# 1 Genomics Characterization of an engineered Corynebacterium glutamicum in

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# **Bioreactor Cultivation under Ionic Liquid Stress**

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#### 22 Abstract

Corynebacterium glutamicum is an ideal microbial chassis for the production of valuable 23 bioproducts including amino acids and next-generation biofuels. Here we resequence engineered 24 25 isopentenol (IP) producing C. glutamicum BRC-JBEI 1.1.2 strain and assess differential transcriptional profiles using RNA sequencing under industrially relevant conditions including 26 27 scale transition and compare the presence vs. absence of an ionic liquid, cholinium lysinate ([Ch][Lys]). Analysis of the scale transition from shake flask to bioreactor with transcriptomics 28 identified a distinct pattern of metabolic and regulatory responses needed for growth in this 29 industrial format. These differential changes in gene expression corroborate altered accumulation 30 of organic acids and bioproducts, including succinate, acetate, and acetoin that occur when cells 31 are grown in the presence of 50mM [Ch][Lys] in the stirred-tank reactor. This new genome 32 assembly and differential expression analysis of cells grown in a stirred tank bioreactor clarify the 33 34 cell response of a C. glutamicum strain engineered to produce IP.

# 35 **1. Introduction**

Due to process advantages, biological methods for the production of amino acids over chemical synthesis methods fostered the identification of natural glutamine overproducing microbes (Kinoshita et al., 1958). Since then, *Corynebacterium glutamicum* has been used

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successfully to produce specialty glutamine and specialty amino acids to meet global demand. The 39 advent of accessible whole-genome sequencing and mutagenesis methods have enabled 40 researchers a clearer understanding of how specific isolates can overproduce these desired 41 42 molecules, as well as how they have maintained productivity across geometrically-larger scales (Wolf et al., 2021; Pérez-García and Wendisch, 2018; Becker et al., 2018). Using C. glutamicum 43 to produce non-native metabolites as next-generation biofuels is an attractive large-volume market 44 with the potential to reduce global carbon emissions. Potential biofuels can be produced from 45 terpenes, which use different metabolic precursors (reviewed in (Pérez-García and Wendisch, 46 2018)). We have previously described the heterologous expression of the terpenoid isopentenol 47 (IP; also known as 3-methyl-3-buten-1-ol or isoprenol) pathway in C. glutamicum (Sasaki et al., 48 49 2019). Isopentenol can be used directly as a drop-in biogasoline (Chou and Keasling, 2012; S-CoA, 2008) or as a precursor to a jet fuel, DMCO (Baral et al., 2021). Producing IP was improved 50 by the use of optimal pathway homologs, specific media formulation and aeration conditions and 51 52 an empirically determined carbon/nitrogen ratio.

53 In this study we build upon this established system to analyze the behavior of C. glutamicum strains engineered to produce IP in a bioreactor. The bioreactor cultivation and process 54 55 conditions can provide key diagnostic information essential to build robust production platform strains (Wehrs et al., 2019). In addition, it is also valuable to have an understanding of microbial 56 57 response to the carbon feedstock that is anticipated for actual production. Here, we explore the use of plant-based lignocellulosic hydrolysate generated using ionic liquid (IL) as a pretreatment 58 reagent. Toxicity from residual pretreatment reagents such as ILs is a known source of growth 59 impediment (Hou et al., 2013; Santos et al., 2014). C. glutamicum is tolerant to many ILs, another 60 attribute that makes it an ideal host for biomass conversion (Sasaki et al., 2019). In this study, we 61 62 characterize an IP producing engineered C. glutamicum strain with long-read PacBio wholegenome sequencing. This high-quality assembly allowed accurate mapping for differential RNA 63 expression analysis from a diagnostic fed-batch C. glutamicum IP production run. These side-by-64 65 side experiments characterize the cellular response to the IL, cholinium lysinate ([Ch][Lys]), when grown in a fed-batch stirred tank bioreactor. 66

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#### 68 **2. Results**

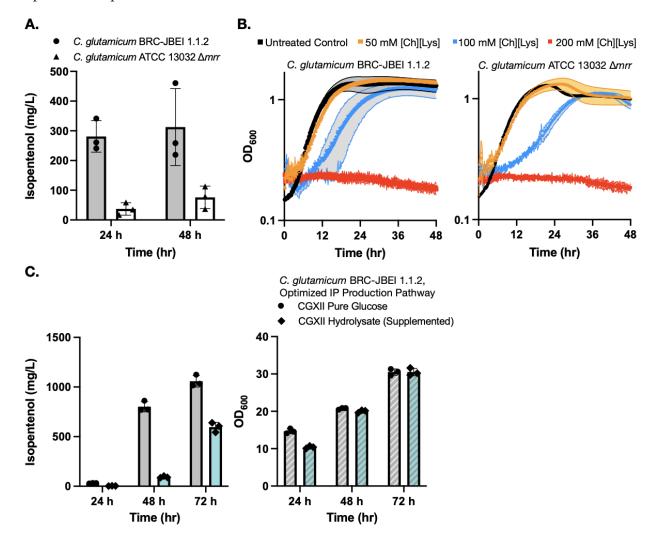
69 2.1. Characterization of Isopentenol Production and Ionic Liquid Tolerance in C. glutamicum70 Strains

71 We established that the strain reported in Sasaki *et al* 2019, *C. glutamicum* (previously referred to as ATCC 13032 NHRI 1.1.2) outperformed another isolate, ATCC 13032  $\Delta cglIM \Delta cgLIR$ 72 73  $\Delta cgLIIR$  (referred to as " $\Delta mrr$ ") (Figure 1A). C. glutamicum  $\Delta mrr$  was first described in 74 Baumgart et al 2013 and is a methylation-deficient strain widely used due to its improved plasmid 75 transformation and genomic integration rate (Schäfer et al., 1997; Baumgart et al., 2013). When C. glutamicum BRC-JBEI 1.1.2 is used in conjunction with an IP production pathway, it can 76 produce 300 mg/L IP from pure glucose, but the product titers are near the lower detection limit 77 78 by GC-FID in the C. glutamicum ATCC 13032  $\Delta mrr$  strain. While only C. glutamicum BRC-JBEI 1.1.2 produced IP, both the type strain and this specific isolate tolerate high concentrations of 79 exogenous ILs (Figure 1B), suggesting that IL tolerance was a shared feature due to the cell 80

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membrane structure between these two isolates even if the available metabolic flux towards IP wasdifferent.

We also confirmed the ability of C. glutamicum BRC-JBEI 1.1.2 to handle renewable 83 carbon streams from sorghum biomass using an improved carbon extraction protocol enhanced by 84 85 the use of ensiled biomass (Magurudeniya et al., 2021). The ensiling process enables naturally occurring lactic-acid secreting bacteria to partially decompose the hemicellulose in sorghum while 86 87 stored in a silo before downstream processing. After ensiling, the biomass was pretreated with 88 [Ch][Lvs] followed by enzymatic saccharification (Materials and Methods). This hydrolysate contained 48.7 g/L glucose, 17.9 g/L xylose, and trace concentrations of aromatic compounds. Our 89 optimized C. glutamicum BRC-JBEI 1.1.2 with an optimized IP production system had no detected 90 91 growth defects when grown with 58% (v/v) hydrolysate supplemented media and produced 1 g/L IP from pure glucose or  $\sim 600 \text{ mg/L}$  IP from sorghum hydrolysate (Figure 1C). These results 92 showcase its versatility with handling real-world plant biomass derived carbon streams. For the 93 remainder of this study, we focus on characterizing the genetic differences present in C. 94 95 glutamicum BRC-JBEI 1.1.2 relative to other closely related C. glutamicum strains that might explain the IP production values between these two strains. 96



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Figure 1. Growth and isopentenol production characterization of two genetically distinct 98 99 engineered C. glutamicum strains. (A) Isopentenol (IP) production in C. glutamicum strains of the genotypes indicated harboring an IP production plasmid. Cells were cultivated in 24-well deep 100 well plates. Isopentenol titers reported at 48-hour time points are corrected for evaporation in this 101 plate format (Materials and Methods). (B) Growth curves for C. glutamicum strains of the 102 indicated strain backgrounds cultivated in CGXII media in the presence or absence of the IL, 103 cholinium lysinate ([Ch][Lys]). [Ch][Lys] was exogenously added to the culture media at the start 104 of the time course. (C) Production of IP from C. glutamium grown in CGXII minimal media with 105 pure glucose (4% w/v) or ensiled [Ch][Lys] pretreated sorghum hydrolysate. An optimized IP 106 production plasmid carrying a *hmgR* variant from *Silicibacter pomeroyi* was used. The optical 107 108 density of cultures as a proxy for cell density is noted on the right-hand panel.

