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1 **Engineered nickel bioaccumulation in *Escherichia coli* by NikABCDE** 2 **transporter and metallothionein overexpression**

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14 **ABSTRACT**

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17 Mine wastewater often contains dissolved metals at concentrations too low to be economically
18 extracted by existing technologies, yet too high for environmental discharge. The most common treatment
19 is chemical precipitation of the dissolved metals using limestone and subsequent disposal of the sludge in
20 tailing impoundments. While it is a cost-effective solution to meet regulatory standards, it represents a lost
21 opportunity. In this study, we engineered *Escherichia coli* to overexpress its native NikABCDE transporter
22 and a heterologous metallothionein to capture nickel at concentrations in local effluent streams. We found
23 the engineered strain had a 7-fold improvement in the bioaccumulation performance for nickel compared
24 to controls, but also observed a drastic decrease in cell viability due to metabolic burden or inducer (IPTG)
25 toxicity. Growth kinetic analysis revealed the IPTG concentrations used based on past studies lead to
26 growth inhibition, thus delineating future avenues for optimization of the engineered strain and its growth
27 conditions to perform in more complex environments.

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29 **Keywords:** industrial biotechnology, wastewater sampling, genetic engineering, metal recovery, ABC
30 transporter

31 **INTRODUCTION**

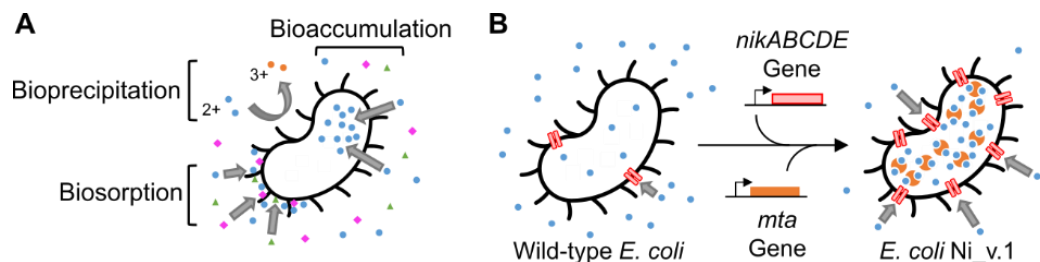
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34 Biomining, the use of biotechnology for mining applications has been gaining new traction with pilot-
35 scale and commercial-scale demonstrations of microbial cultures performing bioleaching processes to aid
36 in the recovery of lithium and other metals from low-grade ores and mine waste (1). One form of mine
37 waste are liquid effluents bearing dissolved metals too low in concentration (\leq low ppm) to be economically
38 extracted with traditional practices, but in excess of regulatory standards prohibiting environmental
39 discharge without some form of treatment. Chemical precipitation of metals by sulfide or hydroxide
40 addition is the primary form of treatment, yet it generates secondary sludge waste that must be disposed of
41 in tailing impoundments. Biomining includes processes like biosorption (*i.e.*, the adsorption of dissolved
42 metals to the surface of cells) and bioprecipitation (*i.e.*, altering the redox state of dissolved metals to
43 decrease their solubility in water), which have been extensively reported in the literature as alternatives
44 (Fig. 1A). While some researchers have focused on leveraging microbes' natural capabilities for biomining,
45 others have explored the expansion the microbes' capabilities through the latest advances in synthetic
46 biology (2–4).

47 Synthetic biology is a growing discipline that seeks to design microorganisms and biomolecular
48 systems by combining decades of life sciences research with design principles and tools from math, physics,
49 and engineering. Biosorption and bioprecipitation have benefited from advances in synthetic biology. For
50 example, the surface of microbes have been designed to bear lanthanide-binding peptides to enhance their

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51 ability to adsorb dissolved rare earth elements (5). Other microbes have been designed to produce H₂S to
52 precipitate dissolved metals as nanoparticles (6). While these advances are promising, biosorption processes
53 need to overcome selectivity issues since the surface of the cell directly interfaces with the aqueous
54 environment and is therefore more susceptible to a molecular form of fouling. Bioprecipitation processes
55 produce metal products with redox states that are insoluble in water. An increasingly important objective
56 in the field, beyond bioremediation, is to recover the metals in a market-ready form. This means one would
57 need to reverse the redox change to re-integrate the metal into existing purification processes, which would
58 pose additional operation costs. A desirable bioprocess that can compete with existing technologies must
59 therefore possess robust selectivity for specific dissolved metals while being able to smoothly integrate
60 with existing hydrometallurgical processes.

61 We thus focused our attention on bioaccumulation. Microbes can naturally bioaccumulate metals
62 selectively through highly specific protein transport systems evolved to capture metals from metal-scarce
63 environments like the human gut (7). We previously reviewed studies where microorganisms were
64 genetically engineered to express heterologous transporters and metal-binding “storage” proteins for the
65 purpose of enhancing the hosts’ abilities to bioaccumulate metal in the cytosol and noted the absence of
66 studies that used ABC transporters for the purpose of metal removal from liquid effluents (11).
67 Bioaccumulation is a unique strategy to develop a bioprocess. While it is generally slower than biosorption,
68 the cell membrane acts as a selectivity barrier, and the presence of transporters allow specific metals to
69 enter the cytosol without the need for a change in the redox state. A critical system is the ATP-binding
70 cassette (ABC) transporter, a class of active transporters that convert the chemical energy from nucleotide
71 triphosphate (NTP) hydrolysis into mechanical energy that drives the movement of chemicals and ions
72 across the lipid membrane (8–10). ABC transporters are comprised of two components: the solute binding
73 protein (SBP) found in the periplasm or the extracellular space via lipid tether to the membrane, and the
74 transmembrane permease complex bearing additional cytosolic NTP-binding domains. Taken together, we
75 briefly proposed in our review the potential for ABC transporters to be an advantageous design choice to
76 enhance a cell’s bioaccumulation performance, defined as the $\text{mg}_{\text{metal}}/\text{g}_{\text{dry cell weight}}$ (or $\text{mg}_x/\text{g}_{\text{dcw}}$ where ‘x’
77 denotes the metal).



78

79 Figure 1. **Ni_v.1 design.** (A) Important cell-metal ion interactions for metal removal bioprocesses. Different colours
80 shapes represent different metals. Biosorption involves metals adhering to moieties on the surface of the cell.
81 Bioprecipitation involves a metal redox change to an insoluble form driven by extracellular and membrane-bound
82 enzymes. Bioaccumulation involves the specific import of metals into the cytosol. (B) Genetic engineering design to
83 enhance *Escherichia coli*'s bioaccumulation performance for importing (*nikABCDE*) and storing (*mta*) dissolved
84 nickel (blue circles).

