

Affinity sedimentation and magnetic separation with plant-made immunosorbent nanoparticles for therapeutic protein purification

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Summary

The virus-based immunosorbent nanoparticle is a nascent technology being developed to serve as a simple and efficacious agent in biosensing and therapeutic antibody purification. There has been particular emphasis on the use of plant virions as immunosorbent nanoparticle chassis for their diverse morphologies and accessible, high yield manufacturing via crop cultivation. To date, studies in this area have focused on proof-of-concept immunosorbent functionality in biosensing and purification contexts. Here we consolidate a previously reported pro-vector system into a single *Agrobacterium tumefaciens* vector to investigate and expand the utility of virus-based immunosorbent nanoparticle technology for therapeutic protein purification. We demonstrate the use of this technology for Fc-fusion protein purification, characterize key nanomaterial properties including binding capacity, stability, reusability, and particle integrity, and present an optimized processing scheme with reduced complexity and increased purity. Furthermore, we present a coupling of virus-based immunosorbent nanoparticles with magnetic particles as a strategy to overcome limitations of the immunosorbent nanoparticle sedimentation-based affinity capture methodology. We report magnetic separation results which exceed the binding capacity of current industry standards by an order of magnitude.

Keywords

Virus-based nanomaterial; molecular pharming; protein purification; bionanotechnology; bio-functionalized magnetic particle; monoclonal antibody; Fc-fusion protein; bioprocessing; tobamovirus; space medicine.

40 1. Introduction

41 Virus-based nanomaterials are proving to be uniquely accessible, precise, and efficacious solutions
42 to problems in fields ranging from energy to medicine (Wen and Steinmetz, 2016). Plant viruses
43 serve as a particularly interesting biologically-derived nanomaterial for their inherent advantages
44 of host specificity-related human safety (Nikitin *et al.*, 2016), simplicity of *in planta* cultivation
45 (Hefferon, 2017), and wide variety of particle architectures and functionalities (Ibrahim *et al.*,
46 2019). Plant viral nanoparticles and virus-like particles have been studied for diverse biotechnical
47 applications including gene therapy (Azizgolshani *et al.*, 2013; Czapar and Steinmetz, 2017),
48 vaccines (Balke and Zeltins, 2019; Canizares *et al.*, 2005), medical imaging (Aljabali *et al.*, 2019;
49 Shukla and Steinmetz, 2015b), drug delivery (Bruckman *et al.*, 2018; Lebel *et al.*, 2016), and
50 biosensors (Bäcker *et al.*, 2016; Soto *et al.*, 2006).

51 The concept of a plant virus-based immunosorbent nanoparticle (VIN), a plant virus or virus-like
52 particle displaying antibody-binding proteins, has been proposed to capture antibodies for
53 biosensing (Kuo *et al.*, 2018; Uhde-Holzem *et al.*, 2016) and therapeutic antibody purification
54 (Werner *et al.*, 2006). This nascent technology is one approach to address the need to reduce capital
55 intensity for equitable and accessible antibody-related healthcare solutions, which could be
56 harnessed to treat more prevalent diseases with availability of inexpensive and adequate
57 production and purification capacity (Buyel *et al.*, 2017). Purification can cost up to 80% of the
58 total manufacturing expenses for antibody and other biopharmaceutical products (Yang *et al.*,
59 2020). The simple and bioregenerable VIN technology is also one that may transcend terrestrial
60 needs as humankind considers extended duration space exploration and is faced with stringent life
61 support system requirements in perhaps the most limited resource environment that humans will
62 face (Aglietti, 2020; Menezes *et al.*, 2015). Recent literature highlights the potential of plant-based
63 manufacturing to close human health risk gaps for manned exploration missions (Matthew J.
64 McNulty *et al.*, 2021).

65 Initial VIN research has primarily focused on nanomaterial design, considering three plant virion
66 chassis (potato virus X (Uhde-Holzem *et al.*, 2016), bamboo mosaic virus (Kuo *et al.*, 2018), turnip
67 vein clearing virus (TVCV) (Werner *et al.*, 2006)) and several ligand display strategies, including
68 multiple fusion sites on the coat protein, linker inclusions, modulations of ligand display density,
69 and two different immunosorbent ligands (both based on functional fragments of *Staphylococcus*
70 *aureus* Protein A). Additional research is needed to evaluate broader functionalities of VIN
71 technology, characteristics for reliable biomanufacturing, and compatibility with advanced multi-
72 material configurations.

73 There have been multiple approaches to engineering virus-based nanomaterials into multi-material
74 configurations including layer-by-layer assembled thin biofilms (Tiu *et al.*, 2017), electrospun
75 nanofibers (Shin *et al.*, 2014), and bio-functionalized magnetic particles, to name a few. Within
76 these approaches, bio-functionalized magnetic particles have been distinguished at large as an
77 important platform within biosensing (Zhang and Zhou, 2014), and protein purification
78 (Schwaminger *et al.*, 2019). However, the virus-based nanomaterial research exploring bio-
79 functionalized magnetic particles to date has been limited to gene therapy (Chan *et al.*, 2005;
80 Majidi *et al.*, 2015) and molecular imaging (Huang *et al.*, 2011; Shukla and Steinmetz, 2015a).

81 Given the demonstrated ability of virus-based nanomaterials as reagents to enhance target binding
82 and sensitivity over traditional ligands (Koch *et al.*, 2015; Sapsford *et al.*, 2006; Soto *et al.*, 2009)
83 we perceive a general synergy and advantage in developing virus-functionalized magnetic particles
84 for sensing and protein purification.

85 In this study we present a new vector for production of VINs, develop an optimized purification
86 process for VINs that is generalizable to other plant virus-based nanomaterials, characterize key
87 functional VIN properties, and in the process, identify potential limitations of the VIN methods
88 used to date. In response to identification of these limitations, we present a novel VIN-magnetic
89 particle coupled system to overcome these limitations. Preliminary results suggest enhanced
90 immunosorbent characteristics as compared to commercial immunosorbent magnetic particle
91 standards and also provide a new perspective for utilization of plant virus-based nanomaterials.

92

93 **2. Results**

94 **2.1. Production of a plant virus-based immunosorbent nanoparticle**

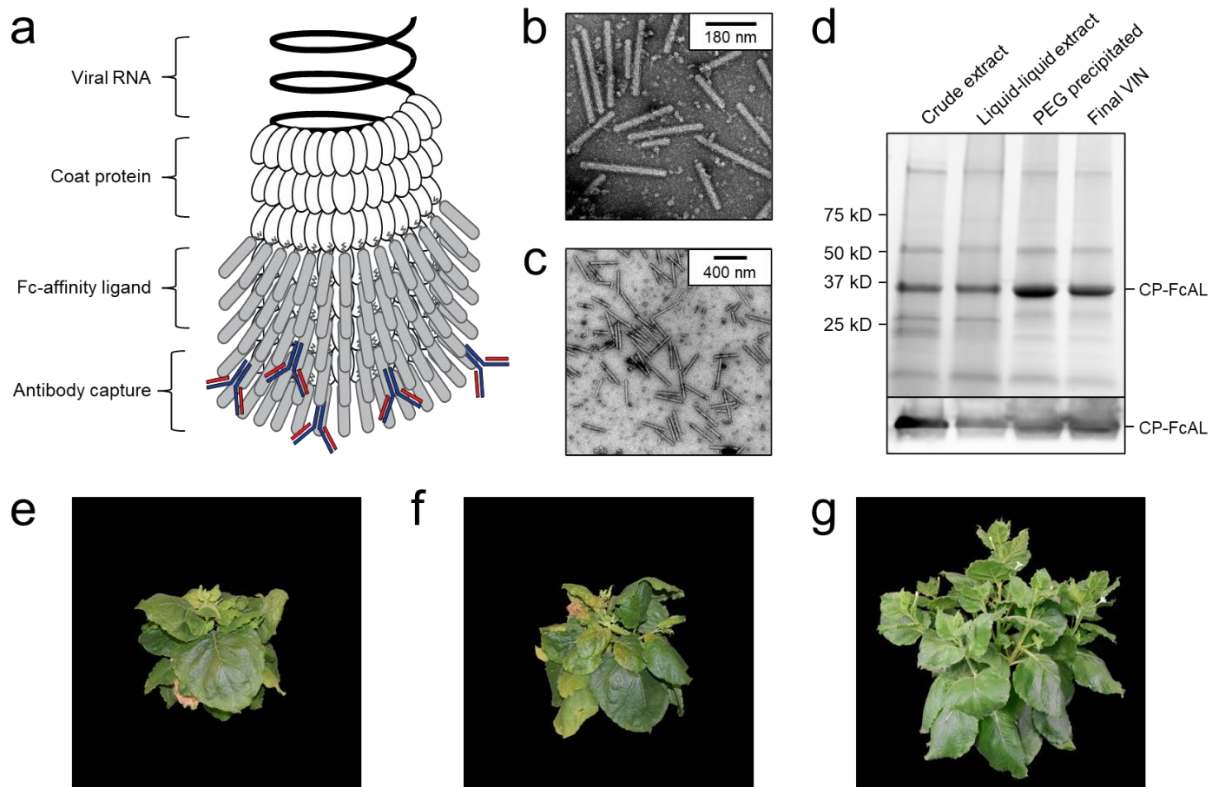
95 Intact VINs consisting of an assembled tobamovirus, TVCV, presenting a C-terminal coat protein
96 fusion to a flexible linker domain (GGGS)₃ coupled to a *S. aureus* Protein A fragment (domains
97 D and E) were successfully produced in *Nicotiana benthamiana* plants via agroinfiltration and
98 subsequently purified to a moderate extent (Figure 1a – d). An illustration of the construct
99 schematic and results of the PCR and DNA sequence verification of the transformation are
100 included in Supporting figures: Figure S1, Figure S2 and Supporting table: Table S1. The vector
101 used here simplifies previously published *A. tumefaciens* vectors (Werner *et al.*, 2006) by
102 combining multiple provectors into a single vector capable of producing intact VINs.

