

1 Host engineering for improved valerolactam production in *Pseudomonas putida*

2 Mitchell G. Thompson<sup>1,2,3</sup>, Luis E. Valencia<sup>1,2,4</sup>, Jacquelyn M. Blake-Hedges<sup>1,2,5</sup>, Pablo Cruz-

3 Morales<sup>1,2,6</sup>, Alexandria E. Velasquez<sup>1,2</sup>, Allison N. Pearson<sup>1,2</sup>, Lauren N. Sermeno<sup>1,2</sup>, William

4 A. Sharpless<sup>1,2</sup>, Veronica T. Benites<sup>1,2</sup>, Yan Chen<sup>1,2</sup>, Edward E. K. Baidoo<sup>1,2</sup>, Christopher J.

5 Petzold<sup>1,2</sup>, Adam M. Deutschbauer<sup>3,7</sup>, Jay D. Keasling<sup>1,2,4,8,9,10</sup>

6 <sup>1</sup>Joint BioEnergy Institute, 5885 Hollis Street, Emeryville, CA 94608, USA.

7 <sup>2</sup>Biological Systems & Engineering Division, Lawrence Berkeley National Laboratory, Berkeley,

8 CA 94720, USA.

9 <sup>3</sup>Department of Plant and Microbial Biology, University of California, Berkeley, CA 94720,

10 USA

11 <sup>4</sup>Joint Program in Bioengineering, University of California, Berkeley/San Francisco, CA 94720,

12 USA

13 <sup>5</sup>Department of Chemistry, University of California, Berkeley, CA 94720, USA

14 <sup>6</sup>Centro de Biotecnología FEMSA, Instituto Tecnológico y de Estudios superiores de Monterrey,

15 Mexico

16 <sup>7</sup>Environmental Genomics and Systems Biology Division, Lawrence Berkeley National

17 Laboratory, Berkeley, California, USA

18 <sup>8</sup>Department of Chemical and Biomolecular Engineering, University of California, Berkeley, CA

19 94720, USA

20 <sup>9</sup>The Novo Nordisk Foundation Center for Biosustainability, Technical University of Denmark,

21 Denmark

22 <sup>10</sup>Center for Synthetic Biochemistry, Institute for Synthetic Biology, Shenzhen Institutes for

23 Advanced Technologies, Shenzhen, China

24

## 25 **ABSTRACT**

26 *Pseudomonas putida* is a promising bacterial chassis for metabolic engineering given its  
27 ability to metabolize a wide array of carbon sources, especially aromatic compounds derived  
28 from lignin. However, this omnivorous metabolism can also be a hindrance when it can naturally  
29 metabolize products produced from engineered pathways. Herein we show that *P. putida* is able  
30 to use valerolactam as a sole carbon source, as well as degrade caprolactam. Lactams represent  
31 important nylon precursors, and are produced in quantities exceeding one million tons per  
32 year[1]. To better understand this metabolism we use a combination of Random Barcode  
33 Transposon Sequencing (RB-TnSeq) and shotgun proteomics to identify the *oplBA* locus as the  
34 likely responsible amide hydrolase that initiates valerolactam catabolism. Deletion of the *oplBA*  
35 genes prevented *P. putida* from growing on valerolactam, prevented the degradation of  
36 valerolactam in rich media, and dramatically reduced caprolactam degradation under the same  
37 conditions. Deletion of *oplBA*, as well as pathways that compete for precursors L-lysine or 5-  
38 aminovalerate, increased the titer of valerolactam from undetectable after 48 hours of production  
39 to ~90 mg/L. This work may serve as a template to rapidly eliminate undesirable metabolism in  
40 non-model hosts in future metabolic engineering efforts.

## 41 **1 INTRODUCTION**

42 *Pseudomonas putida* has attracted great attention as a potential chassis organism for  
43 metabolic engineering due in large part to its ability to metabolize a wide variety of carbon  
44 sources, particularly aromatic compounds that can be derived from lignin [2,3]. To more fully  
45 realize this vision, much effort has been put forth recently to better characterize the central  
46 metabolism of *P. putida* with updated genome-scale models [4], C<sup>13</sup> flux experiments [5,6], and  
47 high-throughput fitness assays, which have all contributed to a more complete understanding of

48 the bacterium [7,8]. Despite these advances, the metabolic capabilities of *P. putida* are not yet  
49 fully understood.

50 One consequence of this omnivorous metabolism is that *P. putida* possesses the ability to  
51 degrade or fully catabolize chemicals metabolic engineers seek to produce in the host. An  
52 ongoing challenge for *P. putida* host engineering will be to rapidly identify catabolic pathways  
53 of important target molecules and eliminate them from the genome. The recent report of a novel  
54 pathway for levulinic acid catabolism in *P. putida* KT2440 underscores the catabolic flexibility  
55 of the host, and an additional obstacle towards producing high product titer [8]. While  
56 challenging, this is not surprising; as a genus, *Pseudomonads* are well known for their ability to  
57 degrade a wide range of naturally occurring or xenobiotic chemicals [9,10].

58 Caprolactam and valerolactam are both important commodity chemicals used in the  
59 synthesis of nylon polymers, with global production of caprolactam reaching over four million  
60 metric tons [1]. Multiple efforts have been made to produce these chemicals biologically, with  
61 the titers of valerolactam approaching 1g/L in *Escherichia coli* [1,11]. The engineered pathway  
62 to valerolactam in *E. coli* converts L-lysine to 5-aminovalerate (5AVA) via DavBA, two genes  
63 endogenous to *P. putida*, and then cyclizes it via a promiscuous coA-ligase [1]. While the  
64 endogenous L-lysine catabolism of *P. putida* has been leveraged to produce the C5  
65 diacid glutarate, there has yet to be any attempt to produce valerolactam in the bacterium [12]. A  
66 recent report that *Pseudomonas jessenii* can catabolize caprolactam suggested that catabolism of  
67 lactams could dramatically impact titers of valerolactam in *P. putida* [13].

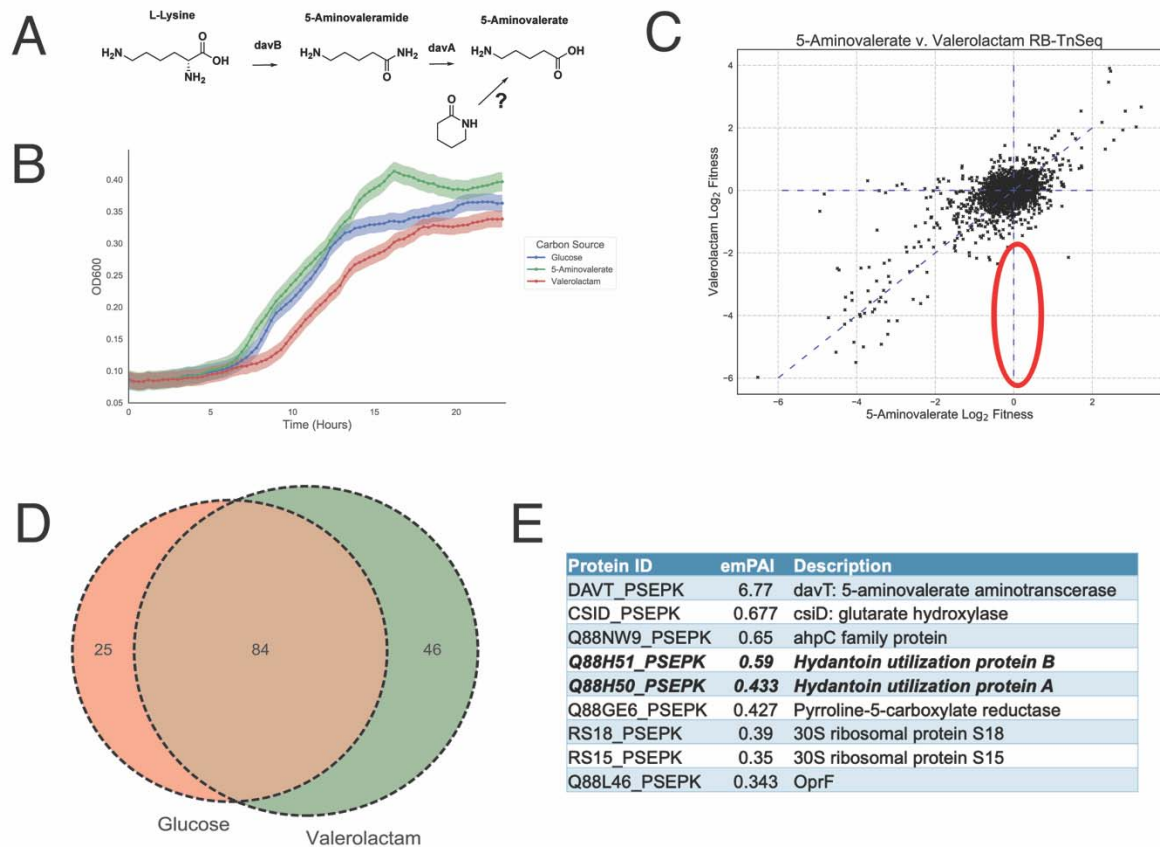
68 In this work we demonstrate that *P. putida* can utilize valerolactam as a sole carbon  
69 source, as well as degrade caprolactam. Using a combination of Random Barcode Transposon  
70 Sequencing (RB-TnSeq) and shotgun proteomics we were able to identify that OplBA, a

71 predicted oxoprolinase, is responsible for this hydrolysis. By knocking out *opIBA* in addition to  
72 two pathways that compete for precursors we were able to dramatically increase the titers of  
73 valerolactam in *P. putida*.

