mem}^H f_{\rm str}^H + j_{\rm LCIB}^H + j_{\rm sp}^H + j_{\rm mem}^H f_{\rm str}^H + j_{\rm LCIB}^H + j_{\rm sp}^H + j_{\rm mem}^H f_{\rm str}^H + j_{\rm sp}^H + j_{\rm mem}^H f_{\rm str}^H + j_{\rm sp}^H + j_{\rm$$

Here, C denotes the concentration of CO_2 , and H denotes the combined concentration of HCO_3^- and $\mathrm{H_2CO}_3$, which are assumed to be in fast equilibrium (43). Thus, their respective concentrations are given by $H^- = \frac{\eta}{1+\eta}H$ for HCO_3^- and $H^0 = \frac{1}{1+\eta}H$ for $\mathrm{H_2CO}_3$, where $\eta = 10^{\mathrm{pH}-\mathrm{pKa}_1}$ is a pH-dependent partition factor and pKa₁ = 3.4 is the first pKa of $\mathrm{H_2CO}_3$ (71). The first terms in Eqs. (1a-1f) describe the diffusive fluxes of inorganic carbon (Ci) within compartments. D^C and D^H denote, respectively, the diffusion coefficients of CO_2 , and HCO_3^- and $\mathrm{H_2CO}_3$ combined, in aqueous solution. In a model with thylakoid stacks slowing Ci diffusion in the stroma, the effective diffusion coefficients $D_{\mathrm{str}}^{C/H}$ are obtained using a standard homogenization approach (see SI Appendix, Sec. IG and Fig. S5); $D_{\mathrm{str}}^{C/H} = D^{C/H}$ otherwise. The other flux terms (j_{X}) in Eqs. (1a-1f) describe enzymatic reactions and inter-compartment Ci transport. Their expressions are provided in subsequent sections.

The boundary conditions at $r=R_{\rm pyr}$ are determined by the diffusive flux of Ci across the starch sheath at the matrix-stroma interface, i.e.,

$$-D^{C}\partial_{r}C_{pyr} = -D_{str}^{C}\partial_{r}C_{str} = \kappa_{starch}(C_{pyr} - C_{str})$$
 [2a]

$$-D^{H}\partial_{r}H_{pyr} = -D_{str}^{H}\partial_{r}H_{str} = \kappa_{starch}(H_{pyr} - H_{str}), \qquad [2]$$

where the starch sheath is assumed to have the same permeability $\kappa_{\rm starch}$ for all Ci species. $\kappa_{\rm starch} \to \infty$ when there is no starch sheath and Ci can diffuse freely out of the matrix. $\kappa_{\rm starch} = 0$ describes an impermeable starch sheath (see SI Appendix, Sec. IF). Similarly, Ci transport flux across the chloroplast envelope yields the boundary conditions at $r = R_{\rm chlor}$, i.e.,

$$\begin{split} D_{\rm str}^{C} \partial_{r} C_{\rm str} &= \kappa^{C} (C_{\rm cyt} - C_{\rm str}) \\ D_{\rm str}^{H} \partial_{r} H_{\rm str} &= \kappa^{H^{0}} (H_{\rm cyt}^{0} - H_{\rm str}^{0}) + \kappa^{H^{-}} (H_{\rm cyt}^{-} - H_{\rm str}^{-}) \\ &+ \kappa_{\rm chlor}^{H^{-}} (H_{\rm cyt}^{-} - \gamma H_{\rm str}^{-}), \end{split} \tag{3a}$$

where $\kappa_{\rm chlor}^{H^-}$ and γ denote the rate and reversibility of inward HCO $_3^-$ transport from the cytosol, representing the action of the uncharacterized chloroplast envelope HCO $_3^-$ transporter LCIA (24, 26); $\gamma=1$ corresponds to a passive bidirectional channel and $\gamma<1$ corresponds to an active pump. The external CO $_2$ conditions are specified by $C_{\rm cyt}$ and all cytosolic Ci species are assumed to be in

equilibrium at pH 7.1 (see SI Appendix, Sec. VIB) (72). We set $C_{\rm cyt}=10~\mu{\rm M}$ for air-level CO₂ conditions, and $C_{\rm cyt}=1~\mu{\rm M}$ for very low CO₂ conditions.

