

1 **Molecular inactivation of exopolysaccharide biosynthesis in *Paenibacillus polymyxa* DSM 365**
2 **for enhanced 2,3-butanediol production**

3

4 Running Title: Metabolic engineering of *Paenibacillus polymyxa*

5

6 Christopher Chukwudi Okonkwo¹, Victor Ujor², and Thaddeus Chukwuemeka Ezeji^{1*}

7

8 1: Department of Animal Sciences, The Ohio State University, and Ohio State Agricultural

9 Research and Development Center (OARDC), 305 Gerlaugh Hall, 1680 Madison Avenue,

10 Wooster, OH 44691, USA

11

12 2: Renewable Energy Program, Agricultural Technical Institute, The Ohio State University, 1328

13 Dover Road, Wooster OH 44691, USA

14

15

16 *To whom correspondence should be addressed: Department of Animal Sciences, The Ohio State

17 University, and Ohio State Agricultural Research and Development Center (OARDC), 305

18 Gerlaugh Hall, 1680 Madison Avenue, Wooster, OH 44691, USA

19 E-mails: Ezeji.1@osu.edu; Phone: 330-263-3796; Fax: 330-263-3949.

20

21

22

23

24

25 **Abstract**

26 Formation of Exopolysaccharides (EPS) during 2,3-butanediol (2,3-BD) fermentation by
27 *Paenibacillus polymyxa* decreases 2,3-BD yield, increases medium viscosity and impacts 2,3-BD
28 downstream processing. Therefore, additional purification steps are required to rid the fermentation
29 broth of EPS prior to 2,3-BD purification, which adds to the production cost. To eliminate EPS
30 production during 2,3-BD fermentation, we explored a metabolic engineering strategy to disable the
31 EPS production pathway of *P. polymyxa*, thereby increasing 2,3-BD yield and productivity. The
32 levansucrase gene which encodes levansucrase, the enzyme responsible for EPS biosynthesis in *P.*
33 *polymyxa*, was successfully disrupted. The resulting *P. polymyxa* levansucrase null mutant showed
34 34% and 54% increases in growth with 6.4- and 2.4-folds decrease in EPS formation in sucrose and
35 glucose cultures, respectively. The observed decrease in EPS formation by the levansucrase null
36 mutant may account for the 27% and 4% increase in 2,3-BD yield, and 4% and 128% increases in
37 2,3-BD productivity when grown on sucrose and glucose media, respectively. Genetic stability of
38 the levansucrase null mutant was further evaluated. Interestingly, the levansucrase null mutant
39 remained genetically stable over fifty generations with no observable decrease in growth and 2,3-
40 BD formation with or without antibiotic supplementations. Collectively, our results show that *P.*
41 *polymyxa* levansucrase null mutant has potential for improving 2,3-BD yield, and ultimately, the
42 economics of large-scale microbial 2,3-BD production.

43

44 **Keywords:** 2,3-butanediol, levansucrase, homologous recombination, exopolysaccharide,
45 polysaccharide polymerase

46

47

48

49 **Introduction**

50 Considering the finite nature of fossil fuels, recurrent instability in oil price and the
51 environmental concerns associated with oil consumption, there is an urgent need to develop
52 sustainable alternatives to fossil fuels and their derivatives. Over the past few decades, significant
53 attention has been devoted to the development of alternative sources of fuels and chemicals. 2,3-
54 Butanediol (2,3-BD) is an industrial platform chemical that is generated via cracking of petroleum-
55 derived hydrocarbons (e.g. butenes). 2,3-BD has wide industrial applications. For instance, 2,3-BD
56 can be used as a feedstock chemical in the production of 1,3-butadiene (1,3-BD), the monomer from
57 which synthetic rubber is produced (1, 2). Also, 2,3-BD can be used as a feedstock for producing
58 methyl ethyl ketone (MEK), a fuel additive which has a higher heat of combustion than ethanol, and
59 as a solvent from which resins and lacquers can be produced (1, 2). Additionally, 2,3-BD has
60 massive potential as a feedstock for the synthesis of a host of numerous pharmaceuticals, cosmetics,
61 paints, and food preservatives (3, 4).

62 Several microorganisms have been shown to possess the metabolic machinery to convert
63 carbohydrates to 2,3-BD. However, 2,3-BD is produced via a mixed acid fermentation pathway
64 where other products such as ethanol, acetoin, lactic, formic and acetic acids in addition to
65 exopolysaccharides (EPS) are co-generated. These co-products compete with 2,3-BD for substrates
66 and pyruvate resulting in decreased 2,3-BD yield (5, 6). Several studies have focused on the
67 manipulation of fermentation medium and conditions as means of reducing the accumulation of
68 competing co-products during 2,3-BD fermentation (7, 8, 9, 10, 11). Although, significant progress
69 has been made, accumulation of competing co-products remains a significant challenge to large-
70 scale production of 2,3-BD. This stems from the fact that considerable levels of co-products are still
71 accumulated in the fermentation broth during 2,3-BD fermentation. Further, genetic manipulation of
72 2,3-BD producers has been explored previously to inactivate lactate dehydrogenase, alcohol

73 dehydrogenase and pyruvate-formate lyase genes - essential genes that encode enzymes involved in
74 the biosynthesis of lactate, ethanol and formic acids, respectively (5, 12, 13, 14). Nevertheless,
75 majority of these studies were conducted with pathogenic 2,3-BD producers which are not ideal for
76 industrial-scale biotechnological applications, as they pose significant health hazards to humans.
77 Thus, we focused on genetic manipulation of *Paenibacillus polymyxa*, a non-pathogenic 2,3-BD
78 producer. *P. polymyxa* was specifically chosen for this study due to its non-pathogenicity and the
79 ability to synthesize levo-2,3-BD, the more desirable 2,3-BD isomer owing to its excellent optical
80 attributes that allow it to be easily dehydrated to 1,3-BD (15, 16). The other 2,3-BD isomers are
81 meso- and dextro-2,3-BD, which are the major fermentation products of the predominantly
82 pathogenic 2,3-BD producers such as *Klebsiella* spp, *Enterobacter aerogenes*, and *Serratia*
83 *marcescens* (1, 2).

84 During 2,3-BD fermentation, *P. polymyxa* synthesizes the exopolysaccharide, levan; a
85 fructose polymer with numerous fructose units in β -(2, 6)-linkages (17). Typically, *P. polymyxa*
86 produces more than 50 g/L EPS during fermentation (9), and this accounts for about 20% of the
87 total consumed carbon. Consequently, EPS biosynthesis reduces 2,3-BD titer and yield by diverting
88 carbon away from 2,3-BD biosynthesis. In addition, EPS formation during 2,3-BD fermentation
89 constitutes a major nuisance by clogging of reactor lines which affects proper mixing of
90 fermentation broth, and most importantly, complicates 2,3-BD downstream processing. Additional
91 purification steps would be required to remove EPS prior to 2,3-BD extraction at industrial-scale,
92 which ultimately adds to the overall cost of production. Collectively, reduction in 2,3-BD yield due
93 to EPS formation and the attendant impact on downstream processing adversely affect the
94 economics of 2,3-BD fermentation. Consequently, it is vital to abolish EPS biosynthesis in *P.*
95 *polymyxa* with a view to re-directing substrate carbons to 2,3-BD biosynthesis for improved titer
96 and yield.

97 Levan is the only known and characterized EPS synthesized by *P. polymyxa*. Levansucrase
98 plays a key role in levan production in *P. polymyxa* by serving as a conduit for the transfer of
99 fructosyl residues to a growing levan chain (18). *P. polymyxa* produces EPS as a means of
100 attachment to plant roots, the natural habitat of this microorganism (19, 20, 21). Comparative
101 analysis of nucleotide and protein sequences of *P. polymyxa* DSM 365 levansucrase relative to other
102 strains of *P. polymyxa* whose genomes have been completely sequenced and annotated was
103 performed to ascertain the number of copies of levansucrase present in *P. polymyxa* DSM 365.
104 Comparisons were conducted due to absence of complete genome information on *P. polymyxa*
105 DSM 365. The results of this study are shown in **Table 1**. *P. polymyxa* DSM 365 possesses a single
106 copy of levansucrase gene with an open reading frame of 1497 bp. Towards eliminating EPS
107 formation during 2,3-BD fermentation, levansucrase gene was targeted for inactivation in *P.*
108 *polymyxa*. Using homologous recombination, we report a pioneer work on the inactivation of
109 levansucrase gene of *P. polymyxa*. The *P. polymyxa* levansucrase null mutant developed in this
110 study was evaluated for growth, 2,3-BD production, substrates consumption, 2,3-BD yield and
111 productivity. Further, stability of the levansucrase null mutant was evaluated.

112

113 **Materials and methods**

114 **Microorganisms and culture conditions**

115 *Paenibacillus polymyxa* DSM 365 used in this study was procured from the German
116 Collection of Microorganisms and Cell Culture, Braunschweig, Germany (DSMZ- Deutsche
117 Sammlung von Mikroorganismen und Zellkulturen). The lyophilized stock was reactivated by
118 inoculating into Luria Bertani (LB) broth, grown overnight (12 h), and then stored as glycerol stock
119 (50 % sterile glycerol) at – 80°C. The microorganisms, vectors and enzymes used in this study are
120 shown in **Table 2**.

121 **Genomic DNA extraction and amplification of levansucrase inactivation constructs**

122 To extract genomic DNA (gDNA), *P. polymyxa* cells were grown in a previously described
123 pre-culture medium (7) to cell OD_{600nm} of 0.7. The cells were harvested by centrifugation at 10,000
124 x g and 4°C for 10 min and then, suspended in Tris-HCl-EDTA (TE) buffer (10 mM Tris-HCl, 1
125 mM EDTA, pH 8.0). Zirconia/Silica beads (0.1 mm, BioSpec Products, Inc., Bartlesville, OK) were
126 added to the cells to a final concentration of 50% (w/v). The cells in the mixture were lysed using a
127 TissueLyzer LT (Qiagen, Hilden, Germany) at 50 oscillations per seconds for 2 min. The cell lysate
128 was centrifuged at 10,000 x g for 10 min and the supernatant was transferred to a clean Eppendorf
129 tube. Phenol-chloroform gDNA extraction method (22) was used to isolate *P. polymyxa* gDNA and
130 then washed with 70% (v/v) ethanol. The gDNA was air-dried at room temperature and re-
131 constituted in 20 µl of nuclease-free water. The gDNA was stored at -20°C until use.

132 PCR primers for levansucrase gene were designed to amplify the entire levansucrase gene of
133 *P. polymyxa* with the incorporation of *XhoI* and *BamHI* restriction sites at the appropriate locations.
134 The design was such that the PCR primers would amplify short sequences (~210 bp) upstream and
135 downstream levansucrase gene designated as LevFragA and LevFragB, respectively. Primers used
136 to generate the constructs and their characteristics are shown in **Table 3**. First, the entire
137 levansucrase gene was amplified from the genomic DNA of *P. polymyxa* DSM 365 using
138 LevFragA_fwd and LevFragB_rev primer pair. Then, LevFragA and LevFragB gene fragments
139 were amplified using Lev-FragA_fwd and LevFragA_rev, and LevFragB_fwd and LevFragB_rev,
140 respectively, using gel-purified levansucrase gene amplicon as template. The erythromycin gene
141 was amplified from the plasmid, pMutin (BGSC, Columbus, OH), with primers (Erm_fwd,
142 Erm_rev1 and Erm_rev2; **Table 3**) designed to incorporate ribosomal binding site, spacer and
143 transcription termination sequences. Erm_fwd and Erm_rev1 were first used to amplify

144 erythromycin gene from pMutin. The PCR product was gel-purified and was re-amplified using
145 Erm_fwd and Erm_rev2 primer pair. The use of Erm_rev2 primer in the second amplification of
146 erythromycin gene ensures complete addition of the entire transcription termination sequence
147 downstream of the erythromycin gene sequence. PCR and gene splicing by overlap extension using
148 PCR or gene SOEing (SOEing-PCR) were carried out in a Bio-Rad iCycler™ Thermal Cycler (Bio-
149 Rad, Hercules, CA) using PrimeStar® GXL DNA polymerase (Clontech-Takara, Mountain View,
150 CA). A 50 µl reaction mix containing 5X PrimeStar® GXL buffer (10 µl), dNTPs (0.25 mM),
151 primers (0.5 µM each), DNA template (~5 ng/ µl) and GXL DNA polymerase (1 µl) was used. The
152 PCR reaction was run using the following conditions: (1) initial denaturation, 98°C for 2 min; (2)
153 98°C for 20 s (1 cycle); (2) 98°C for 30 s, annealing temperature of primers for 30 s, 72°C for 1 min
154 (35 cycles); (3) final extension, 72°C for 10 min; (4) hold, 4°C for 10 min (1 cycle). Nested PCR
155 was used for one-step SOEing-PCR reaction with the following conditions: (1) initial denaturation,
156 98°C for 2 min; (2) 98°C for 30 s, annealing temperature of templates overlap region for 30 s; 72°C
157 for 30 s (5 cycles); (3) 98°C for 30 s, annealing temperature of primers, 72°C for 30 s (30 cycles);
158 (4) final extension, 72°C for 5 min; (5) hold, 4°C for 10 min.

159 Next, splicing by overlap PCR extension (SOEing-PCR) reactions were used to link
160 LevFragA and ERM genes to generate LevFragA-ERM construct using LevFragA_fwd and
161 Erm_rev2 primer pair and LevFragA and ERM genes as templates. The PCR product (LevFragA-
162 ERM) was gel-purified, and used alongside LevFragB as templates to generate the inactivation
163 construct, LevFragA-ERM-LevFragB, in another SOEing-PCR with LevFragA_fwd and
164 LevFragB_rev primer pair.