## 74 **2 RESULTS**

### 75 2.1 Identification of a lactam hydrolase in *P. putida*

76 The hydrolysis product of valerolactam is 5AVA, an intermediate in L-lysine metabolism  
77 (Figure 1A). Growth curves of *P. putida* on valerolactam as a sole carbon source demonstrated  
78 that the bacterium was readily able to catabolize valerolactam and produce biomass, with growth  
79 similar to that on either 5AVA and glucose (Figure 1B). Initially, we attempted to identify the  
80 enzyme responsible for valerolactam hydrolysis using RB-TnSeq, a technique that has previously  
81 been used to identify novel enzymes in D-lysine metabolism [7]. RB-TnSeq measures the  
82 relative fitness of transposon mutant pools to infer gene function through changes in relative  
83 abundance of all non-essential genes in a bacterium under a selective condition [14,15]. Mutant  
84 pools of *P. putida* were grown on either 5AVA or valerolactam as a sole carbon source in an  
85 attempt to identify enzymes solely essential for growth on valerolactam. Results of RB-TnSeq  
86 experiments suggested that valerolactam was indeed being catabolized through the same  
87 pathway as 5AVA with both conditions showing significant defects in the *davTD* and *csiD-lghO*  
88 operons, the known catabolic route of 5AVA to the TCA cycle (Figure S1A). However, there  
89 were no genes that showed obvious fitness defects only under the valerolactam growth condition  
90 (Figure 1C).



91

92 **Figure 1: Identification of the *P. putida* valerolactam hydrolase: (A) Route of valerolactam**

93 **catabolism through the L-lysine catabolic route of *P. putida* (B) Growth of *P. putida* in**

94 **minimal medium supplemented with either 10 mM glucose, 5AVA, or valerolactam.**

95 **Shaded area represents the 95% confidence interval (cI), n=3. (C) RB-TnSeq analysis of**

96 **genome fitness assays of *P. putida* libraries grown on either 5AVA or valerolactam as a sole**

97 **carbon source. Red oval shows the predicted fitness result of a valerolactam hydrolase. (D)**

98 **Results of shotgun proteomics of proteins found in the supernatant of *P. putida* grown on**

99 **either 10 mM glucose or 10 mM valerolactam as a sole carbon source. Venn diagram shows**

100 **the number of proteins with an exponentially modified protein abundance index (emPAI)**

101 **relative abundance above 0.1 shared or unique to each carbon source (E) Table shows the**

102 **most abundant proteins specific to grown on valerolactam. OplA (Q88H50\_PSEPK) and**  
103 **OplB (Q88H51\_PSEPK) are in bold.**

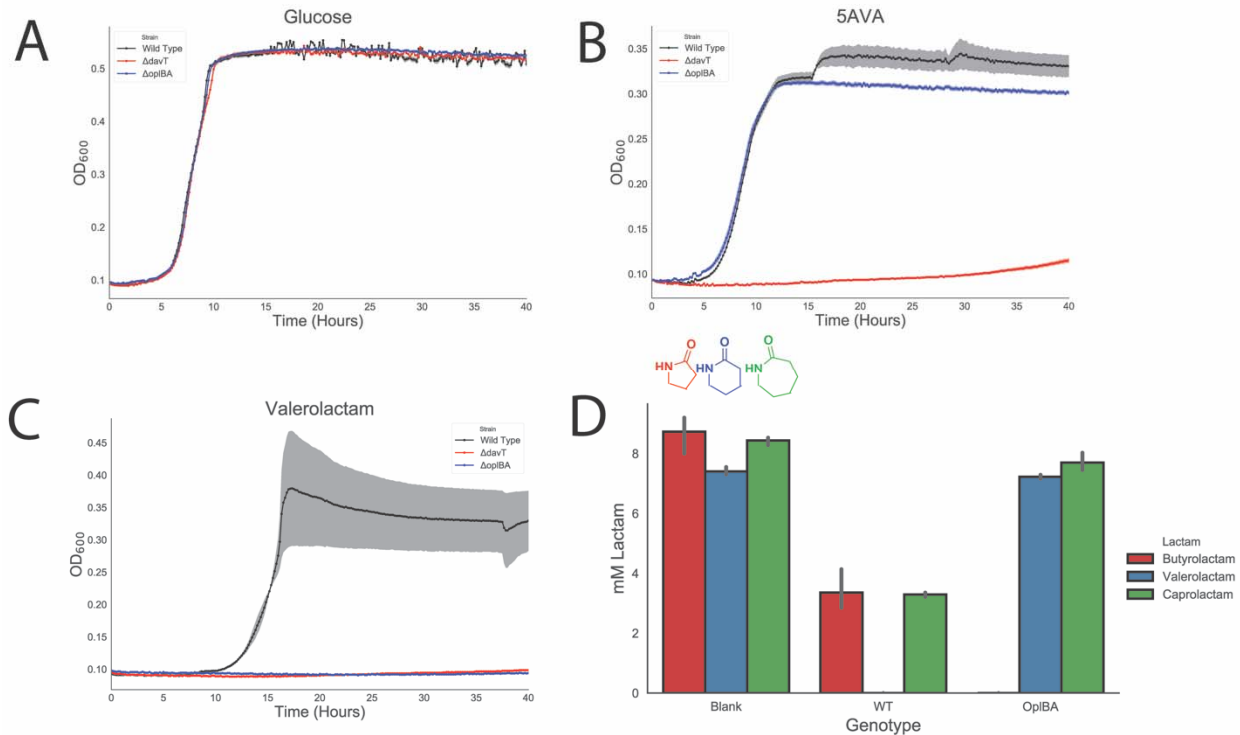
104 The inability of the RB-TnSeq approach to identify the hydrolytic enzyme could result  
105 from the enzyme being secreted from the cell. In this case, the secreted enzymes from cells  
106 containing the intact hydrolase gene produce 5AVA which can freely diffuse into hydrolase  
107 mutant cells, eliminating any selective pressure for lactam-based growth. To test whether the  
108 enzymes responsible for lactam hydrolysis may be secreted, cultures of *P. putida* were either  
109 grown on glucose or valerolactam as a sole carbon source, their supernatants filtered,  
110 concentrated, and then subjected to shotgun proteomics. Of the most abundant proteins in the  
111 supernatant, there were 25 proteins that were specific to glucose, while 46 were specific to  
112 valerolactam, with 86 proteins being shared between the two conditions (Figure 1D). Within the  
113 top five most abundant proteins in the valerolactam supernatant were OplB (Q88H51\_PSEPK)  
114 and OplA (Q88H51\_PSEPK), which together are annotated as the two subunits of a 5-  
115 oxoprolinase, orthologs of which have been suggested to participate in the caprolactam  
116 catabolism of *P. jessenii* (Figure 1E) [13]. Additional shotgun proteomics of cell pellets grown  
117 on either glucose, 5AVA, or valerolactam showed that OplB and OplA were more highly  
118 expressed in the presence of the lactam in comparison to the other carbon sources (Figure S1C).  
119 Interestingly, fitness data from two valerolactam RB-TnSeq experiments in *P. putida* KT2440  
120 show *oplBA* mutants having no significant fitness defects (Figure S1B). Orthologs of *oplBA* are  
121 widely distributed across many bacteria including other attractive metabolic engineering chassis  
122 such as *Rhodococcus opacus*, and are nearly always located adjacent to one another on the  
123 genome (Figure S2).

124 2.2 Deletion of *oplBA* mitigates consumption of valerolactam and caprolactam

125 To confirm the role of OplBA in the catabolism of valerolactam, deletions were  
126 constructed of the *oplBA* locus in *P. putida* via homologous recombination. Growth of the  
127 mutant was compared to the wild type as well as to a deletion mutant of *davT*, which catalyzes  
128 the first step in 5AVA catabolism. All strains showed identical growth on glucose as a sole  
129 carbon source (Figure 2A). In the presence of 5AVA the *oplBA* deletion strain showed no growth  
130 defect compared to the wild-type, while the *davT* mutant predictably was unable to grow (Figure  
131 2B). However, on valerolactam only the wild type strain grew, while both the *oplBA* and *davT*  
132 mutants showed no measurable growth after 40 hours (Figure 2C). These results suggest that  
133 OplBA is the sole enzyme responsible for the conversion of valerolactam to 5AVA under these  
134 conditions.