103 Agroinfiltrated *N. benthamiana* plants showed signs of viral infection typical of tobamoviruses
104 (yellowing of leaves, stunted growth; data not shown). The coat protein fusion was expressed at
105 high levels in *N. benthamiana* plants collected 6-14 days post-infiltration. Furthermore,
106 transmission electron microscope (TEM) images show that fully assembled virion particles were
107 formed (Figure 1b-c).

108 SDS-PAGE results confirm that there is a band at the expected size of the VIN coat protein Fc-
109 affinity ligand fusion (CP-FcAL) (~33.5 kD) and Western blot results confirm that it is an identity
110 match for the expected CP-FcAL (via anti-protein A antibody). We did not observe bands
111 corresponding to unfused Fc-affinity ligand on SDS PAGE gels or in Western blots, although SDS-
112 PAGE results do present the possibility of a minor presence of CP-FcAL degradation products.
113 The CP-FcAL protein identity was also confirmed using mass spectrometry (Supporting figure:
114 Figure S3).

115 In addition to agroinfiltration, we also demonstrated that mechanical transmission using the VINs
116 generated by agroinfiltration is a viable route for production of fully assembled and functional
117 plant virus-based immunosorbent particles. Mechanical transmission of the solution containing
118 fully assembled VINs yielded systemic plant infection and morphological change (Figure 1e – g),

119 indicating that the VINs retain systemic mobility with the immunosorbent fusion protein.
120 Agroinfiltration-based VIN expression induced comparable *N. benthamiana* plant morphology
121 (data not shown).



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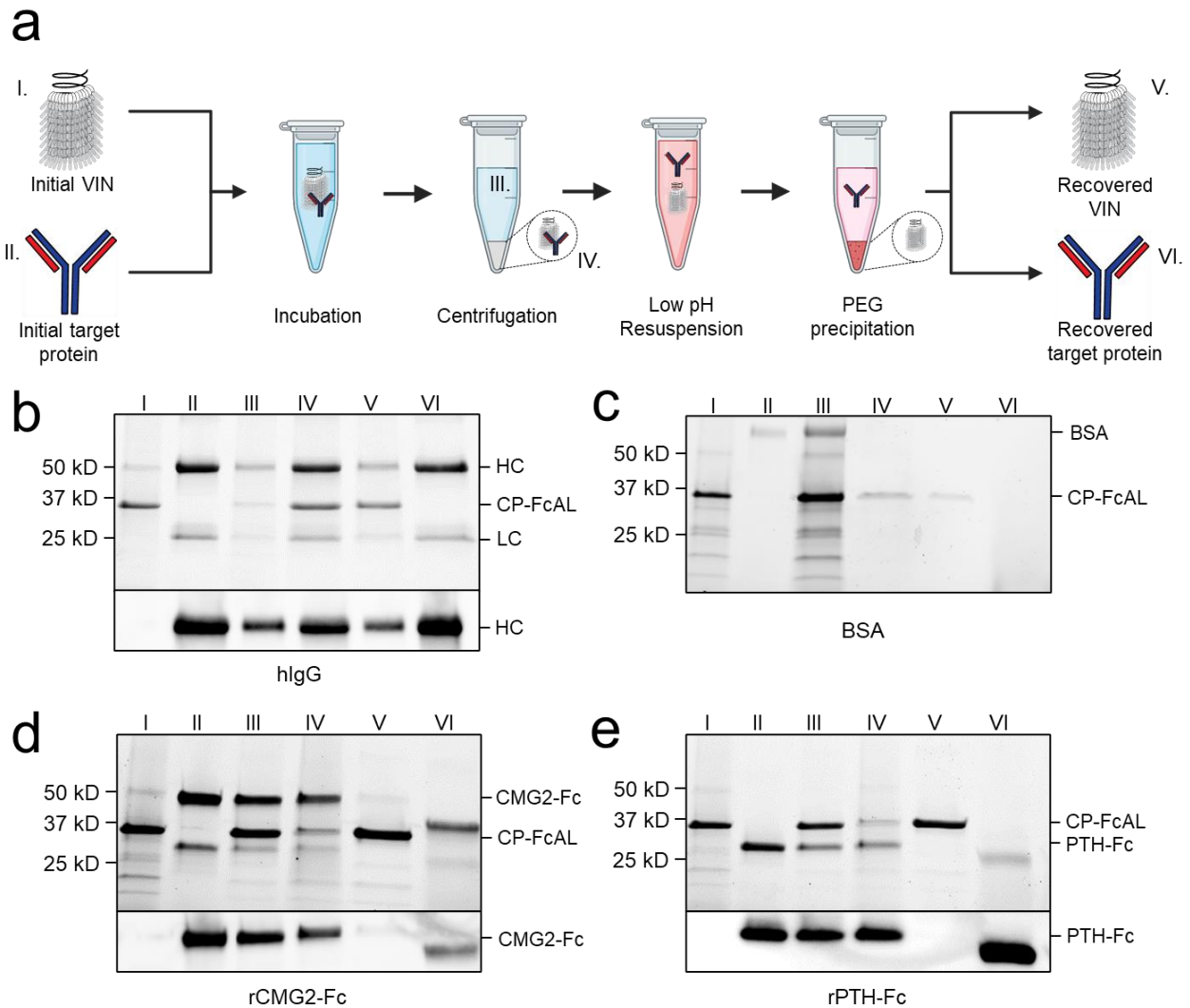
123 **Figure 1. Production of a plant virus-based immunosorbent nanoparticle (VIN).** (a) An
124 illustrative depiction of a VIN. The native plant virus (viral nucleic acid encapsulated by coat
125 protein) is fused via a peptide linker to an Fc-affinity ligand, which confers immunosorbent
126 functionality to the plant virus. (b, c) Negative stain transmission electron microscope images of
127 VIN in crude plant extract solution produced via agroinfiltration in *N. benthamiana* plants. (d)
128 Reducing condition SDS-PAGE (upper) and Western blot (lower) of the VIN preparation marked
129 at the band height corresponding to VIN coat protein Fc-affinity ligand fusion (CP-FcAL).
130 Representative photographs of 7-week-old *N. benthamiana* plants incubated in a controlled
131 environment facility for 14 days post-infection with mechanically transmitted (e) VIN (produced
132 using vector pICH25892), and (f) wild-type tobacco mosaic virus, as compared to (g) uninfected
133 healthy plants.

134

135 2.2 Fc-protein capture and elution

136 Protein A is well known to bind strongly with the conserved fragment crystallizable (Fc) region of
137 many species and subclass variants of IgG. We show that VINs retain general immunosorbence
138 for several species and subclasses of IgG (Supporting figure: Figure S4).

139 Next, we demonstrate that VINs are capable of capturing and then eluting human immunoglobulin
 140 G (hIgG) using a low pH elution mechanism (Figure 2a – b). VINs produced using mechanical
 141 transmission were also shown to retain immunosorbent functionality (Supporting figure: Figure
 142 S5). Tests using bovine serum albumin (BSA) as the target capture protein confirm that
 143 sedimentation of the target protein, and largely that of the VIN, required specific binding
 144 interactions (Figure 2c). It was also observed that VINs would sediment in the absence of binding
 145 target proteins at centrifugation of 20,000 x g for 90 minutes (Supporting figure: Figure S6).