165 **Recombinant plasmid construction**

166 The levansucrase inactivation construct (LevFragA-ERM-LevFragB) was ligated into
167 pGEM®7Zf(+), a high copy number plasmid in *E. coli* JM109, which behaves as a non-replicative
168 vector in *P. polymyxa*. pGEM®7Zf(+) possesses filamentous phage f1 origin of replication
169 recognized by *E. coli* but not by *P. polymyxa*. Consequently, this vector is used to produce circular
170 single stranded DNA (ssDNA) that enhances homologous recombination *in vivo* (23). The presence
171 of phage f1 origin of replication and the ability of pGEM®7Zf(+) to be replicated into stable
172 circular DNA in *E. coli* is important for its application in the inactivation of genes via homologous
173 recombination in *P. polymyxa* and other gram positive bacteria.

174 pGEM®7Zf(+) and LevFragA-ERM-LevFragB were restricted independently with *XhoI* and
175 *BamHI* (New England biolabs, Ipswich, MA) in a 50 µl reaction mixture. The reaction mixture
176 consisted of 5 µl CutSmart buffer (New England biolabs, Ipswich, MA), 1 µl *XhoI*, 0.02 µg/ µl
177 DNA and the reaction volume was made up to 49 µl with nuclease-free water (Amresco®, Solon,
178 OH). The mixture was incubated at 37 °C for 1 h, and 1 µl *BamHI* was added and incubated for
179 additional 1 h at 37 °C. The restricted plasmid and LevFragA-ERM-LevFragB construct were
180 purified by agarose gel electrophoresis using GenCatch and advanced PCR extraction kit (Epoch
181 Life Science, Sugar Land, TX). The purified restriction products, LevFragA-ERM-LevFragB and
182 pGEM®7Zf(+) were ligated in a 20 µl reaction mix to generate the recombinant pGEM®7Zf(+)
183 carrying the levansucrase inactivation construct, LevFragA-ERM-LevFragB. The ligation reaction
184 mixture consisted of 2 µl T4 DNA ligase buffer (New England biolabs, Ipswich, MA), 1 µl T4
185 DNA ligase (New England biolabs, Ipswich, MA), plasmid (pGEM®7Zf(+)) and LevFragA-ERM-
186 LevFragB insert in a ratio of 1:5 with final DNA concentration between 0.02-0.1 pmol. The reaction
187 volume was made up with nuclease-free water (Amresco®, Solon, OH). The reaction mixture was
188 incubated overnight at 16 °C, heat inactivated at 65 °C for 10 min, then chilled on ice for 20 min
189 prior to transformation of competent *E. coli* JM 109 with recombinant pGEM®7Zf(+) carrying the

190 levansucrase inactivation construct, LevFragA-ERM-LevFragB . The ligated pGEM®7Zf(+) and
191 LevFragA-ERM-LevFragB (recombinant pGEM®7Zf(+)) was purified using GenCatch advanced
192 PCR extraction kit (Epoch Life Science, Sugar Land, TX).

193 **Transformation of competent *E. coli* JM 109**

194 The recombinant pGEM®7Zf(+) was used to transform competent *E. coli* JM 109 cells. The
195 recombinant pGEM®7Zf(+) (50 ng) was added to 50 µl of competent *E. coli* JM109 cells
196 previously placed on ice for 20 min.. The mixture was heat-shocked at 42 °C for 1 min. Subsequent
197 transformation steps were carried out as previously described (24). The cells were incubated at 37°C
198 and 250 rpm for 1 h after which the cells were plated on LB agar supplemented with 50 µg/ml
199 ampicillin, and 5-bromo-4-chloro-3-indolyl-β-D-galactopyranoside (X-gal) and isopropyl-β-D-1-
200 thiogalactopyranoside (IPTG) to a final concentration of 20 mg/ml and 1 mM, respectively. The
201 plates were incubated at 37°C for 12 h after which white colonies were selected and screened for the
202 presence of correct insert (recombinant pGEM®7Zf[+]) by colony PCR and restriction digestion.
203 Colonies with the correct insert were grown in LB medium supplemented with 50 µg/ml ampicillin
204 and the recombinant plasmid was isolated and purified using GenCatch plus plasmid DNA miniprep
205 kit (Epoch Life Science, Sugar Land, TX) and stored at -20 °C prior to use.

206 **Electro-transformation of competent *P. polymyxa* protoplasts**

207 Following initial unsuccessful attempts to transform competent *P. polymyxa* cells with the
208 recombinant pGEM®7Zf(+) harboring the levansucrase inactivation construct via electroporation,
209 competent *P. polymyxa* protoplasts were generated and used instead. Indeed, the cell wall of *P.*
210 *polymyxa* was removed by a previously described method (25) with slight modifications. Briefly, *P.*
211 *polymyxa* cells were grown in tryptic soy broth (TSB) for 12 h until cell optical density (OD_{600nm})
212 reached 0.7. The cells were harvested and placed in 50 ml centrifuge tubes pre-chilled on ice for 20

213 min and then washed twice with 50 mM Tris-Maleate buffer (pH 7.1) containing 2 mM
214 dithiothreitol followed by centrifugation at 1000 x g and 4°C for 7 min. The cell pellets were
215 harvested and re-suspended in Tris-Maleate buffer (pH 7.1) containing 0.6 M sucrose, 5 mM MgCl₂
216 and 300 µg/ml lysozyme (Amresco®, Solon, OH). The cell suspension was incubated in an
217 ISOTEMP 220 water bath (Fischer Scientific, Pittsburg, PA) for 60 min at 37°C to make *P.*
218 *polymyxa* protoplasts. *P. polymyxa* protoplasts were harvested by centrifugation at 1000 x g and 4°C
219 for 7 min. *P. polymyxa* protoplasts were made competent by washing the protoplasts twice with
220 10% polyethylene glycol (PEG-8000) and re-suspended in 500 µl of 10% PEG-8000. The
221 competent *P. polymyxa* protoplasts were transformed with recombinant pGEM®7Zf(+) harboring
222 the levansucrase inactivation construct (LevFragA-ERM-LevFragB) via electroporation. Twenty
223 microliters (100 µg DNA) of the recombinant plasmid was gently mixed with 100 µl of competent
224 protoplasts in a pre-chilled 0.2 cm electroporation cuvette and then placed on ice for 5 min.
225 Electroporation was performed at 2.5 kV, 25 µF capacitance and infinite resistance as previously
226 described (26) in a Bio-Rad Gene Pulser Xcell™ electroporator (Bio-Rad, Hercules, CA). Electric
227 pulse was delivered to the protoplasts between 2.5 and 4.1 milliseconds. Following electroporation,
228 the protoplasts were placed on ice for 5 min and then 500 µl of TSB was added and the mixture was
229 incubated at 35 °C for 6 h to allow protoplast recovery. The recovered cells were plated on tryptic
230 soy agar (TSA) supplemented with 35 µg/ml erythromycin and incubated at 35°C for 16 - 24 h.
231 Colonies were selected and mixed with 50 µl of TSB and then re-plated on a fresh TSA plate
232 supplemented with 35 µg/ml erythromycin and incubated at 35°C for 12 h. Fresh colonies were then
233 selected and colony PCR technique was used to screen for the presence of erythromycin gene. The
234 colonies with erythromycin gene were transferred to TSB supplemented with 50 µg/ml
235 erythromycin. The cells were harvested and genomic DNA was extracted as described above. PCR
236 was performed to screen for the presence of LevFragA-ERM, ERM and ERM-LevFragB fragments

237 using genomic DNA as template. The presence of all three fragments confirmed that levansucrase
238 gene was successfully inactivated via double-cross homologous recombination.

239 **Characterization of *P. polymyxa* levansucrase null mutant**

240 The *P. polymyxa* levansucrase null mutant was characterized for cell growth, EPS and 2,3-
241 BD production. Batch fermentations were conducted in sucrose- and glucose-based media. One
242 milliliter of 50% glycerol stock of *P. polymyxa* levansucrase null mutant was inoculated into 30 ml
243 of pre-culture medium supplemented with 35 µg/ml erythromycin and incubated at 35 °C and 200
244 rpm for 6 h until cell optical density (OD_{600nm}) reached 1.0-1.2. The actively growing *P. polymyxa*
245 levansucrase null mutant (10%, v/v) was inoculated into the fermentation medium containing 100
246 g/L sucrose or glucose supplemented with 35 µg/ml erythromycin. The pre-culture and fermentation
247 medium components used in this study have been previously described (7). The fermentation
248 medium was further supplemented with 0 - 0.4 g/L CaCl₂. Wildtype *P. polymyxa* was prepared as
249 described for the levansucrase null mutant without erythromycin supplementation. Batch 2,3-BD
250 fermentations were conducted in loosely-capped 125 ml Pyrex culture bottles with 30 ml
251 fermentation volume. All experiments were carried out in triplicate and 2 ml samples were collected
252 at 0 h and then, every 12 h until the fermentation terminated. Samples were analyzed for cell
253 growth, culture pH, EPS, 2,3-BD, acetoin, acetic acid and ethanol production.

254 **Quantitative reverse transcription polymerase chain reaction (qRT-PCR)**

255 To further validate successful deletion of levansucrase gene in *P. polymyxa* genome, the
256 messenger RNA (mRNA) levels of the levansucrase gene was quantified by quantitative reverse
257 transcription PCR (qRT-PCR) using cells grown in sucrose and glucose media. In addition, qRT-
258 PCR was used to confirm successful erythromycin gene integration in *P. polymyxa*. Specific
259 primers for the disrupted region of levansucrase and erythromycin genes were used. Owing to the
260 presence of small amounts of EPS in the *P. polymyxa* levansucrase null mutant cultures, the mRNA

261 levels of a few putative EPS production genes namely flippase, polysaccharide polymerase and
262 exopolysaccharide biosynthesis protein genes were quantified to ascertain their contributions to EPS
263 production on sucrose and glucose substrates. The specific primers used for qRT-PCR are shown in
264 **Table 3**. Total RNA was isolated from the wildtype and levansucrase null mutant using Tri
265 Reagent® (Sigma, St. Louis, MO) following the manufacturer's protocol. Culture samples for RNA
266 isolation were taken at 12 h of fermentation (point of maximum EPS accumulation). The RNA
267 content was determined spectrophotometrically using NanoDrop (BioTek® Instrument Inc,
268 Winooski, VT). Total RNA (2 ug) was reverse transcribed to cDNA using Random Hexamers
269 (Qiagen, Hilden, Germany) and M-MLV Reverse Transcriptase (Promega, Madison, WI) according
270 to the manufacturer's protocol. The qRT-PCR was conducted in triplicates using the resulting
271 cDNA and GoTaq® qPCR Master Mix containing BRYT Green® (Promega, Madison, WI) in a
272 Bio-Rad CFX96 Touch Deep Well™ Real-Time Detection Systems (Bio-Rad, Hercules, CA). The
273 conditions for the qRT-PCR were: 1 cycle of 95°C at 15 min (initial denaturation), then 40 cycles of
274 55°C at 30 s (annealing and extension), followed by melting curve analysis via heating from 55°C
275 to 95°C with 1°C per 10 s temperature increment. The mRNA expression levels of all the tested
276 genes were normalized to *P. polymyxa* 16S rRNA (internal standard) and relative expression was
277 performed by the $2^{-\Delta\Delta CT}$ method (27).

278 **Analytical methods**

279 Microbial cell growth was determined by measuring its optical density (OD₆₀₀) in a DU®
280 Spectrophotometer (Beckman Coulter Inc., Brea, CA). Changes in pH were measured using an
281 Acumen® Basic pH meter (Fischer Scientific, Pittsburgh, PA). Concentrations of fermentation
282 products, 2,3-BD, acetoin, ethanol, and acetic acid were quantified using a 7890A Agilent gas
283 chromatograph (Agilent Technologies Inc., Wilmington, DE, USA) equipped with a flame

284 ionization detector (FID) and a J x W 19091 N-213 capillary column [30 m (length) x 320 μ m
285 (internal diameter) x 0.5 μ m (HP-Innowax film thickness)] as previously described (28).

286 The concentration of sugars such as sucrose, glucose and fructose was quantified by high
287 performance liquid chromatography (HPLC) using a Waters 2796 Bioseparations Module equipped
288 with an Evaporative Light Scattering Detector (ELSD; Waters, Milford, MA) and a 9 μ m Aminex
289 HPX-87P column; 300 mm (length) x 7.8 mm (internal diameter) connected in series to a 4.6 mm
290 (internal diameter) x 3 cm (length) Aminex deashing guard column (Bio-Rad, Hercules, CA). The
291 column temperature was maintained at 65°C. The mobile phase was HPLC-grade water (Waters
292 Corporation, Milford, MA) maintained at a flow rate of 0.6 ml/min as described previously (29).

293 The EPS produced during fermentation was quantified using a method described by (30)
294 with modifications. Culture broth was centrifuged at 8,000 x g for 10 min to pellet the cells while
295 EPS was retained in the supernatant. The EPS was then precipitated with 95 % ethanol (4°C); 10 x
296 the volume of the supernatant. The supernatant-ethanol mixture was kept overnight at 4 °C followed
297 by centrifugation at 8,000 x g for 10 min. The EPS pellet was dried in the oven at 60°C and
298 reconstituted in distilled water. The EPS containing solution was vortexed vigorously to ensure
299 complete dissolution of the EPS. The EPS was then quantified by Phenol-sulfuric acid method (31,
300 32). Briefly, 25 μ l of 80% phenol was added into test tubes A containing 1 ml glucose standards (0-
301 0.1 g/L) and test tubes B containing 1 ml diluted EPS samples. The mixture was vortexed briefly
302 and 2.5 ml concentrated sulfuric acid (Fischer Scientific, Pittsburg, PA) was added to the mixture.
303 The mixture was left to stand for 10 min. The test tubes containing the mixture were incubated at
304 25°C for 10 min. After incubation, the mixture was gently vortexed and absorbance was measured
305 at 490 nm against reagent blank prepared as the samples. A standard curve was generated by
306 plotting the values of glucose concentration (X-axis) against absorbance (OD_{490nm}) (Y-axis) and
307 EPS concentration was interpolated from the standard curve.