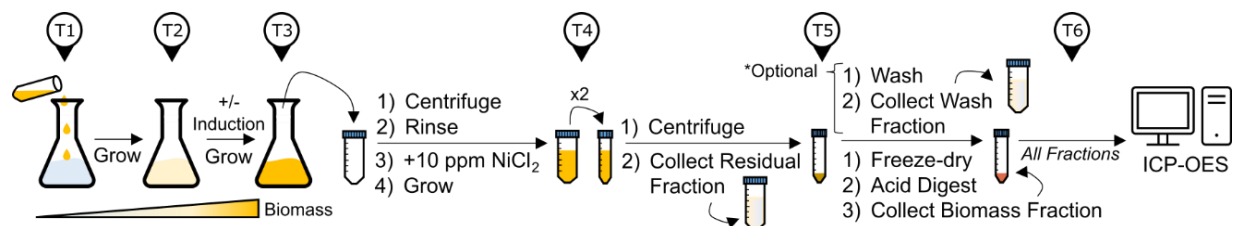
85 Conducting design-build-test-learn (DBTL) cycles is a common engineering practice within synthetic
86 biology to iteratively improve strain performance towards an objective. In this study, we focused on
87 initializing the first DBTL cycle and began by taking inspiration from early work by Deng *et al.* (2003,
88 2005) to design Ni_v.1, an *Escherichia coli* strain with enhanced bioaccumulation performance for nickel
89 using a nickel-specific ABC transporter complemented with a protein-based storage system as described in
90 Fig.1B (12, 13). Specifically, we built the strain by cloning the open-reading frame of *nikABCDE* from *E.*
91 *coli* BL21(DE3) genomic DNA, and *mta* synthesized commercially into the T7-controlled dual expression
92 vector pCDF-Duet, then transformed this plasmid into an *E. coli* BL21(DE3) to heterologously overexpress

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93 the transport-storage system. NikABCDE is an experimentally validated nickel-specific transporter (14),
94 and its periplasmic NikA is especially well-characterized (15–18). MTA is a cysteine-rich metallothionein
95 from *Pisum sativum* previously used successfully for enhancing bioaccumulation of nickel, cobalt, and
96 mercury (11).

97 To guide our testing, we sampled real Canadian liquid mine effluent from the Sudbury, Ontario
98 community and performed a simple compositional analysis to determine the future working constraints (*i.e.*,
99 metal concentrations, salinity, and pH) that Ni_v.1 would need to perform under. Since this was the first
100 DBTL cycle, we benchmarked Ni_v.1's performance in unbuffered 10 ppm NiCl₂ solution (matching the
101 concentration found in the Copper Cliff sample) to understand its performance in simplified ideal conditions
102 (Fig. 2). An initial test of Ni_v.1 compared to its control strains revealed it had the highest bioaccumulation
103 performance for nickel that was comparable to previously reported values in the literature. Finally, we
104 found that induction conditions could be further optimized by reducing the IPTG concentration in favour
105 of better growth kinetics. Based on these findings, we proposed future avenues of research in subsequent
106 DBTL cycles for improving Ni_v.1's bioaccumulation performance for nickel.

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108

109 Figure 2. **Shake flask workflow to assay for bioaccumulation performance.** Timepoints denoted above (T1, T2,
110 *etc.*) to indicate chronological order of steps. The culture begins at T1 inoculation and is grown until protein expression
111 is ready to be induced at T2. After the induction period, at T3 the cell biomass is isolated by centrifugation and
112 resuspended in the nickel solution for the cells to bioaccumulate the nickel. The optical density (O.D.) of the culture
113 can be measured at T1 → T3. At T4, the cells are collected again by centrifugation and the supernatant is collected as
114 the Residual Fraction. At T5, the nickel-loaded cell pellet can be washed to collect a Wash Fraction that enables the
115 differentiation of the nickel biosorbed to the surface of the cell from the nickel bioaccumulate inside the cytosol. The
116 cells are collected by centrifugation to obtain the Biomass Fraction and freeze-dried to obtain the dry cell weight. The
117 dried cell pellets are acid digested overnight and analyzed by ICP-OES at T6.

118 RESULTS AND DISCUSSION

119

120 Test 0: Estimating Ni_v.1 working conditions based on aqueous streams from a mine

121 Sudbury is home to the century-old Vale Copper Cliff site, one of the world's largest active integrated
122 mining complexes. The site includes grinding and milling stations, smelters, refineries, and – critical to this
123 study – tailings deposition sites for both solid and liquid waste. To maintain their water balance, liquid
124 effluents are treated by lime addition to precipitate the metals and neutralize the aqueous stream prior to
125 environmental discharge. Interestingly, these aqueous streams run through several Sudbury communities
126 as part of the Junction Creek Watershed. We sought to ground the testing of Ni_v.1 in real-world
127 constraints, so we identified two water sampling sites of interest: Nolin Creek (N.C.) in the northern part
128 of Sudbury, and a Copper Cliff stream (C.C.) in the southern part (Fig. S1 for aerial view). N.C. was located
129 ~2.3 km from its origin in the Vale Copper Cliff mine and was downstream of a lime treatment plant (Fig.
130 3A). C.C. was located ~1 km from its origin in the same mine, but was not treated yet since it was upstream
131 of a lime treatment plant (Fig. 3C), thus explaining the acid mine drainage characteristics (*e.g.*, reddish-
132 orange iron precipitate and low pH).

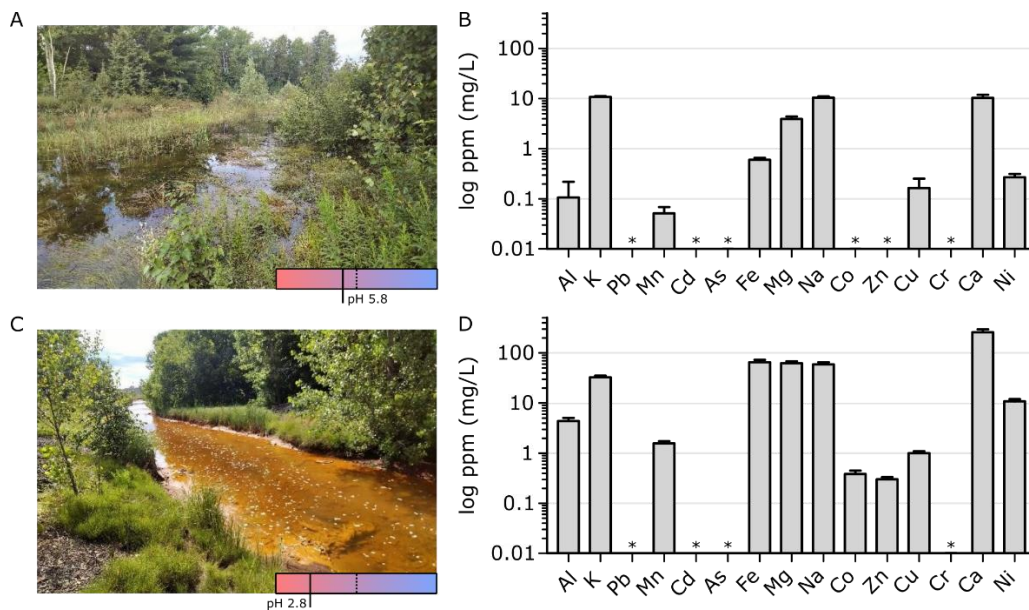
133 We obtained three samples at each of the two sites and analyzed their composition (Fig. 3). The C.C.
134 samples (pH 2.84) were significantly more acidic than the N.C. samples (pH 5.83), thus leading to
135 considerably distinct chemical conditions affecting the solubility of the metals (Table S1, Fig. 3B,D).
136 Several metals (Al, Mn, Fe, Mg, Na, and Ca) were all at least one order of magnitude more concentrated in
137 C.C. samples than N.C. samples (Fig. S2 for side-by-side comparison). Toxic metal ions (As, Pb, Cd, and

