

1 **Charting the metabolic landscape of the facultative**
2 **methylotroph *Bacillus methanolicus***

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11 Running Head: Metabolic states of the methylotroph *B. methanolicus*

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29 **ABSTRACT**

30 **Abstract**

31 *Bacillus methanolicus* MGA3 is a thermotolerant and relatively fast-growing
32 methylotroph able to secrete large quantities of glutamate and lysine. These
33 natural characteristics make *B. methanolicus* a good candidate to become a
34 new industrial chassis organism, especially in a methanol-based economy.
35 This has motivated a number of omics studies of *B. methanolicus* at the
36 genome, transcript, protein and metabolic levels. Intriguingly, the only
37 substrates known to support *B. methanolicus* growth as sole source of carbon
38 and energy are methanol, mannitol, and to a lesser extent glucose and
39 arabitol. We hypothesized that comparing methylotrophic and non-
40 methylotrophic metabolic states at the flux level would yield new insights
41 into MGA3 metabolism. ¹³C metabolic flux analysis (¹³C-MFA) is a powerful
42 computational method to estimate carbon flows from substrate to biomass
43 (i.e. the *in vivo* reaction rates of the central metabolic pathways) from
44 experimental labeling data. In this study, we designed and performed a ¹³C-
45 MFA of the facultative methylotroph *B. methanolicus* MGA3 growing on
46 methanol, mannitol and arabitol to compare the associated metabolic states.
47 The results obtained validate previous findings on the methylotrophy of
48 *B. methanolicus*, allowed us to characterize the assimilation pathway of one
49 of the studied carbon sources, and provide a better overall understanding of
50 this strain.

51 **Importance**

52 Methanol is cheap, easy to transport and can be produced both from
53 renewable and fossil resources without mobilizing arable lands. As such, it is
54 regarded as a potential carbon source to transition toward a greener
55 industrial chemistry. Metabolic engineering of bacteria and yeast able to
56 efficiently consume methanol is expected to provide cell factories that will
57 transform methanol into higher-value chemicals in the so-called methanol
58 economy. Toward that goal, the study of natural methylotrophs such as
59 *B. methanolicus* is critical to understand the origin of their efficient
60 methylotrophy. This knowledge will then be leveraged to transform such
61 natural strains into new cell factories, or to design methylotrophic capability
62 in other strains already used by the industry.

63 **KEYWORDS**

64 Natural methylotrophy, ¹³C metabolic flux analysis, non-stationary MFA,
65 *Bacillus methanolicus* MGA3, methanol

66

67 **Abbreviations**

68 ¹³C-MFA: ¹³C metabolic flux analysis; CID: carbon isotopologue distribution;

69 FBA: Flux Balance Analysis; MS: mass spectrometry; NMR: nuclear magnetic

70 resonance; PTS: phosphotransferase system

71 Pathways

72 SBPase: fructose biphosphate aldolase/sedoheptulose biphosphatase; TA:

73 fructose biphosphate aldolase/transaldolase; PPP: pentose phosphate

74 pathway; RuMP: Ribulose Monophosphate Cycle; TCA: Krebs cycle

75 Reactions

76 akgdh: 2-oxoglutarate dehydrogenase and 2-oxoglutarate synthase; Araupt:

77 arabitol uptake; detox: linear detoxification pathways; fum: fumarate

78 reductase; glpx: sedoheptulose-biphosphatase; gnd: phosphogluconate

79 dehydrogenase; hps: 3-hexulose-6-phosphate synthase ; idh: isocitrate

80 dehydrogenase; Manupt: mannitol uptake; mdh: methanol dehydrogenase;

81 pdh: pyruvate dehydrogenase; pfk: 6-phosphofructokinase and fructose-

82 biphosphatase; pgi: glucose 6-phosphate isomerase ; pgk: glyceraldehyde

83 3-phosphate dehydrogenase, phosphoglycerate kinase, and

84 phosphoglycerate mutase; phi: 6-phospho-3-hexuloisomerase ; pyk: pyruvate

85 kinase; rpe: ribulose-phosphate 3-epimerase; rpi: ribose 5-phosphate

86 isomerase; rpi: ribulose phosphate isomerase; ta: transaldolase; tkt1, tkt2:

87 transketolases; zwf: glucose-6-phosphate dehydrogenase and 6-

88 phosphogluconolactonase.

89 Metabolites

90 Ace: acetate; Aco: aconitate; AKG: 2-oxoglutarate; ala: alanine; Ara: arabitol;
91 arg: arginine; asp: aspartate; Cit: citrate; DHAP: dihydroxyacetone
92 phosphate; Ery4P: erythrose 4-phosphate; For: formaldehyde; Fru6P: fructose
93 6-phosphate; FruBP: fructose 1,6-bisphosphate; Fum: fumarate; G3P: 3-
94 phospho-D-glycerate; GAP: glyceraldehyde 3-phosphate; Glc6P: glucose 6-
95 phosphate; glu: glutamate; gly: glycine; GlyOx: glyoxylate; Gnt6P: 6-
96 phosphogluconate; Hex6P: hexulose 6-phosphate; his: histidine; ile:
97 isoleucine; leu: leucine; lys: lysine; Mal: malate; Man: mannitol; MeOH:
98 methanol; met: methionine; OAA: oxaloacetate; PEP: phosphoenolpyruvate;
99 PGA: 2-phospho-D-glycerate; phe: phenylalanine; pro: proline; Pyr: pyruvate;
100 Rib5P: ribose 5-phosphate; Ribu5P: ribulose 5-phosphate; Sed7P:
101 sedoheptulose 7-phosphate; ser: serine; Suc: succinate; thr: threonine; tyr:
102 tyrosine; val: valine; Xyl5P: xylulose 5-phosphate.

103

104 **1. INTRODUCTION**

105 ^{13}C metabolic flux analysis (^{13}C -MFA) has emerged in the last decade as an
106 outstanding experimental method to describe the metabolic states of
107 microorganisms. It has successfully been used to identify new pathways (1),
108 investigate responses to environmental changes (2), improve the titer of cell
109 factories (3), screen strains based on their enzymatic capacity (4), and more
110 generally to provide a better understanding of the metabolism of
111 microorganisms (5) such as methylotrophs (6–8). Briefly, ^{13}C -MFA exploits a
112 metabolic model and ^{13}C -isotope patterns measured from key metabolites to
113 estimate reaction rates consistent with the observed labeling patterns (see
114 (9, 10) for reviews). Specifically, cells are grown on a ^{13}C labeled carbon
115 source, metabolites of the central metabolism or constituents of the biomass
116 such as proteinogenic amino acids are sampled and quenched, and their
117 carbon isotopologue (i.e. labeling) distribution (CID) is measured by mass
118 spectrometry (MS) and/or nuclear magnetic resonance (NMR). A metabolic
119 model is then used to fit these measurements to theoretical CID data that
120 are simulated by optimizing reaction flux values from the metabolic model.
121 Assuming mass balance, if the measurements are coherent and the topology
122 of the metabolic model is correct, the experimental and simulated data will
123 converge, yielding the estimated reaction fluxes. Finally, ^{13}C -MFA provides a
124 flux map: a predicted snapshot of the metabolic fluxes through the organism
125 of interest during the experiment, i.e. its metabolic state. ^{13}C -MFA flux maps
126 are conceptually similar to those from flux balance analysis (FBA), a purely *in*

127 *in silico* method that, from a metabolic model (typically at the genome scale),
128 computes the optimal reaction flux distribution to maximize an objective
129 defined in terms of metabolite production, often designed to model cell
130 growth. Importantly, ¹³C-MFA flux maps are estimates based on experimental
131 data, whereas FBA flux maps are purely *in silico* predictions, which can be
132 confirmed by gene deletion analysis or ¹³C-MFA for example.

133 *Bacillus methanolicus* MGA3 is a gram-positive bacterium that was first
134 isolated in the 1990s from freshwater marsh soil samples after an
135 enrichment culture on methanol at 55 °C (11). Its ability to grow quickly and
136 to secrete large quantities of glutamate and lysine in methanol at high
137 temperature make it a good candidate for biotech applications. Methanol is
138 indeed viewed as a promising renewable feedstock because of its abundance
139 and low price (12, 13), while high temperature cultures are less prone to
140 contamination and require less cooling when scaled up (14). Furthermore,
141 *B. methanolicus* is able to grow in seawater, which is also cheap and
142 abundant (15). Promising metabolic engineering studies have already
143 established MGA3 as a cell factory for the heterologous production of
144 cadaverine (16) and GABA (17). While the lack of genetic tools must have
145 impaired the development of new applications in the past (18), the
146 establishment of gene expression tools based on theta- and rolling-circle
147 replicating plasmids have made *B. methanolicus* amenable to the
148 overproduction of amino acids and their derivatives (19), and there is hope
149 that recent breakthroughs from CRISPR interference (CRISPRi) will stimulate
150 new innovations (20).

151 As a facultative methylotroph, *B. methanolicus* MGA3 can also grow on non-
152 methylotrophic substrates such as D-mannitol, D-glucose and D-arabitol. The
153 metabolic pathways involved in the uptake of mannitol and glucose have
154 been described (21), as has the organization of genes involved in mannitol
155 utilization (19). Both substrates enter the cells via a phosphotransferase
156 system (PTS), respectively as mannitol 1-phosphate and glucose 6-
157 phosphate, and are further converted to fructose 6-phosphate. Arabitol has
158 recently been characterized as a fourth source of carbon and energy for
159 *B. methanolicus* (22). The operon responsible for arabitol assimilation was
160 identified as harboring a PTS system (AtIABC) and two putative arabitol
161 phosphate dehydrogenases (AtID and AtIF), whose activities were
162 demonstrated in crude extracts. However, as the pathway was not
163 completely characterized, it is unclear whether arabitol is assimilated
164 through arabitol 1-phosphate to xylulose 5-phosphate (Xyl5P), or to ribulose
165 5-phosphate (Rib5P) through arabitol 5-phosphate. It has been suggested
166 that both routes operate in parallel in *Enterococcus avium* and other gram-
167 positive bacteria (23). A series of omics studies comparing these carbon
168 sources with methanol have contributed to a better understanding of
169 *B. methanolicus* metabolism at the genome (21, 24), transcriptome (21, 22,
170 25), proteome (26) and metabolome levels (27, 28). However, a flux level
171 description, which could validate previous findings and provide new insights
172 into the facultative methylotrophy of *B. methanolicus* and its associated
173 metabolic states, is still lacking.