146

147 **Figure 2. Plant virus-based immunosorbent nanoparticle (VIN)-based capture and elution**
 148 **of Fc-proteins from a purified solution.** (a) An illustration of the VIN-based capture and elution
 149 that indicates sample points. SDS-PAGE and Western blot results of VIN-based capture and
 150 elution with pre-purified targets of (b) human immunoglobulin G (hIgG) – reduced into heavy
 151 chain (HC) and light chain (LC) constituents, (c) bovine serum albumin (BSA), (d) plant-expressed
 152 recombinant capillary morphogenesis protein Fc-fusion (rCMG2-Fc), and (e) plant-expressed
 153 recombinant parathyroid hormone Fc-fusion (rPTH-Fc). Lane definitions: I – initial VIN added; II

154 – initial target added; III – VIN/target supernatant (loss); IV – VIN/target pellet resuspension
155 (capture) (2x); V – recovered VIN (a,b – 2x; d,e – 4x); VI – recovered target protein (eluate) (5x).

156

157 VINs are also capable of capturing and eluting Fc-fusion proteins (Figure 2d – e). We successfully
158 tested two pre-purified plant-expressed Fc-fusion proteins with VIN-based capture and elution:
159 recombinant capillary morphogenesis protein Fc-fusion (rCMG2-Fc) and recombinant parathyroid
160 hormone Fc-fusion (rPTH-Fc). We observed that the biophysical characteristics (e.g., molecular
161 mass, Svedberg coefficient) of the domain fused to the Fc region is critical to the sedimentation
162 step (denoted III in Figure 2a) performance.

163 The hIgG sedimentation conditions (12,000 x g, 10 minutes) were not adequate for rCMG2-Fc
164 (100 kDa) and rPTH-Fc (55 kDa). We determined that 20,000 x g for 20 minutes was adequate for
165 sedimentation of the tested Fc-fusion proteins when bound to VINs (screening data not shown).
166 Similarly, the smaller sizes of the Fc-fusion proteins as compared to the hIgG required a higher
167 PEG concentration (25% w/v) for the PEG-based buffer exchange step (screening data not shown).
168 Further optimization is required to remove residual PEG in this higher concentration method, as
169 can be observed by the PEG interference of electrophoresis (lanes VI in Figure 2d – e), although
170 it has been shown that the presence of PEG does not impede performance of subsequent
171 downstream processing operations including ion exchange and affinity chromatography (Roe,
172 2001).

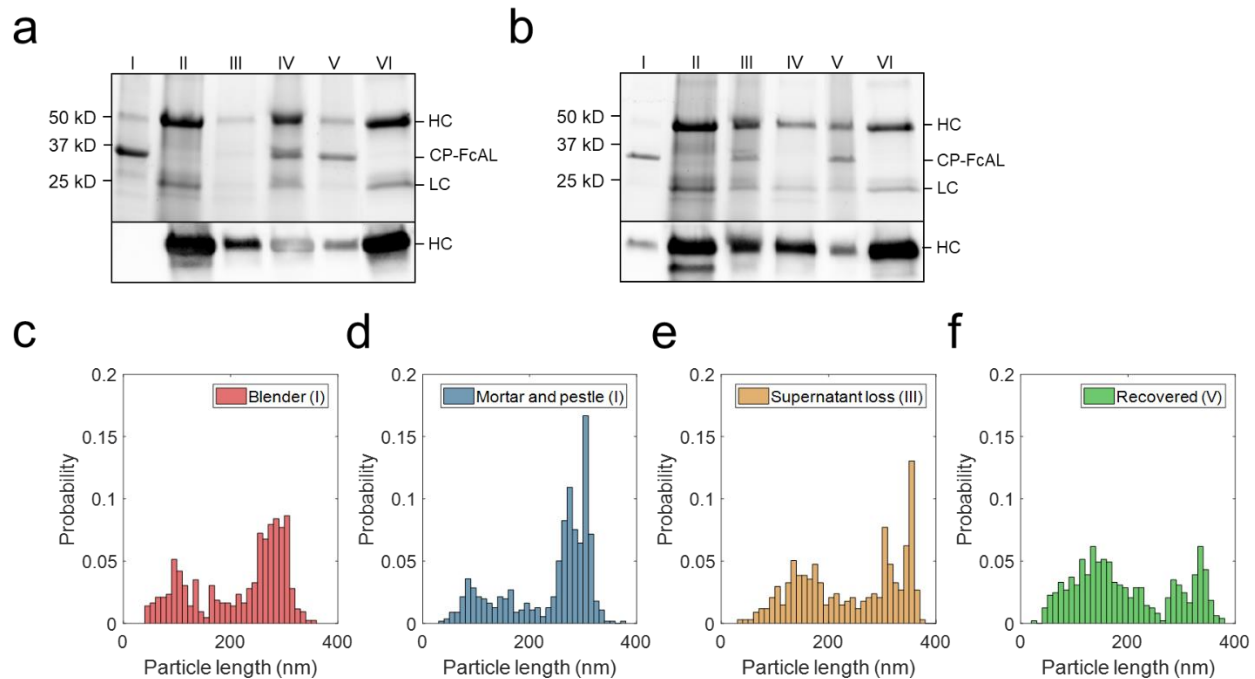
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174 **2.3 Process characterization**

175 We evaluated process performance from the perspective of nanomaterial stability, capture and
176 elution functionality, and particle integrity. VINs are stable throughout the freeze-thaw process for
177 up to 12 cycles without noticeable degradation of CP-FcAL when stored at either -20 °C or -80
178 °C. Long-term stability of VINs was evaluated over a series of timepoints (2 weeks, 4 weeks, 8
179 weeks), temperatures (-20 °C, 4 °C, 20 °C), and protease inhibitors (none, 2 mM
180 ethylenediaminetetraacetic acid (EDTA) and 1 mM phenylmethylsulfonyl fluoride (PMSF))
181 (Supporting figure: Figure S7). VIN CP-FcAL were intact over the duration evaluated at -20 °C
182 and 4 °C, while the addition of protease inhibitors was shown to prolong stability at 20 °C, with
183 no discernable degradation observed for up to 2 weeks (data not shown).

184 Next, we demonstrated that the VIN functionality is retained when using samples of hIgG spiked
185 into wild-type *N. benthamiana* plant extract (Figure 3a). Comparable performance was observed
186 when crude *N. benthamiana* extracts of VIN were used in conjunction with antibodies spiked into
187 crude *N. benthamiana* extracts (data not shown). Furthermore, we were able to demonstrate that
188 the VINs recovered from a single capture and elution cycle can be reused for an additional cycle
189 (Figure 3b). A minor fraction of hIgG was recovered with the VIN in both cycles, suggesting that
190 hIgG recovery could be improved by optimization of the elution step (e.g., CP-FcAL binding
191 affinity, buffer composition). The VIN recovered from the second use cycle could not be used for
192 a third cycle with the established sedimentation conditions.

193 Accordingly, VIN particle integrity was investigated to probe limitations of the sedimentation
194 method. We first compared VINs generated by two different methods of plant extraction, a blender
195 or liquid nitrogen-assisted mortar and pestle (Figure 3c – d). We observed a statistically significant
196 difference in the mean particle length between the two extraction methods ($p < 0.001$), with
197 blender-based extraction resulting in a shorter mean VIN length (blender: $\bar{x} = 217$ nm, $\sigma = 84$ nm,
198 $N = 428$; mortar and pestle: $\bar{x} = 239$ nm, $\sigma = 80$ nm, $N = 558$).



199

200 **Figure 3. Plant virus-based immunosorbent nanoparticle (VIN)-based capture and elution**
201 **of human immunoglobulin G (hIgG) from crude solution over multiple use cycles.** (a) VIN-
202 based capture and elution using a sample of hIgG in crude *N. benthamiana* plant extract, and (b) a
203 second capture and elution cycle of the VIN recovered after the first use cycle. Lane definitions: I
204 – initial VIN added; II – initial target added; III – VIN/target supernatant (loss); IV – VIN/target
205 pellet resuspended (capture) (2x); V – recovered VIN (2x); VI – recovered target (eluate) (5x).
206 Gels are marked with band heights corresponding to VIN coat protein Fc-affinity ligand fusion
207 (CP-FcAL) and hIgG heavy chain (HC) and light chain (LC) constituents. Particle length analysis
208 of negative stain transmission electron microscope images for (c) blender-extracted VIN, (d) liquid
209 nitrogen-assisted mortar and pestle-extracted VIN, (e) VIN in the supernatant lost during the VIN-
210 target complex sedimentation stage, and (f) recovered VIN post-elution. Data from parts e – f are
211 generated using mortar and pestle extracted VIN and the naming convention I, III, and V
212 corresponds to that established in Figure 2a.