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138 Cr) were below the limit of detection at both sites, as were Co and Zn at N.C. Our element of interest nickel
139 was 10.805 ± 1.118 ppm in the C.C. sample, which was a 40-fold higher than N.C. samples. Both sites were
140 predominantly sulfate systems (>99%) with trace amounts of phosphates and no detectable chlorides, which
141 reflected the sulfidic mineral geology native to Copper Cliff. The total positive charge concentrations in the
142 samples from N.C. and C.C. were to 1.63 mM and 27.26 mM of e^- , respectively. For the negative charge
143 concentrations, the calculated values were 1.77 mM and 27.79 mM of e^- . The small errors (2% and 8% for
144 C.C. and N.C., respectively) in these charge balances indicate that most of the ions in the samples had been
145 captured in this analysis.

146 Our goal in this first DBTL cycle was to confirm if Ni_v.1 had appreciable bioaccumulation
147 performance for nickel compared to similarly engineered strains reported in literature. We previously found
148 acidic or high salinity environments could reduce the nickel-binding affinity of a *EcNikA* homologue called
149 *CcSBPII* from *Clostridium carboxidivorans*. Phosphate buffer, compared to more inert buffers like HEPES
150 and MOPS, also reduced *CcSBPII*'s nickel-binding affinity (19). Given the concentration of nickel in the
151 C.C. samples and the above considerations, we prepared 10 ppm NiCl₂ solutions to benchmark Ni_v.1's
152 bioaccumulation performance for nickel. We intentionally i) avoided adding salt (Na, K, Mg, Ca), ii) chose
153 NiCl₂ for a chloride anion system rather than phosphate or sulfate salts that would introduce polyatomic
154 anions (PO₄³⁻, SO₄²⁻), iii) did not buffer the pH as that would require the addition of millimolar levels of
155 buffering compounds that would not be found in nature, and iv) only included nickel in the simulated
156 effluent since we were not studying bioaccumulation selectivity.

157



158

159 **Figure 3. Metal analysis of aqueous streams originating from Vale Copper Cliff.** (A) Westward view of sampling
160 site at Nolin Creek (N.C.) and (B) its metal composition (n=3). Dotted line indicates pH 7 in the bottom right pH
161 indicator box. (C) Eastward view of an aqueous stream flowing from a Copper Cliff tailings dam (C.C.) and (D) its
162 metal composition (n=3). Asterisk (*) denotes measurements below the limit of detection. Metal measurements made
163 using ICP-OES.

164 **Test 1: Benchmarking Ni_v.1 bioaccumulation performance for nickel**

165 The workflow outlined in Fig.2 to measure bioaccumulation performance is laborious, so we
166 performed flask experiments to determine whether Ni_v.1 would function as we expected before testing its
167 reproducibility (Fig. S4). In the absence and presence of IPTG at 0.4 mM based on prior studies (12, 13),
168 we compared the performance of Ni_v.1 with control strains that either had the MTA storage system
169 (“MTA”), the NikABCDE transport system (NikABCDE), or neither system (*i.e.*, “Vector Only”). Our
170 observations suggested Ni_v.1 was indeed functional based on its bioaccumulation performance of 7.51

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171 $\text{mg}_{\text{Ni}}/\text{g}_{\text{dcw}}$ in the presence of IPTG, which was 9.9-fold higher than its absence. In contrast, induction of the
172 Vector Only strain did not lead to a notable change in the bioaccumulation performance, from 0.83 to 1.02
173 $\text{mg}_{\text{Ni}}/\text{g}_{\text{dcw}}$, which we expected. While the addition of IPTG also did not change the MTA control's strains
174 performance (from 0.31 to 0.20 $\text{mg}_{\text{Ni}}/\text{g}_{\text{dcw}}$), it did increase the NikABCDE control's performance by 3-fold
175 from 1.08 to 3.31 $\text{mg}_{\text{Ni}}/\text{g}_{\text{dcw}}$. The 2.3-fold improvement in performance between the induced NikABCDE
176 control and induced Ni_v.1 reflects the importance of having a storage system in the cytosol to sequester
177 the accumulated metal and minimize loss through efflux pumps or cell lysis. Additionally, the 38-fold
178 improvement between the induced MTA control and induced Ni_v.1 reflects the inability of our strain to
179 use its native transport systems with the heterologous storage system to bioaccumulate nickel. Overall,
180 Ni_v.1's performance in this preliminary test is comparable to other engineered strains reported in the
181 literature (*cf.* Test 2).

182 Throughout the workflow, we noticed that induced Ni_v.1 had less biomass at timepoint 3 (T3) than
183 the non-induced Ni_v.1 control and the other controls. At T5, the appearance of the Biomass fraction for
184 induced Ni_v.1 was also different from the other controls (Fig. S3). Instead of solid beige pellet, induced
185 Ni_v.1 had a smaller, darker beige-black pellet with an amorphous pink layer of unknown material on top.
186 We hypothesized the change in appearance was due to cell lysis resulting from a burden imposed by 10
187 ppm nickel or 0.4 mM IPTG. Next, we tested the reproducibility of Ni_v.1's bioaccumulation performance
188 using the Vector Only strain as the control and, considering these growth issues, we monitored the optical
189 density (O.D.) of the cultures from T1 to T3.

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191 **Test 2: Ni_v.1's bioaccumulation performance and the associated burden is reproducible**