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#### 110 2.2 Genomic Characterization of C. glutamicum BRC-JBEI 1.1.2

16S rDNA sequencing (Hahne et al., 2018) confirmed the C. glutamicum  $\Delta mrr$  strain as in the C. 111 glutamicum ATCC 13032 strain background, but this same method indicated that C. glutamicum 112 BRC-JBEI 1.1.2 was genetically closer to C. glutamicum CICC10112 or SCgG1/SCgG2. Only 113 SCgG1 and SCgG2 have been characterized with whole-genome sequencing, and to our 114 knowledge there was no additional information about C. glutamicum CICC10112 beyond the 115 partial 16S ribosomal sequence. As 16S rDNA was not conclusive, we reasoned that the whole-116 genome sequencing in this IP producing strain would ensure an accurate reference genome in 117 downstream RNAseq analysis if the improved performance observed in this strain was due to 118 119 variants in the strain background. One of the major limitations in short-read sequencing is the difficulty in assembling overlapping contigs to generate a high-quality de novo assembly of a 120 121 single contiguous read. Therefore, we chose Pac-Bio long-read sequencing (Koren and Phillippy, 2015) for optimal coverage over short read sequencing as a potential solution. However, routine 122 123 methods for lysing and isolating C. glutamicum genomic DNA were insufficient for building highquality genome assemblies since the physical lysis method we employed (Eng et al., 2018) shears 124 DNA to fragments ranging from 2-8 kb in size. Detergent-based lysis methods failed to extract 125 genomic DNA, even with prolonged incubation times. We developed a method to isolate larger 126 127 DNA fragments approximately 20kb in size for the PacBio Sequel assembly pipeline using a Zymolyase protease treatment for cell lysis (see Materials and Methods). This modified DNA 128 129 extraction protocol enabled us to use PacBio long read sequencing to generate a high-quality de novo genome assembly. 130

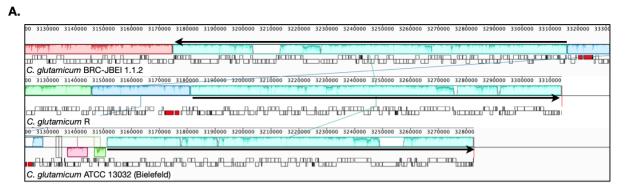
We now report a new genome assembly of a single contiguous scaffold of 3,352,276 bases 131 132 with 53.83% GC content (Figure 2). Genome-wide average nucleotide identity (ANI) confirmed this isolate was 99.9987% identical to C. glutamicum SCgG1 and SCgG2 as well as another 133 sequenced C. glutamicum isolate, Z188. The average nucleotide identity alignment for the 28 134 sequenced C. glutamicum isolates has been deposited at the database of the Joint Genome Institute 135 136 and is also included in Supplementary Table S1. C. glutamicum BRC-JBEI 1.1.2 differs from SCgG1 only by a few single nucleotide polymorphisms (~10) and two additional genes that are 137 absent from SCgG1, a putative transposase and a hypothetical protein coding sequence that is 414 138 139 bp in length. When C. glutamicum BRC-JBEI 1.1.2 was compared with more commonly used reference strains, C. glutamicum R and 13032 (Bielefeld), we identified genomic islands encoding 140 genes unique to BRC-JBEI 1.1.2. Genome topology analysis also identified a 140 kb inversion in 141

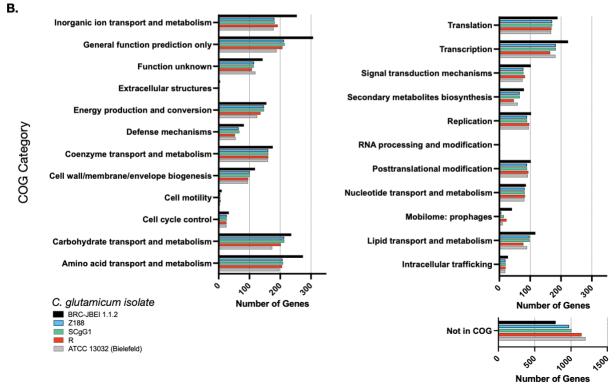
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the genome of BRC-JBEI 1.1.2 isolate (Figure 2A). Out of 3,097 genes, homology mapping
indicated that 85% (2,641 genes) were at least 80% identical to known genes in *C. glutamicum*ATCC 13032. With a less restrictive % identity threshold of 50%, the identical ratio could account
for 89% (2,777 genes). Nonetheless, 320 genes did not meet the minimum % identity threshold
and could not be annotated with this reference genome (Supplementary Figure S1).

147 Some of these unknown genes that were unique to BRC-JBEI 1.1.2 might be related to the 148 catabolism of IL. Intriguingly, a putative choline dehydrogenase, Ga0373873 2846, showed only 149 40% identity to other known choline dehydrogenases primarily found in gram-negative microbes such as Burkholderia phytofirmans PsJN and Cupriavidus basilensis FW507-4G11. Meta-COG 150 analysis of these four C. glutamicum genomes revealed that C. glutamicum BRC-JBEI 1.1.2 151 152 contains over 100 additional genes related to the transport or metabolism of inorganic ions, carbohydrates, and amino acids, suggesting a broader metabolic capacity to utilize a more 153 significant number of substrates than the type strain (Figure 2). In summary, this genome 154 sequencing analysis was valuable for characterizing differences between C. glutamicum BRC-155 JBEI 1.1.2 and the more intensely studied type strain ATCC 13032. Due to its similarity with 156 SCgG1 and SCgG2, C. glutamicum BRC-JBEI 1.1.2 is likely an industrial glutamate 157 158 overproducing isolate but has more annotated transport and metabolic systems than its nearest neighbors, SCgG1, SCgG2, and Z188 that need further characterization. 159

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Figure 2: Comparison of the C. glutamicum BRC-JBEI 1.1.2 strain with closely related C. 161 glutamicum strains. (A) A meta-analysis of gene function using clusters of orthologous genes 162 (COGs) analysis. The total number of genes in each category for each strain is represented with 163 colored bars as indicated. (B) Mauve genome alignment of C. glutamicum BRC-JBEI 1.1.2 with 164 C. glutamicum R and 13032 (Bielefeld). Similar genomic regions share the same color across the 165 3 different genomes compared. A 140 kb chromosomal inversion is highlighted in light blue, and 166 the relative direction of the inversion in each strain is indicated with a black arrow. Individual 167 genes are indicated with open rectangles underneath the colored area. 168

#### 169 2.3. Transcriptome Analysis Identifies Changes in C. glutamicum Metabolism on Scale-up

Next, we sought to build a systems-level understanding of *C. glutamicum* gene expression changes in bioreactors upon exogenous ionic liquid treatment. This data could be useful for subsequent Design-Build-Test-Learn (DBTL) cycles in providing the diagnostic information for future strain optimization strategies (Opgenorth et al., 2019). We prepared samples from sequential

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time points during a scaleup campaign to analyze shifts in gene expression as a proxy for changes 174 in metabolic and regulatory behavior in both [Ch][Lys] treated and untreated runs. First we 175 176 determined if the failure to produce IP was due to loss of the production pathway, possibly due to loss of the plasmid-borne IP pathway genes. The IP production pathway is composed of 5 genes 177 178 in 2 adjacent operons under the trc and lacUV5 promoters, namely mk, pmd and atoB, hmgS, hmgR 179 respectively. Using the transcripts per million (TPM) metric, we examined absolute gene 180 expression levels as well as changes over the course of the production campaign. The IP pathway 181 started off high for both *hmgR* and *hmgS* in the shake flask (200,000 TPM), but expression of these 182 two genes decreased between 10-16 x over the duration of the 65 hour fed-batch. Expression 183 amounts of atoB in the shake flask were comparatively lower (1,500 TPM) but decreased 4 x at 184 the shake flask to bioreactor transition. atoB TPM counts remained low for the duration of the subsequent time points. Since the pathway genes were still expressed during this run, we then 185 focused on analyzing gene expression changes in the native C. glutamicum genome. 186