135 While *P. putida* KT2440 can utilize valerolactam as a sole carbon source, it is unable to  
136 grow on caprolactam (data not shown). In order to determine whether the OplBA of *P. putida* is  
137 capable of degrading other lactams, wild type and  $\Delta oplBA$  strains were grown in LB medium  
138 supplemented with 10 mM caprolactam, valerolactam, or butyrolactam for 24 hours after which  
139 the remaining lactam concentration was compared to an uninoculated medium control. Wild type  
140 *P. putida* consumed all detectable valerolactam within 24 hours, and less than 50% of both  
141 butyrolactam and caprolactam remained compared to the uninoculated control (Figure 2D).  
142 There was no significant decrease in amount of valerolactam in the  $\Delta oplBA$  cultures compared to  
143 the uninoculated control (t-test of  $p=0.178$ ), though there was a slight but significant decrease of  
144 0.74 mM caprolactam (t-test of  $p=0.033$ ). No butyrolactam remained in the  $\Delta oplBA$  culture after  
145 24 hours (Figure 2D). This result was surprising as the annotated substrate of OplBA, 5-  
146 oxoproline, has the same ring size as butyrolactam. Previous work has shown that homologs of  
147 OplBA are ATP-dependent amidohydrolases that hydrolyze 5-oxoproline [16]. However, when

148 purified OplBA was incubated with valerolactam in addition to ATP and magnesium we  
149 observed no hydrolysis relative to boiled enzyme controls (Figure S3).



150  
151 **Figure 2: OplBA controls valerolactam and caprolactam degradation in *P. putida*. Growth**  
152 **of wild-type,  $\Delta davT$ , or  $\Delta oplBA$  in minimal media supplemented with either 10 mM glucose**  
153 **(A), 5-aminovaleroate (B), or valerolactam (C). (D) Remaining butyrolactam, valerolactam,**  
154 **or caprolactam in LB media after 24-hour incubation with no *P. putida*, wild-type, or a**  
155  **$\Delta oplBA$  mutant.**

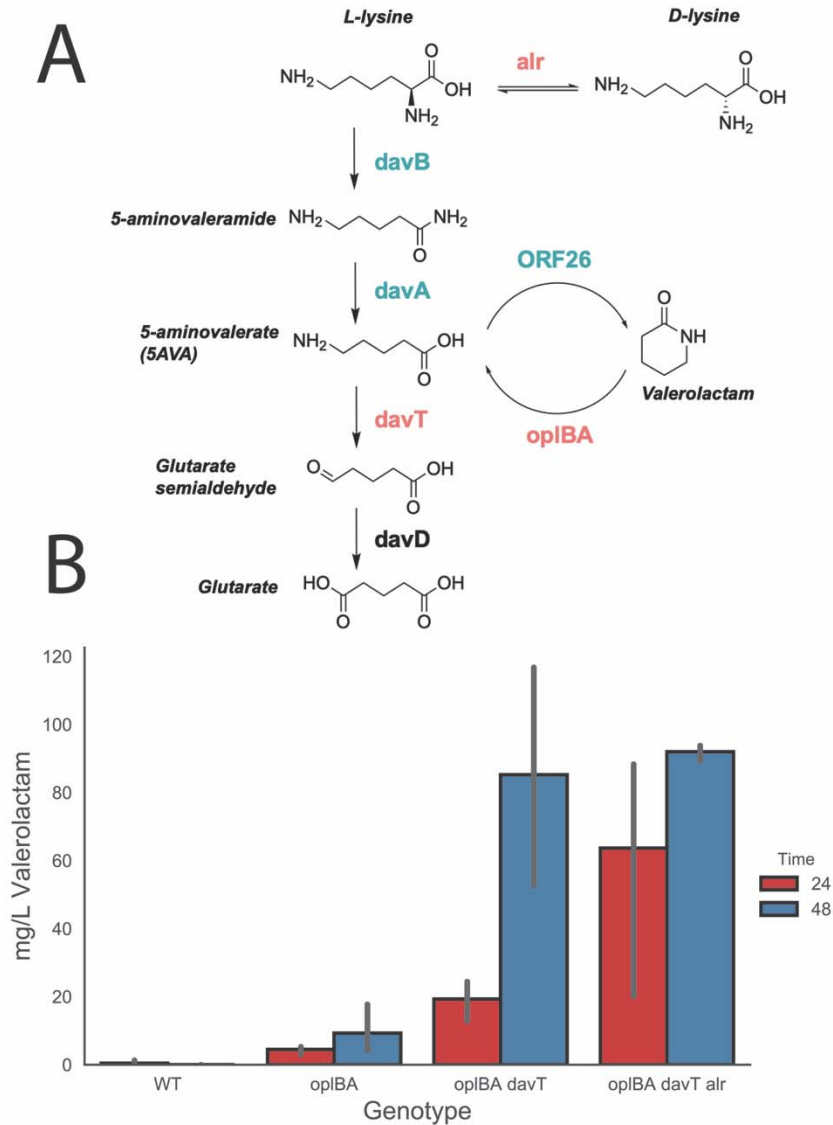
### 156 2.3 Host engineering for increased valerolactam production

157 The published pathway for the production of valerolactam from L-lysine in *E. coli*  
158 utilized the formation of 5AVA via the *davBA* pathway native to *P. putida*, followed by  
159 cyclization to the lactam via a promiscuous acyl-coA ligase from *Streptomyces aizunensis*  
160 (Figure 4A) [1]. To produce valerolactam in *P. putida*, not only will the production pathway  
161 need to be overexpressed, but the *oplBA* locus and pathways that compete for 5AVA must be



162 eliminated. Loss of flux to valerolactam occurs through two known competing pathways: the  
163 Alr-mediated isomerization to D-lysine or catabolism of 5AVA to glutarate via the action of  
164 DavTD (Figure 3A) [7].

165         To investigate the relative contributions of pathways that contribute to either lactam  
166 hydrolysis or loss of substrate, we expressed the *davBA-ORF26* pathway via a arabinose-  
167 inducible broad host range vector pBADT in backgrounds where these pathways had been  
168 sequentially deleted. Wild type *P. putida* produced 0.43 mg/L valerolactam after 24 hours, but no  
169 valerolactam could be detected after 48 hours, presumably due to host consumption (Figure 3B).  
170 Simple deletion of the *oplBA* locus resulted in a 10-fold increase of production at 24 hours to  
171 4.47 mg/L and a 48-hour titer of 9.27 mg/L (Figure 3B). Additional deletion of *davT* resulted in  
172 an increase of titer to 19.29 mg/L and 85.19 mg/L, and by deleting the amino acid racemase *alr*  
173 titers increased to 63.66 mg/L and 91.97 mg/L at 24 and 48 hours, respectively (Figure 3B).



174

175 **Figure 3: Production of valerolactam in *P. putida*: (A) Design of valerolactam**

176 **overproducing *P. putida*. The biosynthetic pathway genes are shown in green and were**

177 **overexpressed heterologously from a pBBR ori plasmid using an arabinose inducible**

178 **promoter. Pathways that catabolize products or divert precursors are shown in red. (B)**

179 **Valerolactam production from different *P. putida* strains grown in LB medium**

180 **supplemented with 25 mM L-lysine and 0.2% (w/v) arabinose at 24 and 48 hours post**

181 **inoculation. Error bars show 95% cI, n=3.**

### 182 3 DISCUSSION

183           Recent economic analyses highlight the necessity of lignin valorization to create a  
184 sustainable bioeconomy [17,18]. With its robust aromatic metabolism combined with novel  
185 methods of biomass deconstruction, *P. putida* has great potential to convert lignocellulosic  
186 biomass to value-added products [19,20]. Though the ability of *P. putida* to catabolize many  
187 carbon sources is often viewed as an asset, it has well documented metabolic pathways to  
188 degrade many compounds that metabolic engineers may wish to produce such as levulinic acid  
189 [8], various alcohols [21], and the diacid glutarate [12]. As these catabolic phenotypes are  
190 encountered it will be critical to rapidly identify the offending genomic loci.

191           The recent surge in development of functional genomics techniques has dramatically  
192 increased the throughput at which we can identify the genetic basis of unknown metabolism. RB-  
193 TnSeq has been used to uncover novel glutarate and levulinic acid metabolism, though was  
194 ineffective at identifying the *oplBA* locus [7,8]. Proteomics techniques have also grown more  
195 robust, and were used in *P. jessenii* to predict a route of caprolactam catabolism [13,22]. Here,  
196 proteomics also proved to be an effective means of identifying the enzyme responsible for the  
197 hydrolysis of the lactam. Our proteomics results showed that OplBA was specifically expressed  
198 when grown on valerolactam, but not 5AVA. These results suggest that *P. putida* may have  
199 lactam-specific transcription factors which could be developed into valuable tools for metabolic  
200 engineering if identified.