308 **Levansucrase assay**

309 Levansucrase activity in the levansucrase null mutant and wildtype *P. polymyxa* were
310 measured using culture supernatant. Levansucrase activity was determined using a method modified
311 from (33). *P. polymyxa* samples (levansucrase null mutant and wildtype) were collected at the
312 exponential growth phase when maximum EPS is produced. The sample was centrifuged for 20 min
313 at 8,600 x g and 4°C. The supernatant from each sample was divided into two portions. One portion
314 was used to quantify EPS as described above and the EPS obtained was designated as [EPS]_B. The
315 other portion was used to assay levansucrase activity and the total EPS produced after levansucrase
316 activity assay was designated as [EPS]_A. The reaction mixture for the levansucrase activity assay
317 consisted of 400 µl of 1 M sucrose in 50 mM phosphate buffer (pH 6.0) and 100 µl of culture
318 supernatant. The mixture was incubated at 35 °C for 1 h. Following levansucrase activity, EPS was
319 precipitated with 95% ethanol (4°C) and the EPS was subsequently quantified and expressed as
320 [EPS]_A. The EPS produced during levansucrase activity was determined from the equation below:

$$321 \text{ [EPS]}_L = \text{ [EPS]}_A - \text{ [EPS]}_B$$

322 Where [EPS]_L represents the concentration of EPS synthesized during levansucrase assay.

323 The concentrations of protein in the supernatants were determined by Bradford method (34).
324 One unit of levansucrase activity was defined as the milligram of protein that catalyzed the
325 formation of one µmoles of EPS (levan) per min at 35°C in 1 M sucrose solution.

326 **Growth rate and generation time of levansucrase null mutant**

327 To determine the stability of the levansucrase null mutant, the growth curve was first
328 obtained. Cells were grown to exponential phase (10 h) in the pre-culture medium (7), then
329 harvested and washed twice with sterile distilled water by centrifugation at 5,000 x g for 3 min. The
330 cell pellet was reconstituted to several dilutions and the optical densities (OD_{600nm}) were measured

331 against sterile distilled water as blank. Each cell dilution was then centrifuged in a pre-weighed
332 Eppendorf tube at 10,000 x g for 10 min and the supernatant was discarded. The cell pellets were
333 dried for 18 h in TempCon™ Oven (American Scientific Products, McGraw Park, IL) at 50 °C. The
334 cells were weighed and the weight of the cells at each OD_{600nm} reading was determined. A standard
335 curve was generated from a plot of cell biomass (mg/L) against absorbance at OD_{600nm}. The
336 standard curve was then used to convert optical density measurements at OD_{600nm} to cell biomass
337 concentrations. The growth curve was obtained by growing the levansucrase null mutant in pre-
338 culture medium and the cell biomass was measured at several time points until the cells reached the
339 death phase of growth. Then, the cell biomass was plotted against time. The generation (doubling)
340 time of levansucrase mutant was determined from the exponential phase of the growth curve (**Fig.**
341 **S1**).

342 **Stability of *P. polymyxa* levansucrase null mutant**

343 The stability of levansucrase null mutant was determined in the presence and absence of
344 antibiotic, erythromycin, for 50 generations. The levansucrase null mutant was grown in pre-culture
345 medium supplemented with 35 µg/ml erythromycin until OD_{600nm} reached 1.0-1.2. The actively
346 growing cells (10%, v/v) were transferred into fermentation medium containing 100 g/L sucrose
347 supplemented with 35 µg/ml erythromycin and this generation was regarded as G₀ (generation
348 zero). The generation time of *P. polymyxa* levansucrase null mutant was pre-determined to be 1.5 h
349 (**Fig. S1**). Several subcultures (every 3 h i.e., 2 generations) were made from G₀ until G₅₀
350 (generation 50) was attained, and in each case, cultures were supplemented with 35 µg/ml
351 erythromycin. Fermentations were conducted using G₀, G₁₀, G₂₀, G₃₀, G₄₀, and G₅₀ under antibiotic
352 selective pressure. Samples (2 ml) were drawn at 0 h and every 12 h until the fermentation ended
353 and then, analyzed for cell growth, EPS and 2,3-BD production. The same experiment was

354 conducted without antibiotic supplementation. Generations G_0 , G_{10} , G_{20} , G_{30} , G_{40} , and G_{50} were
355 obtained as described above and then used to conduct fermentations. The antibiotic resistance of all
356 the generations studied (with and without erythromycin supplementation) was determined by PCR
357 and replica plating onto erythromycin-containing plates. For each generation, samples of *P.*
358 *polymyxa* levansucrase null mutant were drawn during the stationary growth phase (12-16 h of
359 growth) and sub-cultured into fresh pre-culture medium and grown until another stationary growth
360 phase (12-16 h of growth) was attained. The cells were diluted to a concentration of 10^8 cfu/ml and
361 were plated on TSA plates without antibiotic (erythromycin) supplementation. The plates were
362 incubated at 35 °C for 12 h. Colonies from each generation were selected and screened for presence
363 of the erythromycin gene using PCR. Recombinant pGEM®7Zf(+) harboring the levansucrase
364 inactivation construct was used as erythromycin gene control. Gel electrophoresis was performed
365 using the colony PCR products. The presence of erythromycin gene in the colonies confirmed the
366 stability of *P. polymyxa* levansucrase null mutant. Colonies from the TSA plates (without
367 erythromycin supplementation) were transferred by replica plating to fresh TSA plates
368 supplemented with erythromycin (35 µg/ml). The antibiotic-supplemented plates were incubated at
369 35 °C for 12 h and the resulting colonies were quantitatively compared to the plates without
370 antibiotic supplementation. A schematic representation of step-by-step procedure employed to
371 evaluate the stability of the *P. polymyxa* levansucrase null mutant is shown in **Fig S2**.

372 **Statistical analysis**

373 General Linear Model of Minitab 17 (Minitab Inc., State College, PA) was used for all
374 statistical analyses. Analysis of variance (ANOVA) using Tukey's method for pairwise
375 comparisons was employed to compare differences between treatments. Differences in growth,
376 sugar utilization, maximum product concentrations, 2,3-BD yields and productivities were
377 compared at 95 % confidence interval. 2,3-BD yield was expressed as the gram of 2,3-BD produced

378 from one gram of substrate (sucrose or glucose). 2,3-BD productivity was expressed as the gram per
379 liter of 2,3-BD produced per hour of fermentation.

380 **Results**

381 **Levansucrase gene inactivation in *P. polymyxa* DSM 365**

382 The levansucrase gene of *P. polymyxa* was successfully inactivated by double-cross
383 homologous recombination. Erythromycin resistance gene was inserted between a 210 bp upstream
384 fragment and a 213 bp downstream fragment of levansucrase gene creating a 1224 bp levansucrase
385 inactivation construct (**Fig 1**). The inactivation construct design included a stop codon downstream
386 of LevFragA sequence followed with a ribosomal binding site and a spacer sequence upstream of
387 erythromycin gene. In addition, the construct included a transcription terminator sequence
388 downstream of the erythromycin gene that precedes the LevFragB sequence. The strategy and
389 design employed in generating levansucrase inactivation construct is shown in **Fig 1**. Inclusion of
390 stop codon, ribosomal binding site and spacer sequence, and transcription terminator sequences
391 ensured that only erythromycin gene is transcribed into mRNA without creating additional
392 metabolic burden on *P. polymyxa*. Following transformation of *P. polymyxa*, PCR-screening of the
393 levansucrase null mutant colonies using LevFragA_fwd/Erm_rev2, Erm_fwd/Erm_rev2 and
394 Erm_fwd/LevFragB_rev primer pairs showed that the mutant possesses LevFragA-ERM, ERM, and
395 ERM-LevFragB genes corresponding to 1008, 800, and 1015 bp, respectively (**Fig 2**), thus
396 confirming successful double-cross homologous recombination.

397 **Effect of levansucrase disruption on EPS formation**

398 Batch 2,3-BD fermentations were conducted with sucrose and glucose substrates to evaluate
399 EPS formation by the levansucrase null mutant. The fermentation cultures were supplemented with
400 0, 0.2, 0.4 g/L CaCl₂. Fermentation on sucrose showed that EPS formation by the levansucrase null
401 mutant decreased 5.8-, 6.4- and 6.1-fold in the 0, 0.2 and 0.4 g/L CaCl₂-supplemented cultures,

402 respectively, when compared to the wildtype (**Table 4, Fig. 2B**). The levansucrase null mutant
403 showed no measurable levansucrase activity whereas more than 0.6 units of levansucrase activity
404 per milligram protein were detected in the wildtype (**Figs 3F, 4F, 5F**). The absence of any
405 measurable levansucrase activity in the mutant confirms successful inactivation of levansucrase
406 gene in *P. polymyxa*. However, even though no measurable levansucrase activity was detected in
407 the mutant, 2-3 g/L EPS was synthesized by the mutant grown on sucrose (**Table 4**), thus
408 suggesting that *P. polymyxa* produces other EPS forms other than levan.

409 EPS production by the levansucrase null mutant grown on glucose decreased 2.4-, 1.7- and
410 1.9-fold in the 0, 0.2 and 0.4 g/L CaCl₂-supplemented cultures, respectively, when compared to the
411 wildtype (**Table 5; Figs S3-S5**). Interestingly, no levansucrase activity was observed in both the
412 wildtype and the levansucrase null mutant grown on glucose. However, EPS produced by the
413 wildtype cultures in the glucose medium decreased by at least 4-fold when compared to the cultures
414 grown on sucrose (**Tables 4 and 5**).

415 **Effect of calcium supplementation on growth, sugar utilization, 2,3-BD yield and productivity**

416 Initial fermentations with the levansucrase null mutant resulted in a sharp drop in pH, which
417 adversely affected cell growth and product formation, particularly when the pH fell below 5.5 (**Figs**
418 **3A, B and S3A, B**). Thus, medium supplementation with CaCO₃ and CaCl₂ was adopted given pre-
419 reported capacity of calcium to influence key cellular processes such as sugar transport, product
420 formation and tolerance, and most importantly pH stabilization (Han et al., 2013; Okonkwo et al.,
421 2016; Zeng et al., 2010). Medium supplementation with CaCO₃ and CaCl₂ did not improve culture
422 pH of the levansucrase null mutant (data not shown), however, CaCl₂ exerted remarkable influence
423 on cell growth and 2,3-BD production by this strain. Following CaCl₂ supplementation, cell
424 biomass production increased in the sucrose- and glucose-grown cultures for both the wildtype and
425 the levansucrase null mutant with attendant increases in substrate consumption (**Tables 4 and 5**).

426 Growth of the levansucrase null mutant on sucrose increased by 22% and 34%, respectively, with
427 0.2 and 0.4 g/L CaCl₂ supplementation when compared to the wildtype (**Figs 4A and 5A**). As
428 shown in **Figs 4A and 5A**, CaCl₂ supplementation led to increased biomass accumulation. With
429 CaCl₂ (0.2 and 0.4 g/L), 2,3-BD yield on sucrose increased 27% in the levansucrase null mutant
430 relative to the wildtype (**Table 4**). In addition, the 2,3-BD productivity of the null mutant on sucrose
431 increased marginally - approximately 3% and 4% with 0.2 and 0.4 g/L CaCl₂ treatments,
432 respectively, when compared to the wildtype (**Table 4**). Conversely, without CaCl₂ supplementation
433 productivity of the levansucrase null mutant on sucrose decreased 8.8% compared to the wildtype
434 (**Table 4**).

435 With glucose, addition of 0.2 and 0.4 g/L CaCl₂ to cultures of the levansucrase null mutant
436 increased growth by 27% and 34%, respectively, compared to the null mutant grown in cultures
437 without CaCl₂ supplementation (**Table 5**). Similarly, the wildtype exhibited 25% and 17% increased
438 growth with 0.2 and 0.4 g/L CaCl₂ relative to CaCl₂-unsupplemented cultures (**Table 5**). As
439 observed in the sucrose cultures, glucose utilization by the wildtype and levansucrase null mutant
440 improved with 0.2 and 0.4 g/L CaCl₂ supplementation. Glucose utilization by the mutant increased
441 20% and 22% in the 0.2 and 0.4 g/L CaCl₂ -supplemented cultures, respectively, when compared to
442 the null mutant cultures without CaCl₂ supplementation (**Table 5**). The 2,3-BD yield and
443 productivity of the levansucrase null mutant grown on glucose increased from 0.34 g/g and 0.57
444 g/L/h (without CaCl₂), respectively, to at least 0.37 g/g and 1.62 g/L/h (with CaCl₂
445 supplementation), respectively, whereas, 2,3-BD yield and productivity of the wildtype increased
446 from 0.36 g/g and 0.51 g/L/h (without CaCl₂), respectively, to at least 0.36 g/g and 0.71 g/L/h (with
447 CaCl₂ supplementation), respectively. However, the 2,3-BD yield and productivity of the
448 levansucrase null mutant in glucose cultures increased by 3% and 4% (without CaCl₂), and 2% and
449 128%, respectively, in the CaCl₂-supplemented cultures, respectively, relative to the wildtype

450 (**Table 5**). The observed increased glucose utilization rate of the levansucrase null mutant may be
451 responsible for the enhanced 2,3-BD titer, yield and productivity relative to the wildtype.

452 The levansucrase null mutant efficiently converted sucrose to 2,3-BD with diminished
453 ability to produce EPS (**Fig. 2B**). However, the mutant utilized glucose much faster than sucrose
454 resulting in higher 2,3-BD productivity on glucose relative to fermentations conducted with sucrose
455 as substrate (**Tables 4 and 5**). The null mutant achieved a maximum 2,3-BD yield of 0.42 g/g with
456 CaCl₂ supplemented (0.2 g/L) when grown on sucrose, which is 27% more than that (0.33 g/g)
457 achieved by the wildtype (**Tables 4**).

458 **qRT-PCR**

459 To further confirm successful inactivation of levansucrase in *P. polymyxa*, qRT-PCR was
460 conducted to quantify the mRNA transcript levels of levansucrase and erythromycin resistance
461 genes of levansucrase null mutant relative to the wildtype. For these analyses, both strains were
462 grown on sucrose and glucose. As shown in **Fig. 6**, mRNA transcripts of the *P. polymyxa*
463 levansucrase gene were not detected in the null mutant grown on both sucrose and glucose.
464 Conversely, we detected high levels of mRNA transcripts of the erythromycin resistance gene in the
465 levansucrase null mutant (**Fig. 6**). Clearly, this indicates effective levansucrase inactivation and
466 successful integration of the deletion construct in the genome of *P. polymyxa* by double cross
467 homologous recombination.