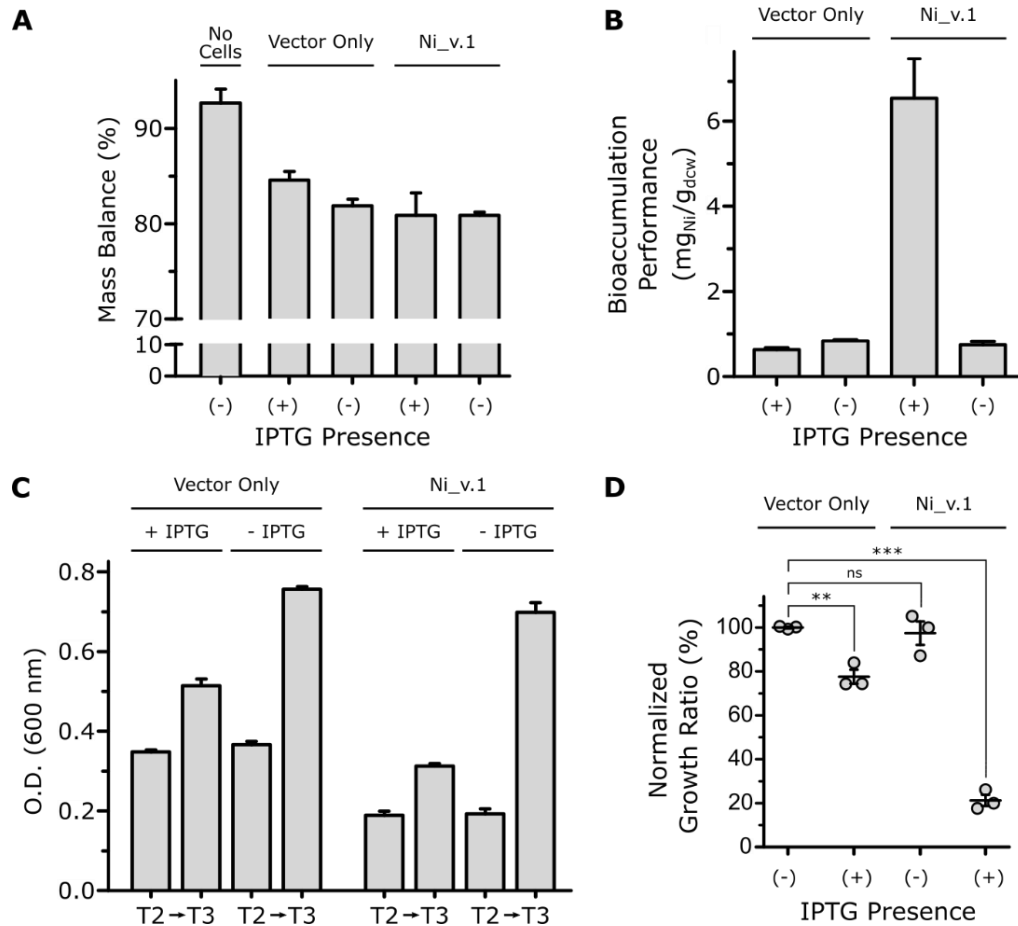
192 We repeated the workflow for the Vector Only control and Ni_v.1 in the presence and absence of 0.4
193 mM IPTG ($n=3$, each). We also included an additional triplicate labelled "No Cells" where no inoculums
194 were added at T1, but the samples were processed exactly the same as the test group. This was to check the
195 sterility of nutrient media and to assess the nickel mass balance. No growth was observed in the No Cells
196 control between T1-T3. The No Cell control experienced a $7.3 \pm 2.1\%$ loss of nickel, which we expected
197 since there were several transferring and vortexing steps where solution adhering to pipettes and lids was
198 not be collected (Fig. 4A). The test group experienced a $17.4 \pm 1.7\%$ loss of nickel, likely because any lost
199 solution would also contain nickel-loaded cells (either biosorbed to the surface or bioaccumulated into the
200 cell) and thus amplify the losses. Nonetheless, the test group had relatively consistent losses of nickel
201 between the samples, which enabled reliable cross-comparisons of their bioaccumulation performance.

202 The results of this test (Fig. 4B) were similar to observations in Fig.S4. Induced Ni_v.1 achieved a
203 performance of $6.53 \pm 1.47 \text{ mg}_{\text{Ni}}/\text{g}_{\text{dcw}}$, which was significantly higher (8.7-fold) than its non-induced control
204 at $0.75 \pm 0.11 \text{ mg}_{\text{Ni}}/\text{g}_{\text{dcw}}$ (unpaired two-tail t-test, $p = 0.0051$, $t = 5.561$). The induced and non-induced
205 Vector Only control displayed no significant change: $0.63 \pm 0.07 \text{ mg}_{\text{Ni}}/\text{g}_{\text{dcw}}$ and $0.92 \pm 0.33 \text{ mg}_{\text{Ni}}/\text{g}_{\text{dcw}}$,
206 respectively (unpaired two-tail t-test, $p = 0.3009$, $t = 1.187$). Compared to other enhanced nickel
207 bioaccumulation strains reported in literature, and factoring in their starting concentration of nickel, Ni_v.1
208 has the second best performance (11). However, the best strain reported by Krishnaswamy & Wilson (2000)
209 used a protocol that deployed a 10 mM phosphate buffer double-wash, compared to our more stringent 10
210 mM EDTA wash, which may have lead to an overestimation of their best strain's performance (20).
211 Nonetheless, standardization of protocols to measure bioaccumulation performance are needed since the
212 contributions of biosorption can lead to overestimations of a bioaccumulation metric. The similarity of
213 Ni_v.1's performance to strains already reported in literature after one DBTL cycle demonstrates promising
214 future iterations. We noted that Ni_v.1 was able to concentrate the nickel 175-fold with the potential to
215 achieve >1000-fold concentration if the dried cell pellet was acid digested in <1 mL as opposed to the 5
216 mL that was used in this test.

217 The total nickel extraction by the cell from solution (Fig. S5), accounting for nickel in both the wash
218 and biomass fractions, was approximately the same between the induced samples ($60.9 \pm 1.6\%$) and
219 between the non-induced samples ($46.6 \pm 3.6\%$). However, when normalized to the mass of the dried cell
220 weight (g_{dcw}), induced Ni_v.1 had 6- to 9-fold higher nickel extraction from solution by bioaccumulation
221 than the other controls. Together, these metrics indicated Ni_v.1 had the highest bioaccumulation

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222 performance, and the best removal of nickel from the 10 ppm NiCl₂ solution specifically due to the
 223 bioaccumulation mechanism. However, Ni_v.1 again had weaker growth.



224

225 **Figure 4. Ni_v.1 bioaccumulation performance and growth analysis.** (A) Determination of mass balance across all
 226 fractions (*i.e.*, residual, wash, and biomass) compared to a control with no cells initially added to the flasks intended
 227 for bioaccumulation cultures (n=3). (B) The bioaccumulation performance of wild-type *E. coli* compared to *E. coli*
 228 Ni_v.1 (n=3). (C) Comparison of growth rate between wild-type *E. coli* and Ni_v.1 before and after the timepoint
 229 where one half of the cultures for each strain are induced by the addition of IPTG (n=3). (D) Negative synergistic
 230 effect of IPTG induction and exposure to Ni²⁺ on Ni_v.1 (n=3).

231 By following the growth kinetics of this test group, we quantified our prior observations in Test 1
 232 (Table S2). Before resuspension in 10 ppm NiCl₂ (Fig. 4C), we found the Ni_v.1 samples' O.D. values at
 233 T2 were roughly half of the Vector Only controls' O.D. values (0.19 ± 0.09 and 0.36 ± 0.17, respectively).
 234 We attributed this inhibition to the burden imposed by the difference in the plasmid sizes since Ni_v.1
 235 carries a larger 8.8 kbp plasmid for the production of the NikABCDE and MTA compared to the empty 3.8
 236 kbp plasmid of the Vector Only control (21). From T2, we found the O.D. of the non-induced Vector Only
 237 controls and Ni_v.1 samples at T3 had increased approximately 207% (from O.D. 0.36 ± 0.01 to 0.76 ±
 238 0.01) and 362% (from O.D. 0.19 ± 0.02 to 0.70 ± 0.03), respectively, which allowed Ni_v.1 to “catch-up”
 239 despite the initial lag at T2. In contrast, the induced groups only increased approximately 148% (from O.D.
 240 0.35 ± 0.01 to 0.51 ± 0.02) and 165% (from O.D. 0.19 ± 0.01 to 0.31 ± 0.01), respectively, meaning the
 241 amount of induced Ni_v.1 biomass going into resuspension with 10 ppm NiCl₂ for bioaccumulation was
 242 ~60% less than least inhibited strain condition (non-induced Vector Only control). We attributed this
 243 difference to the inhibitory effect of IPTG on cell viability (22). Additionally, this may reflect the fact that
 244 MTA is a metallothionein comprised of a large number of cysteine residues. Cysteines are the second most

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245 expensive amino acids to produce in *E. coli* based on the number of ATP molecules consumed to produce
246 one molecule of it (23).