201           The inability of RB-TnSeq to identify these genes is curious as single deletion mutants  
202 were unable to grow on valerolactam. A possible explanation for this is that OplBA may be  
203 secreted, which would create a public pool of 5AVA which *oplBA* mutants could still utilize.  
204 However, OplBA orthologs have been shown to be ATP-dependent [16], which would be

205 inconsistent with this extracellular localization. Unfortunately our attempts to characterize  
206 OplBA *in vitro* were unsuccessful, preventing us from identifying the substrate requirements of  
207 the enzyme. Though we were unable to reconstitute the activity of OplBA *in vitro*, deletion of  
208 *oplBA* did not prevent the degradation of butyrolactam which is a 5-membered lactam ring. The  
209 annotated function of the *oplBA* loci is a 5-oxoprolinase, which hydrolyzes the 5-membered  
210 lactam ring of 5-oxoproline. These results may suggest that the OplBA may function naturally as  
211 something other than a 5-oxoprolinase. More work will be necessary to resolve the results of our  
212 RB-TnSeq and feeding experiments to elucidate the biochemical requirements of OplBA as well  
213 as to better understand its cellular localization.

214         Without deleting *oplBA* *P. putida* is able to metabolize up to 10 mM valerolactam in rich  
215 media after 24 hours, and simple deletion of these genes increases production 10-fold after 24  
216 hours of fermentation. Subsequent deletion of the 5AVA transaminase *davT* and the racemase *alr*  
217 resulted in 48 hour titers of ~90 mg/L, whereas there was no detectable valerolactam production  
218 in wild-type cultures at this time point. To achieve these titers we fed in 25 mM L-lysine (3.65  
219 g/L). Previous work in *E. coli* achieved titers of ~200 mg/L by feeding 1 g/L lysine and ~300  
220 mg/L by feeding 5 g/L after 48 hours [1]. Our results indicate that with significant host  
221 engineering, *P. putida* can produce titers approaching those of model organisms. Optimization of  
222 pathway expression could narrow this gap even further and should be a focus of future efforts.

223         While this initial work is encouraging, it still requires the feeding of L-lysine in rich  
224 media for conversion to valerolactam. Ideally, engineering *P. putida* would be able to metabolize  
225 lignin hydrolysis products directly to L-lysine on the way to the final product. A great deal of  
226 work has been conducted to elucidate the complex catabolism of lysine in *P. putida* [7,12], yet  
227 relatively little work has been done to increase flux to lysine within the bacterium. While there

228 has been little to divert flux to L-lysine in *P. putida*, there is a wealth of evidence in other  
229 bacteria where high titers of intracellular lysine have been achieved [23,24]. The ever increasing  
230 body of research to characterize the sprawling metabolism of *P. putida* will greatly aid in future  
231 efforts of efficient production of valerolactam from lignocellulosic feedstocks.

## 232 **4 METHODS**

### 233 4.1 Media, chemicals, and culture conditions

234 General *E. coli* cultures were grown in Luria-Bertani (LB) Miller medium (BD  
235 Biosciences, USA) at 37 °C while *P. putida* was grown at 30 °C. When indicated, *P. putida* and  
236 *E. coli* were grown on modified MOPS minimal medium [25]. Cultures were supplemented with  
237 kanamycin (50 mg/L, Sigma Aldrich, USA), gentamicin (30 mg/L, Fisher Scientific, USA), or  
238 carbenicillin (100mg/L, Sigma Aldrich, USA), when indicated. All other compounds were  
239 purchased through Sigma Aldrich (Sigma Aldrich, USA) .

### 240 4.2 Strains and plasmids

241 All bacterial strains and plasmids used in this work are listed in Table 1. All strains and  
242 plasmids created in this work are available through the public instance of the JBEI registry.  
243 (<https://public-registry.jbei.org/folders/456>). All plasmids were designed using Device Editor  
244 and Vector Editor software, while all primers used for the construction of plasmids were  
245 designed using j5 software [26–28]. Plasmids were assembled via Gibson Assembly using  
246 standard protocols [29], or Golden Gate Assembly using standard protocols [30]. Plasmids were  
247 routinely isolated using the Qiaprep Spin Miniprep kit (Qiagen, USA), and all primers were  
248 purchased from Integrated DNA Technologies (IDT, Coralville, IA).

### 249 **Table 1: Strains and plasmids used in this study**

<b>Strain</b>	<b>JBEI Part ID</b>	<b>Reference</b>
E. coli DH10B		[31]
E. coli BL21(DE3)		Novagen
P. putida KT2440		ATCC 47054
<i>P. putida</i> $\Delta$ <i>davT</i>		[32]
<i>P. putida</i> $\Delta$ <i>oplBA</i>	JBEI-104285	This work
<i>P. putida</i> $\Delta$ <i>oplBA</i> $\Delta$ <i>davT</i>	JBEI-104286	This work
<i>P. putida</i> $\Delta$ <i>oplBA</i> $\Delta$ <i>davT</i> $\Delta$ <i>alr</i>	JBEI-104287	This work
<b>Plasmids</b>		
pET28		Novagen
pET28 <i>oplA</i>	JBEI-104336	This work
pET28 <i>oplB</i>	JBEI-104337	This work
pBADT		[33]
pBADT- <i>davBA</i> -ORF26	JBEI-104356	This work
pMQ30		[34]
pMQ30 <i>oplBA</i>	JBEI-104355	This work
pMQ30 <i>alr</i>	JBEI-104354	This work
pMQ30 <i>davT</i>		[32]

251

### 252 4.3 Plate based growth assays

253 Growth studies of bacterial strains were conducted a microplate reader kinetic assays.

254 Overnight cultures were inoculated into 10 mL of LB medium from single colonies, and grown  
255 at 30 °C. These cultures were then washed twice with MOPS minimal media without any added  
256 carbon and diluted 1:100 into 500 µL of MOPS medium with 10 mM of a carbon source in 48-  
257 well plates (Falcon, 353072). Plates were sealed with a gas-permeable microplate adhesive film  
258 (VWR, USA), and then optical density and fluorescence were monitored for 48 hours in an  
259 Biotek Synergy 4 plate reader (BioTek, USA) at 30 °C with fast continuous shaking. Optical  
260 density was measured at 600 nm.

### 261 4.4 Production Assays and Lactam Quantification

262 To assess valerolactam production in strains of *P. putida* overnight cultures of strains  
263 harboring pBADT-*davBA-ORF26* were grown in 3 mL of LB supplemented with kanamycin and  
264 grown at 30 °C. Production cultures of 10 mL of LB supplemented with kanamycin, 25mM L-  
265 lysine, and 0.2% w/v arabinose were then inoculated 1:100 with overnight cultures and then  
266 grown at 30 °C shaking at 250 rpm. Samples for valerolactam production were taken at 24 and  
267 48 hours post-inoculation, with 200 µL of culture being quenched with an equal volume of ice  
268 cold methanol and then stored at -20 °C until analysis.

269 For measurement of lactams, liquid chromatographic separation was conducted at 20°C  
270 with a Kinetex HILIC column (50-mm length, 4.6-mm internal diameter, 2.6-µm particle size;  
271 Phenomenex, Torrance, CA) using a 1260 Series HPLC system (Agilent Technologies, Santa  
272 Clara, CA, USA). The injection volume for each measurement was 5 µL. The mobile phase was  
273 composed of 10 mM ammonium formate and 0.07% formic acid in water (solvent A) and 10 mM

274 ammonium formate and 0.07% formic acid in 90% acetonitrile and 10% water (solvent B)  
275 (HPLC grade, Honeywell Burdick & Jackson, CA, USA). High purity ammonium formate and  
276 formic acid (98-100% chemical purity) were purchased from Sigma-Aldrich, St. Louis, MO,  
277 USA. Lactams were separated with the following gradient: decreased from 90%B to 70%B in 2  
278 min, held at 70%B for 0.75 min, decreased from 70%B to 40%B in 0.25 min, held at 40%B for  
279 1.25 min, increased from 40%B to 90%B for 0.25 min, held at 90%B for 1 min. The flow rate  
280 was varied as follows: 0.6 mL/min for 3.25 min, increased from 0.6 mL/min to 1 mL/min in 0.25  
281 min, and held at 1 mL/min for 2 min. The total run time was 5.5 min.