213

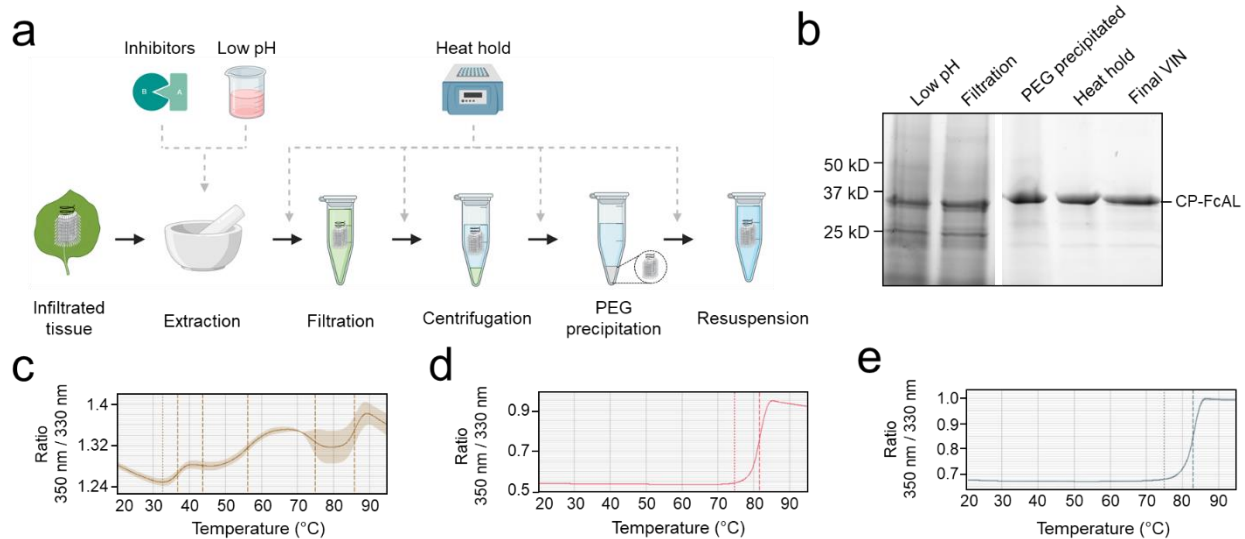
214 We then investigated the VIN particle lengths at steps throughout the capture and elution with
215 initial VIN generated using liquid nitrogen-assisted mortar and pestle extraction, focusing on the
216 VINs lost in the supernatant during the VIN-hIgG complex sedimentation step (Figure 3e) and the

217 final recovered VINs (Figure 3f), denoted III and IV in Figure 2a, respectively. There is an
218 observed statistically significant difference in the mean particle length for the initial VINs, VINs
219 lost in the supernatant ($\bar{x} = 241$ nm, $\sigma = 94$ nm, $N = 337$), and final recovered VINs ($\bar{x} = 196$ nm,
220 $\sigma = 93$ nm, $N = 486$) (I & III, $p = 0.039$; I & IV, $p < 0.001$; III & IV, $p < 0.001$).

221

222 2.4 Process development

223 The appreciable level of impurities present in the purified VIN solutions, as well as an interest in
224 improving scalability of the processing by removing the chloroform-based liquid-liquid extraction
225 step, motivated an investigation into process development of the VIN purification. We performed
226 a 2-factor 2-level process optimization of the extraction step (buffer composition – 50 mM sodium
227 acetate 86 mM NaCl pH 5.0, 100 mM potassium phosphate pH 7.0; protease inhibitors – none, 2
228 mM EDTA + 1 mM PMSF) followed by an addition of a heat hold step that was investigated with
229 a temperature screening (30 – 70 °C) after each processing operation (Figure 4a).



230

231 **Figure 4. A summary of the plant virus-based immunosorbent nanoparticle (VIN)**
232 **preparation process improvement conducted in this study.** (a) An illustration of the VIN
233 preparation stages and the experimental design tested, and (b) SDS-PAGE results of the optimized
234 VIN preparation scheme shown marked at the band height corresponding to VIN coat protein Fc-
235 affinity ligand fusion (CP-FcAL). Nano differential scanning fluorimetry assessment of protein
236 thermostability is shown for (c) crude extract at pH 5, (d) VIN prepared according the optimized
237 scheme, and (e) VIN prepared according to the baseline purification scheme, using the intrinsic
238 tryptophan and tyrosine residue fluorescence at 350 nm and 330 nm.

239

240 Results of the process optimization conditions tested, including verification of bind-and-elute
241 functionality of VIN produced from the different purification schemes, can be found in Supporting
242 figures: Figure S8, Figure S9, and Figure S10.

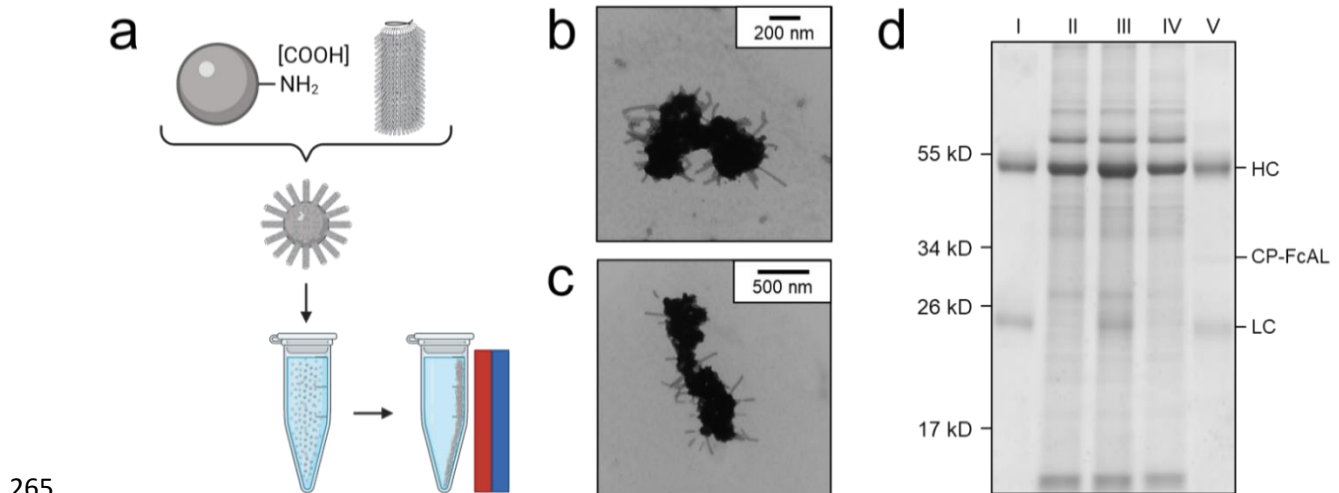
243 The chloroform-based liquid-liquid extraction step was removed from the processing scheme with
244 comparable or improved VIN recovery and purity upon inclusion of a low pH extraction and 60
245 °C heat hold post-PEG precipitation (Figure 4b). Interestingly, the addition of protease inhibitors
246 to the extraction buffer reduced VIN recovery and increased the presence of what appears to be
247 degradation products. Similarly distinct from wild-type virion processing, the heat hold resulted
248 in significant VIN loss when introduced at processing steps prior to PEG precipitation. This
249 behavior can be attributed to the FcAL presentation, as wild-type tobacco mosaic (wt-TMV) is
250 routinely processed with early-stage processing heat holds (Smith *et al.*, 2006).

251 Nano differential scanning fluorimetry results (Figure 4c – e) indicate that the VINs prepared
252 according to either protocol detailed in this study exhibit a melting temperature of ~82 °C,
253 supporting that the improved protocol does not introduce discernible differences in VIN CP-FcAL
254 stability. There are multiple distinct conformational shifts within the crude solution consistent with
255 the heterogeneity of solution.

256

257 2.5 Magnetic separation with VIN

258 Figure 5a illustrates the basic concept and utility of the VIN-coupled magnetic particles (VIN-
259 MPs) generated in this study and Figure 5b – c displays TEM images of the intact VIN-MPs
260 complex. A magnetic separation-based capture and elution method was developed with hIgG
261 spiked into phosphate buffered saline (PBS) (not shown) and crude *N. benthamiana* plant extract
262 that confirms the VIN immunosorbent functionality in this novel configuration (Figure 5d). A faint
263 presence in the elution that may indicate that some minor amount of VIN is recovered in addition
264 to the target hIgG.