247 While the induced Vector Only controls and non-induced Ni_v.1 samples had a $14.3 \pm 7.9\%$ and 7.7
248 $\pm 1.7\%$ reduction in their NGR, respectively, induced Ni_v.1 unexpectedly experienced a $45 \pm 15.6\%$ NGR
249 reduction (Fig. 4D). Additionally, Ni_v.1 reproduced the same cell pellet appearance at the end of T5 as
250 Fig.S3 in Test 1. We interpreted this difference as a consequence of burden-induced sensitization of the
251 Ni_v.1's cell membrane. Specifically, the T7-controlled overexpression of NikABCDE likely overwhelmed
252 membrane protein biogenesis, disrupted homeostasis of the membrane's fatty acid composition, and
253 deteriorated the membrane integrity by physically over-occupying the membrane "real estate" (24–26).
254 Studies have also showed that bacterial membranes and *E. coli* cells treated with EDTA led to significant
255 outer membranes deformations (27, 28). Taken together, the behavior of Ni_v.1's growth kinetics pointed
256 to a need for the IPTG concentration to be re-calibrated for improved cell viability.

257 We confirmed IPTG, and not the nickel solution, imposed the larger burden based on growth curves
258 of the Vector Only control and Ni_v.1 samples in the presence of only 10 ppm NiCl₂, 0.4 mM IPTG, or
259 both (Fig. S6). We observed the non-induced Vector Only controls and Ni_v.1 samples in the absence of
260 nickel or IPTG had the fastest growth rates (Fig. S6A,B). The addition of 10 ppm NiCl₂ did not lead to a
261 significant change in growth rates. However, 0.4 mM IPTG delayed both the Vector Only control and
262 Ni_v.1 samples' exponential phase by ~8-9 hrs. Ni_v.1 was slightly more delayed than the Vector Only
263 control in the presence of nickel (Fig. S6C), but were both equally delayed in the presence of IPTG (Fig.
264 S6D). Next, we tested the effect of different IPTG concentrations on the growth rates and protein expression
265 levels to refine the workflow (Fig.2) for better Ni_v.1 viability.

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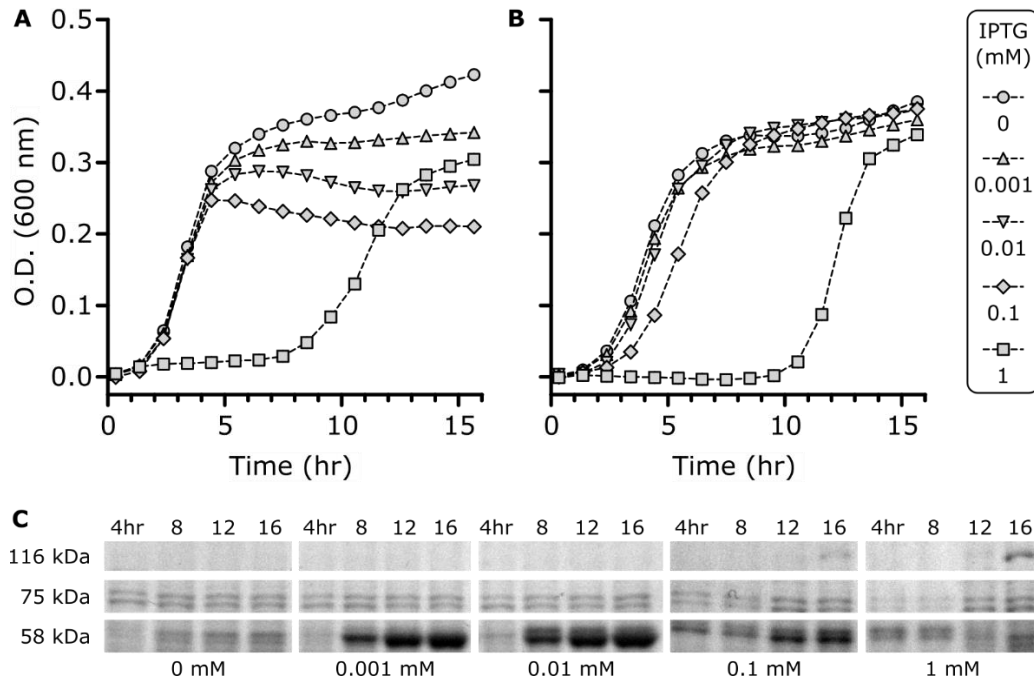
267 **Test 3: Determining minimum IPTG concentrations required to induce Nika expression in Ni_v.1**

268 Due to IPTG's inhibitory effect on the Vector Only control and Ni_v.1 samples' growth rates, we
269 assessed the protein expression levels of the transport and storage system at various IPTG concentrations
270 to determine its minimum order of magnitude required to achieve expression without major losses in cell
271 viability. We obtained their growth curves at 0, 0.001, 0.01, 0.1, and 1 mM IPTG over a 16-hr period, and
272 obtained 1 mL samples of the cultures every 4 hrs to assess the protein expression by SDS-PAGE analysis.
273 We specifically tracked Nika (~58 kDa) as a proxy for the expression of the transport and storage system.
274 The ORF of *nikABCDE* was amplified for cloning using primers complementary to the NikA start codon
275 (front) and the Nike stop codon (end), meaning *nikABCDE*'s native RBS for Nika was not kept when the
276 full ORF was cloned into pCDF-Duet. Consequently, the NikA ORF in pCDF-Duet used the vector's
277 stronger RBS (based on the RBS calculator), and therefore had visibly higher expression than the NikBCDE
278 permease complex (29). To compare samples at different IPTG concentrations and different timepoints
279 more easily, we normalized the amount of protein loaded into each well to ensure the intensity of the
280 positive control bands at ~75 kDa were as consistent as possible on the SDS gel. In earlier purification work
281 (unpublished), we found that Nika and its homologues would dimerize if they were re-solubilized from
282 insoluble pellet fractions due to sub-optimal expression conditions, or if they were exposed to harsh
283 conditions (*e.g.*, high urea or guanidine concentrations). We therefore monitored bands at 116 kDa as well
284 to assess Nika dimerization.