174 In this study, we designed and performed ^{13}C -MFA of the facultative
175 methylotroph *Bacillus methanolicus* MGA3 growing on methanol, mannitol
176 and arabitol. Methanol (CH_4O) and mannitol ($\text{C}_6\text{H}_{14}\text{O}_6$) are the best known
177 carbon sources for this strain (11, 14), with comparable growth rates; while
178 growth on arabitol ($\text{C}_5\text{H}_{12}\text{O}_5$) is significantly slower (22) and its assimilation
179 pathway has not yet been fully described. All three carbon sources are
180 probably present in MGA3's natural habitats, on plant leaves (29) or as plant
181 degradation products (30). With their wide availability and fast associated
182 growth rate, methanol and mannitol are promising feedstocks for industrial
183 applications, while arabitol growth allows the facultative methylotrophy of
184 MGA3 to be studied with a less efficient C source and to finish characterizing
185 its assimilation pathway.

186

187 **2. MATERIALS & METHODS**

188 **2.1 Strain**

189 *B. methanolicus* wild-type MGA3 (ATCC 53907) strain was used for metabolic
190 flux analyses. Strains used for cloning and expression are described in the
191 section 2.5.1 and listed in Table 1.

192 **2.2 Non-stationary ¹³C fluxomics experiment**

193 **2.2.1 Culture conditions and parameters**

194 For the carbon source methanol, two batch cultures were performed in 0.5
195 litre bioreactors (INFORS HT Multifors, The Netherlands) with a working
196 volume of 0.40 litres coupled to a Dycor ProLine Process Mass Spectrometer
197 (AMETEK Process Instruments, USA). The culture medium per litre was:
198 3.48 g Na₂HPO₄·12 H₂O, 0.606 g KH₂PO₄, 2.5 g NH₄Cl, 0.048 g yeast extract,
199 1 ml of 1 M MgSO₄ solution, 1 ml of trace salt solution, 1 ml of vitamins
200 solution, 0.05 ml Antifoam 204 and 150 mM of methanol. The trace salt
201 solution per litre was: 5.56 g FeSO₄·7 H₂O, 0.027 g CuCl₂·2 H₂O, 7.35 CaCl₂·2
202 H₂O, 0.040 g CoCl₂·6 H₂O, 9.90 g MnCl₂·4 H₂O, 0.288 g ZnSO₄·7 H₂O and
203 0.031 g H₃BO₃. The vitamin solution per litre was: 0.10 g D-biotin, 0.10 g
204 thiamine·HCl, 0.10 g riboflavin, 0.10 g pyridoxine·HCl, 0.10 g pantothenate,
205 0.10 g nicotinamide, 0.02 g p-aminobenzoic acid, 0.01 g folic acid, 0.01 g
206 vitamin B12 and 0.01 g lipoic acid. The pre-cultures were grown in two half

207 litre shake flasks containing 150 ml of the pre-culture medium and inoculated
208 with cryostock of *B. methanolicus* wild-type MGA3 cells. The cultures were
209 grown overnight at 50 °C under shaking at 200 rpm, and used to inoculate
210 the reactors. The aeration rate of 1 vvm was controlled by a mass flow meter
211 (INFORS HT Multifors, The Netherlands) and pO₂ were maintained above
212 25 % throughout all cultures. Temperature, pH and stirring speed were
213 maintained at 50 °C, pH 6.8 (with KOH 1 M) and 800 rpm, respectively. The
214 N₂, O₂, Argon, CO₂, ¹³C-CO₂ and methanol concentrations in the bioreactors
215 off-gas were measured on-line with the mass spectrometer.

216 To perform the pulse of tracer, 100 mM of ¹³C-methanol (99 % ¹³C; Euriso-Top,
217 France) were added to the cultures at an OD₆₀₀ of 2.5. Growth curves are
218 available in Supplementary Data 1.

219 **2.2.2 Quantification of cells and supernatant NMR analysis**

220 For determination of the dry weight of cells, a conversion factor of 0.389 g/l
221 (dry weight) of cells per OD₆₀₀ unit was used. Supernatant samples were
222 taken to analyse substrate methanol consumption as well as by-product
223 formation by subtracting 1 ml of culture and centrifuged it at 13000 × g for
224 60 s. Thereafter, supernatant was collected and stored until analysis at -20
225 °C. Supernatant analysis was performed by ¹H 1D-NMR at 292 °K, using a 30°
226 pulse and a relaxation delay of 20 s, with an Avance 800 MHz spectrometer
227 (Bruker, Germany). Deuterated trimethylsilyl propionate (TSP-d₄) was used
228 as an internal standard for quantification.

229 **2.2.3 Sampling and MS analysis of intra and extracellular** 230 **pool sizes**

231 When the cultures reached an OD₆₀₀ of 2, metabolome samples were
232 collected using the optimized method described by (28). Briefly, total broth
233 quenching with correction for metabolites in the extracellular medium was
234 performed in quadruplicates to assess the metabolite pool sizes in the two
235 cultivations performed. Metabolites pool sizes were quantified (Fig. S1) by ion
236 chromatography tandem mass spectrometry (IC-MS/MS) using cell extract of
237 *Escherichia coli*, cultivated on 99 % [¹³C₆] glucose (Euroisotop, France), as
238 internal standard (31). Liquid anion exchange chromatography was
239 performed as described previously (32).

240 **2.2.4 Sampling and MS analysis of labeled metabolites**

241 Label enrichments in the intracellular metabolites were followed after
242 performing a pulse of 100 mM ¹³C-methanol at an OD₆₀₀ 2.5. Whole broth
243 (internal + external pools; WB) and culture filtrate (external pools; CF) were
244 sampled to indirectly track label incorporation in the intracellular
245 metabolites. Specifically, 13 WB and 3 CF samples were collected in 3.5 min
246 in each bioreactor. Exact sampling times can be seen in Supplementary Data
247 1. IC-MS/MS quantification was used to analyse the isotopologues of each
248 metabolite as described by (32). The metabolites analysed were PEP,
249 Rib5P+Ribu5P+Xyl5P, Sed7P, Gnt6P, Glc6P, FruBP, Fru6P, Gly3P, 13PG,
250 G3P+PGA, Cit, Aco, Fum, Mal and Suc. After manual peak integration, the raw
251 peak areas were corrected for the contribution of all naturally abundant

252 isotopes using IsoCor software (33). Some cross-contamination was found in
253 the isotopologues M4 of Aco and M2 and M3 of Gnt6P that were subsequently
254 removed from the analysis (Supplementary Data 1).

255 Additionally, the exact ratio between ^{13}C -methanol and ^{12}C -methanol after
256 the pulse was measured by ^1H 1D-NMR as well as the evolution of $^{12}\text{CO}_2$ and
257 $^{13}\text{CO}_2$ by the mass gas analyser.

258 **2.2.5 Mass balance**

259 Experimental data consistency of the measured rates was verified using
260 standard data reconciliation procedures under the elemental mass balance
261 constraints (34). The biomass elemental composition used in the
262 reconciliation procedure was taken from the closely related non-
263 methylotrophic bacterium *Bacillus subtilis*, $\text{CH}_{1.646}\text{N}_{0.219}\text{O}_{0.410}\text{S}_{0.005}$ (35, 36). The
264 ashes content were considered to be 6 % of the dry cell weight, average
265 value obtained from different microorganisms (i.e. *Escherichia coli*,
266 *Aspergillus niger*, *Penicillium chrysogenum*, *Klebsiella aerogenes* (37)).
267 After no proof of mismatch in the measurements, a better estimation of the
268 physiological parameters were obtained as described by (34).

269 **2.3 Stationary ^{13}C fluxomics experiments**

270 **2.3.1 Culture conditions**

271 For the carbon sources mannitol and arabitol, the culture medium
272 composition remained unchanged. The experiments were performed in

273 500 ml baffled shake flasks using 40 ml of media, and cells were grown at
274 50 °C and 200 rpm. Pre-cultures contained yeast extract and 15 mM
275 unlabeled mannitol or arabitol. They were inoculated as stated previously
276 and grown overnight. The pre-cultures were used to inoculate triplicate main
277 cultures to an OD₆₀₀ of 0.05, after centrifugation and re-suspension in media
278 without yeast extract. The media to perform the ¹³C MFA contained 15 mM
279 [1-¹³C] mannitol, 15 mM [5-¹³C] arabitol or 15 mM of a mixture of 10 % [1-¹³C]
280 arabitol and 90 % [2-¹³C] arabitol (99 % ¹³C; Omicron Biochemicals, Inc.,
281 South Bend, IN, USA). An experimentally determined conversion factor of
282 0.22 g/litre (dry weight) of cells per OD₆₀₀ unit was used. Growth curves are
283 available in Supplementary Data 1.

284 **2.3.2 Measurements of proteinogenic amino acids ¹³C-** 285 **isotopologues**

286 Mannitol (resp. arabitol) cultures were sampled around 10 h (resp. 30 h) once
287 they reached an OD₆₀₀ of 1.3. The pellets obtained from the cellular extract
288 were hydrolyzed 15 h at 110 °C with 500 µl HCL 6N. Samples were
289 evaporated and washed twice with 500 µl of ultrapure water, evaporated to
290 dryness, resuspended (625 µl, water), and diluted (1/1000, water) for the
291 mass spectrometry analysis.

292 Amino acids were separated on a PFP column (150 × 2.1 mm i.d., particle
293 size 5 µm; Supelco Bellefonte, PEN, USA). Solvent A was 0.1 % formic acid in
294 H₂O and solvent B was 0.1 % formic acid in acetonitrile at a flow rate of
295 250 µL/min. The gradient was adapted from the method used by (38).

296 Solvent B was varied as follows: 0 min, 2 %; 2 min, 2 %; 10 min, 5 %; 16 min,
297 35 %; 20 min, 100 %; and 24 min, 100 %. The column was then equilibrated
298 for 6 min at the initial conditions before the next sample was analyzed. The
299 volume of injection was 20 μ L.