Thylakoid geometry. The thylakoid geometry has been characterized by cryo-electron tomography in Chlamydomonas (17). In our model, we account for this geometry by varying the local volume fraction $f_{\rm v}$ and surface-to-volume ratio $f_{\rm s}$ of the thylakoids. These fractions describe a tubule meshwork at the center of the pyrenoid $(r \leqslant R_{\rm mesh})$, extended radially by $N_{\rm tub}$ cylindrical tubules each of radius $a_{\rm tub}$ (see SI Appendix, Sec. IC), i.e.,

$$f_{\rm v} = \begin{cases} (N_{\rm tub}a_{\rm tub}^2)/(4R_{\rm mesh}^2) & \text{for } r\leqslant R_{\rm mesh} \\ (N_{\rm tub}a_{\rm tub}^2)/(4r^2) & \text{for } r>R_{\rm mesh} \end{cases}, \text{ and } \qquad [4a]$$

$$f_{\rm s} = 2/a_{\rm tub}.$$
 [4b]

In the baseline model the thylakoid tubules are assumed to extend to the chloroplast envelope, i.e., the outer radius of tubules $R_{\rm tub} = R_{\rm chlor}$. In a model with shorter tubules, we choose $R_{\rm tub} = 0.4~R_{\rm chlor}$, and set $f_{\rm v} = 0$ and $f_{\rm s} = 0$ for $r > R_{\rm tub}$. Thus, the Laplace–Beltrami operator is given by $\nabla_{\rm thy}^2 = r^{-2} f_{\rm v}^{-1} \partial_r f_{\rm v} r^2 \partial_r$ for the thylakoid tubules, and by $\nabla_{\rm pyr}^2 = \nabla_{\rm str}^2 = r^{-2} (1-f_{\rm v})^{-1} \partial_r (1-f_{\rm v}) r^2 \partial_r$ for the matrix and stroma.

Enzyme kinetics. The model considers three key CCM enzymes, i.e., the carbonic anhydrases (CAs) CAH3 and LCIB and the CO₂-fixing enzyme Rubisco. The interconversion between CO₂ and HCO $_3^-$ is catalyzed by both CAs and follows reversible Michaelis-Menten kinetics (73). The rate of CA-mediated CO₂-to-HCO $_3^-$ conversion is given by

$$j_{\text{CA}}(C, H^{-}) = \frac{\left(V_{\text{max,CA}}^{C}/K_{\text{m}}^{C}\right)\left(C - K^{\text{eq}}H^{-}\right)}{1 + C/K_{\text{m}}^{C} + H^{-}/K_{\text{m}}^{H^{-}}} \mathcal{L}_{\text{CA}},$$
 [5]

where $V^C_{\max, CA}$ denotes the maximum rate of CA, K^C_m and K^H_m denote, respectively, the half-saturation concentrations for CO₂ and HCO $_3^-$, and $V^C_{\max, CA}/K^C_m$ denotes the first-order rate constant which we refer to as the "rate" of the CA (Fig. 2). Finally, $K^{eq}=10^{pK_{eff}-pH}$ denotes the equilibrium ratio of CO₂ to HCO $_3^-$, with the effective pKa pK_{eff} = 6.1 (42, 48). The localization function \mathcal{L}_{CA} is equal to one for r where CA is present and zero elsewhere. The uncatalyzed spontaneous rate of CO₂-to-HCO $_3^-$ conversion, with a first-order rate constant k^C_{sp} , is given by $j_{sp}=k^C_{sp}(C-K^{eq}H^-)$ (74). Note that negative values of j_{CA} and j_{sp} denote fluxes of HCO $_3^-$ -to-CO $_2$ conversion.

The rate of CO₂ fixation catalyzed by Rubisco is calculated from

$$j_{\text{Rbc}}(C) = V_{\text{max,Rbc}}^C \frac{C}{K_{\text{m}}^{\text{eff}} + C} \mathcal{L}_{\text{Rbc}}.$$
 [6]

Here, $V_{\rm max,Rbc}^C$ denotes the maximum rate, and the effective $K_{\rm m}$ (Rubisco $K_{\rm m}$ in Fig. 1) is given by $K_{\rm m}^{\rm eff}=K_{\rm m,Rbc}^C(1+O/K_{\rm m,Rbc}^O)$ to account for competitive inhibition by O₂ (75, 76), where O denotes the concentration of O₂, and $K_{\rm m,Rbc}^C$ and $K_{\rm m,Rbc}^O$ denote the half-saturation substrate concentrations for CO₂ and O₂, respectively. $\mathcal{L}_{\rm Rbc}$ is equal to one where Rubisco is localized, and zero elsewhere.

In our baseline model, we assume that CAH3 is localized in the thylakoid tubules traversing the pyrenoid (33), LCIB is distributed diffusely in the stroma (46), and Rubisco is localized in the pyrenoid matrix (11). To explore the effect of enzyme localization, we vary the start and end radii of the enzymes while maintaining a constant number of molecules (see Figs. 4 and 5 and SI Appendix, Sec. V).