285 At 0 mM IPTG, Vector Only controls and Ni_v.1 samples predictably had the highest growth rates
286 (Fig. 5A,B). Vector Only control growth rates were affected at 1 mM IPTG, whereas Ni_v.1 growth rates
287 were slightly delayed by 0.1 mM IPTG and largely delayed by 1 mM IPTG. In the SDS-PAGE analysis of
288 the Ni_v.1 cell lysates, the intensities of the bands at 75 kDa were consistent across the IPTG concentrations
289 and timepoints, except for the 4hr and 8hr timepoints for 1 mM IPTG that should be interpreted more
290 judiciously (Fig. 5C). At 0 mM IPTG, we observed no noticeable overexpression of Nika across the 16-hr
291 period. Strong Nika overexpression appeared at 0.001 mM and 0.01 mM IPTG, with no dimerization
292 observed at 116 kDa. Combined with the growth rate data, this suggests that a two-order magnitude of
293 decrease in the original 0.4 mM IPTG concentration used in Test 1 and 2 may have been enough to express
294 Ni_v.1's transport and storage system without major losses in the cell viability. At 0.1 mM IPTG, Nika
295 expression appears earlier at the 4hr timepoint compared to the lower IPTG concentrations, however at the

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296 16hr timepoint NikA expression was weaker and its dimerization stronger. Given the Ni_v.1 growth rate
297 (Fig. 5B) was reduced at 0.1 mM IPTG, the NikA dimerization likely reflected the increased burden. At 1
298 mM IPTG, NikA dimerization was more apparent with weaker NikA expression. Taken together, the IPTG
299 concentrations used in previous studies was too high for Ni_v.1. Low micromolar levels of IPTG were
300 sufficient for expression of NikA, and presumably the expression of the transport and storage systems.



301
302 Figure 5. **Ni_v.1 viability and protein expression as a function of IPTG concentration.** (A) Growth curves of
303 Vector Only controls and (B) Ni_v.1 samples (n=3, each). Every third datapoint was plotted to reduce clutter. Dotted
304 lines are based on all data points. (C) SDS-PAGE analysis of Ni_v.1 cell lysates to monitor NikA expression. Samples
305 are normalized based on their O.D. at each timepoint to ensure intensities of 75 kDa bands are consistent across
306 samples in the SDS gel.

307 Conclusion

308 In this study, we engineered an *E. coli* strain to have enhanced bioaccumulation performance for
309 nickel. We first characterized aqueous streams originating from the Vale Copper Cliff site in Sudbury,
310 Ontario to determine real-world constraints that Ni_v.1 would need to operate under. Then, through a series
311 of tests, we demonstrated Ni_v.1 could remove nickel from a 10 ppm NiCl₂ solution (matching the
312 concentration found at the C.C. site) and achieved a bioaccumulation performance of 6.53 ± 1.47 mg_{Ni}/g_{dew},
313 which was comparable to values published in the literature. In an analysis of the Vector Only control and
314 Ni_v.1 samples' growth kinetics, we found IPTG was likely causing burden-induced membrane
315 sensitization in Ni_v.1 cells, and therefore increased cell lysis throughout the workflow outlined in Fig.2.
316 Using a gradient of IPTG concentrations between 0-1 mM IPTG, we found low micromolar levels of IPTG
317 were sufficient for expression of the transport and storage system needed to perform the nickel
318 bioaccumulation task, despite previous studies using 0.4 - 1 mM IPTG.

319 In immediately subsequent DBTL cycles, Ni_v.1's bioaccumulation performance for nickel in more
320 complex solutions matching the working constraints of the N.C. and C.C. sites by first isolating for the
321 effects of pH, salinity, and interfering metals such as Fe^{2+/3+}, Co²⁺, and Cu²⁺ is needed. More rigorous
322 experiments based on factorial designs should be used to systematically understand Ni_v.1's performance
323 in multi-parameter scenarios, which constitutes a novel approach to characterizing engineered strains in
324 this field. Critically, the workflow outlined in Fig.2 needs to be miniaturized to facilitate more rapid DBTL
325 cycles. Test 2 required 15 cultures that took a single person 12 consecutive hours to grow and fractionate,

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326 with an additional two day to process. In other work, we developed protocols on the Tecan Freedom Evo
327 100 to grow and analyze cell cultures in microplates that could be deployed in this work to automate T1→T3
328 and simplify the fractionation steps of T3→T6 (30).

329 In future DBTL cycles, additional objectives could focus on improving the growth kinetics. For
330 example, plasmid burden could be alleviated by genomic integration of the NikABCDE transporter and
331 MTA storage system. Further, functional stability could be improved by controlling a genome-integrated
332 transport and storage system with a strong endogenous promoter to eliminate the need for inducing agents
333 and reduce the metabolic burden associated with T7-based expression. Another objective could be to
334 develop a new genetic system that enables the cell to export the nickel once it has reached a “saturation
335 threshold” such that the cell can be re-used for multiple metal recovery cycles, thus improving its
336 economics. Finally, this was the first demonstration of a nickel-specific ABC transporters heterologously
337 expressed for the purpose of removing nickel from solution. Protein engineering efforts could be undertaken
338 to explore the possibility of altering NikA’s metal specificity – and therefore the strain’s specificity – for
339 other metals with strategic value (*e.g.*, precious metals and rare earth elements) towards stronger supply
340 chains for advanced clean technologies and circular economies.

341 MATERIALS AND METHODS

342 Aqueous stream sample collection and compositional analysis

343 The sampling sites were at Nolin Creek (46°28'21.9"N 81°03'53.9"W; 46.472759, -81.064958) and a
344 Copper Cliff site (46°28'21.9"N 81°03'53.9"W; 46.472759, -81.064958) in Sudbury, Ontario, Canada.
345 Eight 16 oz Nalgene bottles were acid washed in a 10% hydrochloric acid solution, rinsed with deionized
346 water, dried, and weighed. Before taking samples from the two sites, litmus paper was used to determine
347 the pH of the locations. The bottles were filled with water samples on July 28th, 2021, where one of each
348 set was acidified with 25 drops of trace metal grade nitric acid for ICP analysis. Samples were packed in a
349 cooler, with freezer packs, and shipped to University of Toronto on the same day. The water samples
350 collected were stored in a walk-in fridge at 4 °C. To prepare for the elemental analysis, the samples were
351 vacuum filtered (50µm pore size) to remove solid sediments, and then diluted (5 folds) in 5% HNO₃ to
352 stabilize the content. The sample pH values were measured before and after the vacuum filtration, which
353 remained largely constant. Common cation elements (Al, K, Pb, Mn, Cd, Fe, Mg, Na, Co, Zn, Cu, Cr, Ca,
354 and Ni) (Inorganic Ventures, #IV-28) and suspected anion elements (S, P, and As) (Inorganic Ventures,
355 #CGS1; High-Purity Standards, #100039-1; Inorganic Ventures, #IV-28) were measured via ICP-OES. A
356 chloride probe was used to determine the Cl⁻ concentration. Because the water samples were collected at
357 the ground level and have been exposed to atmosphere extensively, it is assumed that all Fe exists as ferric
358 ion, and all S exists as sulfate ion in the valency calculations and subsequent charge balances.