300 High-resolution experiments were performed with an Ultimate 3000 HPLC
301 system (Dionex, CA, USA) coupled to an LTQ Orbitrap Velos mass
302 spectrometer (Thermo Fisher Scientific, Waltham, MA, USA) equipped with a
303 heated electrospray ionization probe. MS analyses were performed in
304 positive FTMS mode at a resolution of 60 000 (at 400 m/z) in full-scan mode,
305 with the following source parameters: the capillary temperature was 275 °C,
306 the source heater temperature, 250 °C, the sheath gas flow rate, 45 a.u.
307 (arbitrary unit), the auxiliary gas flow rate, 20 a.u., the S-Lens RF level, 40 %,
308 and the source voltage, 5 kV. Isotopic clusters were determined by extracting
309 the exact mass of all isotopologues, with a tolerance of 5 ppm. Experimental
310 CIDs of alanine, glycine, valine, serine, threonine, phenylalanine, aspartate,
311 glutamate, histidine, isoleucine, leucine, lysine, arginine, tyrosine, proline
312 and methionine were obtained after correction of raw MS data for naturally
313 occurring isotopes other than carbon, using IsoCor (33).

314 Careful inspection of the CID revealed an overall excellent reproducibility
315 between both the technical and biological replicates (Supplementary Data 1).
316 However, M0 of valine and M0-M1 of glycine had a higher variability which
317 could be due to a signal closer to the noise level.

318 2.3.3 NMR measurements

319 Concentrations in supernatants were measured by ^1H 1D-NMR at 290 °K,
320 using a 30° angle pulse and a presaturation of water signal was applied
321 during a relaxation delay of 8 s. TSP-d4 was used as internal standard for
322 calibration and quantification.

323 The measurement of isotopomers and specific enrichments of targeted
324 biomass components were performed using the same samples used for
325 proteinogenic amino acids ^{13}C -isotopologues MS analysis, redried and
326 suspended in 200 μl D_2O (0.1 % DCI). The positional isotopomer distribution
327 of alanine C2 and C3 was extracted from the analysis of ^{13}C - ^{13}C couplings in
328 2D ^1H - ^{13}C HSQC experiments (39). The carbon isotopic enrichments of
329 alanine (C2 and C3) and histidine (C2 and C5) were extracted from the
330 analysis of ^1H - ^{13}C couplings using 2D-zero quantum filtered-TOCSY (ZQF-
331 TOCSY) (40).

332 NMR spectra were collected on an Avance III 800 MHz spectrometer (Bruker,
333 Germany), equipped with a 5mm z-gradient QPCI cryoprobe. Every
334 acquisition 1D, 2D and absolute quantification were performed on ^1H -1D
335 spectra using TopSpin 3.5 (Bruker, Germany).

336 **2.4 Models and simulations**

337 **2.4.1 Metabolic Flux Analysis software**

338 All simulations needed for Metabolic Flux Analysis (MFA) on methanol,
339 mannitol and arabitol were performed with *influx_si* software v4.4.4 (41),
340 either in stationary or non-stationary mode. *influx* has the advantage to
341 allow for the integration of labeling data coming from different experimental
342 setups (MS, NMR) and to support several integration strategies (stationary,
343 non-stationary, parallel labeling).

344 All input and output files needed for reproducibility are available in an
345 archive in Supplementary Data 2. Importantly, this includes the models in
346 FTBL and SBML file formats.

347 **2.4.2 Metabolic models**

348 We designed the models to cover central carbon metabolism and biomass
349 needs of *B. methanolicus*. *influx_si* uses a non-standard legacy file format
350 (FTBL) to encode the metabolic network and the associated atom-atom
351 transitions. This format centralizes the metabolic network with all biological
352 measurements, i.e. metabolites pool sizes, fluxes, and carbon isotopologue
353 distribution. Consequently, we developed distinct model files for each carbon
354 source. Models share the same nomenclature and the same general topology
355 between them, which is displayed in Fig. 1 and detailed in Supplementary
356 Data 1.

357 Assimilation pathways of methanol, mannitol and arabitol were included
358 when relevant to explain the incorporation of the tracer. The CO₂ pool was
359 explicitly modeled within the system to allow for re-incorporation of tracer
360 via CO₂. Amino acids synthesis pathways were modeled as part of biomass
361 needs along with important precursors. Biomass equation was borrowed from
362 *Bacillus subtilis* genome-scale model (42). Reaction for phosphoenolpyruvate
363 carboxykinase (BMMGA3_RS13120) was not included in the final model as
364 the associated expression level was rather low in proteomics (26) and
365 transcriptomics studies (21, 25).

366 Unless otherwise stated, each culture replicate was processed independently
367 to estimate fluxes for their respective carbon source condition.

368 For MFA on mannitol, we exploited carbon isotopologue distribution data of
369 proteinogenic alanine, glycine, valine, serine, threonine, phenylalanine,
370 aspartate, glutamate, histidine, isoleucine, leucine, lysine, arginine, tyrosine,
371 proline and methionine. Acetate production was modeled with an export flux
372 from acetyl-CoA to which we associated the acetate flux measured from
373 supernatant data. Acetyl-CoA was further constrained using acetate
374 positional labeling measured by ¹H 1D-NMR spectroscopy from the
375 supernatant.

376 For MFA on arabitol, we averaged the proteinogenic labeling measurements
377 of the [5-¹³C] arabitol experiment and exploited it as a parallel labeling
378 dataset for each biological replicate of the [1/2-¹³C] arabitol experiment. We
379 analysed the same proteinogenic amino acids as those mentioned above for

380 mannitol. No acetate was observed in the supernatant and the associated
381 export reaction was consequently excluded from this model. Additionally, we
382 exploited specific labeling enrichment of histidine, alanine and ribulose-5-P,
383 and positional isotopomer data of alanine from labeling samples as described
384 in section 2.3.3.

385 For MFA on methanol, the non-stationary nature of the experiment and the
386 subsequent importance of the pools on flux distributions forced us to explicit
387 most of the reactions of the central metabolism that were lumped for the
388 stationary models. Measurements described above were used to constrain
389 intra and extracellular pools (section 2.2.3), and isotopologues profiles
390 (section 2.2.4) through *influx_si* optimization process. The exchange fluxes of
391 CO₂ and methanol (feed and evaporation) were also exploited. No acetate
392 production was observed.

393 **2.4.3. Quality checks**

394 Experimental data were fitted to our models as per described above. For
395 each culture replicate we performed a Monte Carlo sensitivity analysis
396 (n=100) on the fit to assess its robustness to small variations around the
397 fitted values. We also performed a chi-squared goodness-of-fit statistical test
398 to ensure that simulated data for each biological replicate were significantly
399 close to experimental data. All tests were significant with a significance
400 level (α) of 0.05 (Supplementary Data 2). For convenience, we provide
401 figures of measured vs. simulated data points (Fig. S3).

402 Let us note here that we unfortunately were unable to estimate at a
403 satisfactory precision the fluxes through malate dehydrogenase
404 (BMMGA3_RS12590, 1.1.1.37), malic enzyme (*mae*, BMMGA3_RS12650,
405 1.1.1.38 or 1.1.1.40) and pyruvate carboxylase (*pyc*, BMMGA3_RS05255,
406 6.4.1.1). Those three reactions formed a cycle from pyruvate (Pyr) to
407 oxaloacetate (OAA) and malate (Mal) in all our tested models. However, the
408 Monte Carlo sensitivity analysis revealed that those fluxes were statistically
409 undefined (not shown), meaning that virtually any value through the cycle
410 would satisfy the constraints of the rest of the network. In the absence of
411 biological data to motivate any new constraint on the model, we preferred to
412 leave those reactions out of the analysis.

413 **2.5 Analysis of arabitol phosphate dehydrogenases**

414 **AtID and AtIF**

415 **2.5.1 Strains and culture conditions**

416 In this study, *Escherichia coli* DH5 α (43) was used as the standard cloning
417 host and recombinant protein production was carried out with *E. coli*
418 BL21(DE3) (44). A summary of the strains, primers and plasmids constructed
419 and used in this study can be found in Table 1. *E. coli* strains were routinely
420 cultivated at 37 °C and 180 rpm in Lysogeny Broth (LB) medium or on LB
421 agar plates supplemented with 100 $\mu\text{g ml}^{-1}$ ampicillin and 0.5 mM IPTG when
422 relevant.

423 **2.5.1 Recombinant DNA work**

424 Molecular cloning was performed as previously described (45) using primer
425 sequences listed in Table 1. Total DNA isolation from *B. methanolicus* was
426 performed as described in (46). Inserts were amplified by polymerase chain
427 reactions (PCRs) with ALLin™ HiFi DNA Polymerase (HighQu, Kraichtal,
428 Germany) and purified with the NucleoSpin® Gel and PCR Clean-up kit
429 (Macherey-Nagel, Düren, Germany). Plasmids were constructed from PCR-
430 generated fragments and pET16b vector cut with restriction enzymes using
431 the isothermal DNA assembly method (47). The GeneJET Plasmid Miniprep Kit
432 (Thermo Fisher Scientific, Waltham, USA) was used for plasmid isolation. For
433 the transformation of chemically competent *E. coli* cells, the procedure
434 described by (48) was followed. Colony PCRs were performed using Taq
435 polymerase (New England Biolabs, Ipswich, England) with primers P192,
436 P193, P194 and P195 (Table 1). All cloned DNA fragments were verified by
437 sequencing (Sequencing Core Facility, Bielefeld University).

438 **2.3.2 Overproduction and purification of AtID and AtIF**

439 Plasmids for protein production using *E. coli* BL21 (DE3) were constructed on
440 the basis of pET16b (Novagen, Madison, WI, USA) and are presented in
441 Table 1. The *atID* and *atIF* genes were PCR-amplified from *B. methanolicus*
442 MGA3 genomic DNA using the primers P192 and P193 or P194 and P195,
443 respectively (Table 1). The resulting product was joined with *Bam*HI digested
444 pET16b by applying the isothermal DNA assembly method (47), resulting in
445 pET16b-*atID* and pET16b-*atIF*. The pET16 vector allows for production of N-

446 terminal His₁₀-tagged proteins. Protein production and purification was
447 performed following the indications of (49), except for cell lysis which was
448 performed by sonication (UP 200 S, Dr. Hielscher GmbH, Teltow, Germany) on
449 ice at an amplitude of 55 % and a duty cycle of 0.5 for 8 min with a pause in
450 between. Supernatants were subsequently filtered using a 0.2 µm filter and
451 purified by nickel affinity chromatography with nickel-activated nitrilotriacetic
452 acid-agarose (Ni-NTA) (Novagen, San Diego, CA, USA). His-tagged AtID and
453 AtIF proteins eluted with 20 mM Tris, 300 mM NaCl, 5 % (vol/vol) glycerol and
454 50, 100, 200, or 400 mM imidazole were analysed by 12 % SDS-PAGE (50).
455 Fractions showing the highest protein concentrations (with 100 and 200 mM
456 or 100, 200 and 400 mM imidazole for AtID and AtIF, respectively) were
457 pooled and protein concentration was measured according to the Bradford
458 method (51) using bovine serum albumin as reference. The purified protein
459 was subsequently applied for enzymatic assays.