282         The HPLC system was coupled to an Agilent Technologies 6520 quadrupole time-of-  
283 flight mass spectrometer (QTOF MS) with a 1:6 post-column split. Nitrogen gas was used as  
284 both the nebulizing and drying gas to facilitate the production of gas-phase ions. The drying and  
285 nebulizing gases were set to 12 L/min and 30 lb/in<sup>2</sup>, respectively, and a drying gas temperature  
286 of 350°C was used throughout. Fragmentor, skimmer and OCT 1 RF voltages were set to 100 V,  
287 50 V and 300 V, respectively. Electrospray ionization (ESI) was conducted in the positive-ion  
288 mode for the detection of  $[M + H]^+$  ions with a capillary voltage of 4000 V. The collision energy  
289 voltage was set to 0 V. MS experiments were carried out in the full-scan mode (75–1100  $m/z$ ) at  
290 0.86 spectra/s. The QTOF-MS system was tuned with the Agilent ESI-L Low concentration  
291 tuning mix in the range of 50-1700  $m/z$ . Lactams were quantified by comparison with 8-point  
292 calibration curves of authentic chemical standards from 0.78125  $\mu$ M to 100  $\mu$ M.  $R^2$  coefficients  
293 of  $\geq 0.99$ <sub>[EB1]</sub> were achieved for the calibration curves. Data acquisition was performed by  
294 Agilent MassHunter Workstation (version B.05.00), qualitative assessment by Agilent



295 MassHunter Qualitative Analysis (version B.05.00 or B.06.00), and data curation by Agilent  
296 Profinder (version B.08.00)

#### 297 4.5 RB-TnSeq and Proteomics Analysis

298 RB-TnSeq experiments utilized *P. putida* library JBEI-1 which has been described  
299 previously [7]. Libraries of JBEI-1 were thawed on ice, diluted into 25 mL of LB medium with  
300 kanamycin and then grown to an OD<sub>600</sub> of 0.5 at 30°C at which point three 1 mL aliquots were  
301 removed, pelleted, and stored at -80°C. Libraries were then washed once in MOPS minimal  
302 medium with no carbon source, and then diluted 1:50 in MOPS minimal medium with 10 mM  
303 valerolactam. Cells were grown in 500 µL of medium in 48-well plates (Falcon, 353072). Plates  
304 were sealed with a gas-permeable microplate adhesive film (VWR, USA), and then grown at  
305 30°C in a Tecan Infinite F200 microplate reader (Tecan Life Sciences, San Jose, CA), with  
306 shaking at 200 rpm. Two 500 µL aliquots were combined, pelleted, and stored at -80°C until  
307 BarSeq analysis, which was performed as previously described [8,14]. All fitness data is  
308 publically available at <http://fit.genomics.lbl.gov>.

309 Secretomes of *P. putida* were prepared by growing 500 mL of culture in MOPS minimal  
310 medium supplemented with either 10 mM glucose or 10 mM valerolactam for 24 hours at  
311 30°C, which were subsequently pelleted and filtered through a 0.22 µm filter and then  
312 concentrated 100x via a 10 kD MW cutoff filter. Cultures for intracellular proteomics analysis  
313 were grown in 10 mL cultures in the same conditions on either glucose, 5AVA, or valerolactam  
314 and were then pelleted and stored at -80°C until sample workup and proteomic analysis.  
315 Proteins from secreted and intracellular samples were desalted and isolated using a variation of a  
316 previously-described chloroform/methanol extraction protocol [35]. For secreted proteins, 100-  
317 200 µL of the concentrated protein sample was used; for intracellular samples, cell pellets were

318 thoroughly resuspended in 100  $\mu$ L HPLC water. Then, the following reagents were added to each  
319 sample in sequential order with thorough vortexing after each addition: 400  $\mu$ L of HPLC grade  
320 methanol, 100  $\mu$ L of HPLC grade chloroform, 300  $\mu$ L of HPLC grade water. Samples were  
321 centrifuged for 1 minute at  $\sim$ 21,000g in order to promote phase separation. After centrifugation,  
322 the entirety of the top layer (water and methanol) was removed and discarded, leaving on the  
323 protein pellet and chloroform layer remaining. Another 300  $\mu$ L of HPLC grade methanol was  
324 added, then the samples were vortexed and centrifuged again for 2 minutes at  $\sim$ 21,000g. The  
325 remaining liquid was then removed and discarded, and the cell pellets were allowed to dry in a  
326 fume hood for 5 minutes. Protein pellets were then resuspended in freshly-prepared 100mM  
327 ammonium bicarbonate buffer in HPLC water containing 20% HPLC methanol. Protein  
328 concentrations in the resuspended samples were quantified using a DC Protein Assay Kit (Bio-  
329 Rad Laboratories, Hercules, CA). After quantification, 100  $\mu$ g of protein was transferred to a  
330 PCR strip and tris(2-carboxyethyl)phosphine was added to a final concentration of 5mM.  
331 Samples were incubated at 22°C for 30 minutes, after which iodoacetamide was added (final  
332 concentration 10mM). Samples were again incubated at 22°C in the dark for 30 minutes. Finally,  
333 trypsin was added to a final ratio of 1:25 w/w trypsin:sample, and samples were digested at 37°C  
334 for 5-8 hours before being transferred to conical LC vials for LC-MS analysis. Peptides prepared  
335 for shotgun proteomic experiments were analyzed by using an Agilent 6550 iFunnel Q-TOF  
336 mass spectrometer (Agilent Technologies, Santa Clara, CA) coupled to an Agilent 1290 UHPLC  
337 system as described previously [36]. 20  $\mu$ g of peptides were separated on a Sigma–Aldrich  
338 Ascentis Peptides ES-C18 column (2.1 mm  $\times$  100 mm, 2.7  $\mu$ m particle size, operated at 60°C) at  
339 a 0.400 mL/min flow rate and eluted with the following gradient: initial condition was 98%  
340 solvent A (0.1% formic acid) and 2% solvent B (99.9% acetonitrile, 0.1% formic acid). Solvent

341 B was increased to 35% over 30 min, and then increased to 80% over 2 min, then held for 6 min,  
342 followed by a ramp back down to 2% B over 1 min where it was held for 4 min to re-equilibrate  
343 the column to original conditions. Peptides were introduced to the mass spectrometer from the  
344 LC by using a Jet Stream source (Agilent Technologies) operating in positive-ion mode (3,500  
345 V). Source parameters employed gas temp (250°C), drying gas (14 L/min), nebulizer (35 psig),  
346 sheath gas temp (250°C), sheath gas flow (11 L/min), VCap (3,500 V), fragmentor (180 V),  
347 OCT 1 RF Vpp (750 V). The data were acquired with Agilent MassHunter Workstation  
348 Software, LC/MS Data Acquisition B.06.01 operating in Auto MS/MS mode whereby the 20  
349 most intense ions (charge states, 2–5) within 300–1,400 m/z mass range above a threshold of  
350 1,500 counts were selected for MS/MS analysis. MS/MS spectra (100–1,700 m/z) were collected  
351 with the quadrupole set to “Medium” resolution and were acquired until 45,000 total counts were  
352 collected or for a maximum accumulation time of 333 ms. Former parent ions were excluded for  
353 0.1 min following MS/MS acquisition. The acquired data were exported as mgf files and  
354 searched against the latest *P. putida* KT2440 protein database with Mascot search engine version  
355 2.3.02 (Matrix Science). The resulting search results were filtered and analyzed by Scaffold v  
356 4.3.0 (Proteome Software Inc.).

#### 357 4.6 Protein Purification and Biochemical Analysis of OplBA

358 Both *oplB* and *oplA* were cloned into the expression vector pET28 harboring N-terminal  
359 6x-histidine purification tags. Protein expression and purification were carried out as described  
360 previously [7]. To characterize activity of OplBA we used conditions that were previously  
361 described to characterize 5-oxoprolinase with minor changes [37]. Briefly, 10  $\mu$ M of each OplB  
362 and OplA or boiled controls were incubated for 4 hours at 30 °C with 2 mM valerolactam in 100  
363 mM Tris-HCl pH 7.0, 4 mM MgCl<sub>2</sub>, with or without 2 mM ATP. Reactions were quenched with

364 ice-cold methanol, filtered through a 3kDa MWCO filter, diluted 40-fold with 50%  
365 methanol/50% H<sub>2</sub>O, and stored at - 20 °C until analysis via LC-MS.

#### 366 4.7 Bioinformatic Analyses

367 All statistical analyses were carried out using either the Python Scipy or Numpy libraries  
368 [38,39]. For the phylogenetic reconstructions, the best amino acid substitution model was  
369 selected using ModelFinder as implemented on IQ-tree [40] phylogenetic trees were constructed  
370 using IQ-tree, nodes were supported with 10,000 bootstrap replicates. The final tree figures were  
371 edited using FigTree v1.4.3 (<http://tree.bio.ed.ac.uk/software/figtree/>). Orthologous syntenic  
372 regions of OplBA were identified with CORASON-BGC [41] and manually colored and  
373 annotated.