Transport of Ci across thylakoid membranes. The flux of CO_2 diffusing across the thylakoid membrane from the thylakoid lumen to the matrix or stroma is given by

$$j_{\text{mem}}^{C} = \begin{cases} \kappa^{C} (C_{\text{thy}} - C_{\text{pyr}}) & \text{for } r \leqslant R_{\text{pyr}} \\ \kappa^{C} (C_{\text{thy}} - C_{\text{str}}) & \text{for } r > R_{\text{pyr}} \end{cases},$$
 [7]

where κ^C denotes the permeability of thylakoid membranes to CO₂. Similarly, the cross-membrane diffusive flux of HCO₃⁻ and H₂CO₃,

 j_{mem}^H , is given by

$$j_{\text{mem}}^{H} = \begin{cases} (\kappa^{H^{-}} + \kappa_{\text{thy}}^{H^{-}})(H_{\text{thy}}^{-} - H_{\text{pyr}}^{-}) & \text{for } r \leq R_{\text{pyr}} \\ + \kappa^{H^{0}}(H_{\text{thy}}^{0} - H_{\text{pyr}}^{0}) & , \\ (\kappa^{H^{-}} + \kappa_{\text{thy}}^{H^{-}})(H_{\text{thy}}^{-} - H_{\text{str}}^{-}) & \text{for } r > R_{\text{pyr}} \\ + \kappa^{H^{0}}(H_{\text{thy}}^{0} - H_{\text{str}}^{0}) & \end{cases}$$
(8)

where κ^{H^-} and κ^{H^0} denote, respectively, the baseline membrane permeability to HCO_3^- and $\mathrm{H_2CO}_3$, and $\kappa_{\mathrm{thy}}^{H^-}$ denotes the additional permeability of thy lakoid membranes to HCO_3^- due to be strophin-like channels (30). Note that the final terms of Eq. (1a) and Eqs. (1b,1c) differ by a factor of $\frac{f_{\rm v}}{1-f_{\rm v}}$ because the cross-membrane fluxes have a larger impact on the concentrations in the thylakoid compartment, which has a smaller volume fraction.

Choice of parameters and numerical simulations. The model parameters are estimated from experiment (see SI Appendix, Table S1 and references therein), except for the rates of LCIB and CAH3 and the kinetic parameters of the HCO₃⁻ transporters, which are not known. We performed a systematic scan for these unknown parameters within a range of reasonable values (Fig. 2 and SI Appendix, Fig. S4). The numerical solutions of Eq. (1) were obtained by performing simulations using a finite element method. Partial differential equations were converted to their equivalent weak forms, computationally discretized by first-order elements (77), and implemented in the open-source computing platform FEniCS (78). A parameter sensitivity analysis was performed to verify the robustness of the model results (SI Appendix, Fig. S28). A convergence study was performed to ensure sufficient spatial discretization (SI Appendix, Fig. S29).

Energetic cost of the CCM. We compute the energetic cost using the framework of nonequilibrium thermodynamics (54) (see SIAppendix, Sec. IIB, for details). In brief, the free-energy cost of any nonequilibrium process (reaction, diffusion, or transport) is given by $(j_+ - j_-) \ln(j_+/j_-)$ (in units of thermal energy RT), where j_+ and j_{-} denote the forward and backward flux, respectively. Summing the energetic cost of nonequilibrium processes described in Eq. (1), we show that the total energy required to operate the CCM can be approximated (in units of RT) by

pproximated (in units of
$$KI$$
) by
$$\dot{W}_{\text{CCM}} \approx J_{\text{str}}^{C} \to H^{-} \ln \frac{K_{\text{thy}}^{\text{eq}}}{K_{\text{str}}^{\text{eq}}} + J_{\text{chlor}}^{C} \ln \frac{\gamma^{-1} K_{\text{thy}}^{\text{eq}}}{K_{\text{str}}^{\text{eq}}} + J_{\text{Rbc}} \ln \frac{\gamma^{-1} K_{\text{thy}}^{\text{eq}}}{K_{\text{str}}^{\text{eq}}},$$
[9]

Here, $J_{\rm str}^{C\to H^-} = -\int_0^{R_{\rm chlor}} 4\pi r^2 (1-f_{\rm v}) (j_{\rm LCIB}+j_{\rm sp}) dr$ integrates the flux of LCIB-mediated and spontaneous conversion from CO₂ to HCO₃ in the stroma, with $4\pi r^2 (1-f_{\rm v}) dr$ being the geometric factor. $J_{\rm chlor}^C = 4\pi R_{\rm chlor}^2 \kappa^C (C_{\rm str}|_{r=R_{\rm chlor}} - C_{\rm cyt})$ denotes the flux of CO₂ diffusing from the stroma back out into the cytosol. $J_{\rm Rbc} = \int_0^{R_{\rm chlor}} 4\pi r^2 (1-f_{\rm v}) j_{\rm Rbc} dr$ integrates the flux of CO₂ fixation by Rubisco. The $\ln \gamma^{-1}$ and $\ln \frac{K_{\rm cq}^{\rm eq}}{K_{\rm str}^{\rm cq}}$ terms denote the

free-energy cost of pumping HCO_3^- across the chloroplast envelope and pumping protons across the thylakoid membranes, respectively. Using ATP hydrolysis energy $|\Delta G_{\text{ATP}}| = 51.5 \ RT$ (79), we compute the equivalent ATP spent per CO₂ fixed as $\dot{W}_{\rm CCM}/J_{\rm Rbc}/|\Delta G_{\rm ATP}|$.