460 **2.3.3 Arabitol phosphate dehydrogenase enzymatic assays**

461 Determination of purified AtID and AtIF activities in the reductive reaction
462 using Xyl5P or Ribu5P as substrate were performed as previously described
463 (23). The assay mixture contained 20 mM Tris-HCl buffer (pH 7.2), 1 mM DTT,
464 0.04 to 0.3 mM NADH or NADPH, 0.03 to 0.6 mM Xyl5P or 0.2 to 4 mM Ribu5P
465 and 0.01 to 0.04 mg AtID or 0.2 to 0.4 mg AtIF in a total volume of 1 ml. The
466 oxidation rate of NADH or NADPH was monitored at 340 nm and 30 °C for 3
467 min using a Shimadzu UV-1202 spectrophotometer (Shimadzu, Duisburg,
468 Germany). In order to confirm the presence of arabitol phosphate in the
469 enzyme reactions after reduction of Xyl5P and Ribu5P, samples were

470 subjected to liquid chromatography-mass spectrometry (LC-MS) analyses
471 following the procedure described in (52).

472 **2.4 Data availability**

473 Gene locii mentioned throughout the text are from NCBI annotation of *B.*
474 *methanolicus* MGA3 genome NZ_CP007739.1
475 (https://www.ncbi.nlm.nih.gov/nucore/NZ_CP007739.1).

476 Supplementary Data 1 contains growth curves, processed MS and NMR data
477 and a summary of the reactions modeled.

478 Supplementary Data 2 contains raw models, input and output files for influx
479 software and can be downloaded from
480 https://fairdomhub.org/data_files/3269?version=1.

481 **3. RESULTS & DISCUSSION**

482 **3.1 *In vitro* assessment of arabitol assimilation**

483 The operon responsible for arabitol assimilation in *B. methanolicus* consists
484 of a PTS system (AtIABC) and two putative arabitol phosphate
485 dehydrogenases (AtID and AtIF) (22), which are chromosomally encoded and
486 belong to the diverse superfamily of medium-chain
487 dehydrogenases/reductases (MDRs). However, the physiological roles of AtID
488 and AtIF have not been described to date. Members of the MDR superfamily
489 have high sequence conservation, but sequence-based prediction of their
490 substrate scope is difficult since wide substrate specificity is common (53,
491 54) (see Supplementary Text for a discussion of their phylogeny). The
492 substrate selectivity of AtID and AtIF was therefore studied to identify
493 whether arabitol is assimilated via arabitol 1-phosphate dehydrogenase to
494 Xyl5P, and/or to Ribu5P via arabitol 5-phosphate dehydrogenase (23) (Fig. 2).
495 The enzymes were purified as N-terminally His-tagged proteins from
496 recombinant *E. coli* by nickel chelate chromatography. Arabitol phosphate
497 oxidation could not be assayed because there are no commercial arabitol 1-
498 phosphate or arabitol 5-phosphate standards. Therefore, the reverse reaction
499 was tested, as described in material and methods section 2.3.3, with either
500 Xyl5P or Ribu5P as substrate for NAD(P)H dependent reduction. A number of
501 potential sugars (D-ribose, D-fructose, D-xylose, D-mannose, L-arabinose, D-
502 arabinose, L-sorbose, D-galactose, D-glucose, ribose 5-phosphate, glucose 6-

503 phosphate, glucose 1-phosphate, fructose 6-phosphate and fructose 1-
504 phosphate) and sugar alcohols (D-arabitol, D-mannitol, D-galactitol, D-sorbitol,
505 L-arabitol, D-maltitol, D-xylitol, ribitol and meso-Erythritol) were also tested as
506 substrates but no significant activity (i.e. $> 0.05 \text{ U mg}^{-1}$) was detected. The
507 kinetic parameters measured for AtID and AtIF reduction using either Xyl5P
508 or Ribu5P as substrate are summarized in Table 2. The K_M of $0.07 \pm 0.03 \text{ mM}$
509 for AtID with Xyl5P as substrate and NADH as cofactor was 2.5 times lower
510 than the value obtained for AtIF ($0.18 \pm 0.05 \text{ mM}$). With Ribu5P as substrate,
511 the K_M for AtID was 17 times lower ($1.21 \pm 0.42 \text{ mM}$) (Table 2), and for AtIF,
512 no activity was detected. The V_{\max} for AtID with Xyl5P as substrate and NADH
513 as cofactor was 2.7 times higher than with Ribu5P as substrate ($0.49 \pm$
514 0.06 U mg^{-1}) and 12 times higher than for AtIF with Xyl5P ($0.11 \pm 0.01 \text{ U mg}^{-1}$)
515 (Table 2). NADH was the preferred cofactor over NADPH with a ten times
516 lower K_M (0.01 ± 0.01 vs $0.11 \pm 0.09 \text{ mM}$). The affinity and NADPH
517 dependent activity ($0.24 \pm 0.06 \text{ U mg}^{-1}$) could only be determined with AtID
518 and Xyl5P, as no significant activity was detected for any of the other
519 reactions. LC-MS analyses were performed to confirm the formation of
520 arabitol phosphate in the enzyme reactions catalyzed by AtID. Although
521 arabitol 1-phosphate and arabitol 5-phosphate could not be distinguished,
522 arabitol phosphate was clearly produced with both Xyl5P and Ribu5P as
523 substrates (Fig. S2).

524 Overall, these data suggest that AtID has a major role in arabitol catabolism
525 *in vitro* and that AtID and AtIF both prefer Xyl5P. This suggests that arabitol is
526 mainly assimilated through the arabitol 1-phosphate pathway. However,

527 assimilation via arabitol 5-phosphate cannot be excluded since AtID can also
528 use Ribu5P, albeit with reduced efficiency as shown both by the kinetic
529 parameters (Table 2) and the significant residual Ribu5P detected in the
530 enzyme reactions (Fig. S2). Moreover, *in vitro* enzymatic analyses of purified
531 arabitol phosphate dehydrogenase from *E. avium* (23) and *Bacillus*
532 *halodurans* (55) showed that both could convert arabitol 1-phosphate and
533 arabitol 5-phosphate into both Xyl5P and Ribu5P. By assessing metabolic
534 operations *in vivo*, ¹³C-MFA experiments should identify which assimilation
535 pathway is actually used *in vivo*.

536 **3.2 ¹³C-MFA experimental design**

537 Experimental design is a key step to define the isotopic composition of the
538 label input and the isotopic data to be measured, thereby improving both the
539 number of fluxes that can be estimated from a set of isotopic data and the
540 precision of the flux values. To address this point, we used a dedicated
541 program, IsoDesign (56), using as input metabolic models of each carbon
542 source and several labels as described in the material and methods section.
543 For arabitol and mannitol, good flux precision could be obtained with mass
544 spectrometry labelling data from proteinogenic amino acids. This is
545 advantageous for two reasons. First, the experimental setup is simpler than
546 for intracellular metabolites because no quenching is required and the
547 cellular pellet can just be collected by centrifugation. Second, the labelling
548 can be measured by NMR and MS, providing crucial positional information to
549 distinguish between the two pathways (i.e. via arabitol 5-phosphate or via

550 arabitol 1-phosphate dehydrogenase). Among the different label inputs
551 tested, 100% [5-¹³C] arabitol appeared ideal to identify whether arabitol is
552 converted into arabitol 1-phosphate only or into arabitol 5-phosphate only. In
553 addition, a 9:1 mix of [1-¹³C] and [2-¹³C] arabitol was used to see if both
554 pathways are active. For mannitol, the best label input was 100 % [1-¹³C].
555 Finally, since methanol is a C1 compound, a stationary ¹³C-MFA approach is
556 not suitable since the amino acids become fully labeled in the isotopic
557 steady-state. Non-stationary ¹³C fluxomics should be used instead to follow
558 the incorporation of the tracer after a pulse of labeled substrate; however
559 significantly more ¹³C data are required for this approach (57, 58)
560 (Supplementary Data 1).

561 All labeling samples were collected in the exponential growth phase at
562 metabolic steady state and analyzed by MS or 1D ¹H NMR. The labelling
563 profile of the analyzed metabolites, as measured by their CIDs, were
564 inspected manually and then used with additional NMR and physiological
565 data to fit a model of *B. methanolicus*'s central metabolism (Supplementary
566 Data 1).

567 **3.3. Measurement of physiological parameters**

568 Assessment of physiological parameters is a prerequisite for flux calculation.
569 Here, *B. methanolicus* was grown in batch on three different carbon sources.
570 For each cultivation, growth rate and consumption and production rates were
571 determined. Results are given in Table 3. No significant differences between
572 the physiological parameters obtained for the culture replicates were

573 observed. On methanol (batch cultures at 50 °C), around 35 % of the carbon
574 source was directly evaporated, and biomass and carbon dioxide were the
575 only products formed in detectable amounts. The maximal growth rate
576 obtained here with methanol (0.46 h⁻¹) is slightly higher than reported in a
577 previous proteomic study of *B. methanolicus* MGA3 (0.40 h⁻¹, (14)) or for the
578 growth of the related strain *B. methanolicus* PB1 (0.32 h⁻¹, (15)). Biomass
579 yields did not differ significantly from 0.5 g/g indicating that approximately
580 half of the consumed methanol went to biomass and the other half was
581 oxidized to CO₂. The growth rates with mannitol and arabitol are consistent
582 with published values (22).

583 *B. methanolicus* MGA3 is known to overproduce glutamate at up to 50 g/l
584 (21) on methanol under magnesium or methanol limitation (59, 60). When
585 grown on arabitol or methanol, no metabolite accumulated in the
586 supernatant at concentrations above the NMR detection limit (approximately
587 100 μM). There was therefore little or no metabolite secretion by MGA3 under
588 our chosen methanol and arabitol growth conditions, which is consistent with
589 previous studies and the growth conditions studied here (27, 28). However,
590 acetate was produced at up to 2 mmol/gDCW/h in mannitol cultures (yield,
591 0.3 mol/mol). To the best of our knowledge, acetate production has never
592 previously been reported for *B. methanolicus*. Based on genomics data (21),
593 we hypothesized that acetate is synthesized from acetyl-CoA in a classical
594 two-step process involving phosphate acetyltransferase (EC:2.3.1.8,
595 BMMGA3_RS15725) and acetate kinase (EC:2.7.2.1, BMMGA3_RS12735).
596 Acetate has moreover been discussed at length in the context of overflow

597 metabolism, a special metabolic state in which fermentation pathways are
598 used even though further oxidation (respiration) would be more ATP-efficient
599 (61–64). Overflow metabolism has industrial implications since it could lead
600 to carbon and energy waste.