#### 374 **Acknowledgements**

375 We thank Jesus Barajas for his careful reading of this manuscript and helpful suggestions  
376 during preparation. We also thank Morgan Price for assistance in analyzing RB-TnSeq data. We  
377 would like to thank the Amgen Scholars program for providing funding for Alexandria  
378 Velasquez.

379 This work was part of the DOE Joint BioEnergy Institute (<https://www.jbei.org>)  
380 supported by the U. S. Department of Energy, Office of Science, Office of Biological and  
381 Environmental Research, supported by the U.S. Department of Energy, Energy Efficiency and  
382 Renewable Energy, Bioenergy Technologies Office, through contract DE-AC02-05CH11231  
383 between Lawrence Berkeley National Laboratory and the U.S. Department of Energy. The views  
384 and opinions of the authors expressed herein do not necessarily state or reflect those of the  
385 United States Government or any agency thereof. Neither the United States Government nor any  
386 agency thereof, nor any of their employees, makes any warranty, expressed or implied, or

387 assumes any legal liability or responsibility for the accuracy, completeness, or usefulness of any  
388 information, apparatus, product, or process disclosed, or represents that its use would not  
389 infringe privately owned rights. The United States Government retains and the publisher, by  
390 accepting the article for publication, acknowledges that the United States Government retains a  
391 nonexclusive, paid-up, irrevocable, worldwide license to publish or reproduce the published form  
392 of this manuscript, or allow others to do so, for United States Government purposes. The  
393 Department of Energy will provide public access to these results of federally sponsored research  
394 in accordance with the DOE Public Access Plan ([http://energy.gov/downloads/doe-public-](http://energy.gov/downloads/doe-public-access-plan)  
395 [access-plan](http://energy.gov/downloads/doe-public-access-plan))

#### 396 **Contributions**

397 Conceptualization, M.G.T.; Methodology, M.G.T., L.E.V., J.M.B, P.C.M., E.E.K.B.;  
398 Investigation, M.G.T., L.E.V., J.M.B, P.C.M, V.T.B, W.A.S., A.N.P., A.E.V.; Writing – Original  
399 Draft, M.G.T.; Writing – Review and Editing, All authors.; Resources and supervision, C.J.P.,  
400 A.M.D., J.D.K.

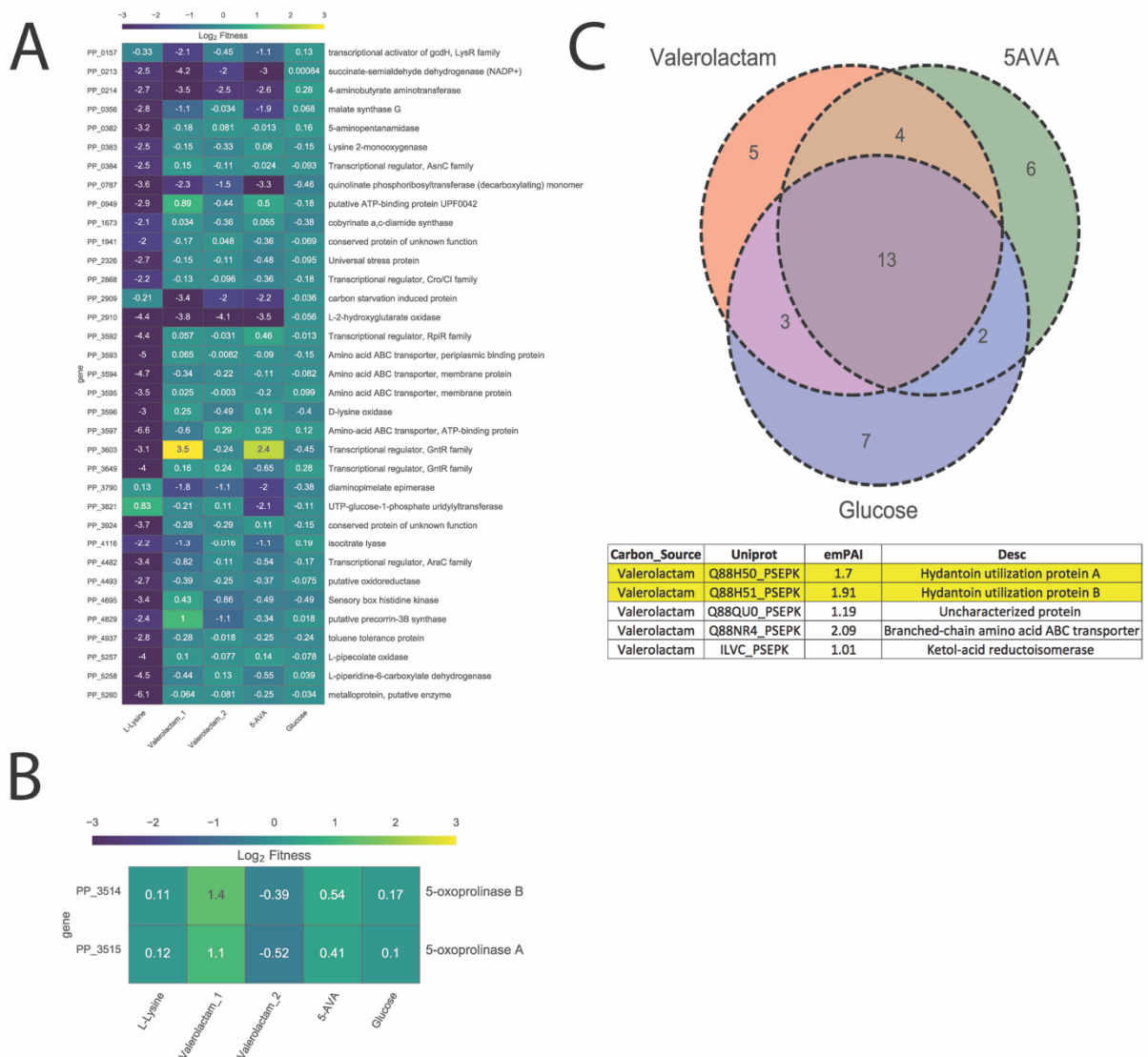
#### 401 **Competing Interests**

402 J.D.K. has financial interests in Amyris, Lygos, Demetrix, Napigen and Maple Bio.

#### 403 **Supplemental Figures**

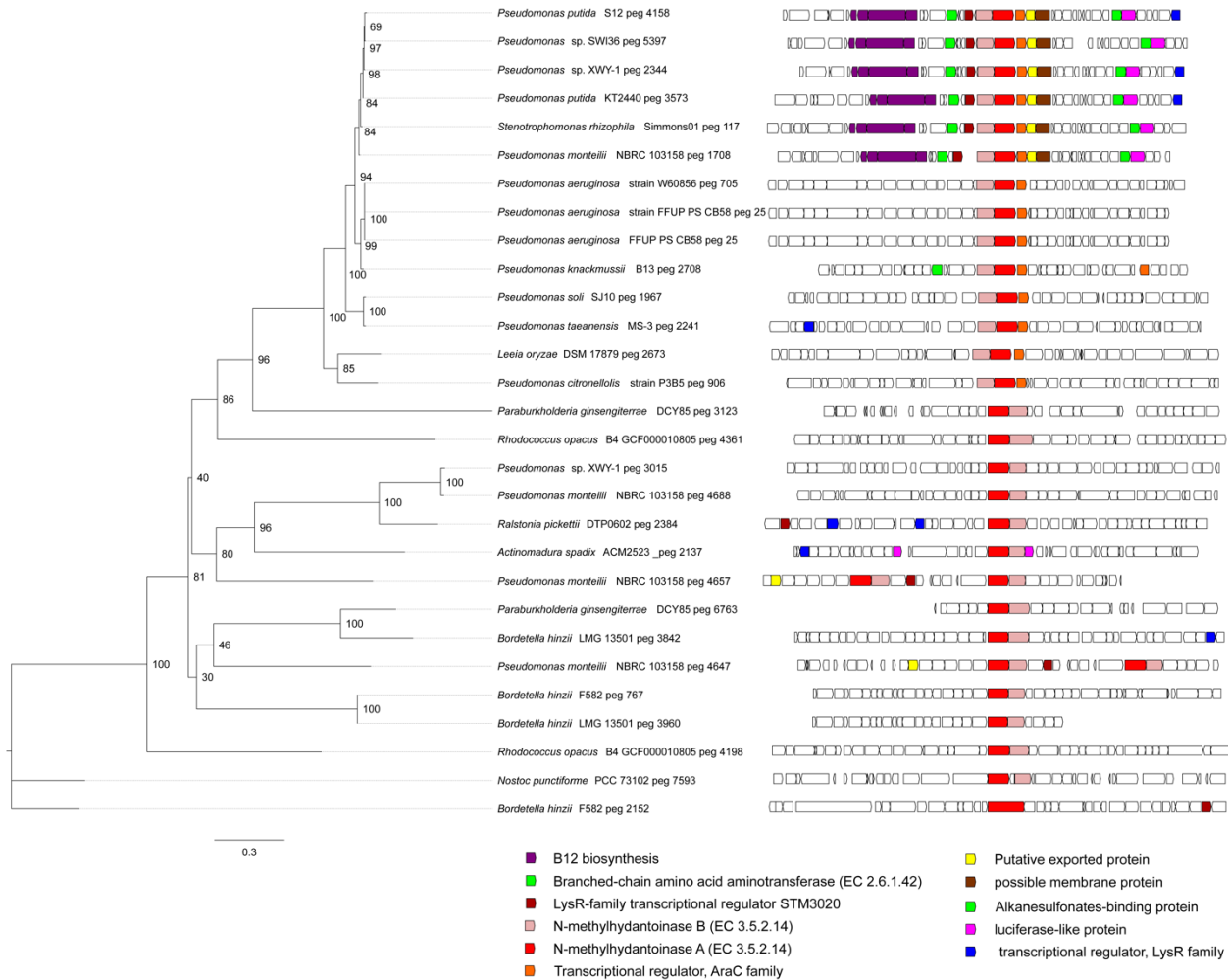
404 **Figure S1: RB-TnSeq and Cellular Shotgun Proteomics Results. (A) Genes that show**  
405 **significant ( $t < -4$ ) and large (fitness  $< -2$ ) fitness defects specific to either L-lysine, 5AVA,**  
406 **or valerolactam, but not glucose. All non-valerolactam fitness experiments are from**