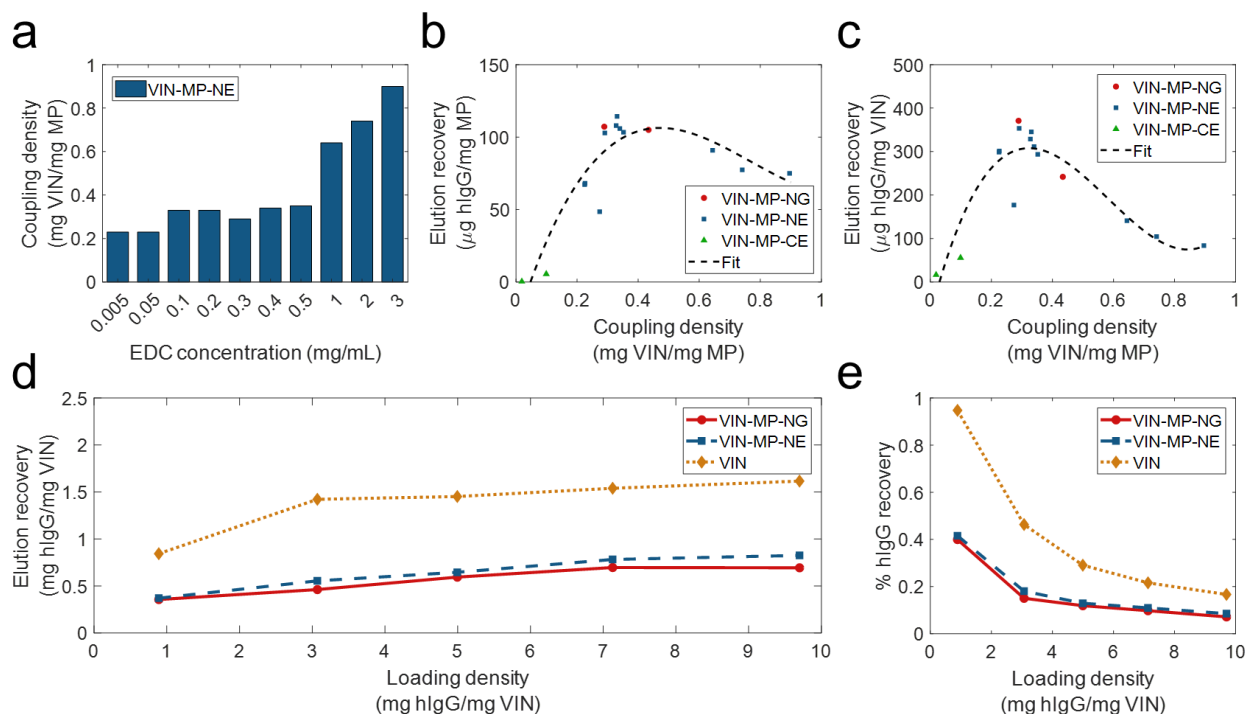
266 **Figure 5. Production of plant virus-based immunosorbent nanoparticles coupled with**
267 **magnetic particles (VIN-MPs).** (a) An illustrative depiction of VIN-MPs. (b, c) Negative stain
268 transmission electron microscope images of VIN-MPs generated using amine-terminated magnetic
269 particles and 5% glutaraldehyde (VIN-MP-NGs). (d) Reducing condition SDS-PAGE of human
270 immunoglobulin G (hIgG) bind-and-elute using VIN-MP-NGs and magnetic separation. Gels are

271 marked with band heights corresponding to VIN coat protein Fc-affinity ligand fusion (CP-FcAL)
272 and hIgG heavy chain (HC) and light chain (LC) constituents. Lane definitions: I – initial hIgG
273 added; II – *N. benthamiana* plant extract; III – hIgG spiked into *N. benthamiana* plant extract; IV
274 – non-bound supernatant after magnetic separation with VIN-MPs; V – hIgG elution from VIN-
275 MPs.

276

277 The VIN-MP were either coupled with amine-terminated (VIN-MP-N) or carboxyl-terminated
278 (VIN-MP-C) superparamagnetic particles. The VIN-MP-N coupled at significantly higher
279 densities (> 0.2 mg VIN/mg MP) than the VIN-MP-C (≤ 0.1 mg VIN/mg MP) and resulted in
280 higher hIgG capture. Therefore, VIN-MP-N were selected as the basis for additional study.

281 Two different coupling agents were tested: glutaraldehyde (VIN-MP-NG) and 1-Ethyl-3-(3-
282 dimethylaminopropyl)carbodiimide (EDC) (VIN-MP-NE). Furthermore, we screened a range of
283 EDC concentrations for use in the VIN-MP-NE synthesis reaction. We observed that the coupling
284 density of VINs to MPs could be tuned with the concentration of EDC used in the covalent
285 coupling reaction (Figure 6a). We also observed that the VIN concentration in the reaction medium
286 could be used to tune coupling density (data not shown).



287

288 **Figure 6. Screening and evaluation of plant virus-based immunosorbent nanoparticle-**
289 **coupled magnetic particle (VIN-MP) coupling density and human immunoglobulin G (hIgG)**
290 **elution.** (a) 1-Ethyl-3-(3-dimethylaminopropyl)carbodiimide (EDC) concentration used during
291 coupling and resultant coupling density for amine-terminated magnetic particles. VIN-MP
292 coupling density and hIgG elution recovery for both amine- and carboxyl-terminated magnetic
293 particles (b) per MP mass basis, and (c) per VIN mass basis. Fits are generated as 3rd order

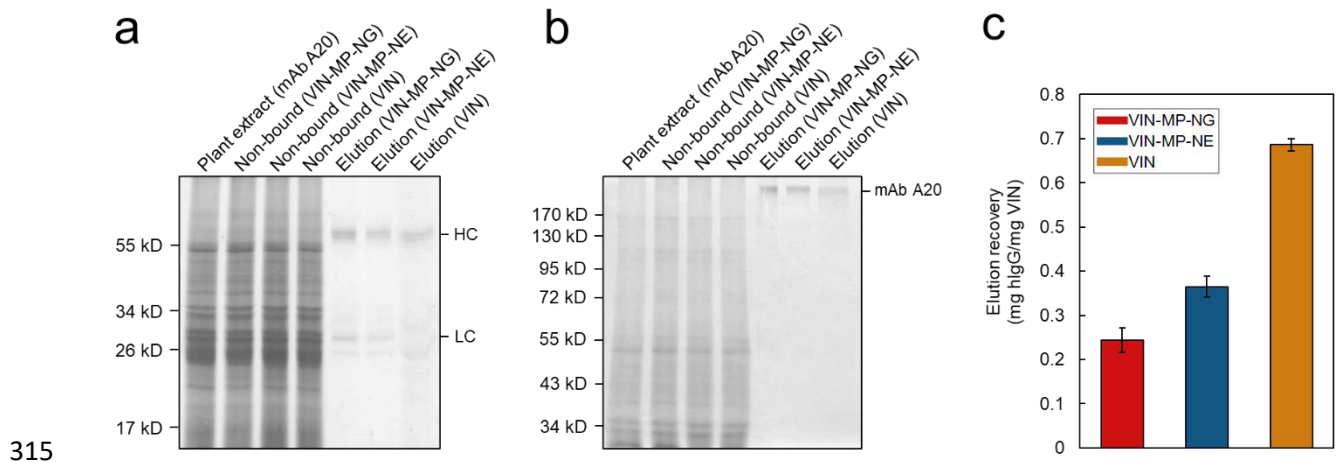
294 polynomials. Elution recoveries of hIgG from PBS are shown over a range of hIgG loading
295 densities for amine-terminated MP (VIN-MP-N) with 5% glutaraldehyde coupling (VIN-MP-NG),
296 0.5 mg/mL EDC coupling (VIN-MP-NE), and uncoupled VIN in free suspension (d) per VIN mass
297 basis, and (e) as an extent of the loading density and of hIgG from PBS.

298

299 We observed a non-monotonic relationship between coupling density and hIgG binding/elution
300 load per mass of MP (Figure 6b). An optimal coupling density of 0.3 – 0.4 mg VIN/mg MP was
301 identified. The hIgG binding/elution load per mass of VIN was consistent at approximately 0.3 mg
302 hIgG/mg VIN below a coupling density of 0.4 mg VIN/mg MP, above which a negative correlation
303 between coupling density and hIgG binding/elution load per mass of VIN is observed (Figure 6c).
304 This suggests that higher coupling densities may provide less available hIgG binding sites due to
305 steric hinderances or electrostatic interactions.