601 Overall, we showed the reproducible growth characteristics of our cultures,
602 and showed an unexpected production of acetate that may have an impact
603 for industrial applications, as overflow metabolism leads to carbon and
604 energy waste.

605 **3.4 *In vivo* characterization of arabitol assimilation**

606 The *in vitro* enzymatic analyses of the two dehydrogenases, AtID and AtIF,
607 suggest that both assimilation pathways (i.e. via arabitol 1-phosphate and
608 via arabitol 5-phosphate) may operate *in vivo*. To confirm whether either or
609 both arabitol assimilation pathways are operative in *B. methanolicus*, as
610 suggested for *E. avium* (23) and *Bacillus halodurans* (55), we carried out a
611 ¹³C-MFA specifically designed to discriminate between the two pathways (see
612 section 3.1, and Fig 2). Interestingly, while the possibility to assimilate
613 arabitol through Xyl5P or Ribu5P or both was a free parameter, the optimal
614 solution found during the fitting process exclusively used the route through
615 Xyl5P (Fig. 1C). This indicates that the (low) activity observed *in vitro* through
616 Ribu5P was not present at a detectable level in our cultures, and that the PTS
617 system imports arabitol as arabitol 1-phosphate. The kinetic parameters
618 obtained for AtID and AtIF are in line with the flux data, i.e. entry of arabitol
619 into the pentose phosphate pathway (PPP) via PTS-mediated uptake and

620 phosphorylation to arabitol 1-phosphate followed by oxidation to Xyl5P with
621 AtID as the major dehydrogenase (Fig. 2 and Table 2).

622 Overall, these data demonstrate for the first time how arabitol is assimilated
623 in *B. methanolicus* and rule out the hypothesis of additional catabolism
624 through arabitol 5-phosphate and Ribu5P derived from our enzymatic
625 analyses (Table 2) and previous reports in *E. avium* (23) and *B. halodurans*
626 (55).

627 **3.5. *In vivo* operation of the pentose phosphate** 628 **pathway with the different carbon sources**

629 *B. methanolicus* assimilates methanol through the ribulose monophosphate
630 (RuMP) cycle that condenses formaldehyde (For) and ribulose 5-P (Ribu5P)
631 into hexulose 6-P (Hex6P) (65). The regenerative part of the RuMP cycle that
632 maintains a pool of Ribu5P overlaps with the non-oxidative pentose
633 phosphate pathway (PPP). Strong flux through the PPP is therefore expected
634 on methanol and indeed, ribulose-phosphate 3-epimerase's relative flux
635 accounted for 67 % of methanol assimilation (*rpe*, Fig. 1A). Interestingly,
636 mannitol and arabitol are closely connected to the PPP since mannitol is
637 converted to fructose 6-P (F6P) (just like methanol), whereas arabitol is
638 converted to Xyl5P as discussed above. On mannitol (Fig. 1B), PPP utilization
639 was low (the estimated *rpe* flux was 15 % of mannitol assimilation), which
640 contrasts with the predominance of the PPP on methanol. On arabitol
641 (Fig. 1C), the fluxes associated with the PPP remained low (*rpe* flux,
642 1.2 mmol/gDCW/h; Fig. 3), but they accounted for a larger fraction of the

643 assimilated carbon flow (the estimated *rpe* flux was 28 % of arabitol
644 assimilation) than on mannitol. This indicates that the PPP is more important
645 for carbon assimilation on arabitol than on mannitol, in spite of similar
646 absolute reaction rates and expression levels (22). Simulations carried
647 without transaldolase activity indicated that it was essential to explain the
648 labeling data given the network topology used (notably *glpx* been
649 irreversible). A possibility for future studies would be to take advantage of
650 adaptive laboratory driven evolution, or overexpression of key enzymes such
651 as transaldolase, to investigate if the PPP could be adjusted to increase
652 growth rates when arabitol is the sole source of carbon and energy.

653 The RuMP cycle has several variants, which differ in their efficiency (66).
654 Genes for two of these have been identified in MGA3, namely, the fructose
655 bisphosphate aldolase/sedoheptulose bisphosphatase (SBPase) cycle (67)
656 and the fructose bisphosphate aldolase/transaldolase (TA) cycle, which as
657 their names suggest favor the regeneration of Rib5P through sedoheptulose
658 bisphosphatase and transaldolase, respectively. It is generally accepted that
659 MGA3 uses the SBPase variant (65). The main evidence for this is the
660 presence of a copy of a characteristic gene of the SBPase variant (*glpX^P*) on
661 the pBM19 plasmid, whereas there is only one transaldolase gene (*ta^C*) in the
662 chromosome. Proteomic (26) and transcriptomic (21) studies have also
663 associated *glpX^P* with a significant increase in expression in methanol
664 compared with mannitol, whereas the expression associated with *ta^C*
665 remained constant. According to the MFA, both *glpx* (associated to *glpX^P*) and
666 *ta* (associated to *ta^C*) carry a comparable flux, thus both variant may be

667 active (Fig. 3). This arrangement may serve as a fail-safe to guarantee the
668 replenishment of Ribu5P. Alternatively, since transaldolase activity is
669 essential to fit the isotopic data for growth on arabitol, an advantage of the
670 TA cycle may be that it increases the flexibility of the PPP and allows the
671 regeneration of important precursors such as Ribu5P from different carbon
672 sources.

673 The labeling data suggest that the oxidative part of the PPP is almost shut
674 down on methanol, with an estimated absolute flux of 0.16 mmol/gDCW/h
675 through glucose 6-phosphate isomerase (*pgi*, < 1 % of the flux relative to
676 methanol assimilation, Fig. 3). On mannitol and on arabitol, utilization of the
677 oxidative part of the PPP is higher, with estimated absolute fluxes of 1.87
678 mmol/gDCW/h and 0.53 mmol/gDCW/h, respectively (Fig. 3). This is in
679 contrast with previous findings that suggested that the oxidative part of the
680 PPP might be used on methanol to provide NADPH while detoxifying
681 formaldehyde (14, 27) via the so-called cyclic dissimilatory RuMP pathway
682 (21, 68). This claim is supported by (27), based on the comparable pool sizes
683 and isotopic labeling incorporation rates between metabolites of the PPP and
684 6-phosphogluconate (Gnt6P), a key metabolite of the oxidative part of the
685 PPP. Additionally, glucose 6-phosphate dehydrogenase (*zwf*,
686 BMMGA3_RS06660) has been found to be highly over-expressed in both
687 transcriptomics and proteomics studies on methanol compared to mannitol
688 (14). Nonetheless, the same studies report that the other steps of the
689 oxidative PPP are not over-expressed, which include the decarboxylation
690 conducted by phosphogluconate dehydrogenase (*gnd*, BMMGA3_RS10800).

691 The utilization of the oxidative part of the PPP is of particular interest
692 because, intuitively, one imagines that decarboxylation should be avoided
693 when growth occurs on a C1 to avoid wasting carbon. This intuition proved to
694 be correct in Bennett et al.'s (69) study of an *E. coli* synthetic methylotroph
695 in which they knocked-out *pgi* to increase the regeneration of Rib5P through
696 the non-oxidative part of the PPP. However, we cannot exclude the possibility
697 that the oxidative part of the PPP serves as a backup formaldehyde
698 dissimilation pathway when the linear dissimilation pathways become
699 saturated at high methanol concentrations. *B. methanolicus* is indeed quite
700 sensitive to variations in methanol concentration (70) and we can assume
701 that this critical biological function is tightly controlled. The true importance
702 of the cyclic dissimilatory RuMP pathway for natural methylotrophic growth is
703 therefore difficult to ascertain without additional experiments to specifically
704 measure utilization of the oxidative part of the PPP at different methanol
705 concentrations.

706 As expected, the ¹³C-MFA shows that the PPP is critical on methanol as it
707 overlaps with the RuMP responsible for methanol assimilation. The SBPase
708 variant of the RuMP is active, however we could not rule out a parallel
709 operation of the TA variant. We suggest that a parallel operation on mixed
710 carbon sources may benefit *B. methanolicus* to replenish important
711 precursors pools. Surprisingly, the oxidative part of the PPP was inactive in
712 our conditions, which question the true importance of the cyclic dissimilatory
713 RuMP for methylotrophic growth.

714 **3.6 *In vivo* operation of the TCA cycle with the** 715 **different carbon sources**

716 *B. methanolicus* has a full gene set for a functional tricarboxylic acid cycle
717 (TCA) and glyoxylate shunt (14, 21). This seems to contrast with some
718 methylotrophs, including some that use the RuMP pathway, that do not need
719 a complete TCA to fulfill their energy requirements (71). Results (Fig. 1A)
720 indicate that the TCA is used much less than the RuMP pathway on methanol,
721 with a rate close to 1 mmol/gDCW/h up to 2-oxoglutarate (AKG) and no flux
722 afterwards (Fig. 3). This small flux is needed to support the synthesis of
723 biomass precursors. On mannitol and arabitol in contrast, the TCA is used
724 intensively, with rates of 3.5 and 4.7 mmol/gDCW/h respectively for isocitrate
725 dehydrogenase (*idh*). These results are in agreement with previous
726 measurements of the actual usage of the TCA during methylotrophic growth.
727 At the transcript and protein levels, it has been suggested that the TCA
728 should be more active on mannitol than on methanol (21, 26). Activity
729 assays in crude cell extracts also showed very low 2-oxoglutarate
730 dehydrogenase (*akgdh*) activity (59). Finally, isotopic labeling experiments
731 have shown slow isotopic enrichment of key TCA metabolites (citrate, 2-
732 oxoglutarate, fumarate) on methanol (27).

733 Although *B. methanolicus* also has glyoxylate shunt genes
734 (BMMGA3_RS01750, 2.3.3.9; and BMMGA3_RS01755, 4.1.3.1), the reported
735 expression levels suggest that this pathway does not carry a high flux under
736 mannitol or under methanol growth conditions (21, 26). In agreement with

737 these findings, the glyoxylate shunt fluxes estimated in this study were
738 negligible under all the tested conditions (Fig. 3).
739 Overall, as reported before, the TCA is mainly active in non-methylotrophic
740 conditions and the glyoxylate shunt was inactive in our conditions.