468 Despite successful levansucrase gene inactivation in *P. polymyxa*, EPS accumulation was
469 not completely abolished in cultures of the levansucrase null mutant. To delineate the source(s) of
470 the observed EPS in the levansucrase null mutant, qRT-PCR was used to probe the mRNA
471 transcript levels of other exopolysaccharide biosynthesis genes in *P. polymyxa*, namely,
472 polysaccharide polymerase (*pop*), flippase (*flip*) and exopolysaccharide biosynthesis protein (*EBP*).

473 *Pop*, *flip* and *EBP* genes are putative genes that have been implicated in the biosynthesis of other
474 EPSs other than levan in *P. polymyxa* (35). *Pop*, *flip* and *EBP* genes were found to be expressed by
475 the levansucrase null mutant grown in sucrose medium, however, only *Pop* was expressed by the
476 levansucrase null mutant on glucose substrate (**Fig. 6**). *Pop* and *EBP* are putative genes that are
477 possibly associated with exopolysaccharide precursors and assemble monomers to growing EPS
478 chain (35). Different studies suggest that flippase might be membrane specific, where it assembles
479 EPS repeating units and then translocates complete EPS across the membrane (35). The expression
480 of *Pop*, *flip* and *EBP* suggests that *P. polymyxa* has the capability to synthesize other forms of EPS
481 when grown on both sucrose and glucose.

482 **Stability of levansucrase null mutant**

483 Stability of the levansucrase null mutant was tested over 50 generations. For this, 2,3-BD
484 fermentations were conducted with different (0, 10, 20, 30, 40 and 50) generations of *P. polymyxa*
485 levansucrase null mutant on sucrose substrate, with and without erythromycin supplementation. As
486 shown in **Figs S6** and **S7**, the maximum growth for each tested generation of levansucrase null
487 mutant under erythromycin pressure was between 11.0 and 13.9 (OD_{600nm}), whereas without
488 erythromycin, the growth ranged from 12.5 to 15.1 (OD_{600nm}).

489 EPS concentrations at each tested generation (G₀-G₅₀) of the levansucrase null mutant, with
490 and without erythromycin supplementation were considerably similar. The maximum 2,3-BD
491 produced by the mutant grown under antibiotic pressure was in the range of 35.3 to 39.4 g/L,
492 whereas without antibiotics, the 2,3-BD production was in the range of 36.1 to 39.0 g/L (**Table S1**).
493 Colony-PCR and replica plating techniques were further employed to characterize the levansucrase
494 null mutant generation (G₀-G₅₀) for antibiotic resistances. The results are shown in **Figs S8** and **S9**.

495 Notably, the levansucrase null mutant developed in this study retained antibiotic resistance to
496 erythromycin after 50 generations of growth with or without erythromycin addition.

497 **Discussion**

498 EPS production during 2,3-BD fermentation constitutes a nuisance during fermentation and
499 diverts substrate carbons away from 2,3-BD biosynthesis, thus decreasing 2,3-BD yield and
500 productivity. Also, viscosity of the fermentation broth increases with EPS production, which
501 impairs mixing (9). More importantly, EPS negatively impacts 2,3-BD downstream processing,
502 thereby increasing the overall cost of production. Therefore, this study was aimed at developing a
503 mutant strain of *P. polymyxa* with diminished ability to synthesize EPS. We employed double cross
504 homologous recombination strategy to inactivate levansucrase gene in *P. polymyxa*. The following
505 objectives were achieved: (i) disruption of levansucrase gene in *P. polymyxa* via erythromycin gene
506 insertion, (ii) phenotypic characterization of the levansucrase null mutant by determining the
507 resultant cell growth, and concentrations of EPS, 2,3-BD, acetoin, ethanol and acetic acid.

508 The genome of *P. polymyxa* DSM 365 is not fully sequenced. Thus, due to insufficient
509 genomic information on this microorganism, the nucleotide and protein sequences of the *P.*
510 *polymyxa* DSM 365 levansucrase from the available shot-gun sequences were compared to those of
511 other *P. polymyxa* strains whose complete genome sequences are available on public databases. As
512 shown in **Table 1**, fully sequenced *P. polymyxa* strains have a single copy of the levansucrase gene,
513 which has 95-97% protein sequence similarity to that of *P. polymyxa* DSM 365. Levansucrase,
514 which is responsible for levan EPS biosynthesis in *P. polymyxa* (36, 37), was targeted for
515 inactivation. The results from the present study are discussed below.

516 **Effect of levansucrase inactivation on EPS biosynthesis by *P. polymyxa* levansucrase null**
517 **mutant**

518 Successful knockout of levansucrase gene in *P. polymyxa* was confirmed by PCR, restriction
519 digest analysis, levansucrase activity assay, quantitative real-time PCR, antibiotic selection and
520 genetic stability. Knockout of levansucrase gene in *P. polymyxa* resulted in significant reduction in
521 EPS formation by the levansucrase null mutant grown on sucrose and glucose (**Figs. 3C, 4C, 5C,**
522 **S3 C, S4 C, S5 C**). Clearly, significant reduction in the amount of EPS accumulated by the
523 levansucrase null mutant confirms that levansucrase is the key player in EPS biosynthesis in *P.*
524 *polymyxa* and that the targeted open reading frame (ORF) in the *P. polymyxa* DSM 365 shotgun
525 sequence encodes levansucrase. Reduction in EPS biosynthesis by the levansucrase null mutant was
526 more pronounced during growth on sucrose relative to glucose. This is ascribable to the fact that
527 EPS formation is more strongly favored by sucrose, which is hydrolyzed by levansucrase to release
528 glucose and fructose (38). The vast majority of the fructose molecules are then linked to form EPS
529 by the same enzyme (levansucrase). Therefore, sucrose consumption by *P. polymyxa* results in
530 significantly higher EPS production, which was almost completely abolished in the null mutant. In
531 fact, levansucrase mRNA and activity were not detected in the levansucrase null mutant grown on
532 both glucose and sucrose. However, levansucrase mRNA expression and activity were observed in
533 the wildtype grown in sucrose-based medium. Levansucrase mRNA transcripts, albeit marginal,
534 were detected in the wildtype cultures grown on glucose without any measurable levansucrase
535 activity (**Fig. 6**). The lack of levansucrase activity in the wildtype in glucose medium coupled with
536 the detection of low levels of levansucrase mRNA transcripts in the corresponding cells suggests
537 that sucrose likely plays a specific role in levansucrase gene expression. In fact, sucrose-mediated
538 induction of levansucrase gene expression has been reported by previous authors (39, 40). However,
539 levansucrase mRNA transcript levels were not quantified in these studies. Notably, (41) observed
540 levansucrase mRNA transcripts in *Z. mobilis* cultures on both glucose and fructose. Perhaps,
541 different mechanisms govern levansucrase expression in different species, which employ EPS for

542 different functions in their different ecological habitats/niches. Further studies are required to better
543 delineate the role of sucrose in levansucrase gene expression in *P. polymyxa*.

544 Despite levansucrase gene inactivation which was confirmed by PCR, antibiotic sensitivity
545 assay and replica plating, and qPCR, EPS was detected in cultures of both the wildtype and the
546 levansucrase null mutant grown on glucose, albeit in significantly low amounts in the levansucrase
547 null mutant. We therefore rationalized that *P. polymyxa* likely produces more than one type of
548 extracellular polysaccharide with different sugars, with sucrose favoring levan biosynthesis, while
549 glucose supports the production of uncharacterized polysaccharide(s). This is not unusual among
550 EPS-producing microorganisms as *Bacillus* spp., *Z. mobilis*, *Leuconostoc mesenteroides*,
551 *Agrobacterium radiobacter*, *Xanthamonas campestris*, and *Pseudomonas aeruginosa* have been
552 shown to produce alginate, xanthan, curdlan or dextran with different sugars (42, 43, 44, 45, 46, 47,
553 48). To test the likelihood that *P. polymyxa* produces another EPS other than levan, we used qPCR
554 to assay for mRNA transcripts of genes likely involved in the expression of other EPSs.
555 Interestingly, polysaccharide polymerase, flippase, and exopolysaccharide biosynthesis protein,
556 which are putatively involved in the synthesis of other EPS, were expressed in both the
557 levansucrase null mutant and the wildtype (**Figs 6 and 7**). The expression of polysaccharide
558 polymerase gene by *P. polymyxa* levansucrase null mutant cultures in both sucrose and glucose
559 indicates that other genes may be involved in the biosynthesis of other forms of EPS by *P.*
560 *polymyxa* (**Fig 7**). Hence, physicochemical characterization of the EPS obtained in glucose cultures
561 of *P. polymyxa* may shed more light on the other EPS forms.

562 Whereas EPS production was significantly reduced in the levansucrase mutant when
563 compared to the wildtype, this did not translate to significant increase in 2,3-BD production with
564 sucrose as substrate. In parallel, while sucrose utilization by the levansucrase null mutant was 1.3-
565 fold lower than that of the wildtype, the amount of 2,3-BD produced was similar for both strains

566 **(Table 4)**. This implies that by utilizing considerably less substrate (sucrose), the levansucrase null
567 mutant produced the same amount of product. This is an attractive trait (higher yield) for potential
568 large-scale application from an economic standpoint. Further, reduced sucrose utilization by the
569 levansucrase null mutant underscores disruption of sucrose utilization or processing following
570 levansucrase inactivation in the null mutant. Comparatively, the levansucrase null mutant
571 utilized 1.1-fold more glucose than the wildtype, which lends further weight to the role of
572 levansucrase in sucrose utilization in *P. polymyxa* and successful inactivation of the encoding gene.
573 Increased glucose utilization by the null mutant therefore accounts for 1.1-fold and 1.7-fold
574 increases in 2,3-BD and ethanol production, when compared to the wildtype. Increased product
575 accumulation (2,3-BD and ethanol) by the levansucrase mutant relative to the wildtype may stem
576 from redirection of free carbons from EPS biosynthesis to the 2,3-BD and ethanol biosynthesis
577 pathways. However, EPS accumulation was only slightly reduced in the levansucrase null mutant
578 grown in glucose-based medium relative to the wildtype, so carbon redirection does not fully
579 account for the increases in product formation. Therefore, it is likely that a different mechanism
580 might be at play. Perhaps, levansucrase inactivation relieved a growth limiting machinery in the
581 levansucrase null mutant leading to the observed increase in growth and consequently, increased
582 product formation. Furthermore, ethanol production was clearly enhanced in the levansucrase null
583 mutant relative to the wildtype when grown on glucose; an effect that was not observed with
584 sucrose. It is not clear why this occurred, thus warranting further study. However, this result
585 highlights ethanol biosynthesis as a veritable candidate for future inactivation towards developing a
586 2,3-BD over-producing strain.

587 **Levansucrase inactivation in *P. polymyxa* interferes with acetic acid re-assimilation**

588 The *P. polymyxa* levansucrase null mutant was characterized for growth by measuring
589 optical density (OD_{600nm}) during 2,3-BD fermentation. Our results clearly suggest that levansucrase

590 inactivation did not significantly impair the growth of *P. polymyxa* (**Tables 4 and 5**). Initial
591 experiments showed low culture pH stemming from the accumulation of acetic acid in cultures of
592 the levansucrase null mutant (**Fig. 3E**). To mitigate pH-related stresses and increase growth and
593 product formation, CaCl₂ was added to *P. polymyxa* levansucrase null mutant and wildtype cultures.
594 CaCl₂ supplementation enhanced the growth, 2,3-BD production, sugar utilization, and tolerance to
595 pH stresses in *P. polymyxa*, particularly, the levansucrase null mutant (**Figs. 3 -5; S3-S5; Tables 4**
596 **and 5**).

597 Typically, 2,3-BD is produced via a mixed acid pathway, which results in the accumulation
598 of acetic, formic and lactic acids during fermentation. However, acetic acid is re-assimilated during
599 fermentation with concomitant increase in culture pH. We observed that inactivation of the
600 levansucrase gene in *P. polymyxa* resulted in acetic acid accumulation, leading to a decrease in
601 culture pH (**Figs 3B and S3 B**). The acetic acid profile of the levansucrase null mutant relative to
602 the wildtype suggests that levansucrase may directly or indirectly influence acetic acid re-
603 assimilation. In both the glucose and sucrose-based cultures, with or without
604 CaCl₂ supplementation, elevated acetic acid accumulation was observed for the null mutant (**Figs.**
605 **3E, 4E, 5E, S3 E, S4 E, and S5 E**). There are no previous reports on possible links between EPS
606 biosynthesis and acetic acid assimilation in *P. polymyxa* or other 2,3-BD producers, hence, this
607 finding warrants further examination. More importantly, this indicates that EPS biosynthesis might
608 play broader roles in the biology of *P. polymyxa*, and perhaps other 2,3-BD producers, as most are
609 known to accumulate EPS during fermentation. Further, it is likely that acetic acid accumulation in
610 the levansucrase null mutant is a secondary or cascade effect stemming from downstream effectors
611 of levansucrase not directly involved in EPS biosynthesis. Solvent-producing, biphasic Gram-
612 positive bacteria typically produce acids and then, reabsorb them during solvent formation.
613 Disruption of their native biology has been reported to engender acid accumulation, due to poor

614 acid assimilation. A similar pattern has been previously reported for *C. beijerinckii* NCIMB 8052
615 following knockdown of acetoacetate decarboxylase (49) and *Clostridium acetobutylicum* ATCC
616 842 (50). Perhaps, a similar phenomenon exists in *P. polymyxa* (which is also a solvent-producing
617 biphasic Gram-positive bacterium). Notably, despite acetic acid accumulation and the attendant
618 drop in culture pH, the levansucrase null mutant exhibited an overall improved growth than the
619 wildtype in all conditions tested. It therefore appears that levansucrase inactivation might confer
620 some form of stress resistance on the mutant cells which mitigates acid-mediated stress.