To interpret the differential gene expression results with genes identified in the new 187 188 assembly for C. glutamicum BRC-JBEI 1.1.2, we mapped gene names and identifiers from C. glutamicum ATCC 13032 back onto the open reading frames (ORFs) in C. glutamicum BRC-JBEI 189 1.1.2 as genes in the type strain genome have been broadly characterized. We used a medium 190 confidence cutoff of 70% identity to capture most homologs when analyzing this dataset. First, we 191 characterised gene expression upon inoculating cells from the seed culture in a shake flask to the 192 bioreactor. This differential gene expression (DEG) was calculated as the ratio of an early time 193 point in the bioreactor (6.5 hours post inoculation in the stirred tank) divided by values from the 194 seed culture immediately before transfer. This time point was chosen to give cells approximately 195 three doublings to ensure the cells were rapidly growing under these new conditions. The result 196 showed differential expression of 258 genes after 6.5 hours (Figure 3, and Supplementary Data, 197 Dataset S1). 198

Many genes encoding metabolic functions were differentially expressed in the transition 199 from shake flask to stirred tank format. We used a fold change cutoff of 4 ( $\log 2 > 2$ ) and a p value 200 < 0.001 to identify both large and statistically significant changes. Gene ontology (GO) enrichment 201 annotations identified the highest number of DEGs belonging to metabolism and transport 202 203 processes (Figure 3B). The strongest fold changes (16-fold increase or higher) were in metabolism; Cgl2807 (adhA, zinc dependent alcohol dehydrogenase), Cgl1396 (acetylglutamate 204 kinase), Cgl2886 and Cgl2887 (two FAD-dependent oxidoreductases) and Cgl3007 (mez, malic 205 enzyme). Of these genes, Cgl2807/adhA encodes for a Zn-dependent alcohol dehydrogenase that 206 together with Cgl2796 has been reported to maintain redox balance (Zhang et al., 2018). While the 207 cells had been previously adapted in CGXII medium for the seed culture, we observed 208 differentially increased gene expression of several amino acid biosynthesis pathways. Increased 209 210 gene expression for nearly complete pathways needed for methionine, leucine, and arginine biosynthesis were detected, as well as the gene responsible for glutamate synthesis, gdh. Three 211 genes responsible for the conversion of propionate to succinate and pyruvate through the 212 methylcitrate cycle were also upregulated. Upregulated DEGs encoding for myo-inositol 213 metabolism directing flux towards acetyl-CoA and DHAP included Cgl0163/iolE, Cgl0161/iolB, 214 215 Cgl0158/iolC, Cgl0160/iolA/msmA, and Cgl0157/iolR. Of the myo-inositol pathway genes, iolR

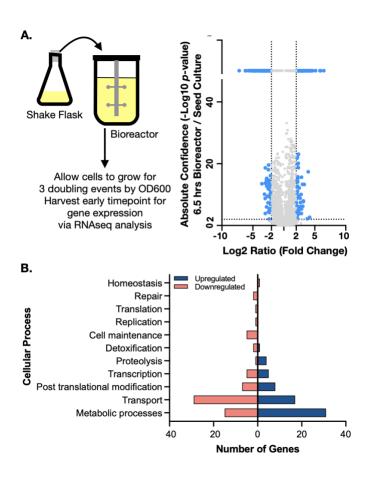
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was reported to regulate PTS-independent glucose uptake by repressing the expression of glucokinases in *C. glutamicum (Zhou et al., 2015)*. The upregulation of myo-inositol catabolic pathways could be attributed to supplemental yeast extract amended to the CGXII medium in the bioreactor. Yeast extract was added to the bioreactors as it was found to improve IP production when *E. coli* was used as the microbial host (Kang et al., 2019). Inositol is found in the yeast extract (>160 mg/g range) for many commercial preparations.

222 A wide range of regulatory factors and stress responsive genes were also upregulated at 223 the shake flask to bioreactor transition time point. Cgl2988/malR, which encodes for a MarR type transcriptional regulator and Cgl3007/mez were both highly upregulated. MalR represses 224 225 expression of the malic enzyme gene, mez (Krause et al., 2012) and is a global regulator of stress-226 responsive cell envelope remodeling in C. glutamicum (Hünnefeld et al., 2019). Cgl2996/ino-1 227 (myo-inositol-1-phosphate synthase) is the first enzyme in mycothiol biosynthesis and plays a 228 major role in the detoxification of stress-inducing factors, maintaining the redox balance and protection against oxidative stress (Chen et al. 2019). The universal stress response protein 229 230 Cgl1407/uspA2 and HSP 60 family chaperonin, Cgl2716/groEL were also upregulated.

231 A similar number of genes were downregulated during the transition from shake flask to 232 bioreactor (Figure 3B). Of the genes uniquely downregulated at 6.5 h, included Cgl1427/cmk, cytidyl kinase, Cgl2605/bioD, thioredoxin reductase. Cgl1427 has been reported to be crucial for 233 maintaining triphosphate pools (ATP, CTP) under oxygen-limiting environments (Takeno et al., 234 235 2013) but it's downregulation implies these early time points are not oxygen-limited. Several genes involved in transport were also significantly downregulated with a cutoff threshold log2 ratio less 236 237 than -4. These included ABC transporter ATPase proteins Cgl1351, Cgl1546/pacL (cation 238 specific) and Cgl1567 along with Cgl2222, a major facilitator superfamily (MFS) transporter. 239 Downregulated genes Cgl0026-Cgl0029 have been reported to be Zur- binding sites that are involved in zinc homeostasis in C. glutamicum (Schröder et al., 2010). Other downregulated 240 241 transporters included the lysine exporter Cgl1262/lysE, exporter systems for branched chain amino acid and methionine (brnE/brnF) along with several MFS transporters (Cgl1065, Cgl1076/pcaK, 242 243 Cgl0380, Cgl0381, Cgl2685/*lmrB*) and the ABC type phosphate uptake system (*pstSCAB*). Several other ABC transporter subunits (permease or substrate-binding domain or the ATPase) responsible 244 for transport of iron, calcium, cobalt, cadmium, copper, sn-glycerol-3-phosphate, etc. were also 245 downregulated. Downregulated transcriptional regulators during this scale transition phase belong 246 to the GntR family (Cgl2316), ArsR family (Cgl2279), PadR family (Cgl2979) and CopY family 247 (Cgl0385). A complete list of DEGs can be found in Supplementary datasets, Datasets S1 248 249 through S6 and at the JGI Genome Portal (https://genome.jgi.doe.gov/portal/) under Project ID 250 1203597.

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252 Figure 3. Genome wide expression differences in diverse cellular processes upon shifting to a stirred tank bioreactor. (A) Left side. Schematic showing scale transition from 25mL seed culture 253 of IP producing C. glutamicum in CGXII media to a stirred tank bioreactor. Right side. Volcano 254 255 plot comparing differential gene expression (6.5 h post inoculation / shake flask) via RNAseq analysis to absolute confidence (p value) of the same time points. Fold changes greater than 4 256 257  $(\log_{2}=2)$  and absolute confidence values >2 (p<0.001) are considered significant. The threshold 258 for significance is demarcated with dotted lines and the corresponding genes are colored blue. Genes with insignificant differential expression are indicated in grey. Genes with confidence 259 values >40 are placed above the break on the y axis. (**B**) Analysis of gene classes enriched in the 260 261 scale transition. Differentially expressed genes from a) were binned into functional categories based on COG annotations and putative function by BLAST alignment. Upregulated genes are 262 263 indicated in dark blue; downregulated genes are indicated in light red.

# 264 2.4. Metabolic Pathway Alterations during Fed-batch Cultivation indicated by differentially 265 expressed genes

After inoculation into the bioreactors, we benchmarked the bioreactor run with online and offline measurements including growth, glucose consumption, and organic acid secretion, with and without [Ch][Lys]. We noted several differences between cells grown in the control reactor and the [Ch][Lys] treated reactor. While cells were pulse-fed the same feed solution to restore glucose levels back to 60 g/L, the [Ch][Lys] treated engineered strain much less acetate and succinate than the control (**Figures 4A** and **5A**). Overall OD<sub>600</sub> measurements indicated similar initial growth

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patterns before the first feeding, but after feeding, OD<sub>600</sub> measurements did not appreciably increase further and instead we detected overflow metabolite accumulation above 10 g/L of succinate and acetate (**Figure 4A**). The control reactor decreased in OD<sub>600</sub> from a high of 49 to a 21 OD<sub>600</sub>. The [Ch][Lys] reactor also decreased in OD<sub>600</sub>, but from a similar high of 50 to 36 OD<sub>600</sub> (**Supplementary Figure S2**). We correlated gene expression changes during this campaign for both reactors using RNAseq analysis to understand how glucose was redirected from growth to the generation of these overflow metabolites (**Supplementary Data, Dataset S2**).