Well-mixed compartment model. To better understand the biophysical limit of the CCM, we consider a well-mixed compartment simplification of the full model. Specifically, we assume that (i) the diffusion of Ci is fast in the matrix and stroma, and therefore the concentrations of CO_2 and HCO_3^- are constant across radii in each of the two compartments, taking values denoted by $C_{\rm pyr}, C_{\rm str}, H_{\rm pyr}^-,$ and $H_{\rm str}^-$; (ii) HCO $_3^-$ transport across the thylakoid membranes is fast, and thus the thylakoid tubule concentration of HCO₃ inside the pyrenoid is equal to H_{pyr}^- , while the thylakoid tubule concentration outside the pyrenoid is equal to $H_{\rm str}^-$; (iii) ${
m HCO}_3^-$ and ${
m CO}_2$ are in equilibrium (catalyzed by CAH3) in the thylakoid tubules inside the pyrenoid, and thus the CO_2 concentration therein is given by $C_{\rm thy} = K_{\rm thy}^{\rm eq} H_{\rm pyr}^{-}$; and (iv) the concentration of CO₂ in the

thylakoid tubules approaches $C_{\rm str}$ toward the chloroplast envelope. Thus, the flux-balance conditions are described by a set of algebraic equations of 4 variables, C_{pyr} , C_{thy} , C_{str} and H_{str}^{-} (see SI Appendix, Sec. III). The algebraic equations are solved using the Python-based computing library SciPy (80). The energetic cost of the well-mixed compartment model is computed similarly as above.

Engineering paths. We are interested in how adding and removing individual components affects the overall functioning of the CCM. We thus measure the efficacy and energy efficiency of 216 CCM configurations, modulating the presence and localization of enzymes, HCO₃ channels, and diffusion barriers. Each configuration is simulated using the reaction-diffusion model above with the appropriate parameters for that strategy (SI Appendix, Fig. S23).

To find all possible engineering paths between these configurations, we consider a graph on which each possible configuration is a node. Nodes are considered to be connected by an undirected edge if they are separated by one engineering step. Thus, by taking steps on the graph, we can search all possible engineering paths given a start node with poor CCM performance and a target node with good performance. A single engineering step could be the addition or removal of an enzyme, a channel, or a diffusion barrier, as well as the localization of a single enzyme. The exception is the localization of Rubisco, which we assume can exclude LCIB from the matrix as it forms a phase-separated condensate (55). We do not consider strategies employing both a starch sheath and thylakoid stacks as diffusion barriers. We use a custom depth-first search algorithm in MATLAB to identify all shortest engineering paths between a start and a target node.

Data and software availability. All data and simulation code required to reproduce the results in this manuscript are available to the readers on GitHub: https://github.com/f-chenyi/Chlamydomonas-

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Table 1: Summary of key parameter values used in the reaction-diffusion model of the algal CCM.

Symbols	Descriptions	Values	Ref.
Chloroplast geometry			
$R_{\rm chlor}$	Radius of the chloroplast	3.14 µm	(17, 81)
$R_{ m pyr}$	Radius of the pyrenoid	$0.3R_{ m chlor}$	(17, 81)
$N_{ m tub}$	Number of thylakoid tubules	40	(17)
R_{mesh}	Radius of the tubule meshwork	$0.4\mu\mathrm{m}$	(17)
$a_{ m tub}$	Cylindrical radius of the thylakoid tubules	50 nm	(17)
Kinetic parameters			
$V_{ m max}^C/K_{ m m}^C$	First-order rate of $CO_2 + H_2O \rightarrow HCO_3^- + H^+$	$10^4 \mathrm{\ s^{-1}}$ for CAH3	*
		$10^3 \mathrm{\ s^{-1}}$ for LCIB	*
$\kappa_{ ext{thy}}^{H^-}$	Rate of HCO_3^- channels at the thylakoid membranes	10^{-2} m/s	*
$\kappa_{ m chlor}^{H^-}$	Rate of chloroplast envelope HCO_3^- transporters	10^{-8} m/s	*

^{*} Values used in the baseline model. See Fig. 2 and SI Appendix, Fig. S4 for a thorough parameter scan. See SI Appendix, Table S1 for a full list of model parameters.