306 A comparison of VIN capture and elution performance with hIgG in PBS is shown in Figure 6d-e
307 for magnetic separation using VIN-MP and sedimentation separation using uncoupled VIN over a
308 range of hIgG loading densities. The VIN-MP hIgG elution recovery normalized by mass of VIN
309 is approximately 35-55% of that of the uncoupled VIN.

310 Sedimentation and magnetic separation-based operations were further compared in purification of
311 plant-expressed monoclonal antibody (mAb) A20 from crude *N. benthamiana* plant extract (Figure
312 7). Non-reducing condition SDS-PAGE results indicate that fully assembled mAb A20 is produced
313 and recovered by VIN in elution. The relative extents of hIgG elution recovery for uncoupled VIN
314 and VIN-MP are consistent with the hIgG in PBS results.



316 **Figure 7. Capture and elution of plant-expressed monoclonal antibody (mAb) A20 by**
317 **sedimentation with uncoupled plant virus-based immunosorbent nanoparticle (VIN) and**
318 **magnetic separation with VIN-coupled magnetic particle (VIN-MP).** (a) Reducing and, (b)
319 non-reducing SDS-PAGE results of the non-bound supernatant and elution recovery of plant-
320 expressed mAb A20 for VIN-MP with 5% glutaraldehyde coupling (VIN-MP-NG), 0.5 mg/mL 1-
321 Ethyl-3-(3-dimethylaminopropyl)carbodiimide coupling (VIN-MP-NE), and uncoupled VIN in
322 free suspension. Gels are marked with band heights corresponding to mAb A20 heavy chain (HC)

323 and light chain (LC) constituents (reduced) or to dimerized mAb A20 (non-reduced). (c) Elution
324 recovery of plant-expressed mAb A20 for VIN-MP-NG, VIN-MP-NE, and uncoupled VIN in free
325 suspension. Error bars represent a single standard deviation of technical triplicate measurements.

326

327 **3. Discussion**

328 **3.1 Biotic purification technologies**

329 Virus-based nanomaterials present promising characteristics as an alternative technological
330 platform to traditional chemical methods of biopharmaceutical purification in their inexpensive
331 and scalable production coupled with their high replication fidelity, biophysical properties,
332 stability, and accessible modifications leading to wide-ranging functionality. There are safety and
333 regulations concerns of commercializing self-replicating technology, but this barrier has been
334 addressed by researchers by removing the requisite replication machinery, as is done to generate
335 virus-like particle technology (Marsian and Lomonosoff, 2016; Zeltins, 2013), using a plant virus
336 to avoid human infection (Balke and Zeltins, 2019), designing the virus-based nanomaterial to
337 rapidly shed the transgenic gene inserts (Torti *et al.*, 2021), and/or inactivating the virus (Koudelka
338 *et al.*, 2015). As these methodologies are well established, we do not address virus nanoparticle
339 containment strategies within the scope of VIN process development.

340 A range of biotic technologies beyond virus-based nanomaterials have been developed and studied
341 for biopharmaceutical purification (Dias and Roque, 2016; Mahmoodi *et al.*, 2019). These can be
342 classified by utility as fusion tags (e.g., inteins (Belfort *et al.*, 1999), carbohydrate binding modules
343 (Shoseyov *et al.*, 2006)), thermo-responsive biopolymers (e.g., elastin-like polypeptides (Sheth,
344 Bhut, *et al.*, 2014)), and hydrophobic nanoparticles (e.g., polyhydroxyalkanoates (Banki *et al.*,
345 2005), oleosins (Bhatla *et al.*, 2010), hydrophobins (Jugler *et al.*, 2020)). Fusion tags have by and
346 large been the most widely adopted biotic purification technology for the accessibility they present
347 to early-stage research labs. However, they are limited as a platform technology by the influence
348 of product-specific characteristics, complications of tag cleavage, and generally unfavorable
349 commercial-scale economics (Fc-fusion tags being a notable exception to most of these
350 limitations) (Bell *et al.*, 2013). There has been some adoption and maturation of the other biotic
351 technologies that overcome these limitations, with an observed emphasis on elastin-like
352 polypeptides (ELPs) (Sheth, Bhut, *et al.*, 2014; Sheth, Jin, *et al.*, 2014) and oleosins (McLean *et al.*,
353 2012). VINs represent another contender within this group of technology, albeit at a more
354 nascent stage of development. Advantages of VIN technology include the simplicity of production
355 (ELP: culture-based system; VIN: plant-based system) and within that the projected high yield per
356 hectare (oleosin: < 1 kg/hectare; VIN: 200+ kg per hectare) (Werner *et al.*, 2006) that position
357 VINs as inexpensive purification reagents.

358 Mechanical transmission-based production of VINs, as we have demonstrated, could be considered
359 for economical manufacturing for its enhanced simplicity over agrobacterium-based methods and
360 its reliability and stability over transcript-based methods. A main barrier to this strategy is the
361 variability and escape of the VIN functionality over the course of multiple virion replication and
362 plant passage cycles. One strategy to alleviate these concerns would be to embed selective

363 pressures into the processing procedure, although this would introduce yet unsolved barriers within
364 quality assurance and quality control that would hinder commercialization. Studies have shown
365 the use of selective pressures during production can cause viruses to sacrifice reproductive fitness
366 for selected characteristics (e.g., thermal and structural stability) (Dessau *et al.*, 2012) and that
367 genetic stability of virus-based nanomaterials can be achieved (Le Nouën *et al.*, 2017).

368

369 **3.2 Affinity sedimentation processing**

370 These technologies have been applied in a diverse range of processing strategies including liquid
371 chromatography, inverse transition cycling, aqueous two-phase partitioning, and affinity
372 precipitation. The uncoupled VIN application methodology presented here is based on what we
373 are terming as pseudo-secondary effect affinity sedimentation, in which the affinity interaction and
374 sedimentation mechanisms are partially coupled with a dependence of the sedimentation on
375 affinity interaction (i.e., VIN-target protein complex characteristics influence sedimentation
376 velocity). We derive this terminology from affinity precipitation processing which has
377 distinguished methodologies as either primary effect (coupled affinity/precipitation) or secondary
378 effect (independent affinity/precipitation) (Hilbrig and Freitag, 2003).

379 We performed initial work to identify centrifugation conditions as a function of target protein
380 characteristics and loading (e.g., antibody versus Fc-fusion protein), but it may be valuable in
381 future works to develop a model to understand this relationship more deeply between the VIN-
382 target protein complex morphology and sedimentation velocity. It was qualitatively observed that
383 Fc-fusion protein recovery was lower than that of hIgG regardless of centrifugation conditions.
384 We hypothesize that lower binding affinities and differing biophysical characteristics of the VIN-
385 Fc-fusion protein complex are contributing to these observed differences. However, future work
386 is required to elucidate these underlying mechanisms.

387 Affinity sedimentation shares several characteristics with affinity precipitation, which provides
388 potential benefits of low cost and buffer usage (Hilbrig and Freitag, 2003), ability to achieve high
389 concentration factors (Low *et al.*, 2007), high throughput (Shukla and Thömmes, 2010), and
390 minimal concerns of fouling at the expense of higher recovery and selectivity generally achieved
391 by a chromatographic counterpart (Mondal *et al.*, 2006), which can consist of as much as 50% of
392 the total pharmaceutical manufacturing costs (Kelley, 2009). Affinity sedimentation and
393 precipitation methods also exhibit generally higher tolerance to variation in feed streams, as we
394 have shown with VINs through processing of crude plant extract, making them well-suited to
395 early-stage downstream processing.

396 A semi-quantitative comparison of hIgG binding capacity between the VINs prepared at two levels
397 of purity (data not shown) indicates that there may be a minor reduction in binding capacity
398 between these conditions, likely associated with non-specific blocking by various expected plant
399 host impurities including proteins, salts, polysaccharides, and phenolics (Dixon *et al.*, 2018).
400 However, there was no discernable impact of the solution type (crude extract or purified solution)
401 on reusability of the VINs for an additional cycle of capture and elution.

402 While protein solids, such as those formed in precipitation and sedimentation, have been shown to
403 be stable in long term storage (Harrison *et al.*, 2015), here we show that sedimentation impacts
404 VIN structural integrity and presumably contributes to the unstable performance over multiple
405 reuse cycles. From these results, one may infer the importance of fully intact VIN on sedimentation
406 characteristics and thus centrifugal recovery. The mechanism of particle breakage is suspected to
407 be mechanically induced from during resuspension and not a direct result of the protein pellet
408 formation from sedimentation. The mechanical properties of viruses have been studied extensively
409 using computational and physical methods (Buzón *et al.*, 2020; Mateu, 2012). TMV, in the same
410 genus as the TVCV used for the VIN in this study, has been attributed a Young's modulus of $6 \pm$
411 3 GPa (Schmatulla *et al.*, 2007), although mixed reports suggest the value could be lower (Falvo
412 *et al.*, 1997). Furthermore, there are reports on icosahedral virions that demonstrate minor changes
413 in coat protein composition resulting in significant modulation of mechanical properties (Medrano
414 *et al.*, 2019).