407 **Thompson et. al 2019. (B) Fitness of the *oplA* and *oplB* genes on all carbon sources (C)**  
 408 **Venn diagram showing the number of specific proteins found in the 100 most abundant**  
 409 **proteins found within *P. putida* grown on either glucose, valerolactam, or 5-aminovaleate,**  
 410 **based on emPAI. Below we can see the 5 most abundant proteins specific to growth on**  
 411 **valerolactam. *OplA* and *OplB* are highlighted.**

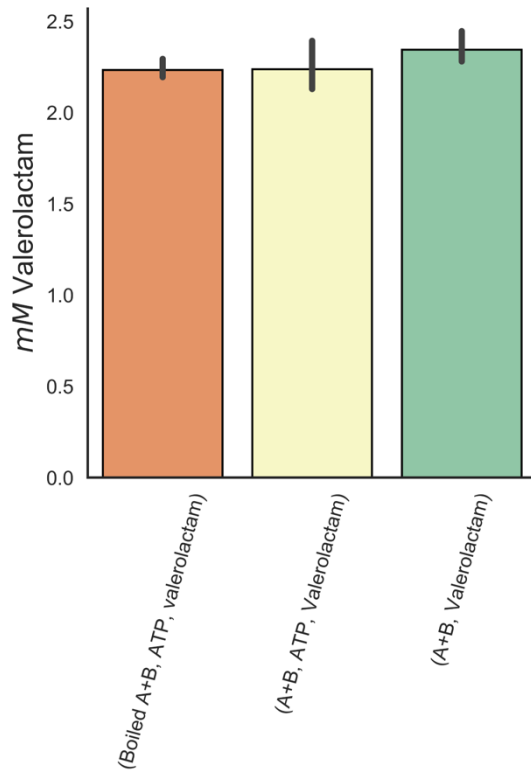


412

413 **Figure S2: Distribution of OplBA orthologs: Phylogenomics of selected OplBA homologs**  
 414 **across bacteria. The boxes represent the gene neighborhood for each homolog. The genes**  
 415 **have been colored to represent their annotated functions.**



420 **significant decrease in lactam concentration compared to boiled enzyme control. Error**  
421 **bars represent 95% cI, n=3.**



422  
423 **Bibliography**

- 424 [1] J. Zhang, J.F. Barajas, M. Burdu, G. Wang, E.E. Baidoo, J.D. Keasling, Application of an  
425 Acyl-CoA Ligase from *Streptomyces aizunensis* for Lactam Biosynthesis., *ACS Synth.*  
426 *Biol.* 6 (2017) 884–890. doi:10.1021/acssynbio.6b00372.
- 427 [2] A. Loeschcke, S. Thies, *Pseudomonas putida*-a versatile host for the production of natural  
428 products., *Appl. Microbiol. Biotechnol.* 99 (2015) 6197–6214. doi:10.1007/s00253-015-  
429 6745-4.
- 430 [3] K. Ravi, J. García-Hidalgo, M.F. Gorwa-Grauslund, G. Lidén, Conversion of lignin  
431 model compounds by *Pseudomonas putida* KT2440 and isolates from compost., *Appl.*  
432 *Microbiol. Biotechnol.* 101 (2017) 5059–5070. doi:10.1007/s00253-017-8211-y.
- 433 [4] J. Nogales, S. Gudmundsson, E. Duque, J.L. Ramos, B.O. Palsson, Expanding The  
434 Computable Reactome In *Pseudomonas putida* Reveals Metabolic Cycles Providing  
435 Robustness, *BioRxiv.* (2017). doi:10.1101/139121.
- 436 [5] M.A. Kukurugya, C.M. Mendonca, M. Solhtalab, R.A. Wilkes, T.W. Thannhauser, L.  
437 Aristilde, Multi-omics analysis unravels a segregated metabolic flux network that tunes  
438 co-utilization of sugar and aromatic carbons in *Pseudomonas putida*., *J. Biol. Chem.*



- 439 (2019). doi:10.1074/jbc.RA119.007885.
- 440 [6] P.I. Nickel, M. Chavarría, T. Fuhrer, U. Sauer, V. de Lorenzo, *Pseudomonas putida*  
441 *KT2440 Strain Metabolizes Glucose through a Cycle Formed by Enzymes of the Entner-*  
442 *Doudoroff, Embden-Meyerhof-Parnas, and Pentose Phosphate Pathways.*, *J. Biol. Chem.*  
443 *290* (2015) 25920–25932. doi:10.1074/jbc.M115.687749.
- 444 [7] M.G. Thompson, J.M. Blake-Hedges, P. Cruz-Morales, J.F. Barajas, S.C. Curran, C.B.  
445 Eiben, et al., *Massively Parallel Fitness Profiling Reveals Multiple Novel Enzymes in*  
446 *Pseudomonas putida Lysine Metabolism.*, *MBio.* *10* (2019). doi:10.1128/mBio.02577-18.
- 447 [8] J.M. Rand, T. Pisithkul, R.L. Clark, J.M. Thiede, C.R. Mehrer, D.E. Agnew, et al., *A*  
448 *metabolic pathway for catabolizing levulinic acid in bacteria.*, *Nat. Microbiol.* *2* (2017)  
449 1624–1634. doi:10.1038/s41564-017-0028-z.
- 450 [9] P.H. Clarke, *The metabolic versatility of pseudomonads*, *Antonie Van Leeuwenhoek.* *48*  
451 (1982) 105–130. doi:10.1007/BF00405197.
- 452 [10] K.W. George, A.G. Hay, *Bacterial strategies for growth on aromatic compounds.*, *Adv.*  
453 *Appl. Microbiol.* *74* (2011) 1–33. doi:10.1016/B978-0-12-387022-3.00005-7.
- 454 [11] T.U. Chae, Y.-S. Ko, K.-S. Hwang, S.Y. Lee, *Metabolic engineering of Escherichia coli*  
455 *for the production of four-, five- and six-carbon lactams.*, *Metab. Eng.* *41* (2017) 82–91.  
456 doi:10.1016/j.ymben.2017.04.001.
- 457 [12] M. Zhang, C. Gao, X. Guo, S. Guo, Z. Kang, D. Xiao, et al., *Increased glutarate*  
458 *production by blocking the glutaryl-CoA dehydrogenation pathway and a catabolic*  
459 *pathway involving L-2-hydroxyglutarate.*, *Nat. Commun.* *9* (2018) 2114.  
460 doi:10.1038/s41467-018-04513-0.
- 461 [13] M. Otzen, C. Palacio, D.B. Janssen, *Characterization of the caprolactam degradation*  
462 *pathway in Pseudomonas jessenii using mass spectrometry-based proteomics.*, *Appl.*  
463 *Microbiol. Biotechnol.* *102* (2018) 6699–6711. doi:10.1007/s00253-018-9073-7.
- 464 [14] K.M. Wetmore, M.N. Price, R.J. Waters, J.S. Lamson, J. He, C.A. Hoover, et al., *Rapid*  
465 *quantification of mutant fitness in diverse bacteria by sequencing randomly bar-coded*  
466 *transposons.*, *MBio.* *6* (2015) e00306-15. doi:10.1128/mBio.00306-15.
- 467 [15] M.N. Price, K.M. Wetmore, R.J. Waters, M. Callaghan, J. Ray, H. Liu, et al., *Mutant*  
468 *phenotypes for thousands of bacterial genes of unknown function.*, *Nature.* *557* (2018)  
469 503–509. doi:10.1038/s41586-018-0124-0.
- 470 [16] A.P. Seddon, L. Li, A. Meister, [54] *5-Oxo-l-prolinase from Pseudomonas putida*, in:  
471 *Glutamate, Glutamine, Glutathione, and Related Compounds*, Elsevier, 1985: pp. 451–  
472 458. doi:10.1016/S0076-6879(85)13057-0.
- 473 [17] N. Baral, O. Kavvada, D.M. Perez, A. Mukhopadhyay, T.S. Lee, B. Simmons, et al.,  
474 *Techno-economic analysis and life-cycle greenhouse gas mitigation cost of five routes to*  
475 *bio-jet fuel blendstocks*, *Energy Environ. Sci.* (2019). doi:10.1039/C8EE03266A.
- 476 [18] J. Becker, C. Wittmann, *A field of dreams: Lignin valorization into chemicals, materials,*  
477 *fuels, and health-care products.*, *Biotechnol. Adv.* (2019).  
478 doi:10.1016/j.biotechadv.2019.02.016.