279 We observed several genes encoding metabolic processes related to succinate and acetate metabolism were downregulated in the time course, such as *ptaA*, *ackA* and *sucC*. Decreasing their 280 gene expression suggests a decrease in activity, enabling greater succinate or acetate accumulation 281 due to fewer competing reactions for these metabolites as precursors. Cgl2211, a putative succinate 282 exporter (Huhn et al., 2011; Litsanov et al., 2012; Prell et al., 2020) was upregulated at 65 h, that 283 might explain higher succinate excretion profile for the fed-batch cultivation in the absence of the 284 IL (Figure 4A). The higher acetate secretion in this bioreactor correlated with upregulated 285 286 Cgl2066 transcripts at 24 h and 41 h, which encodes a putative acyl phosphatase that converts acetyl phosphate to acetate. At the last phase of cultivation Cgl2380/mdh was upregulated (log2 287 288 ratio of 3.14) with 12-fold over expression. Malate dehydrogenase, *mdh*, is involved in a NADH 289 based reversible reaction in TCA and is responsible for NADH balance maintenance and succinate formation. The malic enzyme, Cgl3007/mez, was downregulated across all later time points (Log2 290 -3.1 to -7.65), with 10-fold decrease in expression in the last time point alone. Malic enzyme, 291 292 upregulated during transition from shake flask to a bioreactor scale (log2 ratio of 5.11 at 6.5 h, Section 2.3), is involved in gluconeogenesis important for NADPH regeneration for anabolic 293 294 processes and pyruvate flux at the cost of carbon loss as one mole of CO<sub>2</sub>. Genes encoding cell 295 division proteins including mraZ, ftsX, ftsW, ftsE, sepF, were downregulated for later stage cultivation time points (24 h and later) correlating with the lack of increased OD<sub>600</sub> after glucose 296 297 was fed at the 24 hour time point. Cgl1502, a putative MFS transporter (PTS based sugar importer) 298 was upregulated in all later bioreactor cultivation time points. These later time points had many 299 shared downregulated genes, indicating a phenotyping similarity (Figure 4B).

A more comprehensive analysis of differential gene expression indicated that many 300 transporters were upregulated in these bioreactor time points (Figure 4C, red colored bars). These 301 included ABC transporters for phosphonate (*pctABCD*); sn-glycerol-3-phosphate (*ugpABCE*) and 302 303 phosphate (*pstSCAB*), a branched chain amino acid and methionine exporter (Cgl0258/*brnF*); Cgl0968/lysI, which encodes a protein involved in lysine uptake (Seep-Feldhaus et al., 1991). 304 305 Transcriptional regulators that were upregulated across all the later time points of the bioreactor cultivation and were associated with putative functions included Cgl2496/PucR family, 306 Cgl0962/TetR family, Cgl2934/MarR family, Cgl1367/LacI family and Cgl2616/LysR family. 307 308 Cgl2776 which is a putative XRE family transcriptional regulator MsrR was found to be upregulated from 24 h to 65 h. *msrR* is located downstream of the *cmr* gene that encodes for a 309 MFS multidrug efflux protein and upstream of Cgl2775/sseA1, a sulfurtransferase and Cgl2774. 310 These late-phase upregulated genes have been previously reported to be regulated by MsrR and 311 overexpressed in response to oxidative stress response in C. glutamicum (Si et al., 2020). Genes 312 under the control of DtxR, a master regulator of iron homeostasis at late exponential phase (Küberl 313 et al., 2020), and AmtR, a master regulator of nitrogen metabolism (Beckers et al., 2005) were also 314 upregulated at later time points compared to 6.5 h. The iron homeostasis genes included Cgl0387 315 (putative membrane protein) and Cgl2035, an ABC-type cobalamin/Fe3+-siderophores 316

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transporter. The nitrogen metabolism regulon included genes encoding for ammonium permease, *amt*; a predicted ornithine decarboxylase (*ocd*) and the ABC transporter for urea UrtABCDE.
Ammonium is a critical precursor for growth and tetramethylpyrazine (TMP) production (Xiao et al., 2014).

321 We also observed significant downregulation of *adhA*, *ald*, *sucCD*, *malE/mez* (Figure 4C, blue colored genes), which were previously reported during microaerobic aeration in a bioreactor 322 cultivation of C. glutamicum (Lange et al., 2018). A different complement of transporter-related 323 324 genes was also downregulated across all the later time points that included genes encoding for maltose and trehalose ABC transporter subunits (Cgl2460 and Cgl0727) and the entire glutamate 325 ABC transporter operon gluABCD. This expression profile suggests that at the cell density reached 326 by 20 hours, there was a general cell stress response and the activation of microaerobic-specific 327 genes. The growth conditions did not promote additional cell growth due to the downregulation of 328 329 cell division genes; glucose uptake genes were still highly active, enabling a significant conversion 330 of glucose to organic acids but not biomass accumulation.

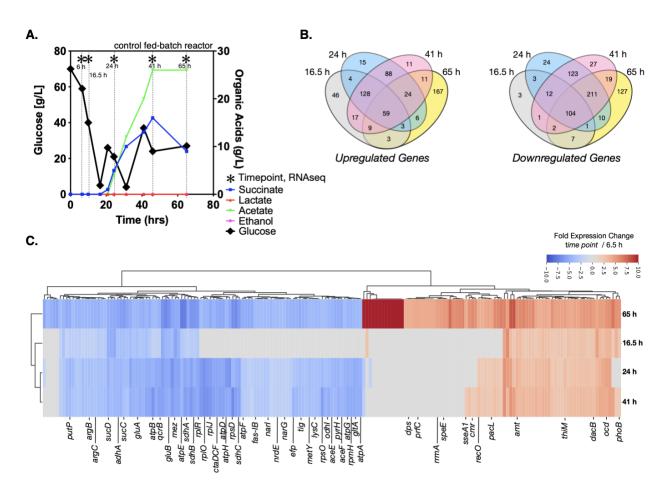
331 We observed a unique class of genes that were only expressed after high accumulation of succinate and acetate at the 65 hour time point. At this time point, glucose consumption has stalled, 332 and the overflow organic acids have plateaued at the  $\sim 10$  g/L concentration. Genes encoding for 333 detoxification including catalase gene Cgl0255/katA, superoxide dismutase gene 334 ROS Cgl2927/sod along with Cgl2003/gor, a mycothione reductase involved in arsenate detoxification 335 were upregulated. DEGs that were downregulated included genes encoding for *catA2*, *catC*, *nagI*, 336 337 qsuB, benC and benD. These are enzymes involved in aromatic compound degradation through beta ketoadipate pathway that would reroute flux into TCA through succinate and acetyl CoA. We 338 interpret the expression of these genes as indicative of the unfavorable cell growth conditions. 339

A regulator involved in diverting acetyl CoA flux towards fatty acid biosynthesis, Cgl2490/*fasR* was constitutively expressed up until the last time point during bioreactor cultivation in absence of IL. This TetR type transcriptional regulator controls fatty acid biosynthesis and malonyl CoA formation from acetyl CoA and has been deleted for improving malonyl CoA production (Milke et al., 2019). Our analysis correlated this repression by *fasR* with down regulated Cgl2495/*fas-IA* as well as downregulation of Cgl0700/*accBC*, Cgl0708/*dtsR1* and Cgl0707/*dtsR2* during later time points in absence of IL.

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Figure 4: Growth of engineered C. glutamicum for isopentenol in a control stir tank bioreactor. 350 (A) HPLC analysis of glucose and organic acids detected in the 2L stirred tank bioreactor. Cells 351 were harvested from the indicated time points with (\*). Refer to Figure 5a for the [Ch][Lys] treated 352 bioreactor. (B) Shared and unique differentially expressed genes. Venn diagrams indicate the 353 number of Upregulated (left) and downregulated (right) genes at the indicated time points. (C) 354 Hierarchical cluster analysis of the top 181 differentially expressed genes at the 65 hr time point 355 vs the 6.5 hr time point for both up or down regulation. A number of genes that are highly expressed 356 357 only in stationary phase vs constitutively expressed are observed.