415 Thus, we hypothesize that the presumably stiff TVCV rod-like particle basis combined with
416 increased drag by the loose affinity ligand display sheath (using the largest genetically inserted
417 virion coat protein presentation to date) surrounding the VIN enhances its vulnerability to applied
418 shear stress during pellet resuspension via repeated pipette tip aspiration. It may be that a smaller
419 affinity ligand presentation, such as an affibody (Frejd and Kim, 2017) or synthetic peptide (Lund
420 *et al.*, 2012), would decrease particle breakage (but also necessitate more aggressive centrifugation
421 conditions with the smaller virion size). Gentler resuspension methods with lower shear would
422 also be worth investigating to decrease breakage. Similar shear sensitivity in pipette-based
423 resuspension has been shown for larger biomolecule systems such as with cell-based pelleting,
424 wherein higher pellet compaction and tip velocities were shown to result in cell losses (Delahaye
425 *et al.*, 2015). Pellets formed during VIN processing and use were highly compacted and required
426 considerable pipetting for complete resuspension, suggesting that pipette-based resuspension
427 could have also played a role of particle degradation in this system. Gentler resuspension
428 techniques should be explored in the future to improve particle integrity during operation.

429 In this study, we investigated stability of the VINs over long term storage, multiple freeze-thaw
430 cycles, and at elevated temperatures, primarily focusing on coat protein fusion primary structure.
431 Additional stability concerns include impact to protein secondary structure, virion particle
432 structure, and nucleic acid integrity. Exposure to multiple freeze-thaw cycles has been shown to
433 degrade virion nucleic acid and infectivity (Krajden *et al.*, 1999). Thermostability was confirmed
434 at the level of secondary protein structure via performance check of bind-and-elute functionality,
435 which led to the integration of a high heat hold into the VIN purification scheme.

436

437 **3.3 VIN process development**

438 The process development investigation presented here provides insights on the differences
439 between wild-type plant virions and protein display plant virions, which is relevant technology for
440 a host of biomedical applications. The improved process can serve as a roadmap for future virus-
441 based nanomaterial purification. We observed that the protein presentation confers additional

442 processing sensitivities to the virion (which is otherwise described as a glassy surface), likely due
443 to the interactions between the presented ligand and *N. benthamiana* plant host cell impurities,
444 noticeable in the heat hold of crude solution and the inclusion of protease inhibitors to extraction.

445 We observed that the two effective unit procedure modifications, low pH extraction and heat hold
446 post-PEG precipitation, possess low orthogonality in impurity clearance mechanisms for the
447 starting stream used although there is still discernable benefit in combining the methods as
448 observed by the improvement in SDS-PAGE band purity.

449 The process development in this work focused on addition and removal of unit procedures at a
450 high-level to inform process design. There is value in future research performing parameter
451 optimization with an emphasis on maximizing recovery and purity with a fixed purification
452 scheme.

453

454 **3.4 Magnetic separation**

455 The VIN-MP results presented in this study, representing the first virus-based nanomaterial system
456 coupled with MPs for protein purification, reflect a greater than 25x increase in binding capacity
457 compared to current industry standards for affinity protein capture with magnetic particles –
458 PierceTM Protein A Magnetic Beads ($\geq 40 \mu\text{g}$ rabbit IgG/mg MP) (ThermoFisher Scientific),
459 SureBeadsTM Protein A Magnetic Beads ($\geq 6 \mu\text{g}$ IgG/mg MP) (Bio-Rad Laboratories), VIN-MP
460 ($> 1,000 \mu\text{g}$ hIgG/mg MP).

461 These exciting results provide stark evidence for the sensitivity-enhancing properties of virus-
462 based nanomaterials and their usefulness as ligand scaffolding in biotechnological applications.

463 Furthermore, the VIN-MP system served to decouple the affinity and separation mechanisms of
464 processing, as compared to the partially coupled behavior in VIN sedimentation operation, thereby
465 increasing the process robustness to changes in the sample solution, including the diversity and
466 concentration of the target protein. Additional work is required to experimentally assess this
467 capability in a larger set of processing conditions. Investigation of the reusability of VIN-MP and
468 for magnetic separation and particle integrity over operation is also of importance for future
469 testing. Preliminary results suggest there may be a minor presence of VIN in the eluate. Two
470 possible means of explaining this observation are proteolytic cleavage along a covalently bonded
471 FcAL resulting in detachment of the VIN from MP or minor particle breakage from resuspension
472 of the VIN-MP after magnetic separation resulting in the presence of VIN fragments.

473 The uncoupled VIN sedimentation operation demonstrated 2-3 times higher capture capacity per
474 VIN mass than the VIN-MP system. The uncoupled VIN operation also resulted in hIgG recoveries
475 as high as 95% of the feed, whereas VIN-MP operation was maximal at 42% recovery of the feed
476 hIgG. It will be important to identify the cause for the lower recovery in future development by
477 additional screening of lower hIgG concentrations and optimization of the capture and elution
478 methodology.

479 Higher capture capacity may be particularly advantageous for large-scale protein purification – an
480 area for which affinity precipitation (Swartz *et al.*, 2018) and magnetic separation (Schwaminger
481 *et al.*, 2019) are receiving growing interest. However, given the nature of VINs as inexpensive and
482 simply produced reagents, the value of maximizing Fc-protein binding per VIN in a small-scale
483 commercial application (as is the current niche of magnetic particle purification) is most likely
484 weighted less than factors such as Fc-protein recovery, process duration, labor time, amenability
485 to automation, and equipment costs.

486 For perspective on these other factors, consider that our recently published study on evaluating the
487 costs of the affinity capture step of mAb purification (McNulty *et al.*, 2021) yielded results that
488 the unit costs of magnetic separation (modeled using an industry standard technology with a
489 comparable capture and elution protocol) were lower than uncoupled VIN sedimentation in
490 process duration (73% reduction), labor time (30% reduction), and equipment mass (71%
491 reduction) when processing a single lab-scale sample (2 mL volume tube). These results support
492 the favorable position of VIN-MP in comparison to uncoupled VIN sedimentation for lab-scale
493 applications.

494

495 **3.5 Summary and future directions**

496 Virus-based nanomaterials provide a highly diverse and tunable technology that can be adapted to
497 overcome the limitations of the application methodology. For example, the length of a rod-like
498 plant virus such as the one used in this study, TVCV, is proportional to the length of the viral
499 genomic information and, as such, the length can be modulated through the addition or subtraction
500 of genomic information (e.g., addition of non-functional genomic information can be used to
501 increase virion particle length) (Saunders and Lomonosoff, 2017). Increasing VIN length in this
502 manner is one approach to investigate for increasing the binding site occupation in the VIN-MP
503 system. Other techniques useful for VIN performance optimization include density modulation of
504 the protein display (Cruz *et al.*, 1996) and a multi-ligand protein display (Werner *et al.*, 2006).
505 Last not least, use of affinity ligands other than Protein A domains, in particular, affibodies evolved
506 from Protein A/Z domains (Nord *et al.*, 1997), should expand the usability of the technology
507 beyond monoclonal antibody binding/capture (Ståhl *et al.*, 2017).

508 In this study, we have presented the development of a virus-based nanomaterial to serve as a
509 protein purification reagent, characterized performance using a pseudo-secondary effect affinity
510 sedimentation bind-and-elute protocol, expanded functionality to Fc-fusion proteins, identified
511 limitations of the technology operated in that procedure, and developed a magnetic particle
512 coupled system for magnetic separation to improve processing. This provides further evidence
513 supporting virus-based nanomaterials as simple and inexpensive reagents for protein purification
514 and suggests a path forward for technological development.

515

516 **4. Experimental procedures**

517 **4.1 Gene constructs**

518 The viral expression vector used in this study is based on previously reported TVCV-based
519 vectors(Werner *et al.*, 2006). The viral expression vector used here (pICH25892; plasmid kindly
520 provided by Nomad Biosciences GmbH) is an assembly of the previously reported 5' provector
521 containing the TVCV coat protein (minus the stop codon) fused to a C-terminal glycine-rich
522 flexible linker (pICH20701) and the 3' provector containing the D and E antibody-binding
523 domains from *S. aureus* protein A with short flanking sequences (amino acids 29 – 161; GenBank
524 accession no. J01786) (pICH21767).