359

360 Plasmid preparation and cloning workflow

361 The open-reading frame of the *nikABCDE* gene was amplified from genomic DNA belonging to
362 *Escherichia coli* BL21(DE3) using the KAPA-HiFi Master Mix kit according to the manufacturer’s
363 instructions (Kapa Biosystems, #KK2601). Primers are found in Supplementary Table 3. The forward
364 primer (#0) included the NcoI cut site, and the reverse primer (#1) included the HindIII cut site. These cut
365 sites were chosen to remove the 6x-HisTag and the majority of the other cut sites. The open-reading frame
366 of the *mta* gene was synthesized through Twist Biosciences (San Francisco, United States) and amplified
367 in the same fashion. Specifically, MTA’s forward primer (#2) included an NdeI cut site and the reverse
368 primer (#3) a PacI cut site for the same reasons as primers #1 & 2. All restriction enzymes were obtained
369 from New England Biolabs. Amplified products were gel-extracted and cleaned using a column prep kit
370 (ThermoFisher, # K0701). Restriction digest procedures followed the manufacture protocol. The dual
371 expression vector pCDF-Duet (Novagen: 71340) was linearized using the appropriate restriction enzyme
372 pair for NikABCDE or MTA, gel-extracted, and cleaned using the column prep kit. T4 DNA ligase (NEB,
373 # M0202) was used to ligate NikABCDE or MTA into the appropriate linearized pCDF-Duet vector, then
374 transformed into in-house calcium-competent *E. coli* strains DH5α and LOBSTR-BL21(DE3) (Kerafast,

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375 #EC1002). NikABCDE was cloned into the first site, and MTA into the second site. To create the full
376 transport-storage system (Ni_v.1), MTA was cloned into the second site of the vector already containing
377 NikABCDE in the first site. The completed plasmids were miniprep (ThermoFisher, #K0502) and
378 sequence verified at ACGT Corp (Toronto, Canada) using primers #4-7. Glycerol stocks were stored at -
379 80°C. Links for the final constructs are found in Supplementary Table 4.

380

381 **Shake flask-based determination of bioaccumulation performance with ICP-OES**

382 Starter cultures of *E.coli* Ni_v.1 were grown overnight in 10 mL of sterile Luria-Bertani media
383 (BioShop: LBL407.1) containing 100 µg/mL of streptomycin for 16 hr at 37 °C with shaking (200 rpm).
384 Bioaccumulation cultures were prepared by inoculating 100 mL of sterile Luria-Bertani media containing
385 100 µg/mL streptomycin with a 1% v/v inoculum of the starter culture and growing for 3 hrs at 37 °C with
386 shaking. Isopropyl β-d-1-thiogalactopyranoside (IPTG) was added to a final concentration of 0.4 mM to
387 induce the expression of the NikABCDE and MTA proteins. Bioaccumulation cultures were grown for
388 another 3 hrs at 37 °C with shaking, then centrifuged (5000 rpm, 10 min, 25 °C) into conical vials (50 mL).
389 The supernatant (*i.e.*, spent media) was discarded and the cell pellet was re-suspended in 10 mM HEPES
390 pH 7.2 to rinse the media. The cells were centrifuged again and the supernatant (*i.e.*, HEPES buffer) was
391 discarded. The cells were then resuspended in 26.4 mL of 10 ppm NiCl₂ prepared in MilliQ water and
392 allowed to bioaccumulate Ni²⁺ for 3 hrs at 37 °C with shaking. Afterwards, the mixtures were individually
393 transferred into smaller conical vials (15 mL) and centrifuged to collect the biomass. This was repeated for
394 the remaining mixture. The supernatants (residual fraction) were collected in new 50 mL conical vials and
395 stored at 4 °C. If a washing step was completed, the cells were then re-suspended in 5 mL 10 mM EDTA,
396 then centrifuged again where the supernatant (wash fraction) was stored at 4 °C in new vials. Whether a
397 wash step was completed or not, the smaller conical vials were pre-weighed to determine their mass of the
398 pellet. Finally, the cell pellet (washed or not washed) was freeze-dried for 24 hr, then re-suspended in 5 mL
399 70% HNO₃ (FisherScientific: A509P500) for a 24 hr acid digestion period (biomass fraction). Fractions
400 (*i.e.*, residual, wash, and biomass) were analyzed by inductively coupled plasma optical emission
401 spectrometry (ICP-OES, Agilent Dual View 720) using a Ni²⁺ calibration curve with 0, 1, 5, 10, and 20
402 ppm standards.

403

404 **Microplate-based determination of cellular growth rates**

405 Growth curves were obtained by tracking the optical density of cells as they grew in 24-well
406 microplates using the Infinite® M200 (Tecan) plate reader. All sample were grown at 37 °C with shaking
407 (orbital, 2mm) for 16 hrs with 20-min interval reads. To prepare each well for inoculation, sterile room
408 temperature LB was first pre-mixed with streptomycin to 100 µg/mL. IPTG (0.4 mM for Test 2 [Fig. S4],
409 0→1 mM for Test 3 [Fig. 6]) and NiCl₂ (10 ppm for Test 2 [Fig. S4]) were added as needed to achieve
410 conditions necessary for experiments. 1000 µL of the mixtures were aliquoted into each well. 5 µL of
411 overnight culture (grown to saturation) were inoculated into the wells as prescribed by the experiment
412 design.

413

414 **SDS-PAGE analysis of Ni_v.1 cell lysates and NikA overexpression**

415 In parallel with cells grown in microplates to obtain their growth curves (Fig. 6), 10 mL LB cultures
416 (pre-mixed with the necessary components as described above) of the same cells were grown in glass test
417 tubes. 1 mL aliquots were taken from cultures every 4 hrs for a 16hr period. The optical densities for each
418 set of aliquots at each time point were measured in cuvettes, then centrifuged to collect the cell pellet
419 (supernatant discarded). Cell pellets were frozen at -20 °C until all pellets were collected after the full 16hr
420 period. For a fair comparison of NikA expression (~58 kDa) across the different IPTG concentrations and
421 timepoints, we normalized the dilution of the cell pellets in BugBuster lysis buffer (Millipore Sigma,
422 #70584) such that the approximate concentration of cells was the same as the 1 mM IPTG induced Ni_v.1
423 sample. We then created mixtures comprised of 20 µL cells + 5 µL of 6X SDS dye, boiled the mixtures for
424 10 min, and loaded 15 µL of the mixtures into wells.

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433 ABBREVIATIONS

- 434 • ABC: ATP-binding cassette (transporter)
- 435 • SBP: solute-binding protein
- 436 • IPTG: isopropyl β -D-1-thiogalactopyranoside
- 437 • NTP: nucleotide triphosphate
- 438 • ICP-OES: inductively coupled plasma optical emission spectrometry
- 439 • LB: Luria-Bertani (nutrient media)
- 440 • kDa: kilodaltons
- 441 • O.D.: optical density
- 442 • NGR: normalized growth ratio