621 Overall, CaCl₂ supplementation enhanced the growth of the mutant and the wildtype on both
622 glucose and sucrose. This is attributable to previously reported global effects of calcium on cellular
623 metabolism, sugar utilization and stress mitigation including upregulation of heat shock proteins
624 (involved in the repair of damaged or aberrant proteins) and DnaK involved in DNA synthesis,
625 transcription and repair in *C. beijerinckii* NCIMB 8052 (51). Additionally, Ca²⁺ has been
626 implicated in the stabilization of bacterial membrane, which reduces the effects of membrane-
627 damaging factors such as acids (52, 53). Therefore, the effects observed with CaCl₂ for both
628 strains, albeit more pronounced in the levansucrase null mutant of *P. polymyxa*, in which acetic acid
629 accumulation was evident, likely stemmed from Ca²⁺-mediated mitigation of pH stresses.

630 **Stability of *P. polymyxa* levansucrase null mutant**

631 The stability of microbial strains intended for industrial bioprocesses is critical for uniform
632 and consistent product generation. This is particularly important when genetically modified strains
633 are used. Hence, stability of the levansucrase null mutant generated in this study was tested.
634 Stability results clearly showed that this mutant is stable as demonstrated by similar fermentation
635 profiles (growth, 2,3-BD concentration, acid and ethanol concentrations, and EPS production) for
636 the levansucrase null mutant grown to different generation times (up to 50 generations) in the
637 presence and absence of antibiotic (**Figs S6 and S7**).

638 **Conclusions**

639 Levansucrase gene was successfully inactivated in *P. polymyxa* via double cross
640 homologous recombination, leading to a stable and faster-growing strain with significantly reduced
641 EPS production, which constitutes a significant nuisance to 2,3-BD fermentation and product
642 recovery. The ability of the levansucrase null mutant to produce higher concentrations of 2,3-BD on
643 glucose makes it attractive as a basis for generating a 2,3-BD overproducing strain from
644 lignocellulosic biomass; of which glucose is the major sugar component. Towards further increasing
645 2,3-BD titer, yield and productivity, inactivation of ethanol biosynthesis appears a rational target
646 considering increased ethanol accumulation by the mutant, especially when grown on glucose.
647 Culture supplementation with small amounts of CaCl₂ has promise as a means of mitigating
648 metabolic disruptions that might arise following metabolic engineering of *P. polymyxa*; a typical
649 occurrence in solvent-producing Gram-positive bacteria.

650

651 **Acknowledgements**

652 Salaries and research support were provided in part by State funds appropriated to the Ohio
653 Agricultural Research and Development Center (OARDC), OARDC graduate and interdisciplinary
654 grants, and Hatch grant (Project No. OHO01222). We would like to also acknowledge Peloton
655 Technologies LLC for financial support.

656

657 **References**

- 658 1. Celinska E, Grajek W. 2009. Biotechnology production of 2, 3- butanediol- Current state
659 and prospects. *Biotechnol Adv* 27: 715-725.
- 660 2. Ji X, Huang H, Ouyang P. 2011. Microbial 2, 3 – butanediol production: a state-of-the-art
661 review. *Biotechnol Adv* 29: 351-364.

- 662 3. Syu MJ. 2001. Biological production of 2,3-butanediol. *Appl Microbiol Biotechnol* 55:10–
663 8.
- 664 4. Garg S, Jain A. 1995. Fermentative production of 2,3-butanediol: a review. *Bioresour*
665 *Technol* 51:103–109.
- 666 5. Guo X, Cao C, Wang Y, Li C, Wu M, Chen Y, Zhang C, Pei H, Xiao D. 2014. Effect of the
667 inactivation of lactate dehydrogenase, ethanol dehydrogenase, and phosphotransacetylase
668 on 2,3-butanediol production in *Klebsiella pneumonia* strain. *Biotechnol Biofuels* 7:44.
- 669 6. Zeng AP, Deckwer WD. 1991. A model for multiproduct-inhibited growth of *Enterobacter*
670 *aerogenes* in 2, 3-butanediol fermentation. *Appl Microbiol Biotechnol* 35(1):1-3.
- 671 7. Okonkwo CC, Ujor V, Mishra PK, Ezeji TC. 2017. Process development for enhanced 2,3-
672 butanediol production by *Paenibacillus polymyxa* DSM 365. *Fermentation* 3(2):18.
- 673 8. Priya A, Dureja P, Talukdar P, Rathi R, Lal B, Sarma PM. 2016. Microbial production of 2,
674 3-butanediol through a two-stage pH and agitation strategy in 150l bioreactor. *Biochem*
675 *Eng J* 105:159-67.
- 676 9. Häbler T, Schieder D, Pfaller R, Faulstich M, Sieber V. 2012. Enhanced fed-batch
677 fermentation of 2,3-butanediol by *Paenibacillus polymyxa* DSM 365. *Bioresour Technol*
678 124:237-244.
- 679 10. Ji XJ, Huang H, Du J, Zhu JG, Ren LJ, Li S, Nie ZK. 2009. Development of an industrial
680 medium for economical 2, 3-butanediol production through co-fermentation of glucose and
681 xylose by *Klebsiella oxytoca*. *Bioresour Technol* 100(21):5214-8.
- 682 11. Biebl H, Zeng AP, Menzel K, Deckwer WD. 1998. Fermentation of glycerol to 1,3-
683 propanediol and 2,3-butanediol by *Klebsiella pneumoniae*. *Appl Microbiol Biotechnol*
684 50:24–9.
- 685 12. Jung MY, Ng CY, Song H, Lee J, Oh MK. 2012. Deletion of lactate dehydrogenase in
686 *Enterobacter aerogenes* to enhance 2, 3-butanediol production. *Appl Microbiol Biotechnol*
687 95(2):461-9.
- 688 13. Jung MY, Mazumdar S, Shin SH, Yang KS, Lee J, Oh MK. 2014. Improvement of 2, 3-
689 butanediol yield in *Klebsiella pneumoniae* by deletion of the pyruvate formate-lyase gene.
690 *Appl Environ Microbiol* 80(19):6195-203.
- 691 14. Jantama K, Polyiam P, Khunnonkwao P, Chan S, Sangproo M, Khor K, Jantama SS,
692 Kanchanatawee S. 2015. Efficient reduction of the formation of by-products and
693 improvement of production yield of 2, 3-butanediol by a combined deletion of alcohol
694 dehydrogenase, acetate kinase-phosphotransacetylase, and lactate dehydrogenase genes in
695 metabolically engineered *Klebsiella oxytoca* in mineral salts medium. *Metab Eng* 30:16-26.
- 696 15. Nakashimada Y, Marwoto B, Kashiwamura T, Kakizono T, Nishio N. 2000. Enhanced
697 butanediol production by addition of acetic acid in *Paenibacillus polymyxa*. *J Biosci Bioeng*
698 90:661-664.
- 699 16. De Mas CD, Jansen NB, Tsao GT. 1988. Production of optically active 2,3-butanediol by
700 *Bacillus polymyxa*. *Biotechnol Bioeng* 31:366–77.
- 701 17. Donot F, Fontana A, Baccou JC, Schorr-Galindo S. 2012. Microbial exopolysaccharides:
702 Main examples of synthesis, excretion, genetics and extraction. *Carbohydr Polym* 87: 951-
703 962.
- 704 18. Liang TW, Wang SL. 2015. Recent advances in exopolysaccharides from *Paenibacillus*
705 spp. production, isolation, structure, and bioactivities. *Mar Drugs* 13(4):1847-63.
- 706 19. Lal S, Tabacchioni S. 2009. Ecology and biotechnological potential of *Paenibacillus*
707 *polymyxa*: a minireview. *Indian J Microbiol* 49(1):2-10.
- 708 20. Haggag WM. 2007. Colonization of exopolysaccharide-producing *Paenibacillus polymyxa*
709 on peanut roots for enhancing resistance against crown rot disease. *Afr J Biotechnol* 6(13).

- 710 21. Lebuhn M, Heulin T, Hartmann A. 1997. Production of auxin and other indolic and
711 phenolic compounds by *Paenibacillus polymyxa* strains isolated from different proximity to
712 plant roots. FEMS Microbiol Ecol 22(4):325-34.
- 713 22. Sambrook J, Russel DW. 2001. Molecular Cloning, third ed. Cold Spring Harbor
714 Laboratory Press, New York.
- 715 23. Yanisch-Perron C, Vieira J, Messing J. 1985. Improved M13 phage cloning vectors and
716 host strains: nucleotide sequences of the M13amp18 and pUC19 vectors. Gene 33: 103-
717 119.
- 718 24. Görke B, Stülke J. 2008. Carbon catabolite repression in bacteria: many ways to make the
719 most out of nutrients. Nat Rev Microbiol 6(8):613-24.
- 720 25. Inukai M, Isono F, Takatsuki A. 1993. Selective inhibition of the bacterial translocase
721 reaction in peptidoglycan synthesis by mureidomycins. Antimicrob Agents Chemother
722 37(5):980-983.
- 723 26. Zhou Y, Johnson EA. 1993. Genetic transformation of *Clostridium botulinum* by
724 electroporation. Biotechnol Lett 15, 121-126.
- 725 27. Schmittgen TD, Livak KJ. 2008. Analyzing real-time PCR data by the comparative CT
726 method. Nat Protoc 3:1101–1110.
- 727 28. Okonkwo CC, Ujor V, Ezeji TC. 2017. Investigation of the relationship between 2,3-
728 butanediol toxicity and production during growth of *Paenibacillus polymyxa*. N Biotechnol
729 34(1):23-31.
- 730 29. Okonkwo CC, Azam MM, Ezeji TC, Qureshi N. 2016. Enhancing ethanol production from
731 cellulosic sugars using *Scheffersomyces (Pichia) stipitis*. Bioprocess Biosyst Eng
732 39(7):1023-1032.
- 733 30. Zhang J, Wang R, Jiang P, Liu Z. 2002. Production of an exopolysaccharide bioflocculant
734 by *Sorangium cellulosum*. Lett Appl Microbiol 34:178-81.
- 735 31. Nielsen SS. 2010. Phenol-sulfuric acid method for total carbohydrates. In *Food Analysis*
736 *Laboratory Manual*, Springer USA. Pp. 47-53.
- 737 32. Dubois M, Gilles JK, Hamilton PA, Rebers PA, Smith F. 1956. Colorimetric method for
738 determination of sugars and related substances. Anal Chem 28(3), 350–356.
- 739 33. Euzenat O, Guibert A, Combes D. 1997. Production of fructo-oligosaccharides by
740 levansucrase from *Bacillus subtilis* C4. Process Biochem 32(3):237-243.
- 741 34. Bradford MM. 1976. A rapid and sensitive method for the quantitation of microgram
742 quantities of protein utilizing the principle of protein-dye binding. Anal Biochem 72: 248-
743 254.
- 744 35. Rütering M, Cress BF, Schilling M, Ruhmann B, Koffas MAG, Sieber V, Schmid J. 2017.
745 Tailor-made exopolysaccharides-CRISPR-Cas9 mediated genome editing in *Paenibacillus*
746 *polymyxa*. Synth Biol 2(1): ysx007.
- 747 36. Rütering M, Schmid J, Rühmann B, Schilling M, Sieber V. 2016. Controlled production of
748 polysaccharides—exploiting nutrient supply for levan and heteropolysaccharide formation in
749 *Paenibacillus* sp. Carbohydr Polym 148:326-34.
- 750 37. Choi HJ, Kim CS, Kim P, Jung HC, Oh DK. 2004. Lactosucrose bioconversion from
751 lactose and sucrose by whole cells of *Paenibacillus polymyxa* harboring levansucrase
752 activity. Biotechnol Prog 20(6):1876-9.
- 753 38. Yanase H, Iwata M, Nakahigashi R, Kita K, Kato N, Tonomura K. 1992. Purification,
754 crystallization, and properties of the extracellular levansucrase from *Zymomonas mobilis*.
755 Biosci Biotechnol Biochem 56(8):1335-7.