741 **3.7 Analysis of cofactor usage with the various** 742 **carbon sources**

743 To assess how *B. methanolicus* balances its redox and energy needs, we used
744 the estimated fluxes from the ¹³C-MFA to infer production and consumption
745 rates of ATP, NADH and NADPH, as displayed in Fig. 4. ¹³C-MFA is constrained
746 by carbon balance and the distribution of the isotopic tracer, but unlike flux
747 balance analysis it is typically not constrained by cofactor balance. We used
748 the estimated fluxes from the MFA and the expected stoichiometry of the
749 associated reactions to assess the absolute rates of cofactor production and
750 consumption. In the absence of specific measurements, we use the biomass
751 requirements of *B. subtilis* (7, 72). Additionally, since the samples were
752 collected in metabolic pseudo steady-state, the production and consumption
753 rates of each cofactor were assumed to be balanced; this allowed us to
754 identify rates that would have been impossible to estimate otherwise such as
755 the proportion of NAD (and ATP) formed from the respiratory chain (with a
756 P/O=1.5) and other production/consumption rates not accounted for by our
757 other assumptions.

758 Despite their different growth rates, which influence their cofactor
759 requirements for growth (Table 3), the cells grown on mannitol and arabitol

760 had a similar absolute usage of NADH, NADPH and ATP (Fig. 4). ATP and
761 NADH came mostly from the same sources. However, the proportion of
762 NADPH generated in the oxidative part of the PPP was three times higher in
763 mannitol growth conditions than in arabitol (3.5 against 1.0 mmol/gDCW/h).
764 This difference was compensated by a higher flux in the TCA for arabitol (4.7
765 against 3.5 mmol/gDCW/h) in excess of the estimated NADPH requirements
766 for growth and even contributing to the production of ~ 3.4 mmol/gDCW/h
767 NADPH whose consumption remains unaccounted for. Discrepancies between
768 estimates of the cofactor requirements for biomass formation and those
769 derived from measured isotopic data are typical for this kind of analysis (73,
770 74), and can be attributed to an underestimation of cofactor requirements,
771 notably for non-essential processes such as cell motility (for ATP). Note,
772 nevertheless, that the estimated biomass requirement for NADPH was not
773 covered under methanol conditions, as 1.5 mmol/gDCW/h is missing from the
774 balance. This may be due to an unaccounted for NADPH-producing process
775 (75), for instance the malic enzyme (*mae*, 1.1.1.40, BMMGA3_RS12650)
776 whose flux could not be estimated with this approach. To the best of our
777 knowledge, there is no evidence of transhydrogenase activity in *B.*
778 *methanolicus*.

779 Comparing methylotrophic and non-methylotrophic growth, it is perhaps
780 unsurprising that NADH is produced at a higher rate on methanol
781 (44 mmol/gDCW/h, versus 30 mmol/gDCW/h on mannitol), because of the
782 conversion of methanol into formaldehyde by methanol dehydrogenase (76).
783 This suggests that at the same growth rate, O₂ consumption should be higher

784 on methanol to provide the additional NAD⁺ required. Unlike NADH, the
785 NADPH total production is estimated to be roughly the same across our
786 conditions, around 6 mmol/gDCW/h (Fig. 4). As discussed above, the linear
787 formaldehyde detoxification pathways are extensively used in our methanol
788 conditions, while usage of the oxidative part of the PPP (which would be part
789 of the cyclic dissemination pathway) is negligible. In term of cofactors, this
790 mostly affects the sources used for NADPH formation, as the major source on
791 methanol is the detoxification pathway (4.8 mmol/gDCW/h), while the main
792 sources on mannitol are the oxidative part of the PPP (3.6 mmol/gDCW/h)
793 and the TCA (3.5 mmol/gDCW/h). These estimates suggest that linear
794 detoxification pathways play an important role in the generation of NADPH
795 on methanol, in addition to their established protective function against
796 formaldehyde.

797 Non-methylotrophic growth on mannitol and arabitol share the same features
798 despite their associated different growth rates (with the notable exception of
799 the contribution of the oxidative PPP for NADPH production). On methanol,
800 however, we observe more differences in the origin of cofactors production
801 which clearly highlight a different metabolic state. Importantly, the linear
802 detoxification pathways could have a more important role in cofactor
803 regeneration than what was previously envisioned.

804 **3.8. Conclusion**

805 In summary, this MFA of *B. methanolicus* MGA3 provides three snapshots of
806 its metabolic states for growth on methanol, mannitol or arabitol. Isotopic

807 data are consistent with prior knowledge of MGA3 methylotrophy, showing
808 greater flux in the RuMP cycle than in the TCA. The ¹³C-MFA provided new
809 insights related to the utilization of cyclic RuMP versus linear dissimilation
810 pathways, and between the RuMP cycle variants; and finally, the
811 characterization of the arabitol assimilation pathway was completed using
812 enzymatic data. In futur studies, these validated flux maps will be used as
813 references for constraint based modelling to validate genome-scale model
814 predictions. Overall, the information provided in this work and previous omics
815 studies on *B. methanolicus* metabolism can be used to improve design
816 strategies for new strains (i.e. by multi-omics analysis). The experimental
817 path outlined here likely leads to *B. methanolicus* becoming a viable
818 alternative to existing cell factories.

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1080 **Figure descriptions**

1081 **Fig. 1: Flux map of *B. methanolicus* central metabolism relative to**
1082 **substrate intake for methanol (A), mannitol (B) and arabitol (C).** The
1083 thickness of the reaction lines represent the flux proportions relative to
1084 substrate incorporation into the metabolism: hps (A), Manupt (B), Araupt (C).
1085 Flux proportions were averaged among the biological replicates ($n_{\text{methanol}}=2$,
1086 $n_{\text{arabitol}} = n_{\text{mannitol}} = 3$). The direction of the reaction arrows represent the
1087 estimated net flux directionality. Large grey arrows represent a flux directed
1088 toward amino acid synthesis and biomass requirements for growth. Pathways
1089 discussed in the text are represented by a background patch of color.
1090 Metabolites are represented by circles and have a solid bottom half if they
1091 are duplicated on the same panel, as per recommended by the SBGN
1092 standard. Metabolites subjected to experimental measurement of ^{13}C
1093 labelling are marked by a yellow box. Some intermediate metabolites are not
1094 needed for ^{13}C -MFA and are consequently lumped in mannitol and arabitol
1095 models (B, C); the same metabolites can be explicitly modelled in methanol
1096 model (A) since non-stationary ^{13}C -MFA requires all intermediates pools (e.g.:
1097 G3P, Cit, Aco). Reactions toward amino acid pools and biomass are not
1098 represented.

1099 **Fig. 2: Alternative assimilation pathways of D-arabitol with an**
1100 **example of the measured and expected labeling of Rib5P.** Arabitol

1101 entry point into the metabolism is expected to be Rib5P or Xyl5P,
1102 depending on the substrate specificity of the PTS system and the arabitol
1103 phosphate dehydrogenase. Taking [5-¹³C]arabitol as an example, we show
1104 that the labeling of downstream metabolites can be used to identify which
1105 pathway is operating *in vivo* (Rib5P, orange; Xyl5P, blue). We exemplify our
1106 approach with one data point: the NMR specific enrichment of Rib5P and the
1107 associated estimates from the best fit of different scenarios in which PTS1 or
1108 PTS5 are allowed to carry flux in the model (barplot). Unlike the others, the
1109 model in which only PTS5 was allowed to carry flux did not fit the data (red
1110 crossmark, ✕). Circles are carbon atoms: solid for ¹³C (●), empty for ¹²C (○),
1111 dotted when irrelevant.

1112 **Fig. 3: Estimated absolute fluxes (mmol/gDCW/h) for methanol**
1113 **(blue), mannitol (orange) and arabitol (green).** The bars represent the
1114 average of the estimated absolute net flux for each biological replicate (black
1115 dot), and the error bar is the associated standard deviation ($n_{\text{methanol}} = 2$,
1116 $n_{\text{arabitol}} = n_{\text{mannitol}} = 3$).

1117 **Fig. 4: Estimated absolute rates of production and consumption of**
1118 **NADPH, NADH/FADH₂, and ATP.** Rates (mmol/gDCW/h) are calculated as
1119 the sum of the estimated flux of the reactions modeled in the MFA that are
1120 expected to produce (positive value) or consume (negative value) those
1121 cofactors. Values are averaged over the biological replicates and the error
1122 bars are the associated standard deviation ($n_{\text{methanol}} = 2$, $n_{\text{arabitol}} = n_{\text{mannitol}} = 3$).
1123 The growth requirements (“biomass”, red) are computed from measures on
1124 *B. subtilis* (mmol/gDCW) and the growth rates we observed. Production and

1125 consumption rates should be balanced in our conditions, so we mark putative
1126 production/consumption rates as “unknown” to complete the balance when
1127 needed. The full production of NADH and FADH₂ is assumed to be consumed
1128 in the respiratory chain (“oxidative phosphorylation”) and to produce ATP
1129 (with $P/O_{\text{NADH}} = 1.5$, $P/O_{\text{FADH}_2} = 1$). We modeled the PTS systems of mannitol
1130 and arabitol as consumers of one equivalent ATP (in “uptake”). NADPH
1131 production: glucose 6-phosphate dehydrogenase (*zwf*), phosphogluconate
1132 dehydrogenase (*gnd*), isocitrate dehydrogenase (*idh*), and
1133 methylenetetrahydrofolate dehydrogenase from the linear detoxification
1134 pathway (detox). NADH production: glyceraldehyde-3-phosphate
1135 dehydrogenase (*pgk*), pyruvate dehydrogenase (*pdh*), 2-oxoglutarate
1136 dehydrogenase (*akgdh*), malate dehydrogenase (assimilated to *fum*),
1137 methanol, mannitol and arabitol dehydrogenase (*mdh*, *manupt*, *araupt*), and
1138 formate dehydrogenase from the linear detoxification pathway (detox).
1139 FADH₂ production: succinate dehydrogenase (*fum*). ATP consumption: 6-
1140 phosphofructokinase (*pfk*), PTS systems of mannitol and arabitol (*manupt*,
1141 *araupt*). ATP production: phosphoglycerate kinase (*pgk*), pyruvate kinase
1142 (*pyk*), succinyl-CoA synthetase (assimilated to *akgdh*), acetate kinase
1143 (*out_Ac*), and formate-tetrahydrofolate ligase from the linear detoxification
1144 pathway (detox).

1145 Tables

1146 **Table 1.** Strains, primers and plasmids used in this study.