443 REFERENCES

- 444
- 445 1. Sedlakova-Kadukova J, Marcincakova R, Luptakova A, Vojtko M, Fujda M, Pristas P. 2020.
- 446 Comparison of three different bioleaching systems for Li recovery from lepidolite. *Sci Rep* 10:14594.
- 447 2. Giachino A, Focarelli F, Marles-Wright J, Waldron KJ. 2021. Synthetic biology approaches to copper
- 448 remediation: bioleaching, accumulation and recycling. *FEMS Microbiol Ecol* 97:fiaa249.
- 449 3. Capeness MJ, Horsfall LE. 2020. Synthetic biology approaches towards the recycling of metals from
- 450 the environment. *Biochem Soc Trans* 48:1367–1378.
- 451 4. Carter L, Mankad A, Hobman EV, Weynberg KD, Kaksonen AH, Cooper C. Three synthetic biology
- 452 applications and their paths to impact in Australia: Cane toads, bacteriophages, and biomining
- 453 microbes. *Biotechnol J* n/a:2200009.
- 454 5. Urbina J, Patil A, Fujishima K, Paulino-Lima IG, Saltikov C, Rothschild LJ. 2019. A new approach
- 455 to biomining: Bioengineering surfaces for metal recovery from aqueous solutions. *Sci Rep* 9:16422.
- 456 6. Sun GL, Reynolds EE, Belcher AM. 2020. Using yeast to sustainably remediate and extract heavy
- 457 metals from waste waters. *Nat Sustain* <https://doi.org/10.1038/s41893-020-0478-9>.
- 458 7. Zeer-Wanklyn CJ, Zamble DB. 2017. Microbial nickel: cellular uptake and delivery to enzyme
- 459 centers. *Curr Opin Chem Biol* 37:80–88.
- 460 8. Locher KP. 2016. Mechanistic diversity in ATP-binding cassette (ABC) transporters. *Nat Struct Mol*
- 461 *Biol* 23:487–493.
- 462 9. Beek J ter, Guskov A, Slotboom DJ. 2014. Structural diversity of ABC transporters. *J Gen Physiol*
- 463 <https://doi.org/10.1085/jgp.201411164>.
- 464 10. Shilton BH. 2015. Active transporters as enzymes: an energetic framework applied to major
- 465 facilitator superfamily and ABC importer systems. *Biochem J* <https://doi.org/10.1042/BJ20140675>.
- 466 11. Diep P, Mahadevan R, Yakunin AF. 2018. Heavy metal removal by bioaccumulation using
- 467 genetically engineered microorganisms. *Front Bioeng Biotechnol* 6.
- 468 12. Deng X, Li QB, Lu YH, Sun DH, Huang YL, Chen XR. 2003. Bioaccumulation of nickel from
- 469 aqueous solutions by genetically engineered *Escherichia coli*. *Water Res* 37:2505–2511.
- 470 13. Deng X, Li QB, Lu YH, He N, Jiang J. 2005. Genetic engineering of *E. coli* SE5000 and its potential
- 471 for Ni²⁺ bioremediation. *Process Biochem* 40:425–430.

08-23-2022

- 472 14. Rowe JL, Starnes GL, Chivers PT. 2005. Complex Transcriptional Control Links NikABCDE-
473 Dependent Nickel Transport with Hydrogenase Expression in *Escherichia coli*. *J Bacteriol* 187:6317-
474 6323.
- 475 15. Navarro C, Wu L-F, Mandrand-Berthelot M-A. 1993. The nik operon of *Escherichia coli* encodes a
476 periplasmic binding-protein-dependent transport system for nickel. *Mol Microbiol* 9:1181-1191.
- 477 16. Heddle J, Scott DJ, Unzai S, Park S-Y, Tame JRH. 2003. Crystal Structures of the Liganded and
478 Unliganded Nickel-binding Protein NikA from *Escherichia coli**. *J Biol Chem* 278:50322-50329.
- 479 17. Cherrier MV, Girgenti E, Amara P, Iannello M, Marchi-Delapierre C, Fontecilla-Camps JC, Ménage
480 S, Cavazza C. 2012. The structure of the periplasmic nickel-binding protein NikA provides insights
481 for artificial metalloenzyme design. *JBIC J Biol Inorg Chem* 17:817-829.
- 482 18. Lebrette H, Iannello M, Fontecilla-Camps JC, Cavazza C. 2013. The binding mode of Ni-(L-His)₂ in
483 NikA revealed by X-ray crystallography. *J Inorg Biochem* 121:16-18.
- 484 19. Diep P, Mahadevan R, Yakunin AF. 2020. A microplate screen to estimate metal-binding affinities of
485 metalloproteins. *Anal Biochem* 609:113836.
- 486 20. Krishnaswamy R, Wilson DB. 2000. Construction and Characterization of an *Escherichia coli* Strain
487 Genetically Engineered for Ni(II) Bioaccumulation. *Appl Environ Microbiol* 66:5383-5386.
- 488 21. Diaz Ricci JC, Hernández ME. 2000. Plasmid effects on *Escherichia coli* metabolism. *Crit Rev*
489 *Biotechnol* 20:79-108.
- 490 22. Dvorak P, Chrast L, Nikel PI, Fedr R, Soucek K, Sedlackova M, Chaloupkova R, Lorenzo V de,
491 Prokop Z, Damborsky J. 2015. Exacerbation of substrate toxicity by IPTG in *Escherichia coli*
492 BL21(DE3) carrying a synthetic metabolic pathway. *Microb Cell Factories* 14:201.
- 493 23. Kaleta C, Schäuble S, Rinas U, Schuster S. 2013. Metabolic costs of amino acid and protein
494 production in *Escherichia coli*. *Biotechnol J* <https://doi.org/10.1002/biot.201200267>.
- 495 24. Gubellini F, Verdon G, Karpowich NK, Luff JD, Boël G, Gauthier N, Handelman SK, Ades SE, Hunt
496 JF. 2011. Physiological Response to Membrane Protein Overexpression in *E. coli*. *Mol Cell*
497 *Proteomics MCP* 10:M111.007930.
- 498 25. Wagner S, Baars L, Ytterberg AJ, Klussmeier A, Wagner CS, Nord O, Nygren P-Å, van Wijk KJ, de
499 Gier J-W. 2007. Consequences of Membrane Protein Overexpression in *Escherichia coli**. *Mol Cell*
500 *Proteomics* 6:1527-1550.
- 501 26. Mathieu K, Javed W, Vallet S, Lesterlin C, Candusso M-P, Ding F, Xu XN, Ebel C, Jault J-M, Orelle
502 C. 2019. Functionality of membrane proteins overexpressed and purified from *E. coli* is highly
503 dependent upon the strain. *Sci Rep* 9:2654.
- 504 27. Prachayasittikul V, Isarankura-Na-Ayudhya C, Tantimongcolwat T, Nantasenamat C, Galla H-J.
505 2007. EDTA-induced Membrane Fluidization and Destabilization: Biophysical Studies on Artificial
506 Lipid Membranes. *Acta Biochim Biophys Sin* 39:901-913.
- 507 28. Rojas ER, Billings G, Odermatt PD, Auer GK, Zhu L, Miguel A, Chang F, Weibel DB, Theriot JA,
508 Huang KC. 2018. The outer membrane is an essential load-bearing element in Gram-negative
509 bacteria. *Nature* 559:617-621.
- 510 29. Reis AC, Salis HM. 2020. An Automated Model Test System for Systematic Development and
511 Improvement of Gene Expression Models. *ACS Synth Biol* 9:3145-3156.
- 512 30. Raj K, Venayak N, Diep P, Golla SA, Yakunin AF, Mahadevan R. 2021. Automation assisted
513 anaerobic phenotyping for metabolic engineering. *Microb Cell Factories* 20:184.

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