- 756 39. Arietta JG, Sotolongo M, Menendez C, Alfonso D, Trujillo LE, Soto M, Ramirez R,
757 Hernandez L. 2004. A type II protein secretory pathway required for levansucrase secretion
758 by *Gluconacetobacter diazotrophicus*. J Bacteriol 186:15031-5039.
- 759 40. Bezzate S, Aymerich S, Chambert R, Czarnes S, Berge O, Heulin T. 2000. Disruption of
760 the *Paenibacillus polymyxa* levansucrase gene impairs its ability to aggregate soil in the
761 wheat rhizosphere. Environ Microbiol 2:333-342.
- 762 41. Gurunathan S, Gunasekaran, P. 2004. Differential expression of *Zymomonas mobilis*
763 sucrose genes (*SacB* and *SacC*) in *Escherichia coli* and sucrose mutants of *Zymomonas*
764 *mobilis*. Braz Arch Biol Technol 47(3):329-338.
- 765 42. Koepsell HJ, Tsuchiya HM, Hellman NN, Kazenko, A, Hoffman CA, Sharpe ES, Jackson
766 RW. 1953. Enzymatic synthesis of dextran acceptor specificity and chain initiation. J Biol
767 Chem 200(2):793-801.
- 768 43. Esser K, Kadereit JW, Lüttge U, Runge M. 2012. Progress in Botany: Genetics Cell
769 Biology and Physiology Systematics and Comparative Morphology Ecology and
770 Vegetation Science. Springer Science & Business Media
- 771 44. Colvin KM, Irie Y, Tart CS, Urbano R, Whitney JC, Ryder C, Howell PL, Wozniak DJ,
772 Parsek MR. 2012. The Pel and Psl polysaccharides provide *Pseudomonas aeruginosa*
773 structural redundancy within the biofilm matrix. Environ Microbiol 14(8):1913-28.
- 774 45. Cooley BJ, Dellos-Nolan S, Dhamani N, Todd R, Waller W, Wozniak D, Gordon VD.
775 2016. Asymmetry and inequity in the inheritance of a bacterial adhesive. New J Phys
776 18(4):045019.
- 777 46. Papagianni M, Psomas SK, Batsilas L, Paras SV, Kyriakidis DA, Liakopoulou-Kyriakides
778 M. 2001. Xanthan production by *Xanthomonas campestris* in batch cultures. Process
779 Biochem 37(1):73-80.
- 780 47. Saudagar PS, Singhal RS. 2004 Fermentative production of curdlan. Appl Biochem
781 Biotechnol 118(1):21-31.
- 782 48. Zhang Z, Chen H. 2010. Fermentation performance and structure characteristics of xanthan
783 produced by *Xanthomonas campestris* with a glucose/xylose mixture. Appl Biochem
784 Biotechnol 160(6):1653-63.
- 785 49. Han B, Gopalan V, Ezeji TC. 2011. Acetone production in solventogenic *Clostridium*
786 species: new insights from non-enzymatic decarboxylation of acetoacetate. Appl Microbiol
787 Biotechnol 91(3):565-76.
- 788 50. Ren C, Gu Y, Hu S, Wu Y, Wang P, Yang Y, Yang C, Yang S, Jiang W. 2010.
789 Identification and inactivation of pleiotropic regulator CcpA to eliminate glucose repression
790 of xylose utilization in *Clostridium acetobutylicum*. Metab Eng 12(5):446-54.
- 791 51. Han B, Ujor V, Lai LB, Gopalan V, Ezeji TC. 2013. Use of proteomic analysis to elucidate
792 the role of calcium in acetone-butanol-ethanol fermentation by *Clostridium beijerinckii*
793 NCIMB 8052. Appl Environ Microbiol 79(1):282-93.
- 794 52. Hansen LT, Austin JW, Gill TA. 2001. Antibacterial effect of protamine in combination
795 with EDTA and refrigeration. Int J Food Microbiol 66: 149 –161.
- 796 53. Kotra LP, Golemi D, Amro NA, Liu GY, Mobashery S. 1999. Dynamics of the
797 lipopolysaccharides assembly on the surface of *Escherichia coli*. J Am Chem Soc
798 121:8707–8711.
- 799

800

801

802 **List of tables**

803 **Table 1.** Comparison of protein and nucleotide sequences between *P. polymyxa* DSM 365
804 levansucrase and other *P. polymyxa* strains with complete genome sequence using NCBI Blastp and
805 Blastn algorithms for alignment.

806 **Table 2.** List of microorganisms, vectors and enzymes used in this study and their respective
807 characteristics and sources

808 **Table 3.** List of primers used to generate levansucrase inactivation construct, and to perform qRT-
809 PCR.

810 **Table 4.** Substrate consumed, growth, maximum products, 2,3-BD yield and productivity during
811 **sucrose** fermentation by *P. polymyxa* DSM 365 wildtype and levansucrase null mutant.

812 **Table 5.** Substrate consumed, growth, maximum products, 2,3-BD yield and productivity during
813 **glucose** fermentation by *P. polymyxa* DSM 365 wildtype and levansucrase null mutant.

814 **Figure legends**

815 **Figure 1.** Levansucrase inactivation construct generation. **A:** Recombinant pGEM7Zf-LevfragA-
816 Erm-LevfragB generated from the parent plasmid, pGEM7Zf(+). **B:** levansucrase gene was
817 amplified from the genome of *P. polymyxa* and was used to generate the inactivation construct with
818 erythromycin gene placed between the upstream (210 bp) sequence (LevFragA) and downstream
819 (213 bp) sequence (LevFragB) of levansucrase gene. The construct was ligated into previously
820 double digested pGEM7Zf(+) and used to inactivate levansucrase gene in the chromosome of *P.*
821 *polymyxa* via double-cross homologous recombination. **C.** Gel image showing levansucrase gene,
822 LevFragA, LevFragB, ERM, LevFragA-ERM and LevFragA-ERM-LevFragB gene fragments
823 during generation of levansucrase inactivation construct.

824 **Figure 2. A:** Gel image showing colony PCR of *P. polymyxa* levansucrase null mutant. Lanes
825 show bands corresponding to LevFragA-ERM, ERM and ERM-LevfragB gene fragments. Other
826 lanes show 1kb DNA ladder and pGEM7Zf+ harboring the levansucrase inactivation construct
827 (bands from colonies 1 and 2). **B:** Precipitation of EPS in the fermentation broth of *P. polymyxa*
828 wildtype and levansucrase null mutant in sucrose medium.

829 **Figure 3:** Fermentation profile of *P. polymyxa* levansucrase null mutant and wildtype grown in
830 **sucrose** medium without CaCl₂ supplementation. X represents no levansucrase activity.

831 **Figure 4:** Fermentation profile of *P. polymyxa* levansucrase null mutant and wildtype grown in
832 **sucrose** medium supplemented with 0.2 g/L CaCl₂. X represents no levansucrase activity.

833 **Figure 5:** Fermentation profile of *P. polymyxa* levansucrase null mutant and wildtype grown in
834 **sucrose** medium supplemented with 0.4 g/L CaCl₂. X represents no levansucrase activity.

835 **Figure 6.** Comparisons of mRNA transcript levels of polysaccharide polymerase (*Pop*), flippase
836 (*flip*), exopolysaccharide biosynthesis protein (*EBP*), levansucrase (*lev*), and erythromycin (*ERM*)
837 genes of *P. polymyxa* wildtype (WT) and levansucrase null mutant (Lev MT) grown in sucrose (**A**)
838 and glucose (**B**) media. X represents no mRNA detection.

839 **Figure 7.** Schematic representation of annotated and putative pathways of EPS production by *P.*
840 *polymyxa*. The schematic diagram was conceived based on our enzymatic assays, qRT-PCR data
841 and annotated metabolic network model of *P. polymyxa* in KEGG databases. The red and black
842 fonts or lines represent annotated and putative EPS production pathways in *P. polymyxa*,
843 respectively. 1, levansucrase; 2, sugar PTS; 3, phosphoglucomutase; 4, UTP-glucose 1-phosphate
844 uridylyltransferase; 5, glucose 1-phosphate thymidylyltransferase; 6, galactose -1-phosphate
845 uridylyltransferase; 7, UDP-glucose 6-dehydrogenase; 8, dTDP-glucose 4,6-dehydratase; 9, dTDP-

846 4-dehydrorhamnose 3,5-epimerase; 10, dTDP-4-dehydrorhamnose reductase; 11, polymerase
847 synthase; 12, exopolysaccharide biosynthesis protein; 13, flippase. The broken black arrows
848 represent EPS polymerization steps from sugar nucleotides. The genes that code the enzymes
849 (numbers 11, 12, and 13) in blue font were analyzed by qRT-PCR.

850

851

852

853

854

855

856

857

858

859

860

861

862

863

864

865

866

867

868

869

870

871

872

873

874

875 **Table 1.**

S/N	Levansucrase	% Protein identity to <i>P. polymyxa</i> DSM 365	% Nucleotide sequence identity to <i>P. polymyxa</i> DSM 365	Accession number
1	<i>P. polymyxa</i> SC2	95	92	NC_014622.2
2	<i>P. polymyxa</i> E681	97	96	NC_024483.2
3	<i>P. polymyxa</i> M1	95	92	NC_017542.1
4	<i>P. polymyxa</i> CR1	97	96	NC_023037.2

876

877

878

879

880

881

882

883

884

885

886

887

888

889

890

891

892

893

894

895

896

897

898 **Table 2.**

Strain/vector/enzymes	Characteristics	Source
<i>Strains</i>		
<i>E. coli</i> JM109	endA1, recA1, gyrA96, relA1	Promega Corporation
<i>P. polymyxa</i> DSM 365	Wildtype	DSMZ, Germany
<i>P. polymyxa</i> DSM 365 Lev null mutant	Δ Lev; Erm ^r	This study
<i>Vectors</i>		
pMutin	Erm ^r	Bacillus Genetic Stock Center, OH
pGEM7Zf(+)	Amp ^r , f1 oriC, lacZ	Promega Corporation
<i>Enzymes</i>		
GXL DNA polymerase	High fidelity, amplifies GC-rich templates	Takara Clontech
BamHI	-	New England Biolabs
XhoI	-	New England Biolabs
T4 DNA ligase	-	New England Biolabs

899

900 **Table 3.**

	Primer code	Primer sequence (5'→3')
Primers used to create levansucrase inactivation construct	LevFragA_fwd:	TGG <u>GGA TCC</u> TTG AAG TTT AAC AAA TGG TTC AGT AAA GC
	LevFragA_rev:	CCT CCT AAA CAG TTA GGA CGG AAC CTC ATA TTT CTC TTT GCC
	LevFragB_fwd:	ACT CTT ATT TTT TTA ATA TTG TTT CAT AGT GGC AAT AAC GTA GTC G
	LevFragB_rev:	GGG <u>CTC GAG</u> TTA TTT CTT TCC ATA CTC ATT TGG AG
	Erm_fwd:	TAA CTG TTT <u>AGG AGG</u> ACT GAT AAT ATG AAC AAA AAT ATA AAA TAT TCT CAA AAC
	Erm_rev1:	TAA AAA AAT AAG AGT TAC CAT TTA TTA TTT CCT CCC GTT AAA TAA TAG ATA AC
	Erm_rev2:	GCC ACT ATG AAA CAA TAT TAA AAA AAT AAG AGT TAC CAT TTA TTA TTT CC
Primers for qRT-PCR	Lev_Fwd	GTACAGCAAAGCGTCGGAAT
	Lev_Rev	CCGGTTTCTGTTCCTGTGTT
	Erythromycin_Fwd	GGTTGCTCTTGCACACTCAA
	Erythromycin_Rev	CTGTGGTATGGCGGGTAAGT
	Polysaccharide polymerase_Fwd	GCGTTCGTCGGTTTATCACT
	Polysaccharide polymerase_Rev	GAATGCAGCCCTAGAACCTG
	Flippase_Fwd	CGTTCCAAGCAGAAAGGAAG
	Flippase_Rev	AGACAACAGCGAACCTGCTT
	Exopolysaccharide biosynthesis protein_Fwd	GGTCACATTCTGGCCTGTCT
	Exopolysaccharide biosynthesis protein_Rev	CTAAACAGCTTCGCCTTTGG
	16S rRNA_Fwd	GGCTTTCCAGCTACCTGTTG
16S rRNA_Rev	ACGGCGTCTTCAAAGGAGTA	

901 *NB: the underlined sequences represent either restriction sites or ribosomal binding site*

902

903

904

905 **Table 4.**

Treatment	WT + 0 g/L CaCl ₂	M + 0 g/L CaCl ₂	WT + 0.2 g/L CaCl ₂	M + 0.2 g/L CaCl ₂	WT + 0.4 g/L CaCl ₂	M + 0.4 g/L CaCl ₂
Sucrose consumed (g/L)	101.9±0.3 ^a	84.7±3.0 ^b	110.1±0.5 ^a	84.5±1.2 ^a	107.9±0.4 ^a	92.8±1.3 ^b
Residual sucrose (g/L)	2.49±0.0 ^a	25.4±3.4 ^b	ND ^a	25.6±1.7 ^b	ND ^a	17.3±1.8 ^b
Residual glucose (g/L)	5.7±0.1 ^a	ND ^b	Nd ^a	Nd ^a	2.2±0.0 ^a	ND ^b
Max. growth (OD _{600nm})	6.8±0.4 ^a	9.7±0.4 ^b	10.4±1.1 ^a	12.7±1.1 ^b	9.6±0.9 ^a	12.8±0.9 ^b
Max. 2,3-BD (g/L)	32.6±0.7 ^a	30.9±2.3 ^a	36.3±2.0 ^a	35.7±1.7 ^a	36.1±2.5 ^a	37.4±0.9 ^a
EPS (g/L)	17.4±2.2 ^a	3.0±0.6 ^b	18.4±2.7 ^a	2.9±0.5 ^b	17.6±0.36 ^a	2.9±0.2 ^b
2,3-BD Yield (g/ g)	0.32±0.01 ^a	0.35±0.02 ^a	0.33±0.02 ^a	0.42±0.03 ^b	0.33±0.02 ^a	0.40±0.02 ^a
2,3-BD Productivity (g/L/h)	0.68±0.01 ^a	0.62±0.05 ^a	1.01±0.05 ^a	1.04±0.14 ^a	0.75±0.05 ^a	0.78±0.02 ^a
Acetoin (g/L)	2.6±0.2 ^a	4.1±0.4 ^b	21.6±3.8 ^a	5.0±0.5 ^b	1.3±0.4 ^b	6.0±0.6 ^b
Ethanol (g/L)	5.7±0.3 ^a	6.8±0.1 ^b	5.8±0.2 ^a	5.1±0.4 ^a	5.8±1.1 ^a	5.5±0.5 ^a
Acetic acid (g/L)	1.5±0.3 ^a	2.8±0.1 ^b	1.8±0.1 ^a	3.9±1.2 ^b	1.2±0.3 ^a	5.5±0.2 ^b

906 Fisher's LSD pairwise comparisons between wildtype and levansucrase mutant were conducted. Treatments with different
907 superscripts across a row are significant at $p < 0.05$. The maximum acetoin, ethanol and acetic acid generated during fermentations are
908 reported.