358

#### 2.5. C. glutamicum exhibits a complex response to the IL, Cholinium Lysinate under fed-batch 359

cultivation in the bioreactor 360

Next we analyzed differential gene expression when cells were grown in the presence of 50 mM 361 [Ch][Lys], simulating hydrolysate prepared under a water-conservation regimen (Neupane et al., 362 2017). Ionic liquids have been reported to increase osmotic pressure, attack lipid structures and 363 consequently disrupt microbial membranes (Pham et al., 2010; Khudyakov et al., 2012; Yu et al., 364 2016). C. glutamicum exhibited differential expression of 727 genes (Supplementary Data, 365 366 **Dataset S3**), during the [Ch][Lys] treated fed-batch bioreactor cultivation in comparison to the untreated culture at the time-matched samples (Figure 5A). While both bioreactors consumed the 367

#### Systems Analysis of C. glutamicum

initial glucose in the reactor at similar rates, their response to the first feeding at 24 hours differed.
The [Ch][Lys] reactor showed maximum accumulation of 4 g/L succinate and 6 g/L acetate over
the duration of this time course, a 4 fold decrease for both organic acids in the absence of [Ch][Lys]
(compare Figure 4A to Figure 5A). In the presence of [Ch][Lys], genes encoding for succinate
utilization such as *sdhA*, *sdhB* and *sdhC* were all upregulated at 24 h and 41 h in contrast to the
control reactor. Similarly, genes encoding for pyruvate decarboxylation to acetyl CoA (instead of
acetate) via *aceE* and *aceF* were also highly upregulated at later time points.

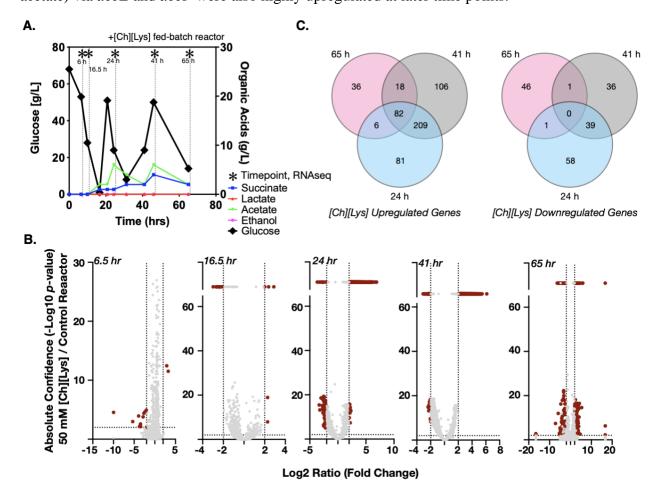


Figure 5: Differential expression of genes in response to 50 mM of [Ch][Lys]. (A) HPLC analysis 376 of glucose and organic acids detected in the 2-L stirred tank bioreactor of cells grown in the 377 presence of an initial concentration of 50 mM [Ch][Lys]. Cells were harvested from the indicated 378 time points with (\*). Refer to Figure 4a for the control bioreactor. The glucose and organic acid 379 values for the time course in this figure panel have been previously described in Eng and Sasaki 380 et al, 2020. (B) Volcano plots of differentially expressed genes for each time point. Genes which 381 have confidence values or log2 ratios greater than the maximum value on each axis are plotted on 382 a discontinuous portion of the axis as indicated with a line break. c) Shared and unique 383 differentially expressed genes in response to [Ch][Lys]. Very few differences were detected in the 384 6 h and 16.5 h time points and are not included in the Venn diagram. DEG was calculated as the 385 ratio between the treated reactor and its corresponding time-matched sample in the other control 386 387 reactor. Venn diagrams indicate the number of upregulated (*left*) and downregulated (*right*) genes at the indicated time points. 388

375

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During the early cultivation time points (6.5 - 16.5 h), only 1.5% of the total pool of 389 390 differentially expressed genes changed in response specifically to [Ch][Lys], but the datasets diverged after the first feeding at 24 hours as biomass formation reached its maximum (Figure 391 392 5B). Only two genes were upregulated at the 6.5 h time point: a MFS transporter (Cgl2611) and its transcriptional regulator (Cgl2612) (Supplementary Data, Dataset S3). The BRC-JBEI 1.1.2 393 homolog is 97.37% identical to Cgl2611 which exports cadaverine, a L-lysine derived product 394 (Kind et al., 2011; Adkins et al., 2012; Jones et al., 2015; Tsuge et al., 2016). Cgl2611 expression 395 was not detected at the control 6.5 h time point, but both genes are highly upregulated with or 396 without [Ch][Lys] treatment in the remaining time points. Cgl1203, which encodes a phospho-N-397 acetylmuramoyl- pentapeptide-transferase associated with cell wall biosynthesis, was only 398 399 upregulated at 16.5 h.

Early transcriptome changes in *C. glutamicum* during bioreactor cultivation post [Chl][Lys] exposure included overexpression of MFS transporters along with repression of mechanosensitive channels that were consistent with IL tolerance mechanisms reported in other microbes (Khudyakov et al., 2012; Martins et al., 2013; Yu et al., 2016). Many genes were downregulated in response to exogenous [Ch][Lys] in the bioreactor and represented 25% of DEGs. Cgl0879/*mscL*, a large-conductance mechanosensitive channel, and is related to osmotic regulation (Krämer, 2009), was uniquely downregulated at 16.5 h.

407 A comprehensive analysis of upregulated DEGs at more than one time point represented around 59% of the total upregulated genes in the presence of IL (Figure 5B). Nearly 15% of those 408 409 genes showed consistent overexpression from 24 h through 65 h (Figure 5C). This differential transcript profile reflects the metabolic perturbation over the course of the fed-batch cultivation 410 after the initial glucose exhaustion followed by glucose pulse feeding and is depicted in Figure 6. 411 Prominent DEGs include those encoding for energy metabolism, amino acids biosynthesis, 412 response to oxidative and other environmental stress conditions (Figure 5E and Supplementary 413 **Data**, **Dataset S4**). Genes involved in energy metabolism were highly upregulated during the later 414 phase of fed-batch cultivation in the presence of IL compared to its absence. These included 415 416 NADH dehydrogenase (Cgl1465), succinate dehydrogenase, *sdhABC* genes at 24 h and 41 h; cytochrome oxidase, *ctaDCEF*, cytochrome reductase, *qcrCAB* and the ATP synthase complex 417 (Cgl1206 to Cgl1213) genes at 24 h, 41 h and 65 h. Amino acid biosynthetic genes upregulated at 418 the later time points included the arginine biosynthetic genes *argC argJ*, *argB* and *argH* at 65 h 419 and argG and argD at mid cultivation phase (41 h). ArgJ protein was also enriched in the 420 acetoin/TMP producing C. glutamicum strain (Eng et al., 2020). Genes encoding for other amino 421 422 acid biosynthesis included Cgl1139/metE, Cgl2446/metB and Cgl0653/metY at 24 h and 41 h from the methionine/homocysteine pathway; Cgl2204/*ilvE* at 24 h and Cgl1273/*ilvC* at 24 h and 41 h in 423 the branched amino acid pathway. Several ribosomal proteins were significantly upregulated 424 425 during the same cultivation phase (24 h and 41 h) including 30S ribosomal proteins S15 (Cgl1976/rpsO) and S18 (Cgl0866/rpsR); 50S ribosomal proteins L28 (Cgl0869/rpmB) and L15 426 (Cgl0542/rplO) along with the ribosome recycling factor Cgl2023/frr. 427

We also observed the upregulation of an ABC transporter (Cgl0946 and Cgl0947), a multidrug transport system (MTS) operon, in part regulated by its adjacent two-component system (TCS) (Cgl0948-Cgl0949, also upregulated). MTS offers a natural defense against toxic compounds and is reported to be upregulated in response to the non-ionic surfactant Tween 40 (Jiang et al., 2020). Also, Cgl2312/*ectP*, a putative BCCT family transporter was overexpressed

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in the bioreactor with IL at 24 h time point. This gene, an orthologue for *betT* gene in *E. coli* and *P. putida*, was under-expressed in the bioreactor without IL at later time points (24 h, 41 h).
Betaine/carnitine/choline (BCCT) family transporters could enable cholinium uptake and
catabolism. An array of other transporters and transcriptional regulators were also downregulated
in the presence of IL (Supplementary Data, Dataset S3).