Strain, plasmid or primer	Relevant characteristics	Reference
Strains		
<i>E. coli</i> DH5 α	F ⁻ <i>thi-1 endA1 hsdR17(r⁻ m⁻) supE44 ΔlacU169 (ϕ80lacZΔM15) recA1 gyrA96 relA1</i>	(43)
<i>E. coli</i> BL21 (DE3)	F ⁻ <i>ompT hsdSB(r_B⁻ m_B⁻) gal dcm</i> (DE3)	(44)
<i>B. methanolicus</i> MGA3	Wild type strain (ATCC 53907)	(11)
Plasmids		
pET16b	Amp ^R ; overproduction of Novagen decahistidine-tagged proteins in <i>E. coli</i> (pBR322 oriVE.c., PT7, lacI)	
pET16b- <i>atID</i>	pET16b derivative for the production of <i>B. methanolicus</i> His ₁₀ -tagged AtID from <i>E. coli</i> BL21 (DE3)	This study

pET16b-*atIF* pET16b derivative for the This study
production of *B. methanolicus*
His₁₀-tagged AtIF from *E. coli*
BL21 (DE3)

Primers	Sequence [5' → 3']	Characteristics
P192	agcttcctttcgggctttgtagcagcc gTTAATCAATAGGTGTCAACAAT AC	Amplification of <i>atID</i> for pET16b- <i>atID</i>
P193	gccatatcgaaggctcgtcatatgctcg agATGAAAGCTTTAGTCAAAAA AG	
P194	agcttcctttcgggctttgtagcagcc gTTATGATTTTTCTGGATGGAAG	Amplification of <i>atIF</i> for pET16b- <i>atIF</i>
P195	gccatatcgaaggctcgtcatatgctcg agATGAAAGCATTAAAGCTGTA TG	

1147 Amp^R: ampicillin resistance; overlapping regions are shown in lower case.

1148 **Table 2.** Kinetic data of purified AtID and AtIF

Condition^a: protein, substrate, cofactor^b	Substrate K_M (mM)	V_{max} (U mg⁻¹)^c	V_{max} / K_M
AtID, Xyl5P, NADH	0.07 ± 0.03	1.33 ± 0.23	19
AtID, Ribu5P, NADH	1.21 ± 0.42	0.49 ± 0.06	0.4
AtIF, Xyl5P, NADH	0.18 ± 0.05	0.11 ± 0.01	0.6

1149 ^a The following reactions were also analysed, but no significant activity (i.e. < 0.05 U mg⁻¹)
 1150 could be detected: AtID, Ribu5P, NADPH; AtIF, Xyl5P, NADPH; AtIF, Ribu5P, NADH; AtIF,
 1151 Ribu5P, NADPH.

1152 ^b Cofactor K_M values were analysed using 0.2 mM Xyl5P and were 0.01 ± 0.01 and 0.11 ±
 1153 0.09 for NADH and NADPH, respectively.

1154 ^c The V_{max} for AtID, Xyl5P, NADPH was calculated using 0.2 mM of substrate and 0.3 mM of
 1155 cofactor, and resulted in 0.24 ± 0.06 U mg⁻¹.

1156

1157 **Table 3: Physiological parameters of *B. methanolicus* cultures used**

1158 **for Metabolic Flux Analysis.** Growth rate and biomass quantities were
 1159 deduced from OD₆₀₀ measurements in the exponential growth phase. Carbon
 1160 source evolution rates were measured from supernatant samples and
 1161 analyzed by NMR. Labelled CO₂ was monitored by MS in the bioreactor's
 1162 outgoing gas flow. All cultures were aerobic. n.a.: not measured; n.d.: not
 1163 detected. The uncertainties shown are standard errors between biological
 1164 replicates.

Method	Methanol (CH₃OH)	Mannitol (C₆H₁₄O₆)	Arabitol (C₅H₁₂O₅)	
	¹³ C INST-MFA bioreactor (n=2)	[1- ¹³ C] MFA flask (n=3)	Mix. [1- ¹³ C] & [2- ¹³ C] MFA, flask (n=3)	[5- ¹³ C] MFA flask (n=3)
Growth rate [h ⁻¹]	0.46 ± 0.002	0.36 ± 0.02	0.15 ± 0.004	0.1411 ± 0.02
Biomass yield [gDCW/gSubstrate]	0.55 ± 0.01	0.34 ± 0.08	0.19 ± 0.02	0.23 ± 0.02
C source [mmolC/gDCW/h]	21.9 ± 2.2	36 ± 7.3	21.4 ± 1.2	24.5 ± 0.75
CO₂_{out} [mmol/gDCW/h]	7.6 ± 0.04	n.a.	n.a.	n.a.
Acetate_{out} [mmol/gDCW/h]	n.d.	1.75 ± 0.32	n.d.	n.d.

1165

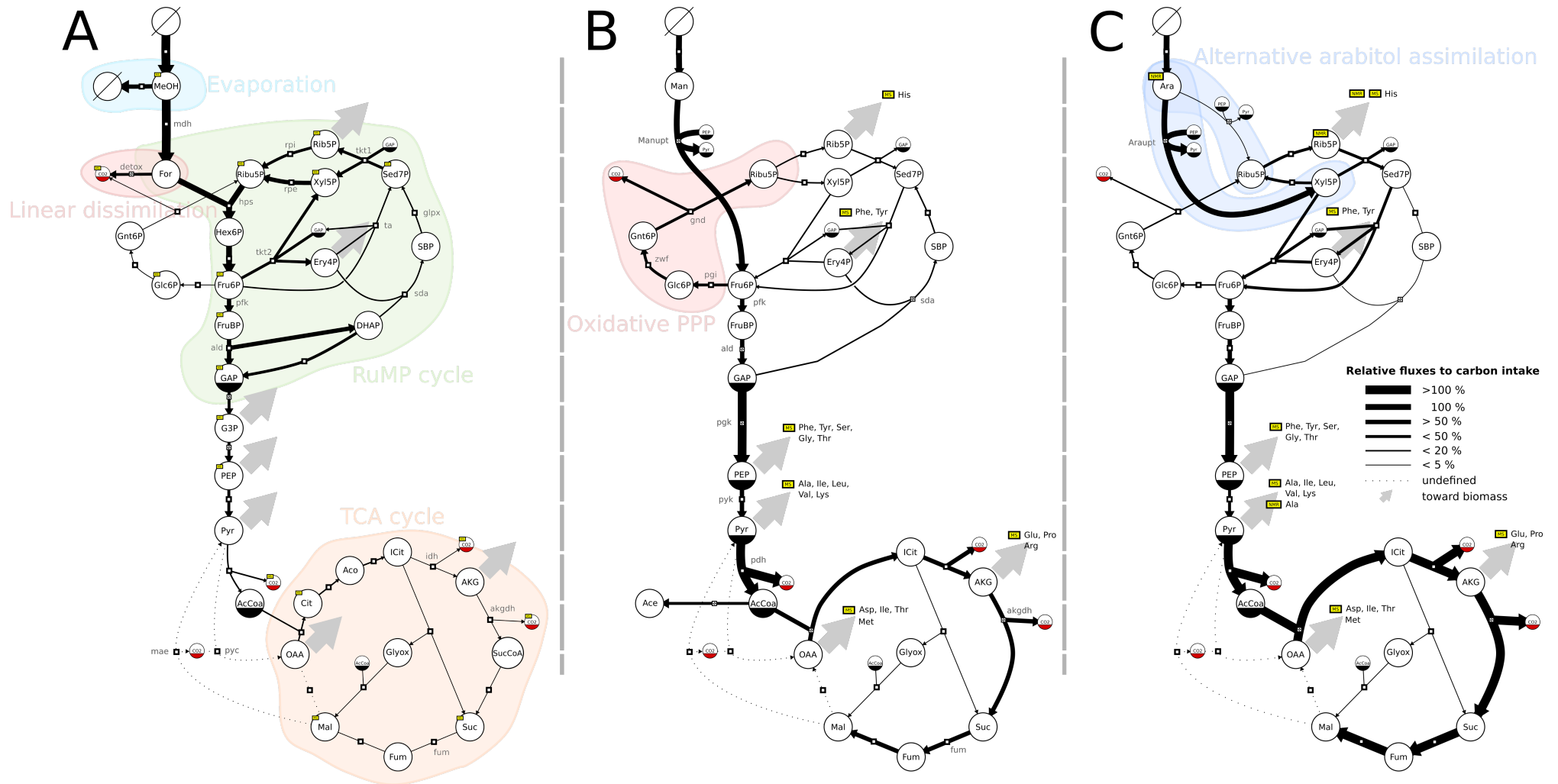


Fig. 1: Flux map of *B. methanolicus* central metabolism relative to substrate intake for methanol (A), mannitol (B) and arabitol (C). The thickness of the reaction lines represent the flux proportions relative to substrate incorporation into the metabolism: hps (A), Manupt (B), Araupt (C). Flux proportions were averaged among the biological replicates ($n_{\text{methanol}}=2$, $n_{\text{arabitol}} = n_{\text{mannitol}} = 3$). The direction of the reaction arrows represent the estimated net flux directionality. Large grey arrows represent a flux directed toward amino acid synthesis and biomass requirements for growth. Pathways discussed in the text are represented by a background patch of color. Metabolites are represented by circles and have a solid bottom half if they are duplicated on the same panel, as per recommended by the SBGN standard. Metabolites subjected to experimental measurement of ¹³C labeling are marked by a yellow box. Some intermediate metabolites are not needed for ¹³C-MFA and are consequently lumped in mannitol and arabitol models (B, C); the same metabolites can be explicitly modeled in methanol model (A) since non-stationary ¹³C-MFA requires all intermediates pools (e.g.: G3P, Cit, Aco). Reactions toward amino acid pools and biomass are not represented.