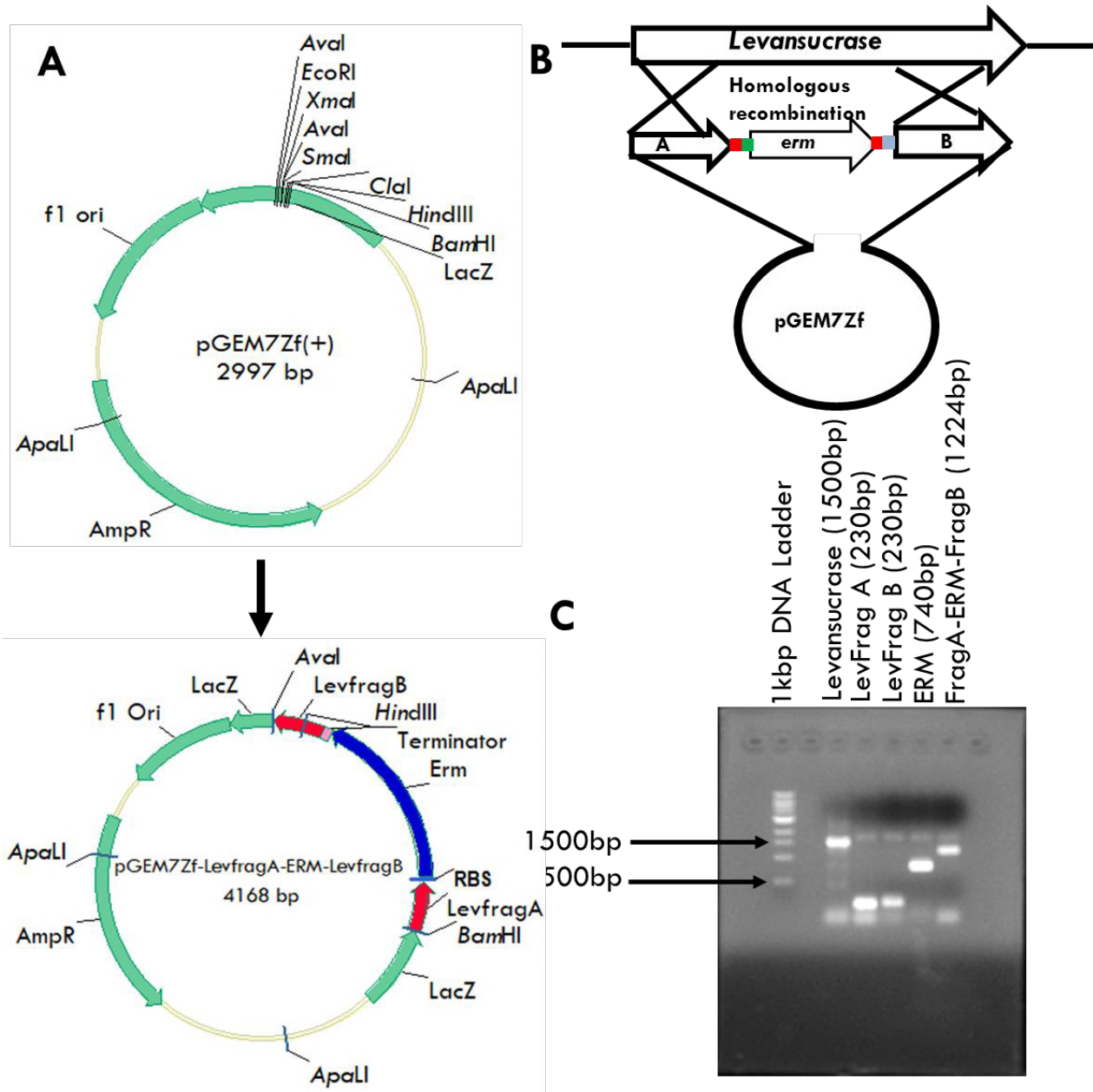
909 **Table 5.**

Treatment	WT + 0 g/L CaCl₂	M + 0 g/L CaCl₂	WT + 0.2 g/L CaCl₂	M + 0.2 g/L CaCl₂	WT + 0.4 g/L CaCl₂	M + 0.4 g/L CaCl₂
Glucose consumed (g/L)	85.6±3.9 ^a	87.8±1.9 ^a	96.1±3.1 ^a	105.0±0.0 ^a	94.7±2.7 ^a	106.7±2.5 ^b
Residual glucose (g/L)	23.7±3.2 ^a	21.45±1.2 ^a	13.2±2.3 ^a	4.3±0.7 ^b	14.5±2.0 ^a	2.5±1.8 ^b
Max. growth (OD _{600nm})	8.9±0.2 ^a	12.1±1.3 ^b	11.2±0.2 ^a	15.4±1.2 ^b	10.5±0.3 ^a	16.1±0.7 ^b
Max. 2,3-BD (g/L)	30.7±1.2 ^a	29.8±2.0 ^a	34.2±2.7 ^a	39.0±1.3 ^a	34.5±3.4 ^a	39.4±4.4 ^a
EPS (g/L)	5.5±0.4 ^a	2.27±0.1 ^b	4.2±0.2 ^a	2.4±0.3 ^b	5.4±0.5 ^a	2.8±0.2 ^b
2,3-BD Yield (g/ g)	0.36±0.01 ^a	0.34±0.02 ^a	0.36±0.02 ^a	0.37±0.01 ^a	0.37±0.04 ^a	0.38±0.04 ^a
2,3-BD Productivity (g/L/h)	0.51±0.02 ^a	0.57±0.09 ^a	0.71±0.06 ^a	1.62±0.05 ^b	0.72±0.07 ^a	1.64±0.19 ^b
Acetoin (g/L)	3.3±0.0 ^a	2.4±0.4 ^b	10.1±2.1 ^a	2.8±0.4 ^b	8.8±1.1 ^a	2.6±0.3 ^b
Ethanol (g/L)	5.8±0.1 ^a	7.1±0.3 ^b	5.6±0.4 ^a	8.7±0.7 ^b	5.4±0.5 ^a	9.4±0.2 ^b
Acetic acid (g/L)	0.0±0.0 ^a	1.7±0.0 ^b	0.6±0.0 ^a	2.5±0.9 ^b	0.0±0.0 ^b	2.9±0.1 ^b

910 Fisher's LSD pairwise comparisons between wildtype and levansucrase mutant were conducted. Treatments with different
911 superscripts across a row are significant at $p < 0.05$. The maximum acetoin, ethanol and acetic acid generated during fermentations are
912 reported.

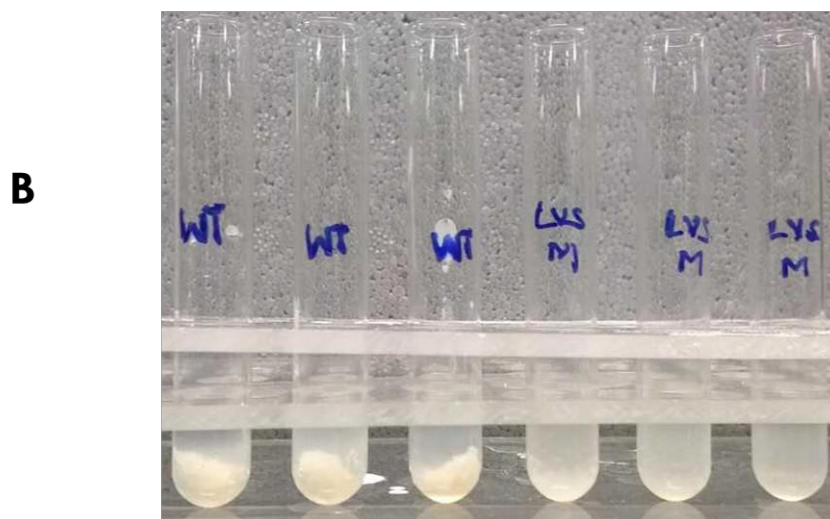
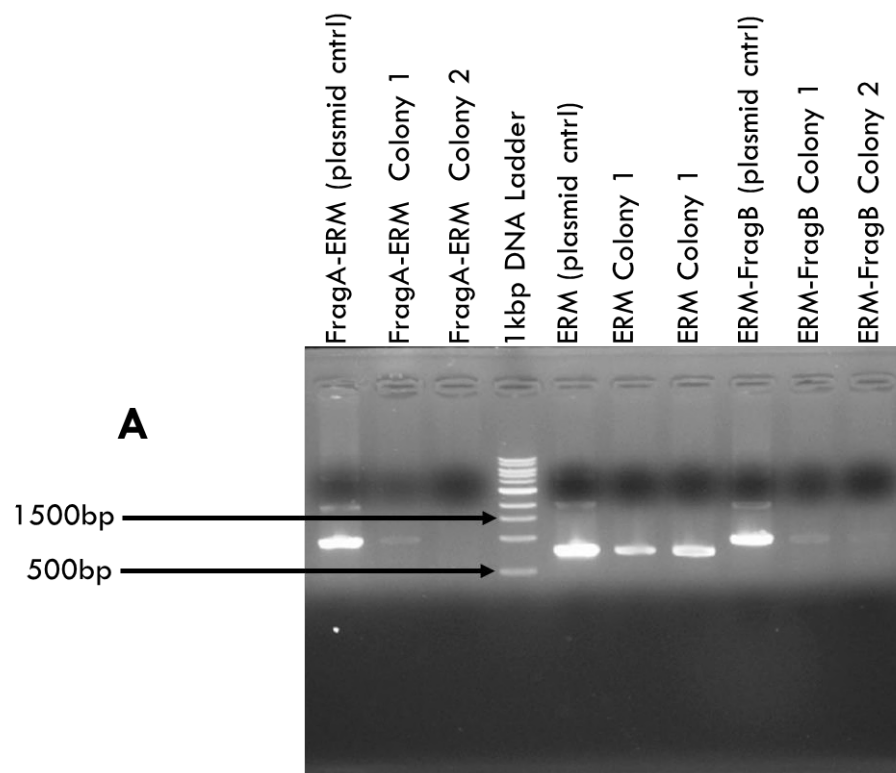
913