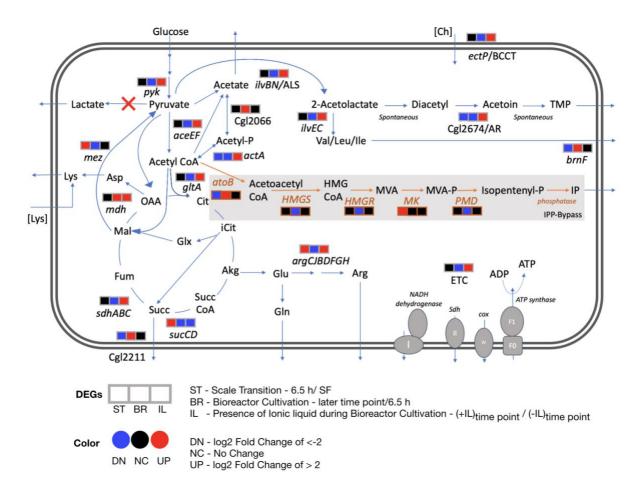
While the analysis above compared matched time points with or without [Ch][Lvs] 438 treatment, we also included one additional analysis to examine DEGs from samples in the same 439 440 reactor but as they progressed from the 41 h to 65 h time point (Supplementary Figure S3, and Supplementary Data, Dataset S6). As observed from our earlier analysis in Figure 4C a set of 441 DEGs in the control bioreactor were detected, consistent with entry into the stationary phase. 442 Significantly downregulated genes also included genes encoding for a stationary phase repressor 443 protein/redox responsive transcription factor, whiB/Cgl0599 (Walter et al., 2020) and a branched 444 chain amino acid transporter (Cgl2250) (Graf et al., 2019). Cgl2250 has been reported to be 445 downregulated during the transition from exponential to stationary phase in C. glutamicum 446 447 (Larisch et al., 2007).

#### 448 2.6. Indication of Flux rerouting in the presence of IL stress during fed-batch bioreactor

449 *cultivation* 

Our transcriptome analysis identified differential profiles for energy metabolism, amino 450 acid biosynthesis and redox related genes as discussed in the previous section (Figure 6). Several 451 genes encoding for metabolic reactions related to acetoin and TMP accumulation were specifically 452 453 upregulated in the presence of 50 mM of [Ch][Lys] at the 24 h or 41 h time points (Supplementary **Data.** Dataset S3. Supplementary Figure S4) when compared to the control samples at the same 454 time points. Of the two subunits of the acetolactate synthase (ALS) ilvB and ilvN, the smaller 455 456 regulatory subunit, Cgl1272/*ilvN* was upregulated in the presence of IL fed-batch cultivation when compared to the absence of IL at 24 h. Acetolactate synthase in C. glutamicum takes part in 457 diverting pyruvate flux towards branched chain amino acids biosynthesis and acetoin biosynthesis 458 and could be a precursor to TMP (Eng et al., 2020) (Figure 5). Although branched chain amino 459 acid biosynthesis has been extensively researched for engineering branched chain alcohol (e.g. 460 isobutanol) producing C. glutamicum strains (Hasegawa et al., 2020) the branched chain amino 461 acid degradation towards isopentenol biosynthesis (through HMG-CoA) and TCA through acetyl 462 CoA still remains to be fully investigated. The other proposed enzyme in TMP accumulation is the 463 NADH consuming acetoin reductase (AR, Cgl2674) and was also significantly upregulated 464 (log2>4) at 41 h in presence of 50 mM of [Ch][Lys] compared to fed-batch cultivation in the 465 absence of IL at similar time points. Genes encoding mechanisms that divert pyruvate flux towards 466 acetyl CoA (Cgl2248/aceE and Cgl2207/aceF) were also upregulated along with genes for 467 pyruvate kinase (Cgl2089/pyk) and citrate synthase (Cgl0829/gltA). 468

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469

Figure 6: Differential transcript profiles of engineered C. glutamicum under fed-batch cultivation. 470 Three DEGs corresponding to three discrete conditions that were analyzed are represented here: 471 ST - scale transition from shake flask (SF) to early bioreactor cultivation (6.5 h), BR - bioreactor 472 later stage cultivation in the absence of IL and IL - bioreactor cultivation in the presence of IL 473 compared to in the absence of IL. The heterologous pathway for IP production is shown in orange. 474 Red crosses show the gene deletions in the C. glutamicum strain used in this study. Abbreviations: 475 Acetyl-P, acetyl phosphate; Akg, alpha ketoglutarate; Arg, arginine; Asp, aspartate; *atoB*, acetyl-476 477 CoA acetyltransferase; Cit, citrate; Ch, cholinium; Cox, cytochrome oxidase; ETC, Electron transport chain; Fum, fumarate; Glx, glyoxylate; Glu, glutamate; Gln, glutamine; HMGS, 478 hvdroxymethylglutaryl-CoA synthase; HMGR, 3-hydroxy-3-methylglutaryl-CoA reductase; 479 480 HMG CoA, 3-hydroxy-3-methyl-glutaryl-coenzyme A; Icit, isocitrate; IP, Isopentenol; Lys, lysine; Mal, malate; MK, mevalonate kinase; MVA, mevalonate; MVA-P, mevalonate; OAA, 481 oxaloacetate; PMD, phosphomevalonate decarboxylase; Succ, succinate; Succ CoA, succinyl-482 483 CoA; Sdh, succinate dehydrogenase; TMP, tetramethylpyrazine.

484

#### 485 **3. Discussion**

486 *C. glutamicum* is a strong contender as a microbial chassis for IP production and is already 487 used at commercial scales. To test IP production in stirred-tank bioreactors, we used process 488 optimizations empirically identified for high IP titers in *E. coli* (Kang et al., 2019). Using this

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alternative microbe, Kang et al reported IP titers > 3 g/L in fed-batch mode production; in contrast, these process parameters led to much lower IP titers in our *C. glutamicum* strains and were instead near the lower detection limit. It is possible that these optimizations were specific to *E. coli*; the impact of this IP production pathway in *C. glutamicum* upon shifting from batch mode to fed-batch mode in a stirred tank bioreactor may have resulted in a different host-specific metabolic response.

What parameters are important in selecting one microbial host over another? From a 494 495 genetic tractability perspective, the biggest drawback of C. glutamicum vs. model microbes such 496 as E. coli could arise from its reduced transformation efficiency, which was lower by 3-5 orders of magnitude (Chung et al., 1989; Inoue et al., 1990; Ruan et al., 2015). However, Baumgart and 497 coworkers made an astute observation; by using a methylation deficient strain of C. glutamicum, 498 499 one could both improve transformation efficiency as well as plasmid copy number (Baumgart et 500 al., 2013). Improved pathway copy number (both genomically integrated or plasmid-borne) in E. 501 coli had already been shown to dramatically improve heterologous isoprenoid titers (Goyal et al., 2018; Chatzivasileiou et al., 2019). With this premise we initially used a methylation deficient 502 503 strain as our starting host. However, the methylation deficient strain only produced trace titers of IP but a related strain produced both improved IP titers 20x or a co-product, tetra-methylpyrazine. 504 505 Understanding the genetic differences in this isolate BRC-JBEI 1.1.2 was the major thrust of this 506 study.