525

526 **4.2 Production of VIN**

527 VINs were primarily produced via whole plant agroinfiltration using *A. tumefaciens* containing
528 viral expression vector pICH25892 according to a previously reported method with minor
529 modifications (Xiong *et al.*, 2018). A final cell density of OD₆₀₀ = 0.2 was used for agroinfiltration.
530 Post-infiltration plants were cultivated at 60% relative humidity with a 16-hour photoperiod, 23
531 °C/20 °C temperature regime, and a photosynthetic photon flux density of 425 μmol/(m²·s) derived
532 from a combination of high-pressure sodium, high-pressure metal halide, and incandescent lights
533 for a duration of 6-12 days post-inoculation.

534 VINs were also produced via direct mechanical transmission of intact VINs. A total volume of 300
535 μL of purified VIN solution (~0.1 mg/mL) was applied per plant in aliquots of 100 μL for each of
536 three middling leaves. An abrasive powder (Celite) was lightly sprinkled on each leaf and each
537 leaf was gently rubbed by hand. The surfaces of the leaves were rinsed with water at 20 minutes
538 post-inoculation to remove excess inoculation reagents.

539

540 **4.3 Purification of VIN**

541 VIN-expressing *N. benthamiana* leaf tissue was stored at -80 °C after harvest and processed with
542 minor modifications to a previously reported protocol (Werner *et al.*, 2006). A single round of
543 PEG-assisted precipitation step was performed rather than two. Extraction was performed using
544 either a blender (NutriBullet; NutriBullet, LLC, Pacoima, CA) or liquid nitrogen-assisted mortar
545 and pestle with 0.1 M potassium phosphate pH 7.0 extraction buffer at a 3:1 buffer volume to
546 biomass weight extraction ratio. In the case of the mortar and pestle method, the homogenized leaf
547 powder was mixed with the buffer and nutated for 30 minutes at 4 °C for extraction.

548

549 **4.4 Binding and elution of Fc-proteins**

550 Binding and elution of Fc-proteins was performed according to a previously reported protocol
551 (Werner *et al.*, 2006). Four different target Fc-proteins were used in this study: hIgG (Sigma-
552 Aldrich, St. Louis, MO), plant-expressed rCMG2-Fc (Xiong *et al.*, 2019), plant-expressed rPTH-
553 Fc (unpublished data), and using the magnICON[®] system (Gritch *et al.*, 2006), plant-expressed
554 mAb A20 (subclass IgG1) (Bendandi *et al.*, 2010; Whaley *et al.*, 2012). Development of target
555 protein-specific modifications to the method are detailed in results.

556

557 **4.5 Coupling VIN with magnetic particles**

558 VIN-MP were generated by covalent attachment of VIN to primary amine-terminated
559 superparamagnetic iron oxide particles (Product No. I7643, Sigma-Aldrich, St. Louis, MO, USA),
560 VIN-MP-N, or carboxyl-terminated superparamagnetic iron oxide particles (Product No. I7518,
561 Sigma-Aldrich, St. Louis, MO, USA), VIN-MP-C, both of approximately 1 μm size, was
562 performed according to the methods detailed in the product data sheets using ~ 2 mL total reaction
563 volumes. VIN stock solutions at ~ 3 -6 mg/mL concentration in 10 mM potassium phosphate buffer
564 pH 7.0 were used in coupling. Coupling efficiency was measured using A280 values for amine-
565 terminated particles and Bradford assay soluble protein values for carboxyl-terminated particles.

566

567 **4.6 Binding and elution of Fc-proteins with VIN-magnetic particles**

568 A VIN-MP solution was prepared by resuspending 2.5 mg of VIN-MP in 0.5 ml of 0.1 M sodium
569 phosphate buffer pH 8.0 binding buffer. Further, the particles were magnetically separated; the
570 supernatant was aspirated and discarded (repeated three times).

571 Crude protein extracts from *N. benthamiana* leaves (leaf juice press extraction followed by
572 microfiltration with filter paper) in binding buffer were spiked with various amounts of hIgG. A
573 volume of 100 μL hIgG-containing crude extract was added to the VIN-MP solution. The mixture
574 was briefly vortexed and then incubated nutating at 4 $^{\circ}\text{C}$ for 30 minutes. The incubated solution
575 was then magnetically separated and washed three times with binding buffer. The binding buffer
576 was removed after wash and 50 μL of 0.2 M glycine buffer pH 2.5 elution buffer was added. The
577 solution was briefly vortexed to resuspend magnetic particles and further incubated nutating at 4
578 $^{\circ}\text{C}$ for 5 min. Particles were again magnetically separated and the supernatant was collected as the
579 eluate. The eluate was then pH neutralized with 13 μL of 1.5 M Tris-HCl buffer pH 8.8. The elution
580 and neutralization steps were repeated three times and pooled together.

581

582 **4.7 Protein analysis**

583 Protein concentration was measured using Bradford and Pierce Modified Lowry assays.

584 Sample protein compositions were analyzed by SDS-PAGE and Western blot. SDS-PAGE
585 samples were loaded using constant volume (30 μL). Western blot analysis was performed using
586 a primary antibody of rabbit anti-protein A (1:25,000 dilution) (Sigma-Aldrich, St. Louis, MO)
587 and a secondary antibody of goat anti-rabbit IgG-HRP (1:3,000 dilution) (Southern Biotech,
588 Birmingham, AL) for detection of VIN CP-FcAL. A secondary antibody of goat anti-human IgG-
589 HRP (1:2,500 dilution) was used to detect human IgG, rCMG2-Fc, and rPTH-Fc.

590 Dot blots were performed using 5 μL liquid samples and 0.45 μm nitrocellulose membrane. The
591 positive control consisted of 100 – 500 ng recombinant Protein A (ThermoFisher Scientific, Santa
592 Clara, CA). The negative control consisted of ~ 2 μg wt-TMV from purified *N. benthamiana*
593 solution. VIN samples consisted of ~ 100 μg of VIN from purified *N. benthamiana* solution based
594 on total soluble protein assay results. Several secondary antibody conditions were used: rat anti-

595 mouse IgG-HRP (1:1,000 dilution) (ThermoFisher Scientific), rabbit anti-goat IgG-HRP (1:3,000
596 dilution) (Invitrogen, Carlsbad, CA), and goat anti-human IgG-HRP (1:3,000 dilution).

597

598 **4.8 Electron microscopy**

599 Carbon film on 300 mesh copper discs (Ted Pella, Redding, CA, USA) were prepared for increased
600 hydrophilicity by glow discharge at 30 mA for 30 seconds on a glass slide. 5 μ L liquid VIN
601 solution samples were loaded onto the prepared disc, incubated 30 seconds, and then blotted with
602 filter paper. Negative stain was applied in five sequential rounds of 5 μ L uranyl sulfate loading,
603 30 second incubation, and filter paper blotting. TEM was performed using a JEM-1230
604 transmission electron microscope (JEOL, Peabody, MA, USA).

605 The lengths of VIN particles imaged by TEM were manually measured using straight line analysis
606 with ImageJ (National Institutes of Health, Bethesda, MD, USA). Statistically significant
607 differences in mean particle lengths of different VIN solutions were determined by equal variance
608 two sample t-test ($\alpha = 0.05$). The equal variance assumption was evaluated by two sample F-test
609 ($\alpha = 0.05$).

610

611 **5. Author contributions**

612 MJM, AS, AG, YG, KAM designed and executed the experiments. All authors were involved in
613 analysis and interpretation of data. MJM wrote the initial manuscript draft. KAM edited the
614 manuscript draft. AG, YG, SN, KAM supervised the project.

615

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627

628 **7. Conflict of interest**

629 The authors declare no conflict of interest.

630

631 **8. Short legends for Supporting Information**

- 632
633 **Figure S1.** Agrobacterium tumefaciens T-DNA vector constructs
634 **Table S1.** Primers used for verifying vector construct DNA sequence
635 **Figure S2.** Gel electrophoresis results of PCR-based sequence verification
636 **Figure S3.** Amino acid analysis coverage
637 **Figure S4.** Dot blot of immunosorbence for various antibodies
638 **Figure S5.** Capture and elution of antibodies with mechanical transmission-generated particles
639 **Figure S6.** Capture and elution using high sedimentation rate
640 **Figure S7.** Freeze-thaw cycle and long-term stability
641 **Figure S8.** Process development observations
642 **Figure S9.** Thermostability assessment results
643 **Figure S10.** Performance verification after process development
644

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852 **10. Tables**

853 No tables to present in this study.