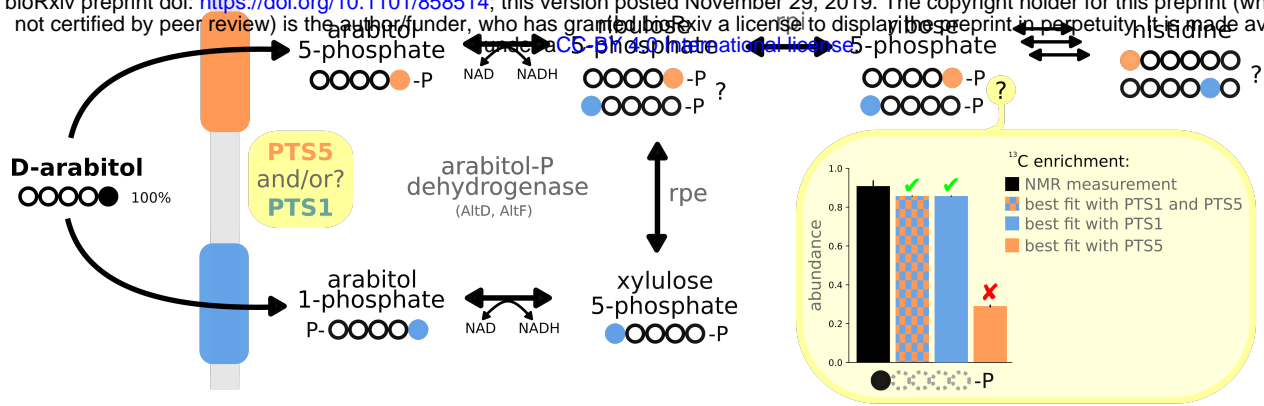


Fig. 2: Alternative assimilation pathways of D-arabitol with an example of the measured and expected labeling of Rib5P. Arabitol entry point into the metabolism is expected to be Rib5P or Xyl5P, depending on the substrate specificity of the PTS system and the arabitol phosphate dehydrogenase. Taking [5- ^{13}C]arabitol as an example, we show that the labeling of downstream metabolites can be used to identify which pathway is operating *in vivo* (Rib5P, orange; Xyl5P, blue). We exemplify our approach with one data point: the NMR specific enrichment of Rib5P and the associated estimates from the best fit of different scenario in which PTS1 or PTS5 are allowed to carry flux in the model (barplot). Unlike the others, the model in which only PTS5 was allowed to carry flux did not fit the data (red cross-mark, ✗). Circles are carbon atoms: solid for ^{13}C (●), empty for ^{12}C (○), dotted when irrelevant.

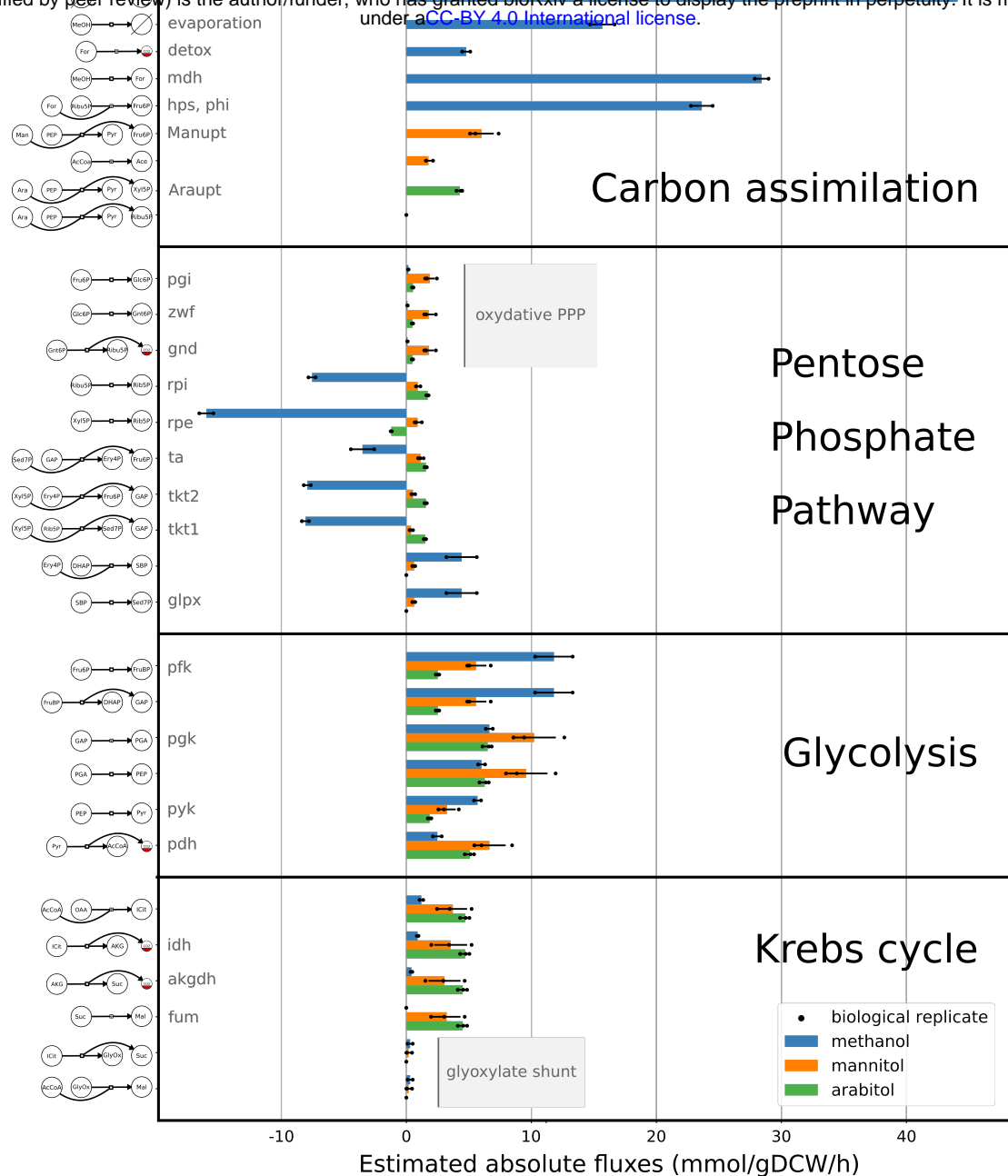


Fig. 3: Estimated absolute fluxes (mmol/gDCW/h) for methanol (blue), mannitol (orange) and arabitol (green). The bars represent the average of the estimated absolute net flux for each biological replicate (black dot), and the error bar is the associated standard deviation ($n_{\text{methanol}}=2$, $n_{\text{arabitol}} = n_{\text{mannitol}} = 3$).

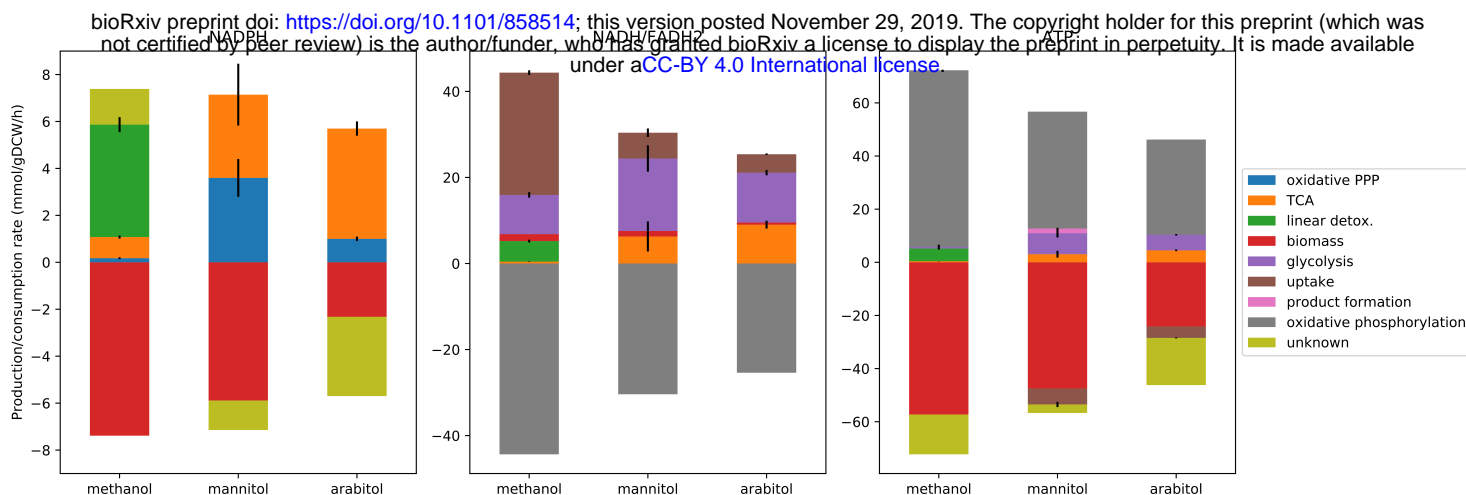


Fig. 4: Estimated absolute rates of production and consumption of NADPH, NADH/FADH₂, and ATP.

Rates (mmol/gDCW/h) are calculated as the sum of the estimated flux of the reactions modeled in the MFA that are expected to produce (positive value) or consume (negative value) those cofactors. Values are averaged over the biological replicates and the error bars are the associated standard deviation ($n_{\text{methanol}}=2$, $n_{\text{arabinol}} = n_{\text{mannitol}} = 3$). The growth requirements (“biomass”, red) are computed from measures on *B. subtilis* (mmol/gDCW) and the growth rates we observed. Production and consumption rates should be balanced in our conditions, so we mark putative production/consumption rates as “unknown” to complete the balance when needed. The full production of NADH and FADH₂ is assumed to be consumed in the respiratory chain (“oxidative phosphorylation”) and to produce ATP (with $P/O_{\text{NADH}}=1.5$, $P/O_{\text{FADH}_2}=1$). We modeled the PTS systems of mannitol and arabinol as consumers of one equivalent ATP (in “uptake”). NADPH production: glucose-6-phosphate dehydrogenase (*zwf*), phosphogluconate dehydrogenase (*gnd*), isocitrate dehydrogenase (*idh*), and methylenetetrahydrofolate dehydrogenase from the linear detoxification pathway (detox). NADH production: glyceraldehyde-3-phosphate dehydrogenase (*pgk*), pyruvate dehydrogenase (*pdh*), 2-oxoglutarate dehydrogenase (*akgdh*), malate dehydrogenase (assimilated to *fum*), methanol mannitol and arabinol dehydrogenase (*mdh*, *manupt*, *araupt*), and formate dehydrogenase from the linear detoxification pathway (detox). FADH₂ production: succinate dehydrogenase (*fum*). ATP consumption: 6-phosphofructokinase (*pfk*), PTS systems of mannitol and arabinol (*manupt*, *araupt*). ATP production: phosphoglycerate kinase (*pgk*), pyruvate kinase (*pyk*), succinyl-CoA synthetase (assimilated to *akgdh*), acetate kinase (*out_Ac*), and formate-tetrahydrofolate ligase from the linear detoxification pathway (detox).