507 Leveraging strain isolate differences is already commonplace when analyzing natively expressed products, such as natural products from *Streptomyces* spp. or wine, beer, and baking in 508 509 Saccharomyces spp. (Nepal and Wang, 2019; Gallone et al., 2016). In E. coli, the Hanahan cloning strain DH1 is the preferred strain for the production of many terpenes, but experimentally 510 identified modifications are needed to translate port pathways to other E. coli isolates as with the 511 512 case for limonene production in E. coli BL21(DE3) (Tsuruta et al., 2009; Rolf et al., 2020). A potential explanation for DH1 being a more robust host may be due to its elevated number of 513 ribosomes compared to strains DH10, BL21, or BW25113 (Cardinale et al., 2013), which may 514 indirectly help with heterologous pathway protein expression. Our whole-genome sequencing 515 analysis identified a large number of genetic differences in our engineered isopentenol producing 516 C. glutamicum BRC-JBEI 1.1.2 isolate (many associated with metabolic functions) that are 517 518 unaccounted for when using the reference C. glutamicum genome. Previously we used computationally driven maximum theoretical yields calculations for a product across several 519 microbes to evaluate microbial potential for a specific product/substrate pair (Banerjee et al., 520 2020). However the accuracy of such predictions rely on the metabolic reactions curated for the 521 reference strain, and are challenging to apply in isolates used with differences at the genomic or 522 metabolic level (refer to IP titers in Figure 1A). Pan-genome assemblies and metabolic models 523 can be applied to this situation (both for BRC-JBEI 1.1.2 and DH1) to more accurately account for 524 525 these metabolic features (Monk et al., 2013; Norsigian et al., 2018).

For emerging processes using IL pretreated lignocellulosic biomass, C. glutamicum as the 526 microbial IP producer for this process is compelling. To the best of our knowledge, this is the first 527 transcriptomics analysis of an engineered isopentenol producing C. glutamicum strain in fed-batch 528 conditions. Due to the relative similarity between this isolate to the type strain, we were able to 529 use existing gene annotations with a fairly low homology cutoff (>70%) for the majority of 530 531 detected transcripts in this study. A large number of significant DEGs identified in this analysis encode hypothetical proteins that lack functional information. These genes can be further 532 533 characterized using functional genomics tools such as parallelized transposon mutant libraries

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(Lim et al., 2019; Cain et al., 2020) or high throughput transcription factor characterization (Rajeev 534 et al., 2014, 2011) to improve our understanding of these useful C. glutamicum isolates. 535 Transcriptomics analysis completed here indicated that in order to improve isopentenol titers under 536 537 stirred tank fed-batch conditions, targeting deleting *mdh* could limit accumulation of succinate, a highly overexpressed gene. gltA, Cgl2211, brnF and arginine biosynthesis genes were also highly 538 upregulated (Figure 6); deleting or down regulating them could enlarge the acetyl-CoA pool, in 539 turn improving IP titers. Additional gene targets include *pta-acka*, *poxB*, *actA* and Cgl2066 to 540 block acetate formation. This transcriptomics analysis also implicated ectP, a BCCT family 541 transporter similar to E. coli betT and P. putida betT-III, as a transporter for [Ch][Lys]; ectP was 542 overexpressed in the presence of ILs. A BCCT transporter has been proposed to be involved in 543 544 uptake and catabolism of the cholinium ion from [Ch][Lys] in both E. coli and P. putida (Park et 545 al., 2020). Characterizing IL tolerance is an active research thrust in our laboratory.

In summary, our transcriptomic analysis under industrially relevant process conditions provides a toehold for future DBTL cycles. Future "learn" steps can leverage the information gleaned here to target the critical features implicated for improved *C. glutamicum* strain performance when producing desirable products, like isopentenol. Even accounting for potential increased cell heterogeneity in the bioreactor (Wehrs et al., 2019), important features both common and unique to conditions allow a closer look into cell physiology.

552

#### 553 **4. Materials and Methods**

#### 554 *4.1. Reagents and Experimental conditions*

In a previous report (Sasaki et al., 2019), we referred to the IP producing *C. glutamicum* strain as ATCC 13032 NHRI 1.1.2, as indicated in our archival notes. As we cannot confirm the provenance of *C. glutamicum* BRC-JBEI 1.1.2 and how it may have been derived from its closest relatives *C. glutamicum* SCgG1 or SCgG2, we opted to give this strain a unique identifier to avoid further confusion.

Unless indicated elsewhere, all reagents used were molecular biology grade or higher. Primers 560 561 were synthesized by IDT DNA Technologies (Coralville, IA). CGXII media was prepared as previously described (Sasaki et al., 2019; Keilhauer et al., 1993). All strains and plasmids used in 562 this study are described in **Supplementary Table S2**. C. glutamicum strains were struck to single 563 colonies from glycerol stock on LB plates containing the appropriate antibiotic and prepared for 564 565 production runs as previously described (Eng et al., 2020). The fed-batch cultivation with 50 mM of [Ch][Lys] supplementation was previously described in (Eng et al., 2020). The control 566 567 bioreactor without [Ch][Lys] was conducted at the same time and the glucose feeding regime was identical to that of the ionic liquid (IL) supplemented reactor. For RNAseq extraction, 5mL culture 568 samples were harvested in 1 mL aliquots, collected by centrifugation at 14,000xg for 3 minutes, 569 and stored at -80 °C until subsequent RNA extraction. The supernatant from one of the appropriate 570 571 time point aliquots was processed for organic acid analysis as described previously (Eng et al., 2020). Lab-scale IP production runs in deep well plates or 5 mL culture tubes were conducted as 572 previously described (Eng et al., 2020). Isopentenol titers reported for the deep well plate format 573 were corrected for evaporation at the 48 h time point as conducted previously (Sasaki et al., 2019). 574 575 Exogenous [Ch][Lys] toxicity against C. glutamicum ATCC13032 and BRC-JBEI 1.1.2 was 576 analyzed in a 48-well microtiter dish format. Cells were first adapted two times in CGXII minimal

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577 media with 4% (w/v) D-glucose. When cells were back diluted into fresh media in the microtiter 578 dish, the starting OD600 was set to 0.1 with a fill volume of 200  $\mu$ L. The plate was incubated with 579 shaking at 30 °C and exogenous [Ch][Lys] added at the start of the time course. OD was monitored 580 at 600 nm on a Synergy 4 plate reader (BioTek Instruments, Winooski VT) with the continuous 581 shaking setting.

582

#### 583 *4.2. Production run with ensiled sorghum hydrolysate*

CGXII minimal media was supplemented with ensiled sorghum biomass hydrolysate to test the 584 585 ability of C. glutamicum BRC-JBEI 1.1.2 to utilize carbon sources from renewable feedstock pretreated with IL. Briefly, the forage sorghum (NK300 type, grown in Fresno, CA) was planted 586 587 in Spring 2020 and harvested in Fall 2020. A forage harvester was used to both harvest and chop 588 the sorghum biomass, which was then loaded in a silage pit, inoculated, and covered to maintain 589 anaerobic conditions. The pit was opened in November 2020 and a sample of the ensiled material was collected, packed with dry ice while in transit, and stored at 4 °C. A 210 L scale Andritz 590 591 Hastelloy C276 pressure reactor (AG, Graz, Austria) with a helical impeller was utilized to process ensiled sorghum for the pretreatment and saccharification processes. Ensiled sorghum biomass 592 was pretreated at 20% w/w solid loading with 10% w/w [Ch][Lys] at 140 °C for 3 h with a mixing 593 speed of 30 rpm. Solid loading was calculated based on the dry matter content determined using a 594 Binder VDL115 vacuum oven. After 3 hours at the target temperature, the reactor was cooled to 595 room temperature before proceeding with the next steps. The Andritz reactor is sealed during this 596 597 process, preventing contamination until further processing. Following pretreatment, the pretreated materials were adjusted to pH 5.1 using 50% v/v sulfuric acid and an enzyme cocktail of 598 Novozyme, Inc Cellic Ctec3 and Cellic Htec3 commercial enzymes in a ratio of 9:1 was added. 599 Concentration of the commercial stocks were determined using Bradford assays and bovine serum 600 albumin as a reference. Enzyme load was conducted at a ratio of 10 mg enzyme per 1 g of dry 601 weight biomass. Following pH adjustment and enzyme addition, RODI water was added to obtain 602 a final solid loading of 18.70%. Saccharification by enzymatic hydrolysis was operated at 50 °C, 603 604 30 rpm for 70 h (Barcelos et al., 2021). The hydrolysate was then sequentially filtered using a filter press through 5 µm, 1 µm, and 0.25 µm filters. Final filter sterilization was completed with a 0.2 605 µm filter and stored at -80 °C until further use. This hydrolysate was thawed and added in place of 606 water in CGXII media (amounting to 2.8 % (w/v) glucose), pH was adjusted to 7.4 and filter 607 sterilized one additional time before use. We make the assumption the hydrolysate contained no 608 biologically available nitrogen. To maintain a C/N ratio of glucose/ammonium sulfate + urea of 609 610 2.8, pure glucose powder was supplemented to the hydrolysate CGXII cultivation medium composition (Sasaki et al., 2019). 611

- 612
- 613 *4.3. DNA and RNA Isolation*

614 Genomic DNA from *C. glutamicum* BRC-JBEI 1.1.2 was isolated with the following protocol. In 615 brief, strains from glycerol stocks were struck to single colonies on LB plates grown at 30 °C

overnight. A single colony was then inoculated into a 250 mL shake flask with 25 mL LB media

and grown overnight to saturation. Cells were collected by centrifugation at  $4,000 \times g$  for 5 minutes.