914



915

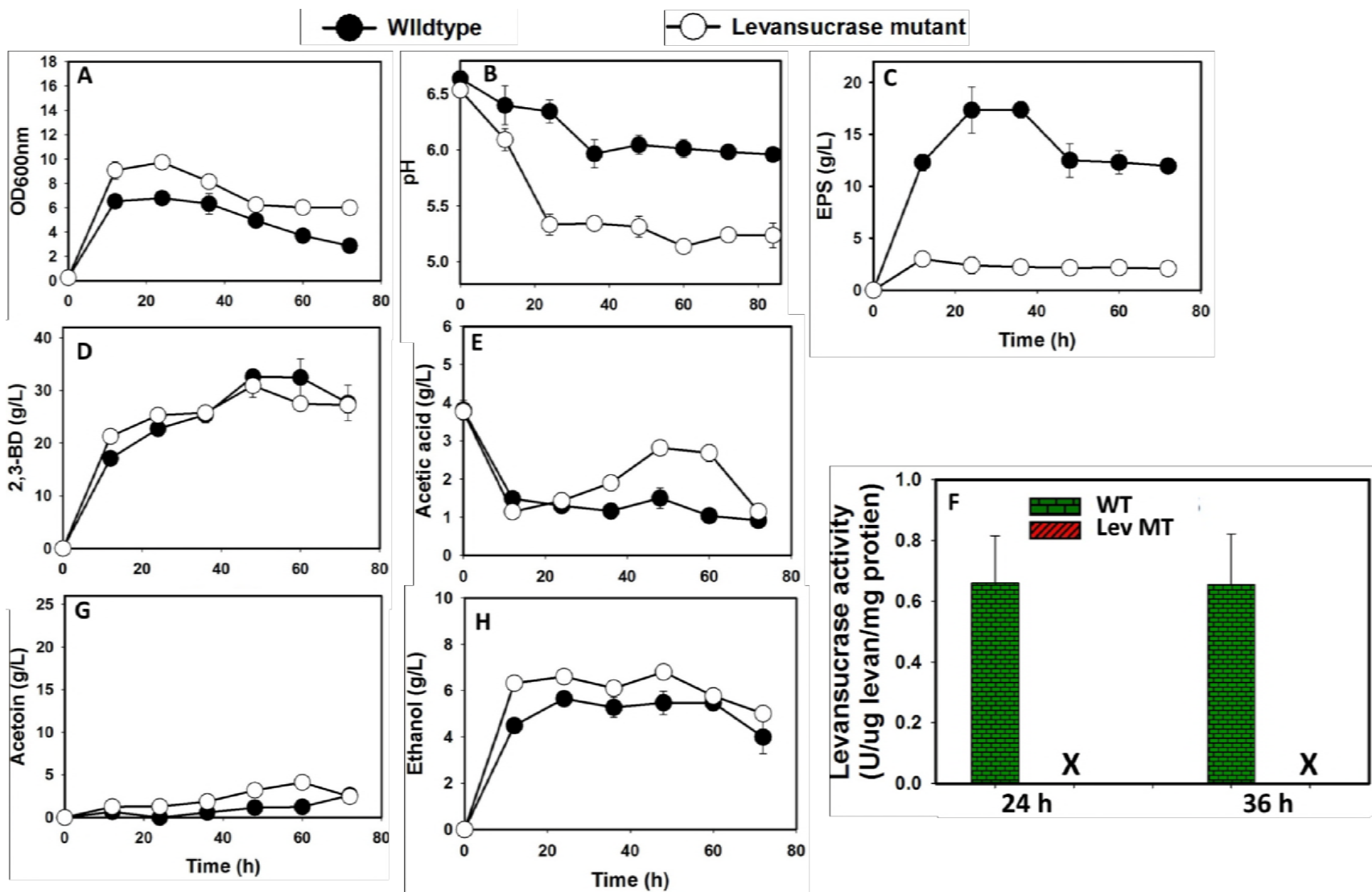
916 **Figure 1**



917

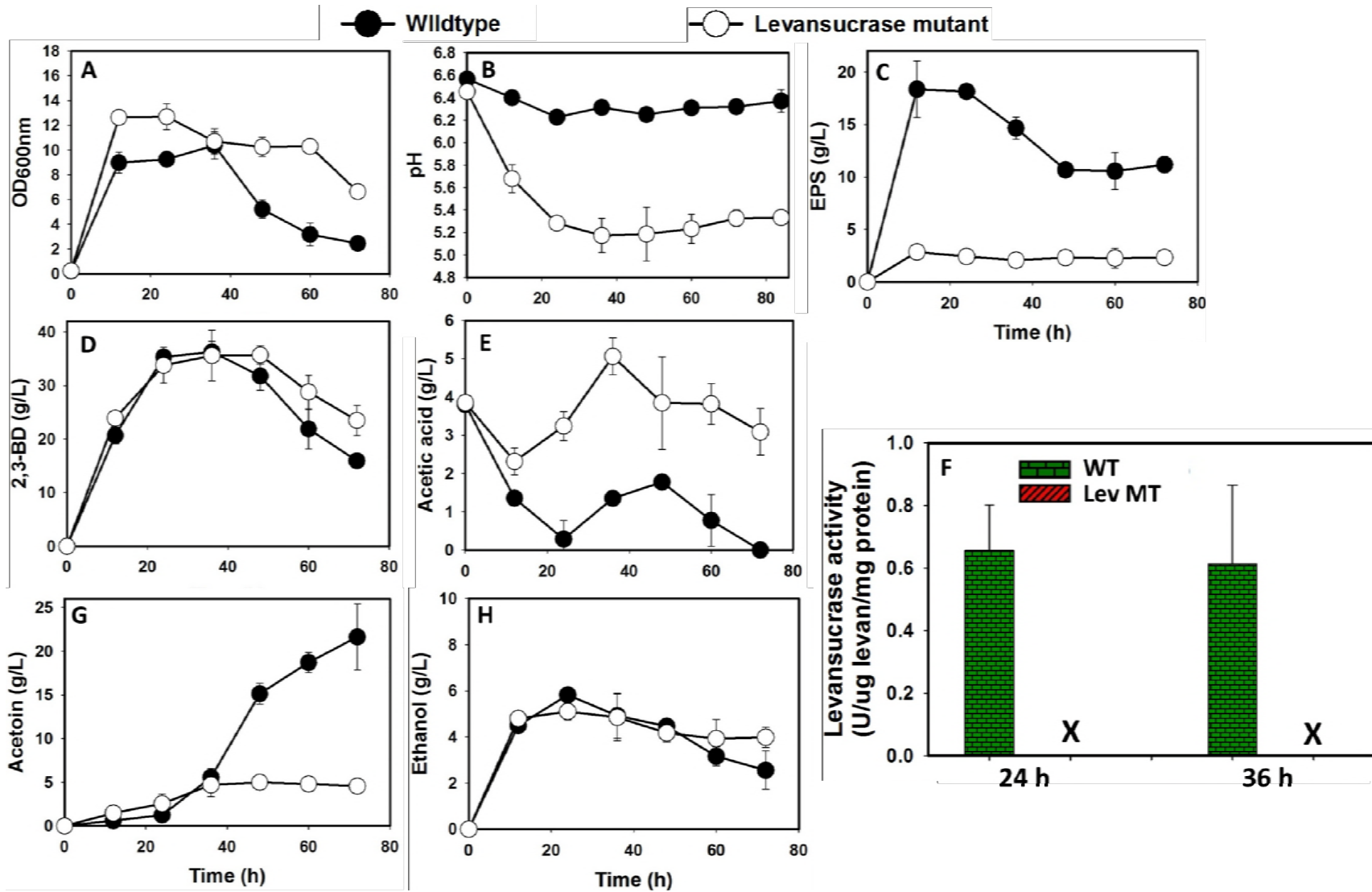
918 **Figure 2**

919



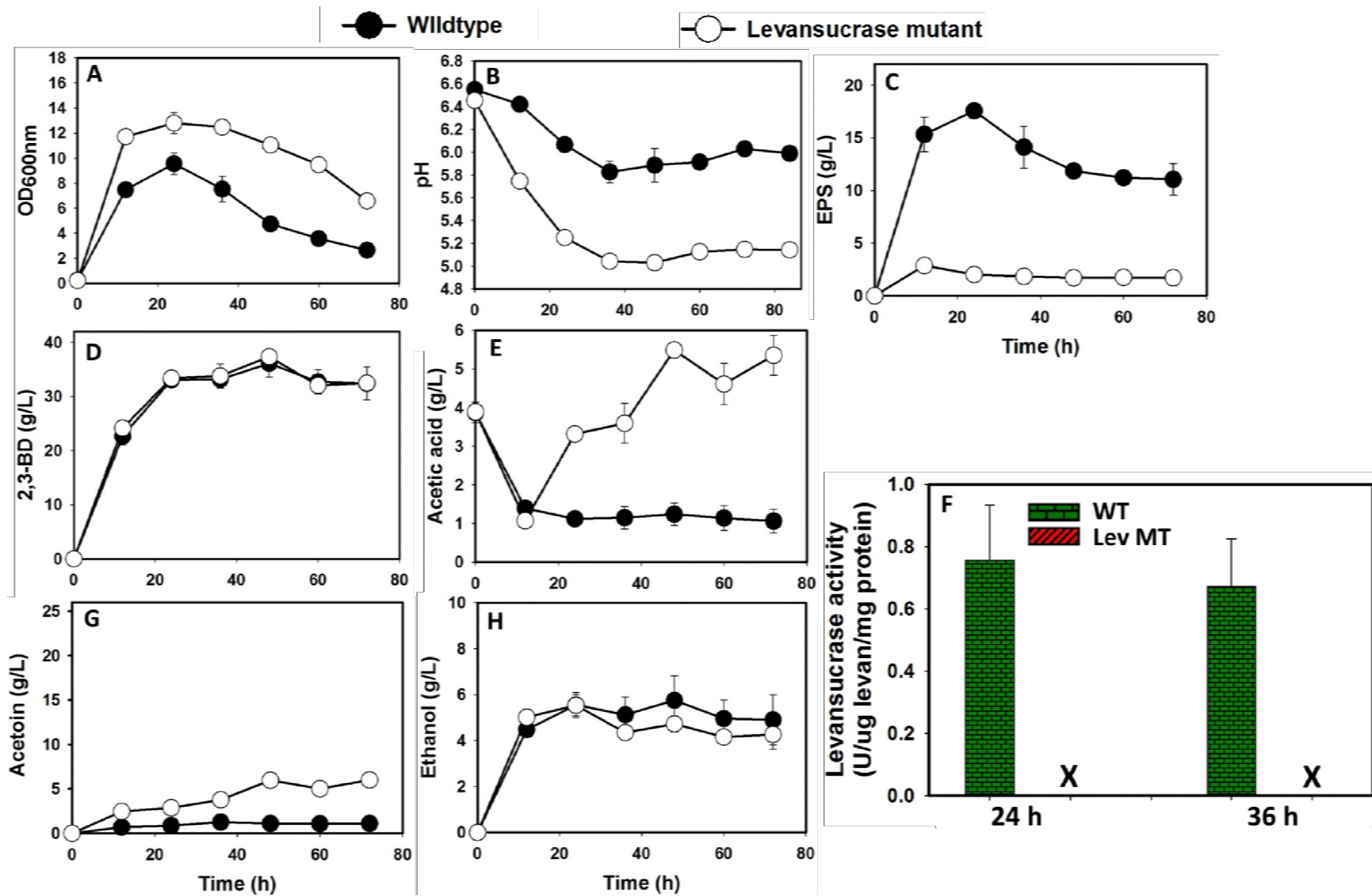
920

921 **Figure 3**



922

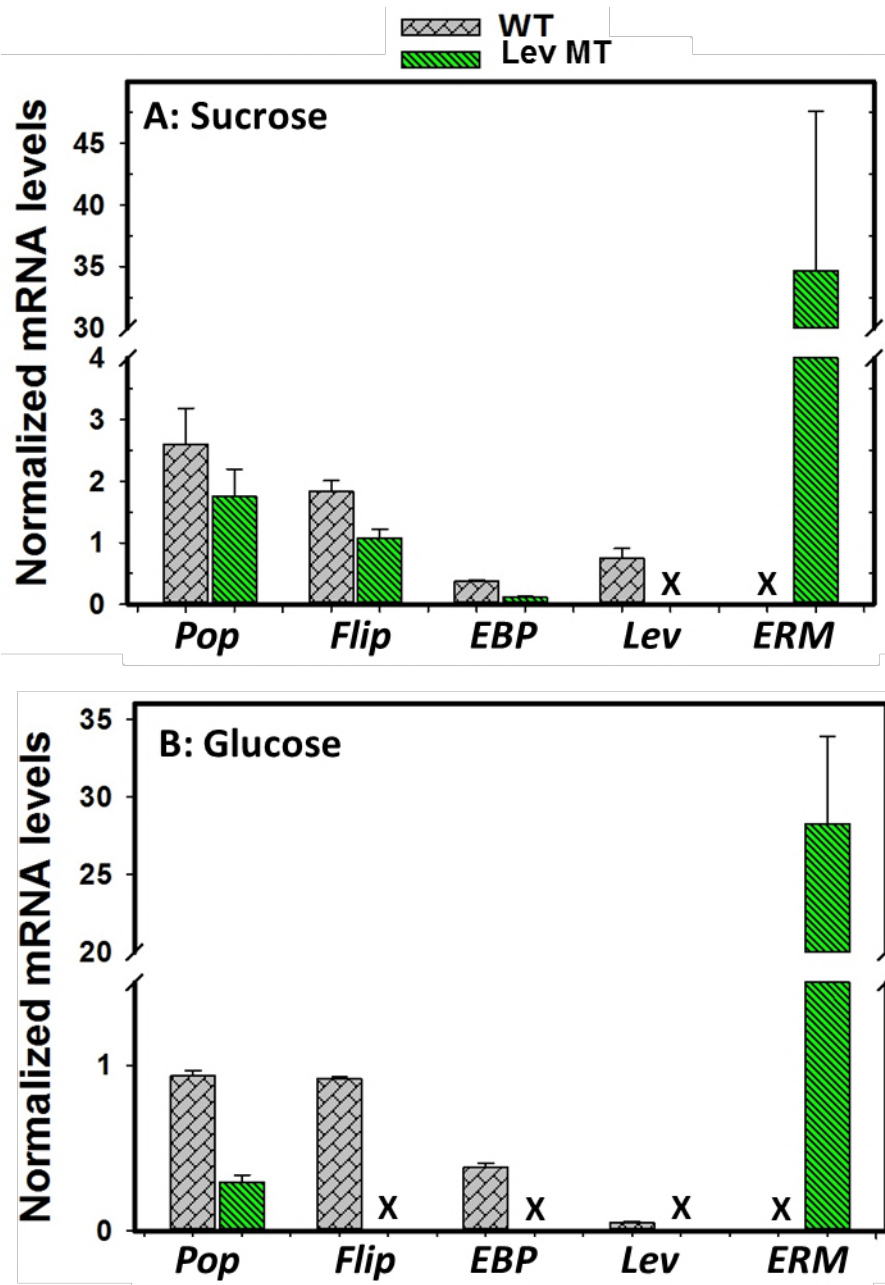
923 **Figure 4**



924
925
926

Figure 5

927



928

929 **Figure 6**

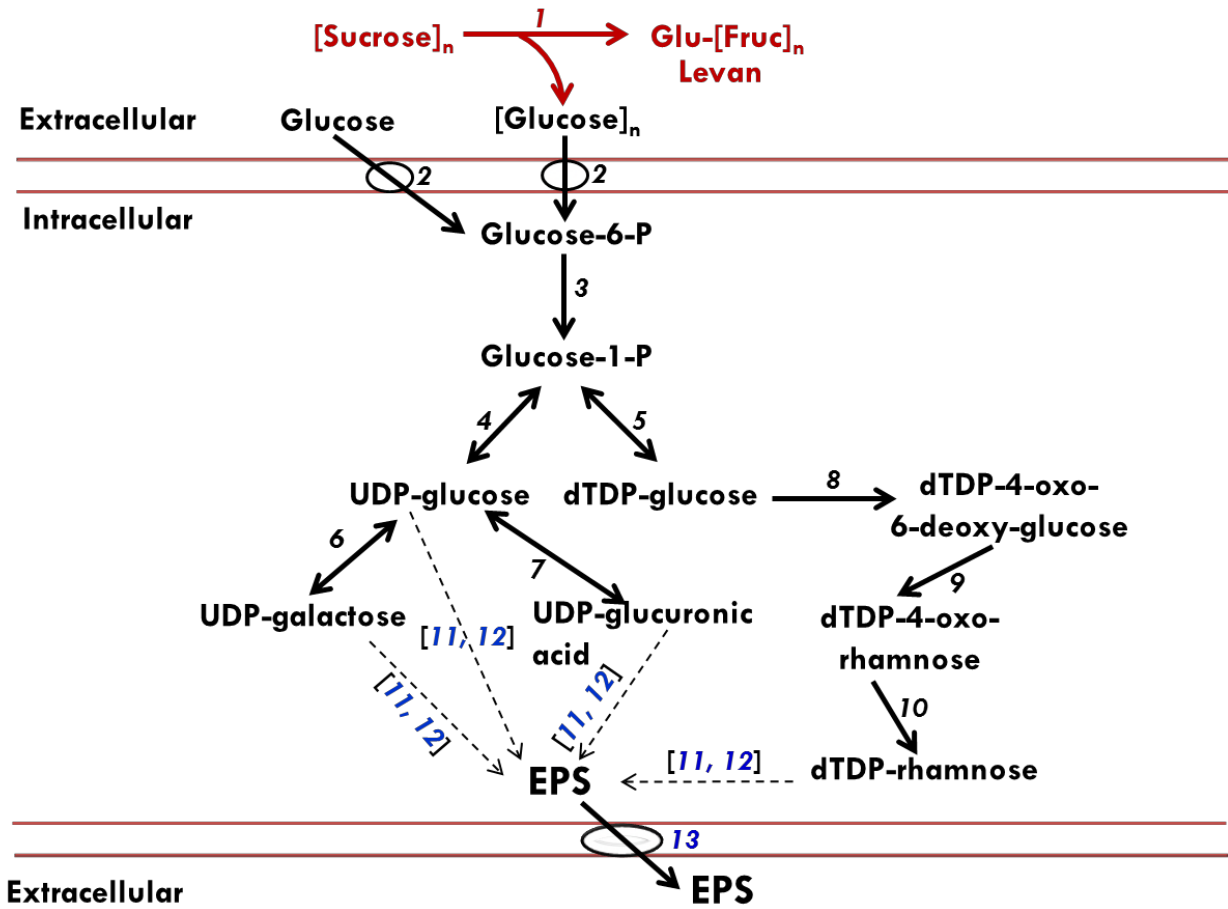
930

931

932

933

934
935
936



937

938 **Figure 7**