- 479 [19] A. Rodriguez, D. Salvachúa, R. Katahira, B.A. Black, N.S. Cleveland, M. Reed, et al.,  
480 Base-Catalyzed Depolymerization of Solid Lignin-Rich Streams Enables Microbial  
481 Conversion, *ACS Sustain. Chem. Eng.* 5 (2017) 8171–8180.  
482 doi:10.1021/acssuschemeng.7b01818.
- 483 [20] M. Kohlstedt, S. Starck, N. Barton, J. Stolzenberger, M. Selzer, K. Mehlmann, et al.,  
484 From lignin to nylon: Cascaded chemical and biochemical conversion using metabolically  
485 engineered *Pseudomonas putida*., *Metab. Eng.* 47 (2018) 279–293.  
486 doi:10.1016/j.ymben.2018.03.003.
- 487 [21] M. Wehrmann, P. Billard, A. Martin-Meriadec, A. Zegeye, J. Klebensberger, Functional  
488 Role of Lanthanides in Enzymatic Activity and Transcriptional Regulation of  
489 Pyrroloquinoline Quinone-Dependent Alcohol Dehydrogenases in *Pseudomonas putida*  
490 KT2440., *MBio.* 8 (2017). doi:10.1128/mBio.00570-17.
- 491 [22] Y. Chen, J. Vu, M.G. Thompson, W.A. Sharpless, L.J.G. Chan, J.W. Gin, et al., A rapid  
492 methods development workflow for high-throughput quantitative proteomic applications.,  
493 *PLoS ONE.* 14 (2019) e0211582. doi:10.1371/journal.pone.0211582.
- 494 [23] I. Nærdal, R. Netzer, T.E. Ellingsen, T. Brautaset, Analysis and manipulation of aspartate  
495 pathway genes for L-lysine overproduction from methanol by *Bacillus methanolicus*.,  
496 *Appl. Environ. Microbiol.* 77 (2011) 6020–6026. doi:10.1128/AEM.05093-11.
- 497 [24] M. Rajvanshi, K. Gayen, K.V. Venkatesh, Lysine overproducing *Corynebacterium*  
498 *glutamicum* is characterized by a robust linear combination of two optimal phenotypic  
499 states., *Syst. Synth. Biol.* 7 (2013) 51–62. doi:10.1007/s11693-013-9107-5.
- 500 [25] A.E. LaBauve, M.J. Wargo, Growth and laboratory maintenance of *Pseudomonas*  
501 *aeruginosa*., *Curr. Protoc. Microbiol.* Chapter 6 (2012) Unit 6E.1.  
502 doi:10.1002/9780471729259.mc06e01s25.
- 503 [26] T.S. Ham, Z. Dmytriv, H. Plahar, J. Chen, N.J. Hillson, J.D. Keasling, Design,  
504 implementation and practice of JBEI-ICE: an open source biological part registry platform  
505 and tools., *Nucleic Acids Res.* 40 (2012) e141. doi:10.1093/nar/gks531.
- 506 [27] J. Chen, D. Densmore, T.S. Ham, J.D. Keasling, N.J. Hillson, DeviceEditor visual  
507 biological CAD canvas., *J. Biol. Eng.* 6 (2012) 1. doi:10.1186/1754-1611-6-1.
- 508 [28] N.J. Hillson, R.D. Rosengarten, J.D. Keasling, j5 DNA assembly design automation  
509 software., *ACS Synth. Biol.* 1 (2012) 14–21. doi:10.1021/sb2000116.
- 510 [29] D.G. Gibson, L. Young, R.-Y. Chuang, J.C. Venter, C.A. Hutchison, H.O. Smith,  
511 Enzymatic assembly of DNA molecules up to several hundred kilobases., *Nat. Methods.* 6  
512 (2009) 343–345. doi:10.1038/nmeth.1318.
- 513 [30] C. Engler, R. Kandzia, S. Marillonnet, A one pot, one step, precision cloning method with  
514 high throughput capability., *PLoS ONE.* 3 (2008) e3647.  
515 doi:10.1371/journal.pone.0003647.
- 516 [31] S.G. Grant, J. Jessee, F.R. Bloom, D. Hanahan, Differential plasmid rescue from  
517 transgenic mouse DNAs into *Escherichia coli* methylation-restriction mutants., *Proc Natl*  
518 *Acad Sci USA.* 87 (1990) 4645–4649.

- 519 [32] M.G. Thompson, P. Cruz-Morales, R.N. Krishna, J.M. Blake-Hedges, M.R. Incha, J.D.  
520 Keasling, Glutarate metabolism in *Pseudomonas putida* is regulated by two distinct  
521 glutarate sensing transcription factors, *BioRxiv*. (2019). doi:10.1101/557751.
- 522 [33] C. Bi, P. Su, J. Müller, Y.-C. Yeh, S.R. Chhabra, H.R. Beller, et al., Development of a  
523 broad-host synthetic biology toolbox for *Ralstonia eutropha* and its application to  
524 engineering hydrocarbon biofuel production., *Microb. Cell Fact.* 12 (2013) 107.  
525 doi:10.1186/1475-2859-12-107.
- 526 [34] R.M.Q. Shanks, D.E. Kadouri, D.P. MacEachran, G.A. O'Toole, New yeast  
527 recombineering tools for bacteria., *Plasmid.* 62 (2009) 88–97.  
528 doi:10.1016/j.plasmid.2009.05.002.
- 529 [35] D. Wessel, U.I. Flügge, A method for the quantitative recovery of protein in dilute  
530 solution in the presence of detergents and lipids., *Anal. Biochem.* 138 (1984) 141–143.  
531 doi:10.1016/0003-2697(84)90782-6.
- 532 [36] S.M. González Fernández-Niño, A.M. Smith-Moritz, L.J.G. Chan, P.D. Adams, J.L.  
533 Heazlewood, C.J. Petzold, Standard flow liquid chromatography for shotgun proteomics  
534 in bioenergy research., *Front. Bioeng. Biotechnol.* 3 (2015) 44.  
535 doi:10.3389/fbioe.2015.00044.
- 536 [37] L.Y. Li, A.P. Seddon, A. Meister, Interaction of the protein components of 5-  
537 oxoprolinase. Substrate-dependent enzyme complex formation., *J. Biol. Chem.* 263 (1988)  
538 6495–6501.
- 539 [38] E. Jones, T. Oliphant, P. Peterson, Others, *SciPy: Open source scientific tools for Python*,  
540 (n.d.).
- 541 [39] S. van der Walt, S.C. Colbert, G. Varoquaux, The NumPy Array: A Structure for  
542 Efficient Numerical Computation, *Comput. Sci. Eng.* 13 (2011) 22–30.  
543 doi:10.1109/MCSE.2011.37.
- 544 [40] S. Kalyanamoorthy, B.Q. Minh, T.K.F. Wong, A. von Haeseler, L.S. Jermin,  
545 ModelFinder: fast model selection for accurate phylogenetic estimates., *Nat. Methods.* 14  
546 (2017) 587–589. doi:10.1038/nmeth.4285.
- 547 [41] P. Cruz-Morales, H.E. Ramos-Aboites, C. Licona-Cassani, N. Selem-Mójica, P.M. Mejía-  
548 Ponce, V. Souza-Saldívar, et al., Actinobacteria phylogenomics, selective isolation from  
549 an iron oligotrophic environment and siderophore functional characterization, unveil new  
550 desferrioxamine traits., *FEMS Microbiol. Ecol.* 93 (2017). doi:10.1093/femsec/fix086.