- The cell pellet was then resuspended in 2 mL lysis buffer (2mM EDTA, 250mM NaCl, 2% (w/v)
  SDS, 2% (v/v) Triton-X 100, 2% (v/v) Tween-80, 5 mM DTT, 30 units Zymolyase 100T, 1 mg/mL
  - 19

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RNaseA). Zymolyase was supplied by US Biological (Salem, MA). The cells were initially
incubated at 50 °C to promote protease activity and then incubated for an additional 3 hours at 37
°C with occasional mixing, at which point the lysate became noticeably viscous. DNA was
extracted following standard protocols for isolation of DNA using phenol chloroform: isoamyl
alcohol and subsequent isopropanol precipitation (Sambrook and Russell, 2001).

RNA was extracted from C. glutamicum samples using a Direct-Zol RNA Kit (Zymo Research, 625 626 Irvine, CA) following the manufacturer's protocol. C. glutamicum cells were lysed after initially 627 resuspending the cell pellet in 500 µL TRI reagent and mixed with glass beads. This mixture was then subject to cell disruption using a bead-beater (Biospec Inc, Bartlesville, OK) with a 3 minute 628 homogenization time at maximum intensity. After bead beating, samples were collected following 629 630 the manufacturer's protocol without any additional modifications. RNA quality was assessed using a BioAnalyzer (Agilent Technologies, Santa Clara, CA) before RNA library preparation and 631 downstream analysis. 632

633 For 16S ribosomal sequencing, *C. glutamicum* ATCC 13032 Δ*mrr* and *C. glutamicum* JBEI-BRC

634 1.1.2 were struck from glycerol stocks to single colonies on LB plates and incubated overnight at 635  $30^{\circ}$  C. A single colony was isolated and boiled in 50 µL dH<sub>2</sub>0 for 10 minutes. 1 µL of the boiled

colony was used for PCR with primer pair (JGI\_27F: 5'-AGAGTTTGATCCTGGCTCAG-3' and
 JGI\_1391R: 5'-GACGGGCRGTGWGTRCA-3') with NEB Q5 Polymerase (New England
 Biolabs, Ipswitch, MA). The PCR amplicon was confirmed by agarose gel electrophoresis and the
 sequence was determined using conventional Sanger Sequencing (Genewiz LLC, Chelmsford,
 MA).

641

# 642 *4.4. PacBio Genome Assembly*

643 DNA sequencing was generated at the DOE Joint Genome Institute (JGI) using the Pacific 644 Biosciences (PacBio) sequencing technology. A Pacbio SMRTbell(tm) library was constructed 645 and sequenced on the PacBio Sequel and PacBio RS II platforms, which generated 397,096 filtered 646 subreads (1,418,602,725 subread bases) totaling 3,352,276 bp. The mean coverage for this genome 647 was 432.21x. All general aspects of library construction and sequencing performed at the JGI can 648 be found at http://www.jgi.doe.gov.

649

# 650 *4.5. RNAseq Library Generation and Processing for Illumina NGS*

Stranded RNAseq library(s) were created and quantified by qPCR. Sequencing was performed 651 using an Illumina instrument (refer to Sample Summary Table for specifics per library). Raw fastq 652 file reads were filtered and trimmed using the JGI QC pipeline resulting in the filtered fastq file 653 (\*.filter-RNA.gz files). Using BBDuk (https://sourceforge.net/projects/bbmap/), raw reads were 654 655 evaluated for artifact sequence by kmer matching (kmer=25), allowing for 1 mismatch and detected artifacts which were trimmed from the 3' end of the reads. RNA spike-in reads, PhiX 656 657 reads and reads containing any Ns were removed. Quality trimming was performed using the phred 658 trimming method set at Q6. Following trimming, reads that did not meet the length threshold of at 659 least 50 bases were removed.

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Filtered reads from each library were aligned to the reference genome using HISAT2 version 2.2.0 660 (Kim et al., 2015). Strand-specific coverage bigWig files were generated using deepTools v3.1 661 (Ramírez et al., 2014). Next, featureCounts (Liao et al., 2014) was used to generate the raw gene 662 counts (counts.txt) file using gff3 annotations. Only primary hits assigned to the reverse strand 663 were included in the raw gene counts (-s 2 -p --primary options). Raw gene counts were used to 664 evaluate the level of correlation between biological replicates using Pearson's correlation and 665 determine which replicates would be used in the DEG analysis (Supplementary Figure S5). In 666 the heatmap view, the libraries were ordered as groups of replicates. The cells containing the 667 correlations between replicates have a purple (or white) border around them. For FPKM and TPM, 668 normalized gene counts refer to SRA reads (Data availability section). A sample legend and 669 670 description of RNAseq libraries used in this paper is described in Supplementary Table S3.

671

### 672 *4.6. Transcriptome Analysis*

Global transcriptome response under various experiment conditions were measured using 673 674 Geneious Prime 2021 (https://www.geneious.com). The normalized expression was calculated and the differentially expressed genes (DEGs) were filtered for absolute  $\log 2$  ratio > 2 (i.e. a 4-fold up 675 or down regulation), absolute confidence >3 (p<0.001) and >90% sequence identity. The DEGs at 676 various conditions were functionally annotated using Blast2GO suite (Götz et al., 2008) to assign 677 GO annotations (Galperin et al., 2014). Each DEG was subjected to pathway analysis using the 678 **KEGG** (Kyoto Encyclopedia of Genes and Genomes) database 679 680 (http://www.kegg.jp/kegg/pathway.html) to explore the biological implications. Biocyc (https://biocyc.org/) was used to calculate pathway enrichment for the last 65 h/41 h time point 681 and for additional gene orthologs identification. Pathways were considered significant if p<0.05. 682 Hierarchically clustered heat maps were generated with average linkage method and euclidean 683 distance metric in Jupyter notebook using Python library Seaborn 0.11.1 (Waskom et al., 2020). 684

685

# 686 5. Data Availability Statement

687 All datasets generated in this study are included in the article and Supplementary material. The 688 RNAseq datasets generated and analyzed for this study can be found at the JGI Genome Portal under Project ID 1203597. RNAseq datasets have also been deposited at the NCBI SRA database 689 under the following sample accession numbers: SRP239962; SRP239973; SRP239963; 690 691 SRP239971; SRP239972; SRP239970; SRP239968; SRP239969; SRP239966; SRP239967; SRP239964 ; SRP239965. The draft genome assembly of C. glutamicum BRC-JBEI 1.1.2 has been 692 693 deposited at the NCBI BioProject database with accession number PRJNA533344 and scaffold assembly accession number GCA 011761195.1. The IMG accession number of this genome 694 assembly on the JGI IMG database is 2821586876. 695

696

# 697 6. Supplementary Material

- 1) List of Supplementary Figures S1 to S5 and Supplementary Tables S1 to S3.
- 6992)Supplementary Data: Datasets S1 to S6
- 700

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### 701 7. Conflict of Interest

- The authors declare that the research was conducted in the absence of any commercial or
- financial relationships that could be construed as a potential conflict of interest.
- 704

# 705 8. Author Contributions

706 Raised Funds: AM BS. Conceptualization of the project: AM TE. Strain construction, molecular

- <sup>707</sup> biology, bioreactor sample collection and processing: YS TE RH JT. Analytical Chemistry, IP
- 708 Production Assays, IL toxicity assays: YS, TE, AS. Interpreted results: YS DB TE AM.
- 709 Contributed critical reagents: NS AO CS DP TE YS JT BS. RNAseq library generation, data
- collection, validation: VS, YS, TE. Drafted the manuscript: DB TE AM. All authors read,
- contributed feedback, and approved the final manuscript for publication.
- 712

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# 725 **11. References**

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